

## Supporting Information

### Energy Consumption in Capacitive Deionization for Desalination: A Review

Yuxin Jiang <sup>1</sup>, Linfeng Jin <sup>1</sup>, Dun Wei <sup>1</sup>, Sikpaam Issaka Alhassan <sup>2</sup>, Haiying Wang <sup>1,3,4,\*</sup>,  
and Liyuan Chai <sup>1,3,4</sup>

<sup>1</sup> School of Metallurgy and Environment, Central South University, Changsha 410083, China

<sup>2</sup> Chemical and Environmental Engineering Department, College of Engineering, University of Arizona, Tucson, AZ 85721, USA

<sup>3</sup> Chinese National Engineering Research Center for Control and Treatment of Heavy Metal Pollution, Changsha 410083, China

<sup>4</sup> Water Pollution Control Technology Key Lab of Hunan Province, Changsha 410083, China

\* Corresponding author

#### 1. Calculation of Parameters

Desalination capacity (salt removal capacity) is defined as the weight of salt removal per unit weight of active material, and it is calculated as Equation (S1):

$$SAC = \frac{\Delta C \times V}{m}. \quad (S1)$$

As above, SAC is the desalination capacity ( $\text{mg} \cdot \text{g}^{-1}$ ),  $\Delta C$  refers to the salt concentration change in the feed solution ( $\text{mg} \cdot \text{L}^{-1}$ ) during charging,  $V$  stands for the volume of the feed solution (L), and  $m$  denotes the weight of the active material (g). On the other hand, energy consumption is the energy consumed per gram of salt removal, and it is calculated as Equation (S2):

$$W = \frac{\int (I \times U) dt}{\Delta C \times V}. \quad (S2)$$

As above,  $W$  is the energy consumption ( $\text{Wh} \cdot \text{g}_{\text{NaCl}}^{-1}$ ), and  $I$  and  $U$  denote the instantaneous current (A) and voltage (V) during charging, respectively. Charge efficiency refers to the ratio of the charge amount correspondent to the actual salt removal and the overall consumed charge amount, and it is calculated as Equation (S3):

$$\Lambda = \frac{\Delta C \times V \times F}{\int I dt \times 1000 \times M_{\text{NaCl}}}. \quad (S3)$$

As above,  $F$  is the Faraday constant ( $96,485 \text{ C} \cdot \text{mol}^{-1}$ ),  $t$  demonstrates the time consumed in the deionization process, and  $M_{\text{NaCl}}$  is the molar mass of sodium chloride ( $\text{g} \cdot \text{mol}^{-1}$ ). Besides, deionization is also a process of energy storage, thus

recovered energy is the energy regenerated per unit of salt removal in the desalination device. The calculation of recovered energy is similar to the energy consumption as shown in Equation (S4):

$$ER = \frac{\int (I_R \times U_R) dt}{\Delta C \times V}. \quad (S4)$$

As above,  $ER$  is the recovered energy ( $\text{Wh} \cdot \text{g}_{\text{NaCl}}^{-1}$ ), and  $I_R$ ,  $U_R$ , and  $\Delta C$  denote the instantaneous current (A), voltage (V), and concentration change during discharging, respectively. Energy recovery rate ( $ERR$ ) is the ratio of recovered energy and energy consumption, which is calculated as follows:

$$ERR = \frac{ER}{W}. \quad (S5)$$

## 2. Deduction of the Relationship of Parameters

In the capacitive deionization (CDI) process of constant voltage mode, the energy consumption is calculated as Equation (S6):

$$W = \frac{U \times \int I dt}{\Delta C \times V}. \quad (S6)$$

As above,  $U$  is the voltage applied in the CDI cell. Together with Equation (S3), the product of energy consumption and charge efficiency is demonstrated as follows:

$$W\Lambda = \frac{U \times F}{3600 \times M_{\text{NaCl}}}. \quad (S7)$$

As above,  $U$ ,  $F$ , and  $M_{\text{NaCl}}$  are all constant parameters. As such, we could figure out the energy consumption is in inverse proportion with charge efficiency.

### 3. Supplementary Table

**Table S1.** The comparison of CDI and MCDI.

	Incorporation of ion-exchange membrane		Charge efficiency		Energy consumption	Desalination capacity
CDI	no		lower		higher	lower
MCDI	yes		higher		lower	higher
	Electrode material	Electric intensity	Initial salinity	Energy consumption	Desalination capacity	Reference
CDI	activated carbon	1.2 V	200 ppm	$1.55 \text{ Wh} \cdot \text{g}_{\text{NaCl}}^{-1}$	$2.27 \text{ mg} \cdot \text{g}^{-1}$	[1]
	activated carbon	1.4 V	600 ppm	$1.17 \text{ Wh} \cdot \text{g}_{\text{NaCl}}^{-1}$	$14.9 \text{ mg} \cdot \text{g}^{-1}$	[2]
	activated carbon	1.2 V	10 mM	$1.04 \text{ Wh} \cdot \text{g}_{\text{NaCl}}^{-1}$	$\sim 3 \text{ mg} \cdot \text{g}^{-1}$	[3]
	carbon	1.2 V	20 mM	$\sim 0.71 \text{ Wh} \cdot \text{g}_{\text{NaCl}}^{-1}$	---	[4]
	activated carbon	1.2 V	20 mM	$0.97 \text{ Wh} \cdot \text{g}_{\text{NaCl}}^{-1}$	$2.37 \text{ mg} \cdot \text{g}^{-1}$	[5]
MCDI	activated carbon	1.2 V	200 ppm	less than half of that of CDI in [1]	$3.54 \text{ mg} \cdot \text{g}^{-1}$	[1]
	activated carbon	1.4 V	600 ppm	$0.92 \text{ Wh} \cdot \text{g}_{\text{NaCl}}^{-1}$	$20.0 \text{ mg} \cdot \text{g}^{-1}$	[2]
	porous carbon	1.2 V	20 mM	$\sim 0.56 \text{ Wh} \cdot \text{g}_{\text{NaCl}}^{-1}$	---	[6]
	activated carbon	1.0 V	10 mM	$\sim 0.49 \text{ Wh} \cdot \text{g}_{\text{NaCl}}^{-1}$	$\sim 13.6 \text{ mg} \cdot \text{g}^{-1}$	[7]
	biowaste carbon	1.2 V	2500 ppm	$0.63 \text{ Wh} \cdot \text{g}_{\text{NaCl}}^{-1}$	$38 \text{ mg} \cdot \text{g}^{-1}$	[8]

## References

1. Kim, Y. J.; Choi, J. H., Enhanced desalination efficiency in capacitive deionization with an ion-selective membrane. *Sep. Purif. Technol.* **2010**, 71, (1), 70-75.
2. Zornitta, R. L.; Ruotolo, L. A. M., Simultaneous analysis of electrosorption capacity and kinetics for CDI desalination using different electrode configurations. *Chem. Eng. J.* **2018**, 332, 33-41.
3. Kang, J.; Kim, T.; Jo, K.; Yoon, J., Comparison of salt adsorption capacity and energy consumption between constant current and constant voltage operation in capacitive deionization. *Desalination* **2014**, 352, 52-57.
4. Kim, T.; Dykstra, J. E.; Porada, S.; van der Wal, A.; Yoon, J.; Biesheuvel, P. M., Enhanced charge efficiency and reduced energy use in capacitive deionization by increasing the discharge voltage. *J. Colloid Interface Sci.* **2015**, 446, 317-326.
5. Dykstra, J. E.; Porada, S.; van der Wal, A.; Biesheuvel, P. M., Energy consumption in capacitive deionization - Constant current versus constant voltage operation. *Water Res.* **2018**, 143, 367-375.
6. Wang, L.; Lin, S. H., Membrane Capacitive Deionization with Constant Current vs Constant Voltage Charging: Which Is Better? *Environ. Sci. Technol.* **2018**, 52, (7), 4051-4060.
7. Choi, J.-H., Comparison of constant voltage (CV) and constant current (CC) operation in the membrane capacitive deionisation process. *Desalin. Water Treat.* **2015**, 56, (4), 921-928.
8. Sriramulu, D.; Vafakhah, S.; Yang, H. Y., Activated Luffa derived biowaste carbon for enhanced desalination performance in brackish water. *Rsc Advances* **2019**, 9, (26), 14884-14892.