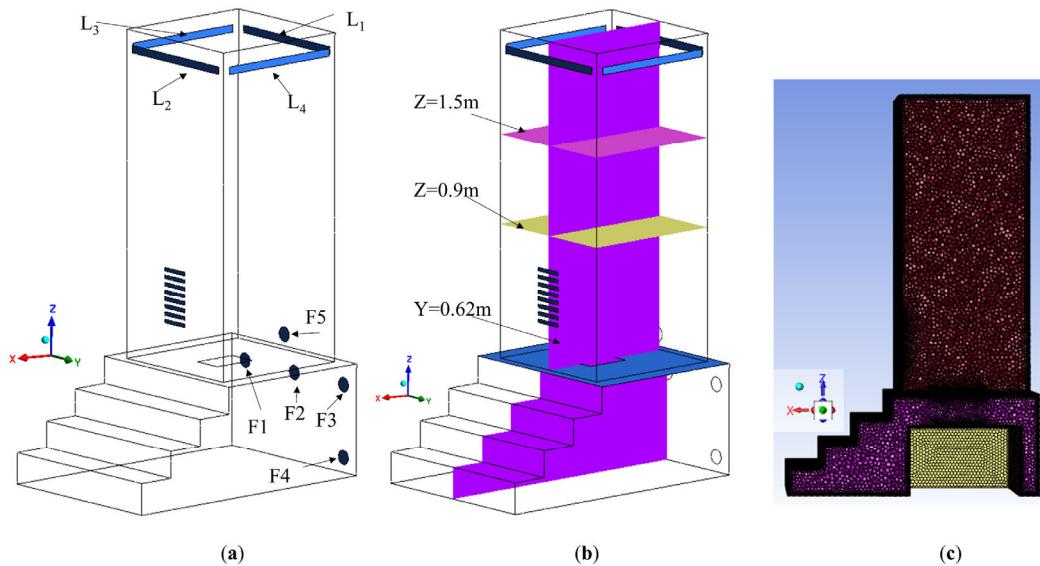




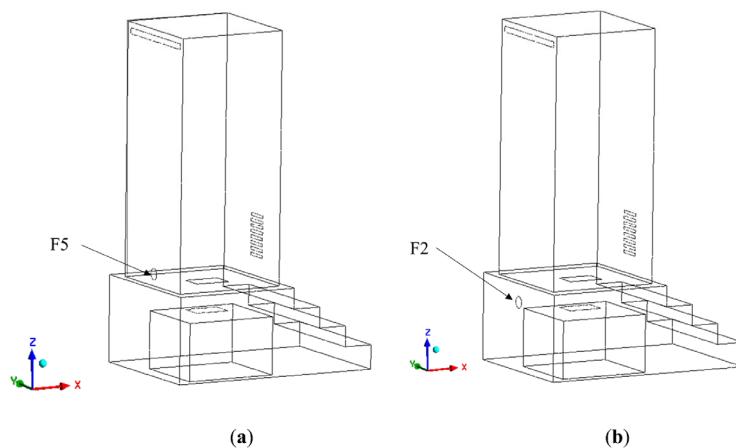
Article

# Dynamics and Numerical Simulation of Contaminant Diffusion for a Non-Flushing Ecological Toilet

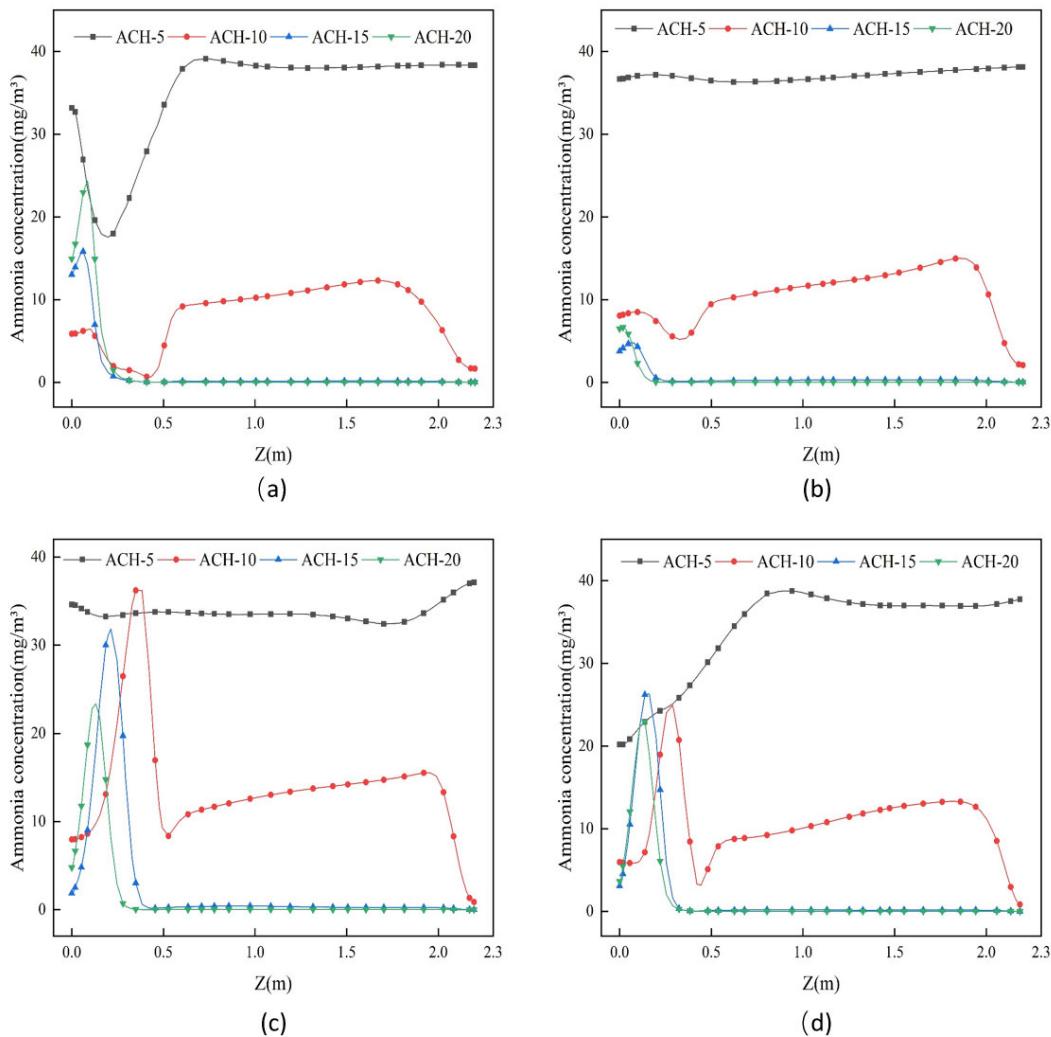
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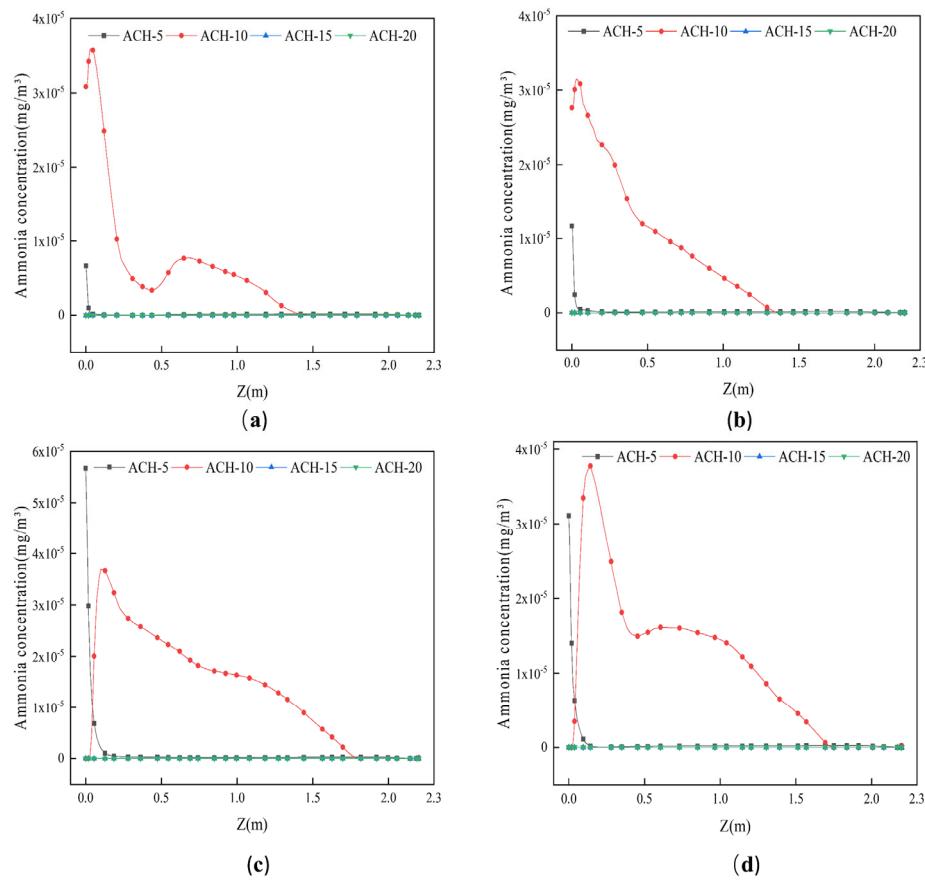
**Figure S1.** Grid condition of CFD model and plane of observation. (a): CFD model; (b): Observation plane; (c): Grid condition of CFD model.



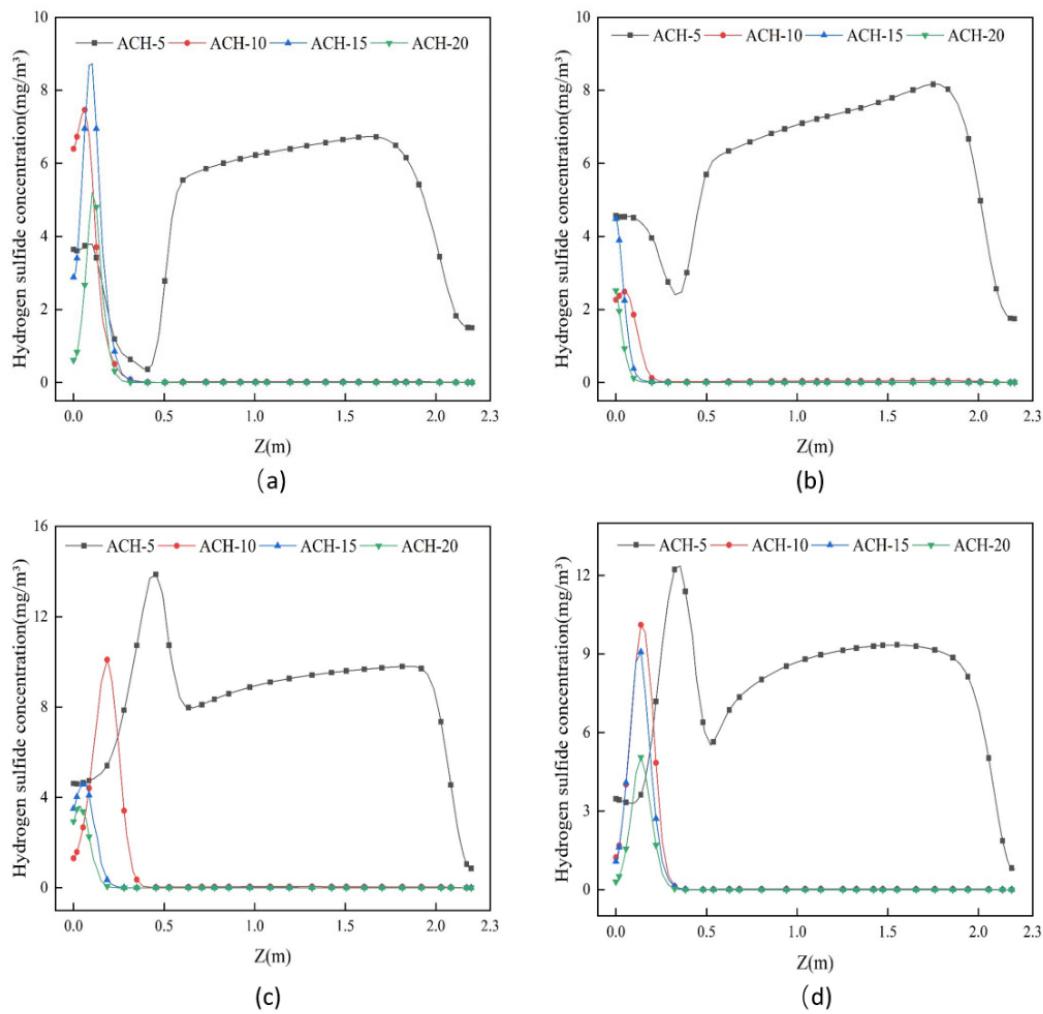
**Figure S2.** Case descriptions. Case 1-F (0,0.62,0.59), Case 2-F (0.07,0.62,0.85); unit: m.(a) Case 1;(b) Case 2.



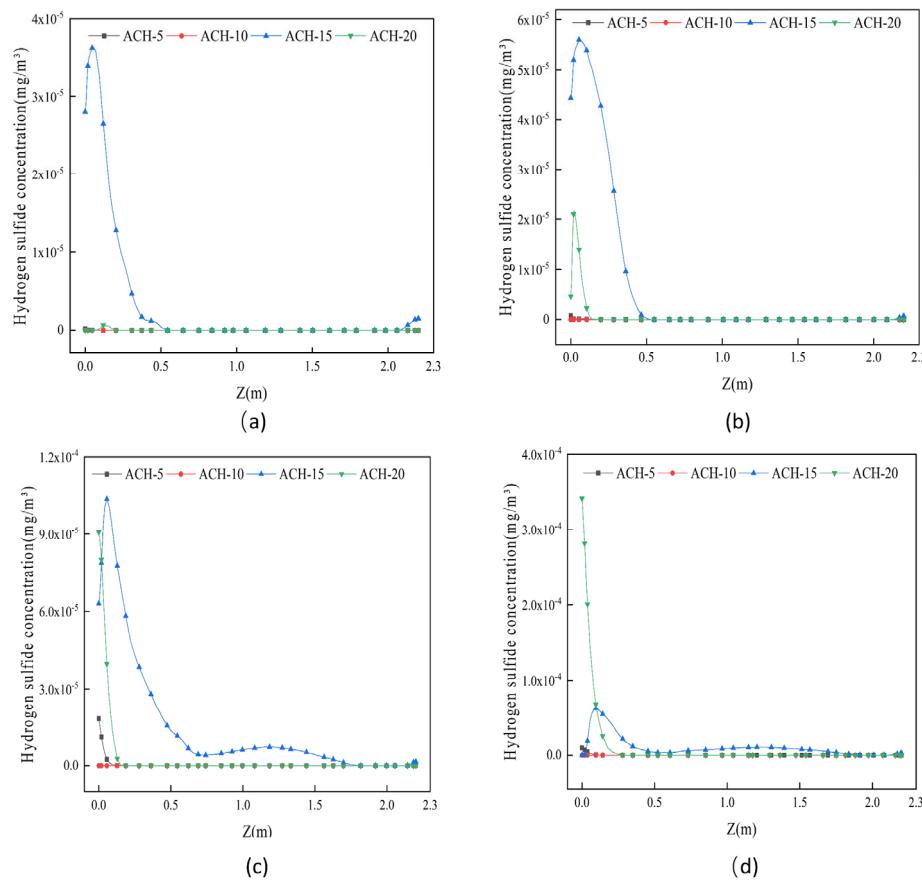
**Figure S3.** Ammonia concentration at ABCD four-point vertical line in Case 1; ACH unit:  $\text{h}^{-1}$ . **(a)**: Point A **(b)**: Point B; **(c)**: Point C, **(d)**: Point D.



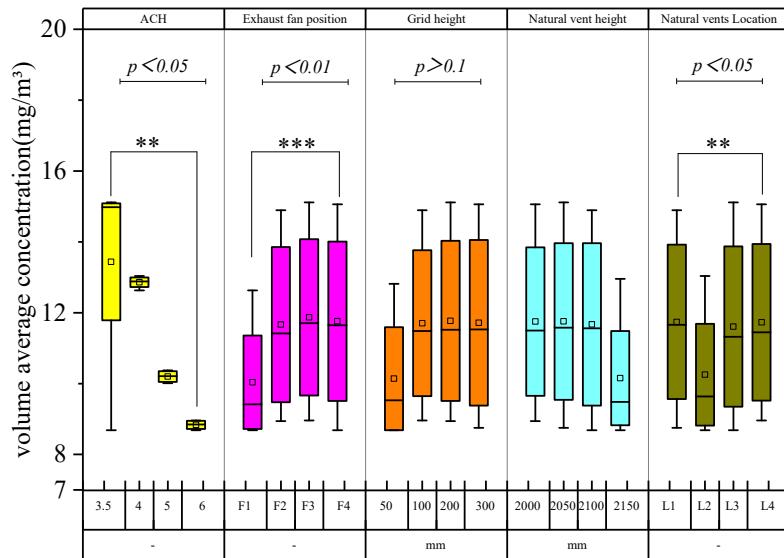
**Figure S4.** Ammonia concentration at ABCD four-point vertical line in Case 2; ACH unit:  $\text{h}^{-1}$ . **(a)**: Point A **(b)**: Point B; **(c)**: Point C, **(d)**: Point D.



**Figure S5.** Hydrogen sulfide concentration at the ABCD four-point vertical line in Case 1; ACH unit: h<sup>-1</sup>. (a): Point A (b): Point B; (c): Point C, (d): Point D.

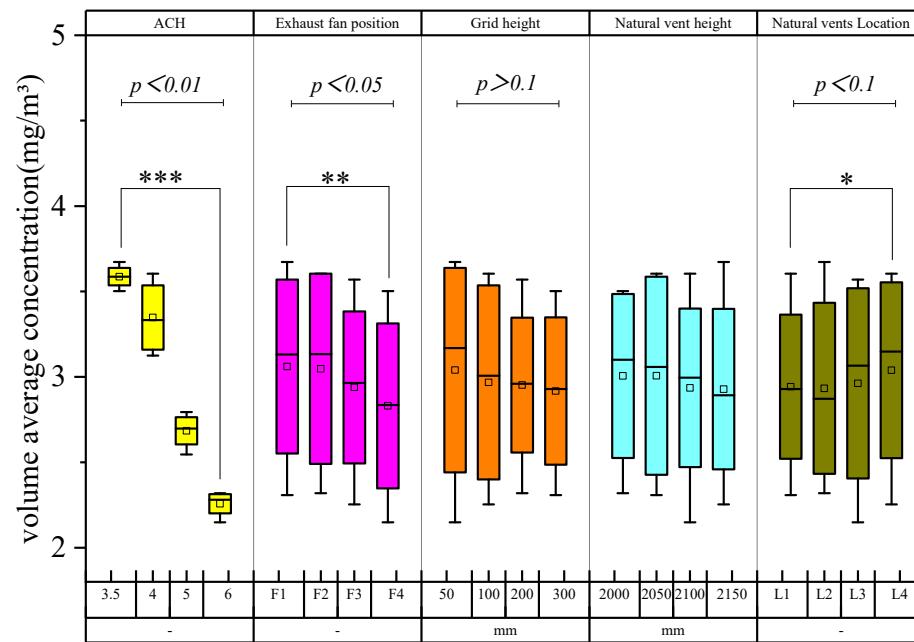


**Figure S6.** Hydrogen sulfide concentration at the ABCD four-point vertical line in Case 2; ACH unit:  $\text{h}^{-1}$ . (a): Point A (b): Point B; (c): Point C, (d): Point D.



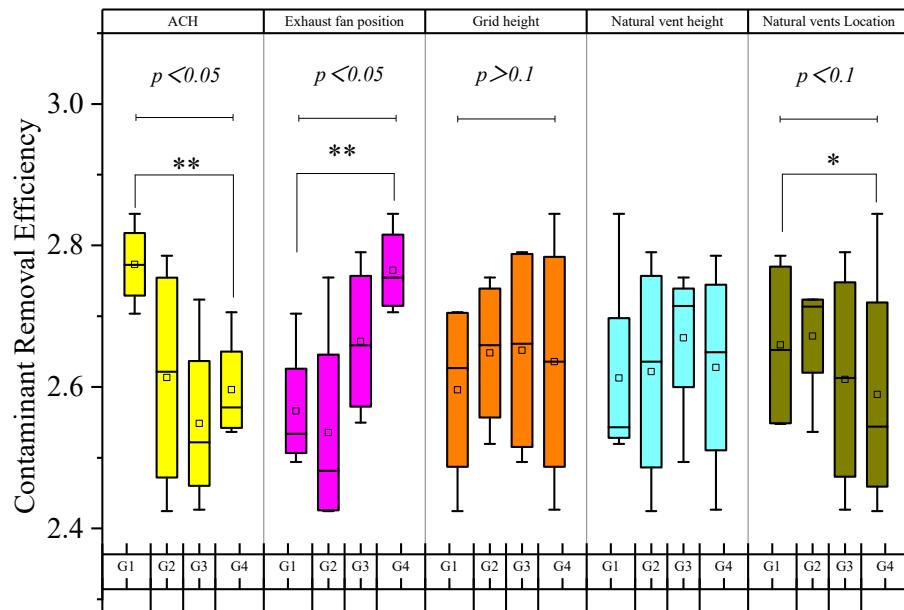
Each box of results illustrate the findings of orthogonal experiments under each condition.  
\*, \*\* and \*\*\* represent the significant difference via the F test levels of 0.1, 0.05 and 0.01, respectively.

**Figure S7.** Statistical significance analysis of the orthogonal experiment results regarding the VAC of ammonia.



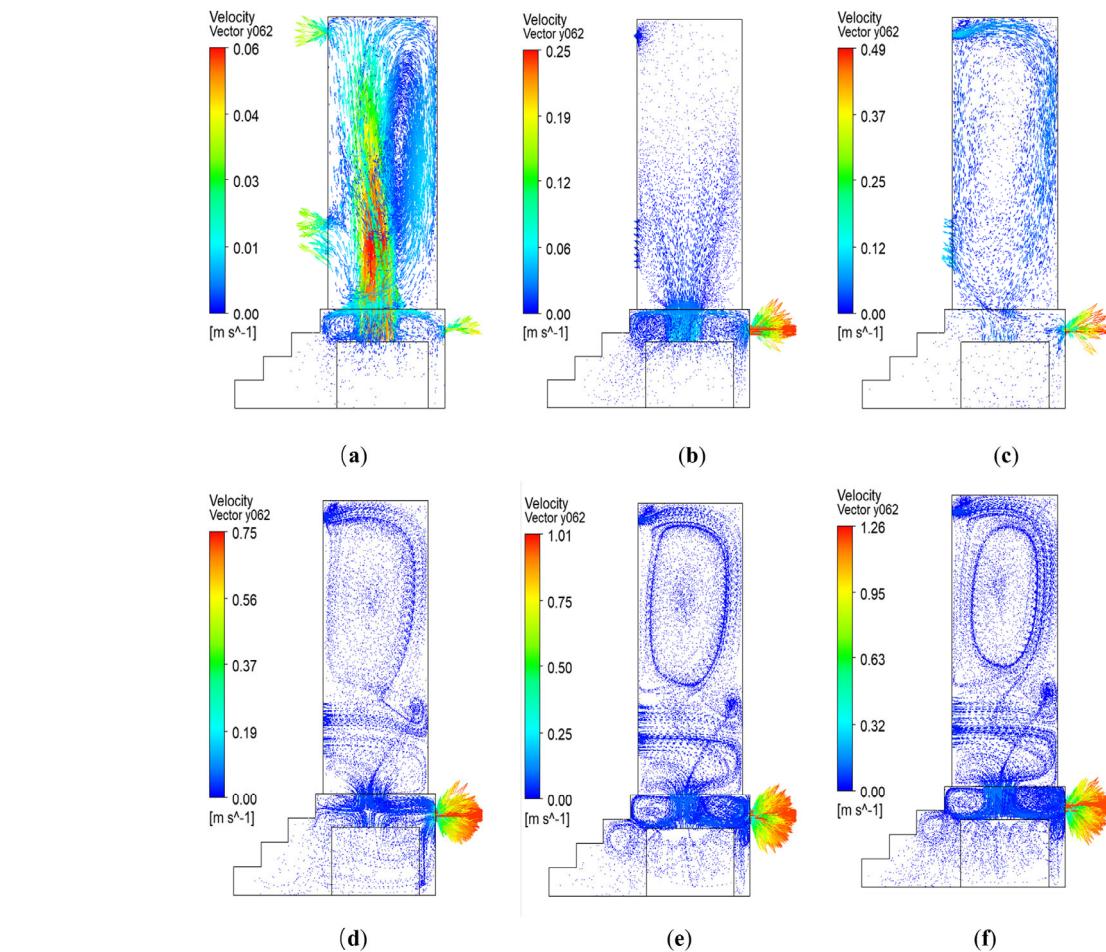
Each box of results illustrate the findings of orthogonal experiments under each condition.  
\*, \*\*and \*\*\*represent the significant difference via the F test levels of 0.1, 0.05 and 0.01, respectively.

**Figure S8.** Statistical significance analysis of the orthogonal experiment results regarding the VAC of hydrogen sulfide.

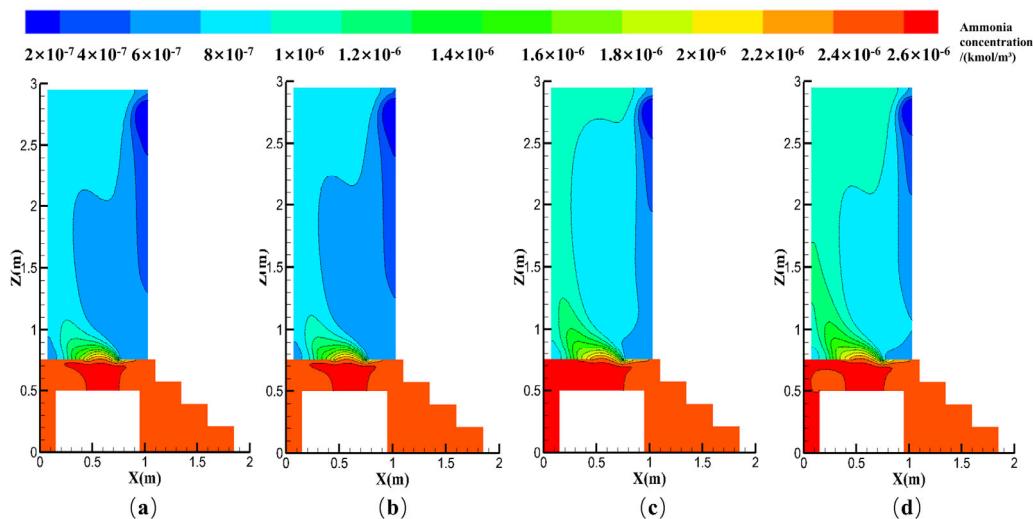


Each box of results illustrate the findings of orthogonal experiments under each condition.  
\*, \*\*and \*\*\*represent the significant difference via the F test levels of 0.1, 0.05 and 0.01, respectively.

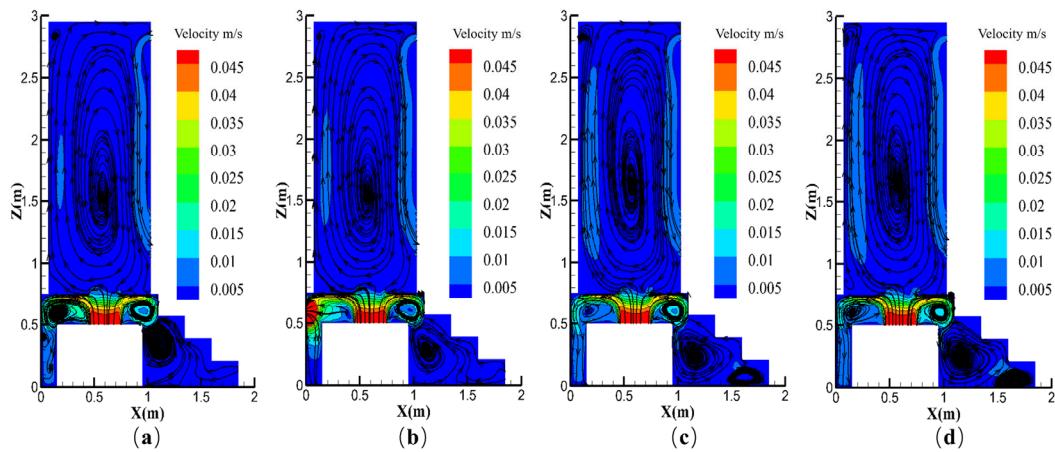
**Figure S9.** Statistical significance analysis of the orthogonal experiment results regarding the CRE of hydrogen sulfide.



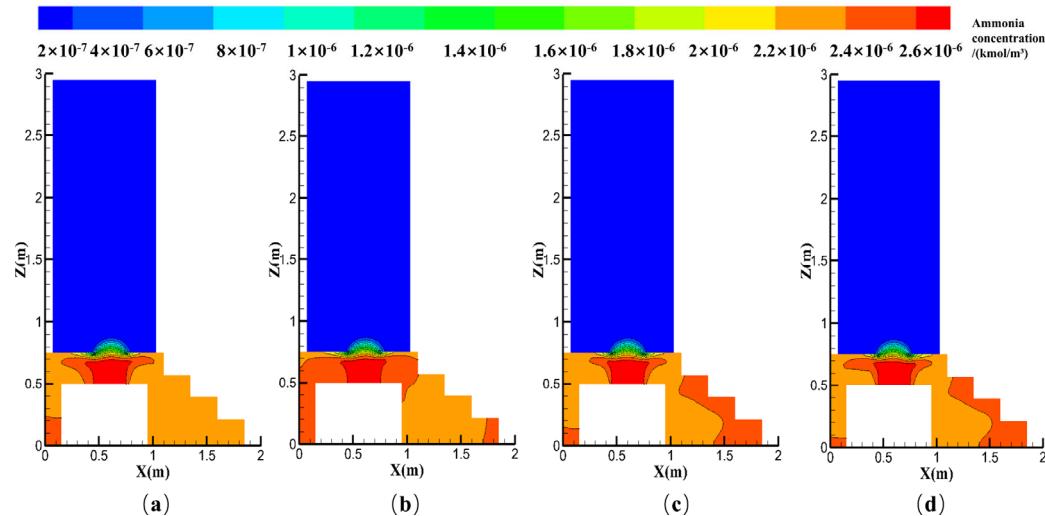
**Figure S10.** Velocity vector contours for different ACH (unit:  $\text{h}^{-1}$ ) values. (a): ACH=0; (b): ACH=2; (c): ACH=4; (d): ACH=6; (e): ACH=8; (f): ACH=10.



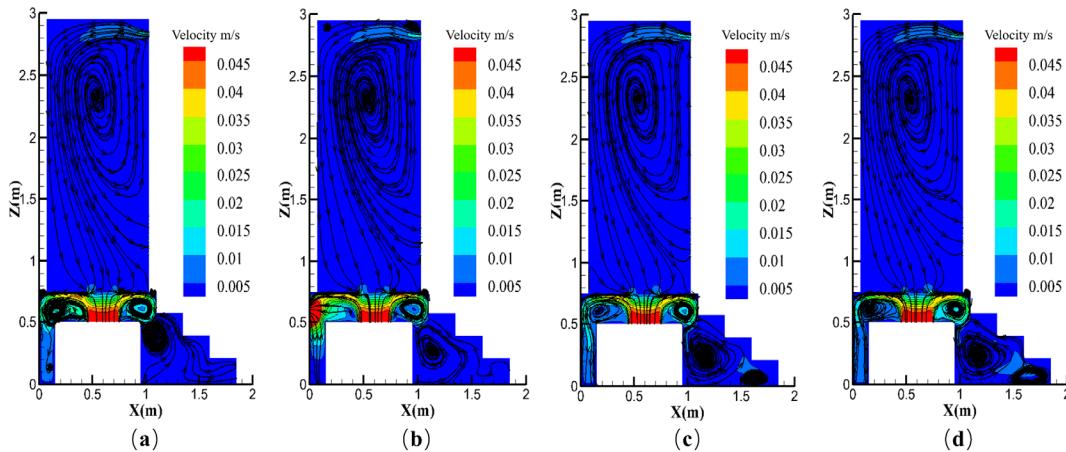
**Figure S11.** Ammonia concentration distributions for different positions of the exhaust fan ( $ACH=3.3 \text{ h}^{-1}$ ). (a): F1, (b): F2; (c): F3, (d): F4.



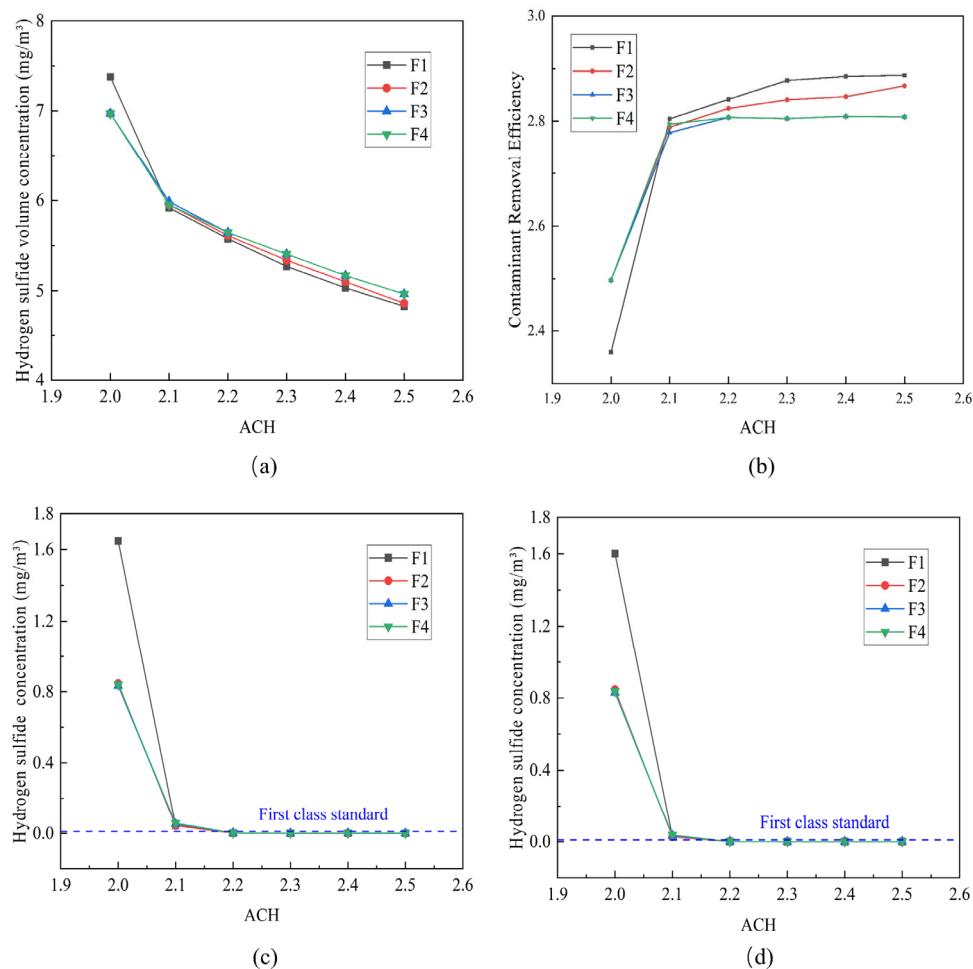
**Figure S12.** Ammonia diffusion dynamics for different positions of the exhaust fan ( $\text{ACH}=3.3 \text{ h}^{-1}$ ). (a): F1, (b): F2; (c): F3, (d): F4.



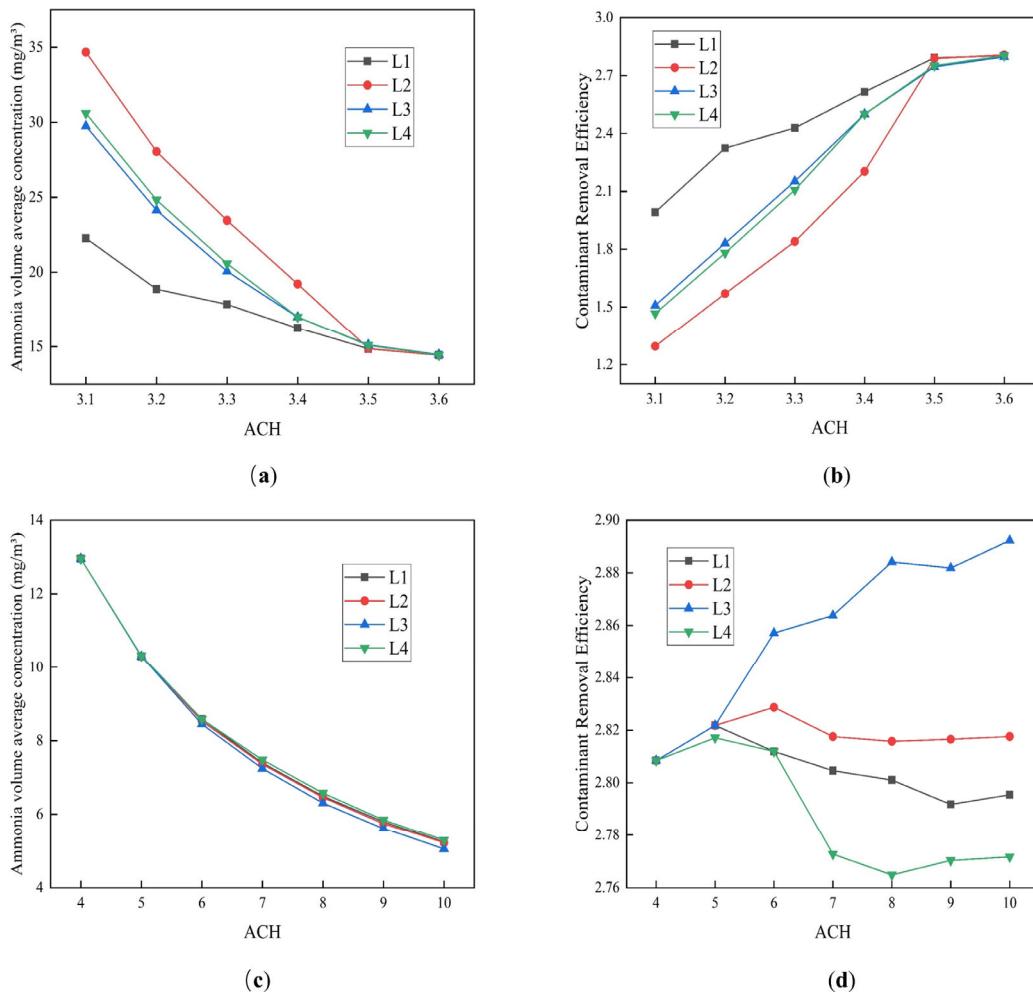
**Figure S13.** Ammonia concentration distributions for different positions of the exhaust fan ( $\text{ACH}=3.6 \text{ h}^{-1}$ ). (a): F1, (b): F2; (c): F3, (d): F4.



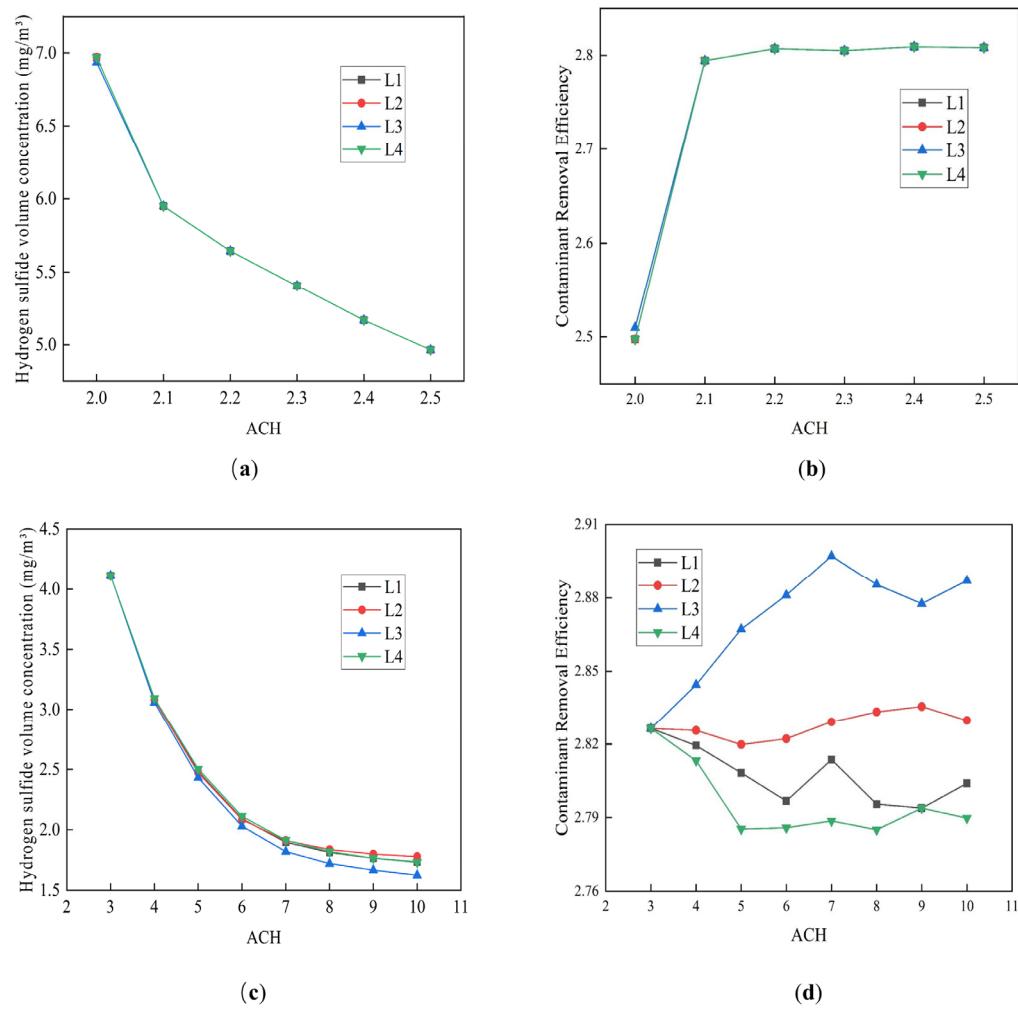
**Figure S14.** Ammonia diffusion dynamics for different positions of the exhaust fan ( $\text{ACH}=3.6 \text{ h}^{-1}$ ). (a): F1, (b): F2; (c): F3, (d): F4.



**Figure S15.** Average concentration and CRE of (a, b) hydrogen sulfide and (c, d) hydrogen sulfide in the breathing zone for different ACH values. VAC: volume average concentration; CRE: contaminant removal efficiency; ACH unit:  $\text{h}^{-1}$ . (a): VAC, (b): CRE; (c):  $Z=0.9\text{m}$ , (d):  $Z=1.5\text{m}$ .



**Figure S16.** (a, c) Average volume concentration and (b, d) CRE of ammonia in the breathing zone for different ACH (unit:  $\text{h}^{-1}$ ) values. (a): VAC(ACH=3.1–3.6), (b): CRE(ACH=3.1–3.6); (c): VAC(ACH=4–10), (d): CRE(ACH=4–10).



**Figure S17.** (a, c) Average volume concentration and (b, d) CRE of hydrogen sulfide in the breathing zone for different ACH (unit:  $\text{h}^{-1}$ ) values. (a): VAC(ACH=2–2.5), (b): CRE(ACH=2–2.5); (c): VAC(ACH=3–10), (d): CRE(ACH=3–10).

**Table S1.** Summary of the experiments proposed according to the orthogonal design approach.

Case	ACH	EFP	G-h	NVL	NV-h
Case 1	3.5	F <sub>1</sub>	50	L2	2150
Case 2	3.5	F <sub>2</sub>	100	L1	2100
Case 3	3.5	F <sub>3</sub>	200	L3	2050
Case 4	3.5	F <sub>4</sub>	300	L4	2000
Case 5	4	F <sub>1</sub>	100	L3	2000
Case 6	4	F <sub>2</sub>	50	L4	2050
Case 7	4	F <sub>3</sub>	300	L2	2100
Case 8	4	F <sub>4</sub>	200	L1	2150
Case 9	5	F <sub>1</sub>	200	L4	2100
Case10	5	F <sub>2</sub>	300	L3	2150
Case11	5	F <sub>3</sub>	50	L1	2000
Case12	5	F <sub>4</sub>	100	L2	2050
Case13	6	F <sub>1</sub>	300	L1	2050
Case14	6	F <sub>2</sub>	200	L2	2000
Case15	6	F <sub>3</sub>	100	L4	2150
Case16	6	F <sub>4</sub>	50	L3	2100

Unit:  $\text{h}^{-1}$