

Article **Production of Biohydrogen from Organ-Containing Waste for Use in Fuel Cells**

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Abstract: The production of low-carbon hydrogen based on renewable energy sources is considered a promising direction in the development of the modern world economy. The purpose of the presented research is to develop technologies and study the processes of converting biogases into hydrogen, as well as its use in low-temperature fuel cells. The methodology for organizing a multi-stage laboratory experiment for obtaining biogas, its purification from impurities and, in the future, the production of biohydrogen was developed based on field studies in Peter the Great St. Petersburg Polytechnic University. The results of modeling studies have shown that during biogas reforming, it is possible to obtain a hydrogen mixture with a hydrogen content of 98% vol and methane 2% vol. Based on the results of the research, the possibility of using the significant potential of "weak" biogas containing methane 30–45% vol to produce biohydrogen (more than 93% vol) was proved. A technique for using biohydrogen in low-temperature fuel cells for energy generation has been substantiated and tested.

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Keywords: waste; biogas; biohydrogen; hydrogen fuel; residual methane; low-temperature fuel cell; energy efficiency

1. Introduction

The production of low-carbon hydrogen based on renewable energy sources is considered a promising direction in the development of the modern world economy. The use of low-carbon hydrogen as the most important industrial raw material, as well as a high-quality efficient energy carrier, will reduce the consumption of fossil fuels and reduce greenhouse gas emissions, which will contribute to solving the pressing environmental and social problem—global climate change [\[1\]](#page-8-0).

In 2020, the global demand for hydrogen was about 90 million tons, of which more than 70 million tons were used in the form of pure hydrogen and less than 20 million tons were mixed with carbonaceous gases in the production of methanol and steel. Nearly all of this demand was for oil refining and industrial use. To date, the use of hydrogen in the transport sector is limited to 0.01% of total consumption. In the electric power industry, it is practically not used [\[2\]](#page-8-1).

Currently, the bulk of hydrogen in the world is obtained from fossil fuels—about 96% of the total, including from natural gas (49%), liquid hydrocarbons (29%), and coal (18%). Steam reforming of natural gas is currently one of the most common, and at the same time the least expensive, processes for producing hydrogen. Its main disadvantage is the emission of greenhouse gases (10 kg $CO₂/kg H₂$). Hydrogen production by water electrolysis is 3.9%; an insignificant part (0.1%) is obtained from other sources [\[3\]](#page-8-2). The high cost of producing hydrogen limits its wider application.

By 2050, the role of hydrogen in the global energy sector may be comparable to that of fossil fuels. In addition, hydrogen is one of the most effective ways to create long-term energy storage [\[4\]](#page-8-3).

Biomass is an attractive renewable energy resource for obtaining relatively cheap low-carbon hydrogen due to its large resources, its almost universal availability (wood and wood waste, agricultural crops, aquatic plants, microalgae, waste from the agro-industrial and food sectors, housing and communal services, etc.), the possibility of its effective use in various energy technologies, as well as transport systems [\[5](#page-8-4)[,6\]](#page-8-5).

Biomass is the largest source of renewable energy used globally today. In 2017, the production of primary energy resources in the world was estimated at 13,972 million toe, including 1992 million toe of renewable energy resources (14.3% of total), of which 1385 million toe (about 70% of renewable) was biomass.

The production of primary energy resources by 2040 in the world is estimated to reach 17,715 million toe. It is assumed that the production of renewable energy resources will reach 3605 million toe (20.3% of the total), of which 1851 million toe (about 51.4%) will be biomass [\[7\]](#page-8-6). An analysis of the global energy balance shows that in the foreseeable future, bioenergy will play an important role in the energy supply and decarbonization of transport, housing, agriculture, and other industries due to the possibility of emission-free (without greenhouse gas emissions) efficient conversion into liquid and gaseous fuels, heat and electricity. The special importance of bioenergy in creating a climate-friendly circular economy is noted as a new socially and environmentally acceptable economic model for the development of society [\[8](#page-8-7)[,9\]](#page-8-8). Technically realizable resources of primary biomass for the world energy industry, according to a conservative estimate, are a significant value of 160–270 EJ/year (3.82–6.45 billion toe), even considering possible restrictions on use by agriculture and water economy, wood-processing industries, and the social and environmental sphere. This is 3–4.5 times higher than their current use [\[9\]](#page-8-8).

Russia has significant bioenergy potential. For energy purposes, it is possible to use (annually) $[10-14]$ $[10-14]$:

- About 800 million tons of woody biomass;
- About 500 million tons (by dry matter) of organic waste from agricultural production;
- Up to 70 million tons of waste from the forestry and woodworking industries;
- 60 million tons of municipal solid waste;
- Up to 10 million tons of sludge from municipal wastewater.

The main directions of development of bioenergy in the world are [\[15\]](#page-9-0):

- The creation of highly efficient technologies for energy waste disposal and obtaining alternative fuel products based on biogas and synthesis gas;
- The production of low-carbon hydrogen for fuel cells.

Obtaining biogas from waste is an effective traditional way of use their energy potential [\[16\]](#page-9-1). Biogas can also be used as an available raw material for the subsequent production of low-carbon hydrogen [\[17\]](#page-9-2), which will allow organizing the local production and use of hydrogen, providing local consumers with a relatively cheap, high-quality, and environmentally friendly energy carrier.

The type of organic waste determines the morphological composition of biogases, the summarized data for which are presented in Table [1](#page-2-0) [\[18\]](#page-9-3). The methane content of biogas typically ranges from 45% to 75% by volume, with most of the remainder being $CO₂$. This variation means that the energy content of biogas can vary; the lower heating value (LHV) is between 16 megajoules per cubic meter (MJ/m 3) and 28 MJ/m 3 [\[19\]](#page-9-4).

The purification of biogas is a complex task and requires the use of a combination of different methods due to its contamination with harmful impurities, the instability of formation, and the variability in time of the content of the methane component [\[20\]](#page-9-5). This task is discussed in detail in many publications, e.g., in [\[21](#page-9-6)[,22\]](#page-9-7).

Solving the problem of biogas purification opens prospects of using biomethane instead of natural gas, which is the main raw material for hydrogen production. Biogas can be obtained almost everywhere since organic waste is constantly generated in the process of human economic activity. Meanwhile, natural gas resources are limited, their use is limited, and they become more expensive over time. The anaerobic decomposition process converts the waste into a valuable fuel, biomethane, which can be steam-reformed to produce low-carbon hydrogen instead of natural gas. At the same time, carbon dioxide contained in biogas, as well as arising from the production of hydrogen, is characterized by an environmentally friendly origin (through biological processes). Carbon dioxide was originally taken from the atmosphere by plants and converted into primary biomass and then through the life cycle into organic waste. The biogas waste disposal process produces a by-product—effluent (fermented residue)—that can be used as a high-quality agricultural fertilizer.

Table 1. Composition of biogases.

The cost of hydrogen from biogas is comparable to the cost of electrolytic hydrogen produced using electrical energy, hydraulic and wind power plants, and cheaper than hydrogen produced using photovoltaic plants [\[23,](#page-9-8)[24\]](#page-9-9). Therefore, the expediency of obtaining hydrogen from biogases with its subsequent use to produce electrical energy is quite obvious.

Biohydrogen can be obtained from the fermentation of various waste products. The article [\[25\]](#page-9-10) discusses the fermentation of liquid waste from dairy production (whey) to produce biohydrogen. It is shown that the yield of hydrogen and the purity of the hydrogen mixture depend on the pH of the process (optimal $pH = 6$) and the inoculant. The authors of articles [\[26,](#page-9-11)[27\]](#page-9-12) showed that industrial wastewater is a cheap substrate for cost-effective production of biohydrogen. Pre-treatment of the inoculant and selective immobilization of hydrogen-producing microorganisms make it possible to obtain the maximum amount of biohydrogen. The processing of organic waste using microbes under dark or photofermentation is an economical and promising way to obtain biohydrogen [\[28\]](#page-9-13). In [\[29](#page-9-14)[,30\]](#page-9-15), the authors showed the possibility of obtaining biohydrogen from the biomass of microalgae and creating a closed biocatalytic system for hydrogen production due to water biophotolysis.

In addition, also of great interest nowadays are the technologies of biological methanation of hydrogen (generated by electrolysis using wind and solar energy) with carbon dioxide in biogas to form methane. This makes it possible to increase the methane yield of the biogas system by 70%. However, due to the complex biochemical processes in bioreactors, these technologies require serious refinement, which is currently being addressed by numerous researchers. [\[31](#page-9-16)[,32\]](#page-9-17)

It should be noted that for the widespread use of technologies for producing hydrogen from waste, it is necessary to reduce costs, which can be carried out using the existing technological reserve for the key stages of hydrogen production from biogases.

The production of hydrogen for low-temperature PEM (proton exchange membrane) fuel cells is of particular interest because they are most suitable for autonomous consumers in a wide range of loads from hundreds of watts to several tens of kilowatts. Fuel cells can become an effective alternative to burning fuel for primary electricity generation by stationary and mobile sources. The critical question concerns the source of hydrogen, because in many ways, the purity and cost of hydrogen determines the efficiency of fuel cells [\[33\]](#page-9-18). Work on the production of hydrogen from biogases and its use in the power supply of small consumers is carried out in EU countries, the USA, and Japan. The following shortcomings of the installations were revealed: the low hydrogen content in the reformate

 $(70-80\% \text{ vol.})$ and the presence of harmful impurities in it $[34]$. This requires the use of expensive and difficult-to-operate systems for its purification, which leads to an increase in the energy intensity of the process and a decrease in efficiency. Therefore, it is extremely important to develop an efficient technology for converting readily available hydrocarbon fuel (biogas) into relatively cheap, "low-carbon" hydrogen as an alternative to electrolysis, as well as methods for its direct use in low-temperature hydrogen fuel cells [\[35\]](#page-9-20).

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The purpose of the presented research is to develop technologies and study the processes of converting biogases into hydrogen, as well as its use in low-temperature fuel cells.

2. Materials and Methods

The methodology for organizing a multi-stage laboratory experiment (Figure 1) for obtaining biogas, its purification from impurities and, in the future, the production of biohydrogen was developed based on field studies in Peter the Great St. Petersburg Polytechnic University [\[36\]](#page-9-21).

Figure 1. Figure 1. Scheme of a multi-stage laboratory experiment. Scheme of a multi-stage laboratory experiment.

The first stage of the laboratory experiment involved a preliminary assessment of the biogas potential of the studied organic waste using the OxiTop Control AN6|WTW (Germany). In the studied composition, the total and specific volume of biogas, as well as its morphological composition, were determined.

The second stage of the experiment was the assessment and forecast of the dynamics of biogas formation using the automated complex "BIOREACTOR", certified according to international requirements [\[37\]](#page-9-22). The "BIOREACTOR" complex included: a thermobox, fermenters, a system for monitoring and managing waste biodegradation processes, gas meters, etc. [\[36\]](#page-9-21).

At the third stage of the experiment, studies were carried out on the energy use of biogas based on the created unique laboratory complex [\[38\]](#page-9-23). The laboratory complex consisted of the following modules: a biogas generation module (bioreactor module), a biogas storage and purification module, a methane reforming module to produce hydrogen, and a module consisting of low-temperature fuel cells (Figure [2\)](#page-4-0).

Figure 2. The composition of the modules of the laboratory complex. **Figure 2.** The composition of the modules of the laboratory complex.

Model samples of the studied wastes, from which biogas was formed in the process Model samples of the studied wastes, from which biogas was formed in the process of methanogenesis, were placed in the bioreactor module. Within the framework of the first here is a state of the first module, the volume and composition of biogas were controlled, and the chemical composi-
with a settle site of the view of the chemical composition of the chemical composition of the chemical composi tion of the filtrate was determined. In the second module, based on adsorption–cryogenic
the filtrate was determined. In the second module, based on adsorption–cryogenic cryogenic treatment impurities were removed from biogas and the methane completion was isolated. Furthermore, the biomethane purified from impurities was supplied to
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electrical energy treatment, harmful impurities were removed from biogas and the methane component the reforming module for its steam conversion into biohydrogen. Next, biohydrogen enelectrical energy.

into electrical energy. Absorption and catalytic purification (operation in a periodic mode) were used to obtain hydrogen from purified methane in the reforming module [\[39\]](#page-9-24). A mixture of methane and water vapor was converted and pre-treated by the adsorption–catalytic method, after which the gas was supplied for additional purification from CO in a methanator—KONIK-TECH. The operating temperature of adsorption–catalytic processes was 600–850 ◦C, and the methanator was 250 ◦C. The main technical characteristics of the reformer module are shown in Table [2.](#page-4-1)

Table 2. Reformer module specifications.

The functional diagram of the reformer module is shown in Figure [3.](#page-5-0)

Figure 3. Scheme of the reformer module: 1—adsorption-catalytic blocks; 2—evaporator with per ature controller; $\frac{1}{2}$ and \frac temperature controller; 3—methanator; 4—distillate; 5—liquid pump; 6—gas flow regulator; 7—gas throttle; 8—methane concentration control.

The concentration of hydrogen and impurities in the gas flow was determined using a gas analyzer AVP-02G and an IR Fourier spectrophotometer FSM1202.

It was thermodynamically substantiated that $CH₄$ is not oxidized in a low-temperature fuel cell; however, its presence in a hydrogen mixture can create the effect of shielding the catalytic membrane surface and, therefore, hinder the kinetics of hydrogen oxidation. Traditionally, methods are used to separate hydrogen from CO , $CO₂$, $CH₄$, and other impurities using, for example, expensive membrane technologies [\[40\]](#page-10-0). The problem arises of direct use of hydrogen with a residual content of methane in the fuel cell and determination of the effect of non-oxidizing gas on the electrochemical kinetics of hydrogen oxidation.

The possibility of direct use of biohydrogen (obtained from the methane component of biogas) in a fuel cell instead of electrolytic hydrogen was studied on an E-Tek low-temperature fuel cell ($P = 5$ W with a proton-exchange membrane) [\[41\]](#page-10-1). The main characteristics of the E-Tek fuel cell when tested on electrolytic hydrogen and oxygen are shown in Table [3.](#page-6-0)

Cell Name Platinum Content, mg/cm² Open-Circuit Voltage, mV Rated Power during Cycling, mW Rated Power Under Stationary Conditions, mW Ohmic Resistance, Ohm·**cm²** E-Tek_12W_MEA_Pol_1 6.25 940 130 E-Tek_12W_MEA_Pol_1 6.25

Table 3. E-Tek fuel cell parameters.

The feed rate of the hydrogen-containing gas obtained in the reformer was \sim 20 mL/min, which provided a sufficient overpressure on the fuel cell membrane $(\sim 0.02 \text{ atm})$. The automatic second-by-second registration of realized dependencies was carried out in digital and graphical format, and fuel consumption was also recorded (H_2 or $H_2 + CH_4$).

3. Results

At the first stage of the laboratory experiment, samples of model waste mixtures were loaded into bioreactors, which correspond to the average morphological composition of municipal solid waste landfilled at Russian solid waste landfills. 6-week-old compost from MSW containing methanogenic bacteria was used as an inoculum. Then, the process of their biodegradation was organized according to the method described in articles [\[42](#page-10-2)[–44\]](#page-10-3). The volume of biogas generated as a result of waste methanogenesis during the entire duration of the experiment was constantly monitored. The composition of biogas was periodically determined, which made it possible to create model mixtures of biogas with different methane content of 40–51% vol. (the rest is carbon dioxide). The model mixtures were fed into the adsorption–cryogenic module, where impurities were removed. As a result, methane was released with a concentration of 94.1–97.5% vol.

The sorption–catalytic scheme was used to produce hydrogen. This scheme combined the process of steam reforming of hydrocarbons with high-temperature purification from carbon dioxide. The studies were carried out on an experimental setup (Figure [3\)](#page-5-0) with a capacity of up to 60 L H_2 /hour with thermal regeneration of the absorber. The synthesized granular calcium oxide was used as an absorber [\[45\]](#page-10-4), as a catalyst for steam reforming—NIAP-03 $(11\% NiO/Ca₂Al₂O₅)$ and methanation—NIAP-07 (36 wt.% NiO/Al₂O₃).

The composition of landfill biogas was modeled with three different gas mixtures: methane, $CO₂$ and nitrogen with a gas content of 94.8; 5.2; 0 vol.% (I mixture—treated biogas), 35.4; 54.9; 9.7 vol.% (II mixture—"weak" biogas) and 44.6; 40; 15.4 vol.% (III mixture), respectively. The temperature at the conversion stage was 680 ◦C, at the regeneration stage 820 \degree C, and in the methanator it was 400 \degree C; the pressure at the conversion stage was 1.6 atm, and the vapor/C ratio = 4 .

To assess the stability of the process and the reliability of the laboratory unit, the authors used in addition to the main gas mixture (mixture #1), simulating enriched biogas, also "weak" biogas (mixture #2) and a mixture simulating typical biogas from a landfill in the stage of active methanogenesis (mixture #3). The main results of the experiments on the steam reforming of biogases into hydrogen are presented in Table [4](#page-7-0) [\[46\]](#page-10-5).

A hydrogen-containing mixture with a hydrogen content of up to 98% vol. and methane up to 2% vol. was obtained experimentally when methane was supplied to the reformer (about 95% vol.) in a wide range of loads (30–100% of the nominal). Furthermore, experiments were carried out on the supply of "weak" biogas containing methane 30–45% vol. to the reformer. At the same time, the hydrogen concentration in the reformate remained high (more than 93% vol). This circumstance expands the possibilities of using the significant potential of "weak" biogases with a relatively low concentration of the methane component in the autonomous energy sector to produce electrical and thermal energy.

The resulting hydrogen-containing mixture (with a hydrogen content of up to 98% by volume) was fed into a low-temperature fuel cell. Tests have shown that a hydrogen mixture containing up to 2% CH₄ (vol.), with direct supply (dead end) to the fuel cell in a potentiostatic mode at a constant potential $E = 500$ mV, using air oxygen as an oxidizer (Figure [4,](#page-7-1) curve 1), for a sufficiently long time (\sim (1.2 \div 1.4) 104 s) does not require adjustment for the discharge of unspent fuel from the anode [\[47,](#page-10-6)[48\]](#page-10-7). Similar studies were carried out using electrolytic hydrogen (99.999% vol) (Figure [4,](#page-7-1) curve 2).

Table 4. Indicators of steam reforming of biogas.

Figure 4. Dependence of current on time (potentional mode), E = 500 mV) when supplied to the theory of the supplied to the sup fuel cell: (1) H_2 –98% + C H_4 –2% (vol.); (2) H_2 (99.999% v/v). **Figure 4.** Dependence of current on time (potentiostatic mode, $E = 500$ mV) when supplied to the

characteristics with direct supply of a hydrogen-containing mixture with a residual methane content obtained from biogas, and with the supply of electrolytic hydrogen. A comparison of the data obtained showed that the fuel cell has similar current

However, it should be noted an increase in the number and frequency of fuel discharges to clean the anode surface of accumulating methane molecules, causing a shielding
- charges to clean the anode surface of accumulating methane molecules, causing a shielding effect. This icaus to some decrease in the fact dimization factor and increases the loss of the
hydrogen-containing mixture. Therefore, it is advisable to clean the hydrogen-containing ing enegen community mature. Therefore, it is una sense to create the higher gardgen community mixture from residual methane. effect. This leads to some decrease in the fuel utilization factor and increases the loss of the

The results of the studies performed on a fuel cell confirmed the fundamental possibility of using a hydrogen-containing mixture with a residual methane content obtained from

biogas during the fermentation of organic waste (biohydrogen) under conditions of direct supply to a low-temperature fuel cell.

4. Discussion

Based on field studies, a complex was created that allows simulating the process of obtaining biogas from organic waste with its further conversion into hydrogen for supply to a fuel cell to generate electricity.

Now the authors are conducting research in laboratory conditions. The next stage of research may be the creation of a pilot industrial model with a further assessment of the possibility of commercialization of this area of energy use of biogas.

5. Conclusions

The results of modeling studies have shown that during biogas reforming, it is possible to obtain a hydrogen mixture with a hydrogen content of 98% vol and methane 2% vol. Based on the results of the research, the possibility of using the significant potential of "weak" biogas containing methane 30–45% vol to produce biohydrogen (more than 93% vol) was proved. A technique for using biohydrogen in low-temperature fuel cells for energy generation has been substantiated and tested.

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