

*Article*



# **Research on the Dynamic Leaking and Diffusion Law of Hydrogen-Blended Natural Gas under the Soil–Atmosphere Coupled Model**

**Shuai Ren <sup>1</sup> , Jingyi Huang <sup>2</sup> , Jiuqing Ban <sup>3</sup> , Jiyong Long <sup>4</sup> , Xin Wang <sup>2</sup> and Gang Liu 2,[\\*](https://orcid.org/0000-0002-6476-3395)**

- <sup>1</sup> PipeChina Southwest Pipeline Company, Chengdu 610094, China; rs18380359536@163.com
- <sup>2</sup> College of Safety Science and Engineering, Chongqing University of Science & Technology,
- Chongqing 401331, China; 2023207002@cqust.edu.cn (J.H.); sanjin997@163.com (X.W.) <sup>3</sup> Research Institute of Natural Gas Technology, PetroChina Southwest Oil and Gas Field Company, Chengdu 610213, China; banjiuqing@hotmail.com
- <sup>4</sup> Branch Company in Northeast of Sichuan Province, PetroChina Southwest Oil and Gas Field Company, Chengdu 610000, China; ifhope@126.com
- **\*** Correspondence: liugang@cqust.edu.cn

**Abstract:** With the breakthrough in mixing hydrogen into natural gas pipelines for urban use, the widespread application of hydrogen-blended natural gas (HBNG) in energy delivery is imminent. However, this development also introduces significant safety concerns due to notable disparities in the physical and chemical properties between methane and hydrogen, heightening the risks associated with gas leaks. Current models that simulate the diffusion of leaked HBNG from buried pipelines into the atmosphere often employ fixed average leakage rates, which do not accurately represent the dynamic nature of gas leakage and diffusion. This study uses computational fluid dynamics (CFD) 2024R1 software to build a three-dimensional simulation model under a soil–atmosphere coupling model for HBNG leakage and diffusion. The findings reveal that, in the soil–atmosphere coupling model, the gas diffusion range under a fixed leakage rate is smaller than that under a dynamic leakage rate. Under the same influencing factors in calm wind conditions, the gas primarily diffuses in the vertical direction, whereas under the same influencing factors in windy conditions, the gas mainly diffuses in the horizontal direction.

**Keywords:** hydrogen-doped natural gas; porous media; coupled model; influencing factors; dangerous areas

## **1. Introduction**

At present, countries mainly rely on traditional fossil energy sources to facilitate development, with them playing an important role in promoting economic development but also bringing about problems such as carbon pollution and emissions. This runs counter to the existing concept of sustainable development. Therefore, governments are committed to the development of clean energy, and there is growing demand for sustainable, lowpollution clean energy [\[1](#page-17-0)[–3\]](#page-17-1). Hydrogen energy is seen as an important carrier to ensure energy security and renewable energy [\[4–](#page-17-2)[6\]](#page-17-3). In recent years, governments and researchers have been focusing on the development of hydrogen energy, which has the advantages of 'high calorific value and zero carbon emissions' [\[7–](#page-17-4)[9\]](#page-17-5).

Currently, many countries including Russia [\[10\]](#page-17-6), France [\[11\]](#page-17-7), the United Kingdom [\[12,](#page-17-8)[13\]](#page-17-9), the Netherlands [\[14\]](#page-17-10), Australia [\[15\]](#page-17-11), and others are conducting tests and research on hydrogen delivery via natural gas pipelines. Figure [1](#page-1-0) illustrates the blending ratios of hydrogen in the major natural gas pipelines of developed countries, with the current safety limit not exceeding 50% [\[16\]](#page-17-12). Additionally, the Chinese government has incorporated 'hydrogen energy technology' into its upcoming five-year plan for national key research and development [\[17–](#page-17-13)[19\]](#page-17-14). Concurrently, it has initiated projects involving hydrogen blending in urban gas pipelines [\[20\]](#page-17-15).



**Citation:** Ren, S.; Huang, J.; Ban, J.; Long, J.; Wang, X.; Liu, G. Research on the Dynamic Leaking and Diffusion Law of Hydrogen-Blended Natural Gas under the Soil–Atmosphere Coupled Model. *Energies* **2024**, *17*, 5035. <https://doi.org/10.3390/en17205035>

Academic Editor: Sanghyun Kim

Received: 2 September 2024 Revised: 29 September 2024 Accepted: 7 October 2024 Published: 10 October 2024



**Copyright:** © 2024 by the authors. Licensee MDPI, Basel, Switzerland. This article is an open access article distributed under the terms and conditions of the Creative Commons Attribution (CC BY) license [\(https://](https://creativecommons.org/licenses/by/4.0/) [creativecommons.org/licenses/by/](https://creativecommons.org/licenses/by/4.0/)  $4.0/$ ).

<span id="page-1-0"></span>

gen blending in urban gas pipelines [20].

**Figure 1.** Proportion of hydrogen blended in different countries or regions. **Figure 1.** Proportion of hydrogen blended in different countries or regions.

However, according to relevant researchers and academics [21], mixing hydrogen However, according to relevant researchers and academics [\[21\]](#page-17-16), mixing hydrogen with natural gas changes the original properties of natural gas and increases the risk of pipeline operation issues, including pipeline leaks and compressor failure. Hydrogen-doped natural<br>
intervalsed in the leaks and compressor failure. Hydrogen-doped natural gas pipelines are not only affected by pipeline aging and third-party damage but also by<br>gas pipelines are not only affected by pipeline aging and third-party damage but also by significant potential impacts such as hydrogen embrittlement, leading to inevitable leaks in<br>such a ineliger [20,22] such pipelines [\[20](#page-17-15)[,22\]](#page-17-17).

inevitable leaks in such pipelines [20,22]. In recent years, a number of explosion accidents related to gas leakage from buried In recent years, a number of explosion accidents related to gas leakage from buried pipelines have occurred both at home and abroad, causing significant loss of personnel pipelines have occurred both at home and abroad, causing significant loss of personnel and property as well as serious damage to the surrounding environment. For example, in 2019, a hydrogen cylinder fire and explosion occurred at a South Korean enterprise; 2019, a hydrogen cylinder fire and explosion occurred at a South Korean enterprise; Airgas Airgas Corporation in the United States also experienced a hydrogen explosion [\[23](#page-17-18)[,24\]](#page-18-0). The Compression coefficient, ignition energy, and other parameters of hydrogen and methane pression coefficient, and hydrogen has a wider range of explosion limits [\[25\]](#page-18-1). Comparative are quite different, and hydrogen has a wider range of explosion limits [25]. analysis of hydrogen and natural gas incidents reveals that hydrogen accidents tend to have a higher fatality rate and more severe consequences than natural gas accidents.

Bu et al. [\[26\]](#page-18-2) carried out a numerical simulation study on the diffusion law after the leakage of buried natural gas pipelines using the numerical simulation software CFD, focusing on the formation of hazardous area time (FDT) and the farthest diffusion range (GDR) after the gas diffusion. According to the simulation results, the nature of the soil has a significant effect on the diffusion of the gas, and the FDT increases by 5 times when the soil type changes from sandy soil to clay. The increase in pipeline pressure leads to an increase in the hazardous area. Zhang et al. [27] established a three-dimensional simulation model of leakage diffusion for underground hydrogen pipelines, focusing on the effects of leakage holes, soil type, pipeline pressure, and pipeline diameter on hydrogen diffusion. The results of the study show that when the hydrogen pipeline leaks, the hydrogen concentration increases with the increase in the leakage time, showing a symmetrical distribution trend; hydrogen has a large difference in different soil properties, and its diffusion is the fastest in sandy soil, and the diffusion range and concentration are higher in than other soil types. Hu [28] conducted a simulation study using Computational Fluid Dynamics (CFD) software to investigate the diffusion characteristics of buried pipelines containing hydrogen doping or pure hydrogen, influenced by porous media. The study revealed that diffusion of the gas through the soil is notably slow. Moreover, it was found that a higher ratio of pore diameter to pore length and width correlates with an increased risk of hydrogen leakage. Su et al.  $[29]$  carried out a numerical simulation study of urban buried hydrogen-doped Su et al. [\[29\]](#page-18-5) carried out a numerical simulation study of urban buried hydrogen-doped<br>pipeline leakage, focusing on exploring the extent of the influence of hydrogen doping doping or pure hydrogen, influenced by porous media. The study revealed that diffusion of<br>the gas through the soil is notably slow. Moreover, it was found that a higher ratio of pore<br>diameter to pore length and width corre ratio (5–20%), leakage pressure, leakage aperture, and other factors on gas diffusion. The results showed that the leakage of the hydrogen-doped pipeline had no significant effect on the generation of relevant risk factors. Zhang et al. [\[30\]](#page-18-6) used the numerical simulation software CFD to carry out a numerical simulation of pinhole leakage in medium-pressure (≤0.4 MPa) buried hydrogen pipelines under different working conditions, focusing on

exploring the effects of pipeline pressure, soil properties, pinhole locations, and pinhole diameters on leakage diffusion. According to the simulation results, the correlation between surface disaster radius and time was established. Zhu et al. [\[31\]](#page-18-7) set up an experimental platform for the leakage of buried hydrogen-doped natural gas pipelines, focusing on different hydrogen doping ratios, the location of leakage holes, and leakage pressure, and measured the leakage of hydrogen-doped natural gas through experiments. The results of the study showed that leakage pressure exhibited a wide diffusion range when a significant proportion of individual components existed in hydrogen-doped natural gas. Peng [\[16\]](#page-17-12) and others investigated the diffusion problem of hydrogen-doped natural gas in longdistance pipelines. A two-dimensional planar model was established using CFD numerical simulation software, focusing on the effects of hydrogen doping ratio, leakage aperture, temperature, and other factors on the diffusion of hydrogen-doped natural gas leakage. Ye [\[32\]](#page-18-8) and others used CFD numerical simulation software to investigate gas diffusion in the coupled environment of soil and atmosphere. The results showed that compared to underground leakage, the diffusion distance and height of aboveground leakage under different conditions exhibit errors, with horizontal diffusion distance errors generally being larger.

Currently, most mainstream research simplifies leakage sources to a constant leakage area and leakage rate, which deviates significantly from real-world conditions. As a result, the potential impact zones obtained are conservative and do not provide a more accurate range of hazardous areas. Therefore, this study addresses this issue by fitting the gas leakage velocity and diffusion area and by developing a User-Defined Function (UDF) to control the dynamic changes in leakage velocity and area, thereby reflecting the actual gas leakage conditions. Compared to previously developed fixed leakage source models, this approach better simulates the gas leakage and diffusion patterns under real conditions. Consequently, this research employs the coupled model to investigate the diffusion characteristics of hydrogen-blended natural gas leaking from buried pipelines into the atmosphere, considering factors such as the hydrogen blending ratio (HBR), wind speed, temperature, and soil properties. The findings of this study can inform the development of future emergency decision-making procedures for managing pipeline leaks.

#### **2. Numerical Method**

#### *2.1. Physical Model*

To investigate the diffusion patterns of natural gas in the atmosphere after soil seepage, a three-dimensional simulation model is employed. Initially, an underground leakage diffusion model was established with dimensions of  $4 \text{ m} \times 4 \text{ m} \times 3 \text{ m}$  (length  $\times$  width  $\times$  height). Upon solving the underground leakage diffusion model, it was observed that the velocity of hydrogen-doped natural gas seeping from the soil to the surface approximates an elliptical distribution. Consequently, the gas diffusion inlet into the atmospheric domain model is configured as a circular region located at the center of the model's bottom. To comprehensively examine the coupled diffusion of hydrogen-doped natural gas from soil to atmosphere, the dimensions of the atmospheric domain model were set to 450 m  $\times$  300 m  $\times$  150 m (length  $\times$  width  $\times$  height). The geometric configuration is illustrated in Figure [2.](#page-3-0)

<span id="page-3-0"></span>

**Figure 2.** Schematic of the geometric model. **Figure 2.** Schematic of the geometric model.

## *2.2. Mathematical Model 2.2. Mathematical Model*

The following assumptions were made for this study:

- (a) The soil is set up as an isotropic homogeneous porous medium and the spatial struc-structure of the soil does not change during mass transfer. (a) The soil is set up as an isotropic homogeneous porous medium and the spatial
- ture of the soil does not change during mass transfer. (b) There is no chemical reaction between the leaking gas and the surrounding soil.
- $\overline{b}$  Therefore is no chemical reaction between the case and the soil. is ignored. Only the mass transfer (c) Heat transfer between the gas and the soil is ignored. Only the mass transfer process (c) Heat transfer between the gas and the soil is ignored. Only the mass transfer process occurs.
- (d) Assume that the soil pores are filled with air and ignore moisture in the soil.

 $\overline{d}$  When gas flows and diffuses, the fluid dynamics conservation equations, namely mass conservation, momentum conservation, and energy conservation, are usually followed. Therefore, the corresponding continuity, momentum, and energy equations can be derived. In addition, there are gas state equations and component transport equations [\[33\]](#page-18-9).

The continuity conservation equation is shown in Equation (1):

$$
\frac{\partial(\rho \varepsilon)}{\partial t} + \nabla \cdot (\rho v_i) = 0
$$
\nre  $v_i$  is the gas velocity in  $x$ ,  $y$ , and  $z$  directions,  $m/s$ .

\n(1)

 $\frac{z}{z}$  directions, m/s. where  $v_i$  is the gas velocity in *x*, *y*, and *z* directions, m/s.<br>The memorium concernation equation is above in

The momentum conservation equation is shown in Equation (2):

$$
\frac{\partial(\rho v_i)}{\partial t} + \frac{\partial(\rho v_i v_j)}{\partial x_j} = -\frac{\partial P}{\partial x_i} + \frac{\partial \theta_{ij}}{\partial x_j} + F_i
$$
 (2)

 $($ <sup>*j*</sup> $)$   $\frac{1}{2}$   $($ *j*<sub>2</sub> $\frac{1}{2}$   $)$   $\frac{1}{2}$   $\frac{1}{$ *i v v v P* where *ρ* is the fluid density, kg/m<sup>3</sup>;  $\theta_{ij}$  is the shear stress, N/m<sup>2</sup>;  $F_i$  is *i* the directional mass *t x x x* force,  $m/s^2$ .

The substance transport equation is shown in Equation (3):

$$
\frac{\partial}{\partial t}(\varepsilon \rho \omega_i) + \nabla \cdot (\rho \omega_i \nu) = \nabla \cdot (\rho D \nabla \omega_i) + S_i \tag{3}
$$

where *v* is the velocity vector, m/s; *D* is the diffusion coefficient;  $\nabla$  is the Hamiltonian operator; *ε* is the porosity;  $S_i$  is the user-determined rate of the *i* substance, m/s; *ρ* is the fluid density, kg/m<sup>3</sup>;  $\omega_i$  is the volume fraction of component *i*.

The turbulent flow of gases presents a highly intricate issue necessitating the selection of appropriate turbulence models tailored to specific scenarios. Factors influencing model selection typically include whether the fluid behaves as an ideal gas, the requisite computational precision, and the computational capabilities available. In this study, the *k*-*ε* model was employed, with its specific equations detailed in Equations (4) and (5) below:

*k* equation:

$$
\frac{\partial(\rho k)}{\partial t} + \frac{\partial(\rho k u_i)}{\partial x_i} = \frac{\partial}{\partial x_j} \left[ \left( \mu + \frac{\mu_t}{\sigma_k} \right) \frac{\partial k}{\partial x_j} \right] + G_k - \rho \varepsilon \tag{4}
$$

*ε* equation:

$$
\frac{\partial(\rho \varepsilon)}{\partial t} + \frac{\partial(\rho \varepsilon u_i)}{\partial x_i} = \frac{\partial}{\partial x_j} \left[ \left( \mu + \frac{\mu_t}{\sigma_{\varepsilon}} \right) \frac{\partial \varepsilon}{\partial x_j} \right] + \rho C_1 E \varepsilon - \rho C_2 \frac{\varepsilon^2}{k + \sqrt{\nu \varepsilon}}
$$
(5)

#### *2.3. Implementation of the Soil Atmosphere Coupled Diffusion Dynamic Leakage Source*

Firstly, according to the calculation of Le Chatelier's law in Formula (6) for the explosive limit of mixed gases [\[34–](#page-18-10)[37\]](#page-18-11), the lower explosion limit (LEL) of the gas mixture at various HBRs is determined, as shown in Table [1.](#page-4-0) The potential explosion zone of the gas mixture is defined by its LEL, while for methane and hydrogen, their respective lower explosion limits mark their potential explosion zones.

$$
\frac{1}{\text{LEL}_{\text{mix}}} = \sum_{i=1}^{N} \frac{Y_i}{\text{LEL}_i}
$$
(6)

where *LELmix* is the lower explosive limit of the gas mixture; *i* and *mix* are gas component i and the gas mixture;  $Y_i$  is the concentration of component i, %;  $LEL_i$  is the lower explosive limit of component i, %; *N* is the amount of combustible gas components.

<span id="page-4-0"></span>**Table 1.** Lower explosive limit of HBNG.

HBR $(\%)$			10		20		30
LEL $(vol\%)$	ັ	4.94	$\circ$ 4.OO	$\circ$ I.VZ	76	<b>I.I</b>	4.65

Based on the diffusion law of gas under the influence of porous media, we fit the diffusion range and diffusion rate of gas on the ground surface over time. According to GB/T 20936.1-2022 "Gas detectors for explosive environments—Part 1: Performance requirements for combustible gas detectors" and references [\[33,](#page-18-9)[38\]](#page-18-12), the maximum alarm concentration of gas shall not exceed 20% of the LEL. Therefore, relevant regulations are also adopted in the UDF compilation. Taking HBR = 15% as an example, if the LEL of the mixed gas is 4.82%, the alarm concentration should not exceed 0.96%. The diffusion range and gas diffusion rate when the HBNG concentration on the ground reaches 0.96% will be recorded, and the values will be fitted. Gas leakage is a process that changes dynamically with the leakage time. The dynamic change rate of gas leakage is obtained by integrating the dynamic change curve, which truly reflects the situation of gas leakage. We obtained

btain Formulas (2) and (3) as the formulas for compilation in the UDF. Figure [3](#page-5-0) shows the gas diffusion range and leakage rate under loam soil conditions at HBR = 15%.

$$
R_0 = 2.1 - [3.4/(1 + (\exp(t + 39.95)/453.89))]
$$
\n(7)

$$
V_0 = 9.44 \times 10^{-5} + [0.015 / (1 + \exp((t + 5871.52) / 1046.43))]
$$
\n(8)

where  $R_0$  is the radius of gas diffusion, m;  $V_0$  is the gas diffusion velocity, m/s; *t* is the leakage time, s.

<span id="page-5-0"></span>

**Figure 3.** Diffusion range versus diffusion rate.

ranction (CDT). This CDT was accelepted to harmate his importation this the nature has simulation solution via the C editor in Visual Studio 2019. This integration aims to dy-region. Figure [4](#page-6-0) illustrates the flowchart of the UDF compilation process. The essential In this study, Equations (7) and (8) were fitted and integrated into a user-defined function (UDF). This UDF was developed to facilitate its importation into the numerical namically adjust both the diffusion range and diffusion rate over time within the specified code snippets are detailed below:

 $begin\_ref\_loop(f, t)$ 

 ${F_{\text{-}}CENTROID(xc, f, t)}$ 

temp = sqrt((xc[0]-pX)\*(xc[0]-pX) + (xc[1]-pY)\*(xc[1]-pY));// Determine the coordinates of the point of the center of diffusion of the dynamic circle leakage.

if (temp  $<$  R0)

 ${F_PROFILE(f, t, i) = flow_V0;}}$ 

After compilation via UDF, Figure 5 illustrates the variation in leakage velocities across different time points within the dynamic circular domain for  $HBR = 15%$ . In this figure, leakage velocities are centered at the circle's midpoint and progressively expand over time.

### $\overline{f}$   $\overline{f}$ ;  $\overline{f}$ ;  $\overline{f}$ ;  $\overline{f}$ 2.4. Simulation Parameters and Boundary Conditions

This article chooses a three-dimensional model with a velocity inlet set on the bottom wall and a wind speed inlet set on the left wall. Typically, researchers set the wind speed to a constant value to simplify model calculations, but this differs greatly from reality. The present article employs variable wind speed and utilizes an exponential function to depict the near-ground wind speed. The mathematical expression is shown in Equation (9) [\[39\]](#page-18-13). Other walls are set as pressure outlets to simulate the free flow of gas. The ground is set as "Wall", and the specific boundary conditions are shown in Table [2.](#page-7-0)

$$
u_z = u_1 \left(\frac{z}{z_1}\right)^{\alpha} \tag{9}
$$

where  $u_z$  is the average wind speed at a near-surface height of  $z$ ;  $u_1$  is the standard wind speed  $(m/s)$ ;  $\alpha$  is the surface roughness, which generally takes the value of 0.1–0.4; in this paper, it takes 0.4  $[40]$ ;  $z_1$  is the height from the ground and  $z_1$  is taken as 10 m.

<span id="page-6-0"></span>

<span id="page-6-1"></span>**Figure 4.** UDF compilation flow chart. **Figure 4.** UDF compilation flow chart.



**Figure 5.** Plot of inlet dynamic circle changes at different moments under UDF compilation. Figure 5. Plot of inlet dynamic circle changes at different moments under UDF compilation.<br> **Figure 5.** Plot of inlet dynamic circle changes at different moments under UDF compilation.



<span id="page-7-0"></span>**Table 2.** Setting of boundary conditions.

The soil can be roughly classified into sandy and loamy soils by the average grain size of the soil [\[41](#page-18-15)[,42\]](#page-18-16). China has abundant and diverse soil resources, which can be roughly divided into sandy soil and loam soil based on their average particle size. Table [3](#page-7-1) provides the physical parameters of different soil properties.

<span id="page-7-1"></span>**Table 3.** Physical parameters of different soil types.



According to the common pressure range of medium- and low-pressure pipelines in GB 55009-2021 [\[43\]](#page-18-17) Gas Engineering Project Specification and referencing relevant literature [\[28,](#page-18-4)[30,](#page-18-6)[44–](#page-18-18)[49\]](#page-18-19), we set the pipeline pressure to 0.4 MPa and selected three hydrogen blending ratios of 5%, 15%, and 30%. Due to the characteristic of pipeline leakage mostly being small hole leakage [\[50\]](#page-18-20), in this study, we mainly explore the leakage of small holes with a leakage aperture of 10 mm. Based on the research of relevant researchers and relevant references [\[40,](#page-18-14)[51\]](#page-18-21), the wind speed was selected based on the annual average wind speed in a certain area of southwestern Chongqing, which ranges from  $0.6$  m/s to  $7$  m/s, and we selected the temperatures of 278 K, 288 K, and 300 K.

#### *2.5. Model Reliability and Grid Independence Verification*

Despite the correlation analysis of the mathematical model, it is still necessary to verify the model to ensure the reliability of the simulation. Liang [\[52\]](#page-18-22) calculated the leakage and diffusion law of natural gas in the atmospheric domain through a simulation model of 50 m  $\times$  50 m  $\times$  50 m, in which the mass flow rate was defined as 0.07 kg/s and the leakage time was 60 s. In this paper, the physical model, boundary conditions, and parameter values consistent with the beam are selected, and the numerical simulation results of this study are compared with those of the beam, as shown in Figure [6](#page-8-0) below. Through comparison, it can be observed that the gas diffusion law in the two cloud images after the gas leakage is roughly similar, showing an upward diffusion plume, and the development direction of the jet is basically the same. Therefore, it can be considered that the numerical simulation model proposed in this paper is feasible.

The computational domain was meshed using unstructured meshing with Fluent Meshing software, as illustrated in Figure [7.](#page-8-1) The grid size was locally refined to 0.01 m at the leakage points. After verification, the grid quality exceeded 0.7, ensuring sufficient calculation accuracy. For simulating gas leakage in the atmosphere, the model was tested with four different grid densities: 580,000, 1,210,000, 2,020,000, and 3,100,000 grid cells. A monitoring point positioned 10 m above the leakage source tracked the methane concentration over time, depicted in Figure [8.](#page-8-2) After evaluating calculation accuracy and computer performance, a grid of 1,210,000 cells was selected for the final simulation.

<span id="page-8-0"></span>

Figure 6. Model validation: (a) the research model and (b) the literature [\[52\]](#page-18-22) research model.  $p$  grid of 1,210,000 cells was selected for the final simulation.

<span id="page-8-1"></span>

**Figure 7.** Unstructured grid. **Figure 7.** Unstructured grid.

<span id="page-8-2"></span>

**Figure 8.** Grid-independent verification. **Figure 8.** Grid-independent verification.

## **3. Results and Discussion 3. Results and Discussion**

To ensure the safety of personnel in the vicinity following a gas leak, this study ad-to relevant national standards [\[53\]](#page-18-23) and references [\[54](#page-19-0)[–56\]](#page-19-1). As a precautionary measure, the heres to relevant national standards [53] and references [54–56]. As a precautionary meas-concentration limit is set at 1/50 of the 10% Lower Explosive Limit (LEL). Areas where gas concentration limit is set at 1/50 of the 10% Lower Explosive Limit (LEL). These writes gas<br>concentrations exceed this limit are identified as potentially hazardous and require safety investigation. Consequently, subsequent sections will present diffusion distribution cloud maps of hydrogen-blended natural gas (HBNG) under varying operational conditions. These maps will delineate potentially hazardous areas bounded by  $1/50$  of the 10% LEL of the gas mixture's concentration.  $\overline{0}$ To ensure the safety of personnel in the vicinity following a gas leak, this study adheres

#### *3.1. Comparative Analysis of the Leakage Fixed Source and Dynamic Leakage Source*

The leakage velocity of hydrogen-doped natural gas from the soil to the ground surface typically forms an elliptical distribution. There exists a significant disparity between the diffusion rates of the gas in soil and in the atmospheric environment. Consequently, many researchers use the stabilized surface leakage velocity as the initial condition. To determine this average leakage velocity, one must first integrate the leakage velocity over time, as demonstrated in Equation (10).

$$
\int_{100}^{1800} v_0(t)dt\tag{10}
$$

When considering the average leakage velocity, Figure [9](#page-9-0) illustrates contour plots depicting the diffusion distribution of HBNG in the atmosphere at various time intervals. Within 60 s of the leakage, the gas diffusion range expands rapidly vertically due to minimal wind turbulence. By 600 s, the gas concentration reaching hazardous levels extends vertically to the model boundary, covering a distance of 150 m, with a horizontal diffusion of 41 m. Between 600 and 1800 s, the diffusion range stabilizes under the influence of atmospheric buoyancy forces. Over time, the diffusion range of low-concentration areas distant from the leakage point exhibits significant changes, with vertical diffusion distances of HBNG increasing gradually while the growth rate diminishes.

<span id="page-9-0"></span>

**Figure 9.** HBNG diffusion range for fixed leakage rate at different moments of time.

When the leakage rate varies over time (dynamic leakage rate), Figure [10](#page-10-0) presents contour plots illustrating the diffusion distribution of HBNG in the atmosphere at different time intervals. The plots indicate that as leakage time increases, the gas diffusion range gradually expands vertically. Although the diffusion patterns of dynamic and fixed leakage rates are generally similar, the dynamic rate results in a larger diffusion range. For instance, at a leakage time of 10 s, the vertical extent of the hazardous area calculated using a fixed velocity is 18.2 m, whereas with dynamic leakage velocity calculation, it extends to 18.45 m vertically.

<span id="page-10-0"></span>

Figure 10. Contour plots of HBNG gas concentration distribution in the Z-X plane at different moments.

Figure [11](#page-10-1) shows the range of potential ignition and explosion region formed by gas in a vertical direction calculated by using the fixed leakage source and dynamic leakage source at different times. It shows that the use of UDF dynamic leakage velocity results in a greater vertical spread of the potential explosion area compared to using a fixed leakage velocity. For instance, at 5 s of HBNG leakage, the vertical extent of the potential explosive region measures 5.65 m with dynamic leakage velocity and 5.4 m with fixed leakage velocity. Similarly, at 30 s of leakage, the vertical extent is 25.3 m with dynamic leakage velocity compared to 25.22 m with fixed leakage velocity.

<span id="page-10-1"></span>

Figure 11. Vertical diffusion range of HBNG at different moments.

## $\overline{\phantom{a}}$  are at diffusion at diffusion at diffusion at diffusion at diffusion at diffusion at different wind speeds in the diffusion at diffusion at diffusion at diffusion at different wind speeds in the different wind 3.2. Analysis of Dynamic Leakage Sources<br> **3.2. Analysis of Dynamic Leakage Sources**

3.2.1. Effects of Different Wind Speeds<br>3.2.1. Effects of Different Wind Speeds

speed increases, the vertical diffusion range decreases, showing a negative correlation. (1) Z-X planar HBNG leakage cloud map (1) Z-X planar HBNG leakage cloud map

In [th](#page-11-0)is section, conditions 1, 2, 3 and 4 in Table 4 are used to study the diffusion law of HBNG in the atmosphere under different wind speeds, and the influence of different wind fibred in the atmosphere under different wind speeds, and the influence of different wind<br>speeds on gas diffusion after leakage is discussed. Simulations are conducted under four area's cloud diagram resulting from HBNG diffusion at different wind speeds in the Z-X piane. From Figure 12, it is evident that wind speed significantly influences the di paul of Tibryd. At 0 m/s wind speed, the gas primarily diffuses vertically. A wind speeds on gas diffusion after realings is discussed. Simulations are conducted under road wind speed conditions:  $0 \text{ m/s}, 1.5 \text{ m/s}, 3 \text{ m/s},$  and  $5 \text{ m/s}$ . Figure [12](#page-11-1) depicts the hazardous plane. From Figure [12,](#page-11-1) it is evident that wind speed significantly influences the diffusion  $\frac{1}{2}$ -x plane. From Figure 12, it is evident that wind speed significantly influences the diffuse vertically  $\Lambda_5$  wind speed path of HBNG. At 0 m/s wind speed, the gas primarily diffuses vertically. As wind speed increases, the vertical diffusion range decreases, showing a negative correlation. Conversely, the horizontal diffusion range increases with wind speed, indicating a positive correlation. Hence, greater safety risks exist for populations residing in downwind directions.

<span id="page-11-0"></span>**Table 4.** Operating condition setting table.



<span id="page-11-1"></span>

**Figure 12.** Distribution of HBNG gas concentration in the Z-X plane at different wind speeds.

#### (2) HBNG diffusion range

Different wind speeds affect the diffusion of HBNG in potentially hazardous and explosive areas, as illustrated in Figure [13.](#page-12-0) It is evident from the figure that both the vertical diffusion range of potentially hazardous areas and explosive areas of HBNG decreases with increasing wind speed. Conversely, the horizontal diffusion range increases with wind speed. The maximum vertical diffusion range of the potentially hazardous area of HBNG ranges from 24 m to 150 m. At a wind speed of 0 m/s, the vertical diffusion range HBNG ranges from 24 m to 150 m. At a wind speed of 0 m/s, the vertical diffusion range of the potential explosive area of HBNG is greatest. At a wind speed of  $5 \text{ m/s}$ , the vertical diffusion range decreases to a minimum of 2.82 m. diffusion range decreases to a minimum of 2.82 m.

<span id="page-12-0"></span>

**Figure 13.** HBNG potentially hazardous area and explosive area spreading range under different wind speeds.

#### 3.2.2. Effect of Different HBR

(1) Z-X planar HBNG leakage cloud map

The study investigated the impact of varying HBR ratios on gas diffusion following leakage. Calculations were conducted for three scenarios: HBR = 5%, HBR = 15%, and HBR = 30%. Figure [14](#page-13-0) illustrates the gas diffusion distances for HBNG under these conditions. From the figure, it can be observed that at  $HBR = 5\%$ , the vertical diffusion extends up to 24 m within the potential explosive zone, whereas at HBR =  $30\%$ , it extends to 28 m, indicating a significant increase with higher HBR ratios. In the horizontal direction, the diffusion range at HBR =  $5\%$  spans 4.05 m, while at HBR =  $30\%$ , it slightly increases to 4.15 m. This minor change suggests that higher HBR ratios do not significantly enhance gas diffusion in the horizontal plane.

#### (2) HBNG diffusion range

In this section, conditions 1–12 in Table [4](#page-11-0) are selected, the ranges of potentially hazardous and explosive areas formed by gases under different HBRs are shown in Figure [15,](#page-13-1) from which it can be observed that the vertical diffusion range of the potentially hazardous and explosive areas of HBNG decreases with the increase in wind force, while the horizontal diffusion range increases with the increase in the wind speed. The maximum vertical diffusion range of the potentially hazardous area of HBNG is 150 m, and the minimum diffusion range is 23 m; the maximum vertical diffusion range of the potential explosive area is 28 m, and the minimum diffusion height is only 2 m.



(a) HBR =  $5\%$ 

**Figure 14.** *Cont*.

<span id="page-13-0"></span>

(c) HBR =  $30\%$ 

Figure 14. Contour map of gas hazard and explosion zones at different HBRs. play are conveniently to got minimum diffusion here in interesting

<span id="page-13-1"></span>

**Figure 15.** Curves of potentially hazardous areas formed by different HBRs versus the range of **Figure 15.** Curves of potentially hazardous areas formed by different HBRs versus the range of explosive areas. explosive areas.

3.2.3. Effect of Different Temperature 3.2.3. Effect of Different Temperature

(1) Z-X planar HBNG leakage cloud map (1) Z-X planar HBNG leakage cloud map

In order to study the influence of different temperatures on the gas diffusion after In order to study the influence of different temperatures on the gas diffusion after leakage, a city in southwest China was taken as an example, and the typical temperatures leakage, a city in southwest China was taken as an example, and the typical temperatures of T = 278 K, T = 288 K and T = 300 K were analyzed by selecting working conditions 1, and 18 in Table 4. [Th](#page-11-0)e gas diffusion ranges of HBNG at these temperatures are illustrated 17 and 18 in Table 4. The gas diffusion ranges of HBNG at these temperatures are illustrated in Figure [16. A](#page-14-0)nalysis of Figure 1[6 in](#page-14-0)dicates that temperature minimally affects the gas in Figure 16. Analysis of Figure 16 indicates that temperature minimally affects the gas diffusion range in the atmospheric environment post leakage. After 1800 s of leakage, the vertical diffusion heights of the potentially explosive gas region measure 21.5 m at  $T = 278$  K, 25.41 m at T = 288 K, and 26.1 m at T = 300 K. The vertical diffusion heights of hazardous regions have fully extended to the model's boundary. potentially hazardous regions have fully extended to the model's boundary.

<span id="page-14-0"></span>

 $(c) T = 300 K$ 

**Figure 16.** HBNG gas concentration distribution at different temperatures. **Figure 16.** HBNG gas concentration distribution at different temperatures.

## (2) HBNG diffusion range (2) HBNG diffusion range

The range of potentially hazardous and explosive areas formed by HBNG at various The range of potentially hazardous and explosive areas formed by HBNG at various temperatures is depicted in Figure [17.](#page-14-1) The figure illustrates that the extent of these areas temperatures is depicted in Figure 17. The figure illustrates that the extent of these areas increases slightly with rising temperature, although the overall change is minimal. At 278 K, the vertical diffusion height of the potentially explosive gas region measures 21.5 m, with a horizontal diffusion range of 3.95 m. When the temperature rises to 300 K, these measurements change to a vertical diffusion height of 26 m and a horizontal diffusion range of 4.15 m. inperatures is depicted in Figure 17. The figure indicates that the extent of the

<span id="page-14-1"></span>

**Figure 17.** Potential hazards of HBNG at different temperatures and vertical and horizontal **Figure 17.** Potential hazards of HBNG at different temperatures and vertical and horizontal dispersion ranges of explosive regions.

- 3.2.4. Effect of Different Soil Properties
- (1) Z-X planar HBNG leakage cloud map

In previous studies, we have observed significant effects of soil properties on gas diffusion. Thus, this section examines gas diffusion patterns in the atmosphere by considering gas diffusion velocities under different soil conditions as the initial boundary conditions. Prior research indicates that gas diffusion concentrations from clay soil on the ground surface do not reach hazardous levels. This study focuses on comparative analysis between loamy and sandy soils. Figure [18](#page-15-0) illustrates the variation in HBNG gas concentrations over time following leaks under different soil conditions. The figure demonstrates that the gas concentration at ground level significantly influences diffusion. Specifically, after 1800 s of leakage, HBNG reaches 33.8 m at the lower explosive limit contour in sandy soil compared to 25.41 m in loamy soil, marking a 33% difference between the two.

<span id="page-15-0"></span>

**Figure 18.** HBNG gas diffusion cloud map under different soil properties.

#### (2) HBNG diffusion range

Working conditions 1–4 and 13–16 in Table [4](#page-11-0) were selected for research, the distribution of potentially hazardous and explosive zones created by HBNG under varying soil properties is illustrated in Figure [19.](#page-16-0) The figure highlights significant differences in the extent of explosion and hazard zones resulting from gas leakage under sandy and loamy soil conditions. In sandy soil, the vertical diffusion height of the potential explosive zone at wind speeds of  $0 \text{ m/s}$  reaches 33.8 m, whereas in loamy soil, it only extends to 25.41 m. As the wind speed increases, the vertical difference between the two zones gradually diminishes, and the horizontal extent of the potential explosive zone expands approximately linearly with wind speed. Regarding the hazardous area's diffusion range, at a vertical wind speed of  $0 \text{ m/s}$ , gas diffuses up to 150 m from the top boundary of the model after 1800 s of leakage. As the wind speed increases, vertical diffusion diminishes while horizontal spread increases; at wind speeds of  $1.5 \text{ m/s}$  and above, gas diffuses to the model's boundary under wind influence.

<span id="page-16-0"></span>

**Figure 19.** HBNG hazardous area and explosive area range for different soil properties. **Figure 19.** HBNG hazardous area and explosive area range for different soil properties.

#### **4. Conclusions**

To characterize the similarities and differences in the diffusion patterns of leaking gases from the soil to the atmosphere coupled, a model using a fixed leakage rate and a dynamic leakage rate was used. In this study, based on CFD numerical simulation and the three theoretical equations of fluid dynamics, a functional relationship between leakage velocity and time is proposed and compiled and solved using the UDF. On this basis, a three-dimensional model with a length  $\times$  width  $\times$  height of 450 m  $\times$  300 m  $\times$  150 m was established to study the diffusion characteristics of the gas, and the effects of different wind speeds, HBR, temperature, and soil properties on the gas leakage and diffusion characteristics were mainly analyzed, and the main conclusions were drawn as follows:

- (1) After comparative analysis of the leakage source and dynamic leakage source, the diffusion range of the potential explosion region formed by gas in the dynamic leakage source is larger than that obtained by the leakage source used by previous researchers;
- (2) Wind speed has a significant impact on the hydrogen-doped natural gas leakage; with the increase in ambient wind speed, the vertical diffusion height of hydrogendoped natural gas is gradually reduced, and the two show a negative correlation. The horizontal diffusion distance of the gas increases with the increase in wind speed, and the two show a positive correlation;
- (3) Different hydrogen doping ratios (HBR) have a certain effect on the diffusion range of the gas in the vertical region and have less effect on the diffusion range of the gas in the horizontal direction;
- (4) At atmospheric temperatures of 278 K, 288 K and 300 K, the diffusion pattern of the leaking gas and the range of potentially hazardous areas and explosive areas formed in the atmosphere are not greatly changed, and the atmospheric temperature has less influence on the diffusion pattern of the gas after the leakage and the range of potential influence areas formed;
- (5) At the same moment, the gas diffusion velocity of different soil properties has a significant effect on the diffusion of gas in the atmosphere; the vertical diffusion height of hydrogen-doped natural gas from sandy soil to the atmospheric domain after diffusion for 1800 s is 33.8 m and that of loamy soil is 25.41 m, which is a 33% difference between the two.

**Author Contributions:** S.R. and J.H.: writing—original draft and writing—review and editing. G.L. and X.W.: methodology, writing—review and editing, project administration, and supervision. J.L.: formal analysis. J.B.: resources and project administration. All authors have read and agreed to the published version of the manuscript.

**Funding:** This study was financially supported by the National Natural Science Foundation of China (Grant no.: 52104063).

**Data Availability Statement:** All data are provided within the manuscript.

**Acknowledgments:** The authors wish to express their sincere thanks to the anonymous editors and reviewers for their conscientious reading and numerous valuable comments which greatly improved the presentation of this paper.

**Conflicts of Interest:** Author Shuai Ren was employed by the PipeChina Southwest Pipeline Company. Author Jiuqing Ban and Jiyong Long were employed by the PetroChina Southwest Oil and Gas Field Company. The remaining authors declare that the research was conducted in the absence of any commercial or financial relationships that could be construed as a potential conflict of interest.

#### **References**

- <span id="page-17-0"></span>1. Qiu, Y.; Zhou, S.; Gu, W.; Pan, G.; Chen, X. Application prospect analysis of hydrogen enriched compressed natural gas technologies under the target of carbon emission peak and carbon neutrality. *Proc. CSEE* **2022**, *42*, 1301–1320.
- 2. Yin, Z.; Yang, G.; Liu, H.; Ma, Q.; Hao, J. Research status and prospect analysis of key technologies for hydrogen energy storage and transportation. *Mod. Chem. Ind.* **2021**, *41*, 53–57.
- <span id="page-17-1"></span>3. Ban, J.; Yan, X.; Song, B.; Deng, S.; Wu, H.; Tang, Y.; Yin, W. Research Progress and Prospects on Hydrogen Damage in Welds of Hydrogen-Blended Natural Gas Pipelines. *Processes* **2023**, *11*, 3180. [\[CrossRef\]](https://doi.org/10.3390/pr11113180)
- <span id="page-17-2"></span>4. Tong, S.; Li, X.; Ding, H.; Shuai, J.; Mei, Y.; Chan, S.H. Large-scale transient simulation for consequence analysis of hydrogen-doped natural gas leakage and explosion accidents. *Int. J. Hydrog. Energy* **2024**, *54*, 864–877. [\[CrossRef\]](https://doi.org/10.1016/j.ijhydene.2023.08.088)
- 5. Huang, W.; Gong, J. Prospect for the development of natural gas network and the multi-energy integration technology in pipeline networks. *Oil Gas Storage Transp.* **2023**, *42*, 1321–1328.
- <span id="page-17-3"></span>6. Zhu, H.; Chen, J.; Su, H.; Tang, T.; He, S. Numerical Investigation of the Natural Gas-hydrogen Mixture Stratification Process in an Undulating Pipeline. *J. Southwest Pet. Univ. (Sci. Technol. Ed.)* **2022**, *44*, 132–140.
- <span id="page-17-4"></span>7. Wang, L.; Chen, J.; Ma, T.; Ma, R.; Bao, Y.; Fan, Z. Numerical study of leakage characteristics of hydrogen-blended natural gas in buried pipelines. *Int. J. Hydrog. Energy* **2024**, *49*, 1166–1179. [\[CrossRef\]](https://doi.org/10.1016/j.ijhydene.2023.07.293)
- 8. Amin, M.; Shah, H.H.; Fareed, A.G.; Khan, W.U.; Chung, E.; Zia, A.; Farooqi, Z.U.R.; Lee, C. Hydrogen production through renewable and non-renewable energy processes and their impact on climate change. *Int. J. Hydrog. Energy* **2022**, *47*, 33112–33134. [\[CrossRef\]](https://doi.org/10.1016/j.ijhydene.2022.07.172)
- <span id="page-17-5"></span>9. Hassan, Q.; Abdulateef, A.M.; Hafedh, S.A.; Al-samari, A.; Abdulateef, J.; Sameen, A.Z.; Salman, H.M.; Al-Jiboory, A.K.; Wieteska, S.; Jaszczur, M. Renewable energy-to-green hydrogen: A review of main resources routes, processes and evaluation. *Int. J. Hydrog. Energy* **2023**, *48*, 17383–17408. [\[CrossRef\]](https://doi.org/10.1016/j.ijhydene.2023.01.175)
- <span id="page-17-6"></span>10. Vechkinzova, E.; Steblyakova, L.P.; Roslyakova, N.; Omarova, B. Prospects for the Development of Hydrogen Energy: Overview of Global Trends and the Russian Market State. *Energies* **2022**, *15*, 8503. [\[CrossRef\]](https://doi.org/10.3390/en15228503)
- <span id="page-17-7"></span>11. Li, J.; Su, Y.; Zhang, H.; Yu, B. Research progress of hydrogen-doped natural gas pipeline transportation. *Nat. Gas Ind.* **2021**, *41*, 137–152.
- <span id="page-17-8"></span>12. Edwards, R.L.; Font-Palma, C.; Howe, J. The status of hydrogen technologies in the UK: A multi-disciplinary review. *Sustain. Energy Technol. Assess.* **2021**, *43*, 100901. [\[CrossRef\]](https://doi.org/10.1016/j.seta.2020.100901)
- <span id="page-17-9"></span>13. Neil, E. UK Hydrogen Strategy. *Chem. Ind.* **2021**, *85*. Available online: <www.gov.uk/official-documents> (accessed on 1 September 2024).
- <span id="page-17-10"></span>14. Wang, H.; Xiong, S.; Zhang, X.; Wang, M.; Sun, M.; Wang, Z.; Wu, R.; Fu, P. Application status and analysis of hydrogen blending technology of natural gas. *Gas Heat* **2021**, *41*, 12–15+45.
- <span id="page-17-11"></span>15. Kar, S.K.; Sinha, A.S.K.; Bansal, R.; Shabani, B.; Harichandan, S. Overview of hydrogen economy in Australia. *Wiley Interdiscip. Rev. Energy Environ.* **2023**, *12*, e457. [\[CrossRef\]](https://doi.org/10.1002/wene.457)
- <span id="page-17-12"></span>16. Peng, S.; Luo, X.; Yang, L. Numerical simulation of leakage and diffusion rules of hydrogen blended natural gas long-distance transportation pipelines. *Chem. Eng. Oil Gas* **2023**, *52*, 44–52+59.
- <span id="page-17-13"></span>17. Zhang, C.; Song, P.; Hou, J.; Wang, X. A new development mode for deep integration between natural gas and hydrogen energy industries in carbon neutralization progress. *Mod. Chem. Ind.* **2022**, *42*, 7–12.
- 18. Zhong, B.; Zhang, X.; Zhang, B.; Peng, S. Industrial Development of Hydrogen Blending in Natural Gas Pipelines in China. *Strateg. Study CAE* **2022**, *24*, 100–107. [\[CrossRef\]](https://doi.org/10.15302/J-SSCAE-2022.03.011)
- <span id="page-17-14"></span>19. Lu, Y.; Zhao, J. Hydrogen entering myriad homes helps achieving the "double carbon" goal and constructing ecological civilization. *Mech. Eng.* **2022**, *44*, 489–490.
- <span id="page-17-15"></span>20. Qiao, J.; Guo, B.; Ma, X.; Hou, J.; Yan, S. Discussion on key technologies of hydrogen blending transportation in city gas pipeline network. *GAS HEAT* **2023**, *43*, 19–22.
- <span id="page-17-16"></span>21. Yang, F.; Wang, T.; Deng, X.; Dang, J.; Huang, Z.; Hu, S.; Li, Y.; Ouyang, M. Review on hydrogen safety issues: Incident statistics, hydrogen diffusion, and detonation process. *Int. J. Hydrog. Energy* **2021**, *46*, 31467–31488. [\[CrossRef\]](https://doi.org/10.1016/j.ijhydene.2021.07.005)
- <span id="page-17-17"></span>22. Zhang, H.; Li, J.; Su, Y.; Wang, P.; Yu, B. Effects of hydrogen blending on hydraulic and thermal characteristics of natural gas pipeline and pipe network. *Oil Gas Sci. Technol.–Rev. D'ifp Energ. Nouv.* **2021**, *76*, 70. [\[CrossRef\]](https://doi.org/10.2516/ogst/2021052)
- <span id="page-17-18"></span>23. Shang, M. Simulation and Analysis of Influencing Factors of Hydrogen Leakage, Combustion and Explosion in Hydrogen Refueling Station. Master's Thesis, Shandong Jianzhu University, Jinan, China, 2022.
- <span id="page-18-0"></span>24. Pagliaro, M.; Iulianelli, A. Hydrogen refueling stations: Safety and sustainability. *Gen. Chem.* **2020**, *6*, 190029. [\[CrossRef\]](https://doi.org/10.21127/yaoyigc20190029)
- <span id="page-18-1"></span>25. Wu, Q.; Zhang, H.; Zhang, M.; Zhang, X.; Dong, S. Research status and evolution trend of pipeline transportation of hydrogenblended natural gas based on knowledge graph. *Oil Gas Storage Transp.* **2022**, *41*, 1380–1394.
- <span id="page-18-2"></span>26. Bu, F.; Liu, Y.; Liu, Y.; Xu, Z.; Chen, S.; Jiang, M.; Guan, B. Leakage diffusion characteristics and harmful boundary analysis of buried natural gas pipeline under multiple working conditions. *J. Nat. Gas Sci. Eng.* **2021**, *94*, 104047. [\[CrossRef\]](https://doi.org/10.1016/j.jngse.2021.104047)
- <span id="page-18-3"></span>27. Zhang, W.; Zhao, G. Leakage and diffusion characteristics of underground hydrogen pipeline. *Petroleum* **2024**, *10*, 319–325. [\[CrossRef\]](https://doi.org/10.1016/j.petlm.2023.06.002)
- <span id="page-18-4"></span>28. Hu, W.; Chen, G.; Qi, B.; Zhang, Y. Numerical simulation of leakage and diffusion of buried pure hydrogen/hydrogen-doped natural gas pipeline. *Oil Gas Storage Transp.* **2023**, *42*, 1118–1127+1136.
- <span id="page-18-5"></span>29. Su, Y.; Li, J.; Yu, B.; Zhao, Y.; Han, D.; Sun, D. Modeling of Hydrogen Blending on the Leakage and Diffusion of Urban Buried Hydrogen-Enriched Natural Gas Pipeline. *CMES-Comput. Model. Eng. Sci.* **2023**, *136*. [\[CrossRef\]](https://doi.org/10.32604/cmes.2023.026035)
- <span id="page-18-6"></span>30. Zhang, Y.; Yang, Y.; Wu, F.; Li, Q.; Wang, J.; Liu, H.; Che, D.; Huang, Z. Numerical investigation on pinhole leakage and diffusion characteristics of medium-pressure buried hydrogen pipeline. *Int. J. Hydrog. Energy* **2024**, *51*, 807–817. [\[CrossRef\]](https://doi.org/10.1016/j.ijhydene.2023.04.209)
- <span id="page-18-7"></span>31. Zhu, J.; Pan, J.; Zhang, Y.; Li, Y.; Li, H.; Feng, H.; Chen, D.; Kou, Y.; Yang, R. Leakage and diffusion behavior of a buried pipeline of hydrogen-blended natural gas. *Int. J. Hydrog. Energy* **2023**, *48*, 11592–11610. [\[CrossRef\]](https://doi.org/10.1016/j.ijhydene.2022.10.185)
- <span id="page-18-8"></span>32. Ye, Y.; Wang, Y. Numerical analysis on leakage and diffusion of buried gas pipeline based on atmosphere soil coupling. *J. Saf. Sci. Technol.* **2018**, *14*, 107–113.
- <span id="page-18-9"></span>33. *GB/T 20936.1-2022*; Gas Detectors for Explosive Atmospheres-Part 1: Performance Requirements for Combustible Gas Detectors. State Administration for Market Regulation; Standardization Administration of China: Beijing, China, 2022.
- <span id="page-18-10"></span>34. Gao, B.; Zhao, R.; Kuai, C.; Hu, M.; Wang, G. Numerical Simulation of Leak Diffusion and Failure Consequences of High-Pressure Hydrogen-Doped Natural Gas Pipelines. *J. Liaoning Petrochem. Univ.* **2023**, *43*, 60–66.
- 35. Han, H.; Chang, X.; Duan, P.; Li, Y.; Zhu, J.; Kong, Y. Study on the leakage and diffusion behavior of hydrogen-blended natural gas in utility tunnels. *J. Loss Prev. Process Ind.* **2023**, *85*, 105151. [\[CrossRef\]](https://doi.org/10.1016/j.jlp.2023.105151)
- 36. Koshiba, Y.; Hasegawa, T.; Kim, B.; Ohtani, H. Flammability limits, explosion pressures, and applicability of Le Chatelier's rule to binary alkane–nitrous oxide mixtures. *J. Loss Prev. Process Ind.* **2017**, *45*, 1–8. [\[CrossRef\]](https://doi.org/10.1016/j.jlp.2016.11.007)
- <span id="page-18-11"></span>37. Molnarne, M.; Schroeder, V. Hazardous properties of hydrogen and hydrogen containing fuel gases. *Process Saf. Environ. Prot.* **2019**, *130*, 1–5. [\[CrossRef\]](https://doi.org/10.1016/j.psep.2019.07.012)
- <span id="page-18-12"></span>38. *GB 50838-2015*; Technical Specification for Urban Integrated Pipe Corridor Engineering. Ministry of Housing and Urban-Rural Development of the People's Republic of China; General Administration of Quality Supervision, Inspection and Quarantine of the People's Republic of China: Beijing, China, 2015.
- <span id="page-18-13"></span>39. Zhang, X. *Structural Wind Engineering*; China Architecture & Building Press: Beijing, China, 2006.
- <span id="page-18-14"></span>40. Zhang, L. Application Research of City gas 3D Dynamic Leakage and Diffusion Coupled with CFD and GIS. Master's Thesis, Chongqing Jiaotong University, Chongqing, Chinam, 2015.
- <span id="page-18-15"></span>41. Ma, M.; Jiang, Z. Study on leakage and diffusion law of buried gas pipeline in tunnel. *Chem. Eng. Gas* **2022**, *51*, 132–137.
- <span id="page-18-16"></span>42. Zou, H.; Pei, P.; Hao, D.; Wang, C. Numerical analysis of the effect of different soil types and water content on heat transfer performance of horizontal buried pipes. *Coal Geol. Explor.* **2021**, *49*, 27.
- <span id="page-18-17"></span>43. *GB 55009-2021*; Project Code for Gas Engineering. Ministry of Housing and Urban-Rural Development of the People's Republic of China: Beijing, China, 2021.
- <span id="page-18-18"></span>44. Su, Y.; Li, J.; Yu, B.; Zhao, Y.; Li, J.; Han, D. Simulation study on the mixing of hydrogen and natural gas in static mixers. *Nat. Gas Ind.* **2023**, *43*, 113–122.
- 45. Sang, R. Study on Leakage and Diffusion of Pipeline Gas in Soil under Hardenedpavement. Master's Thesis, Shandong Jianzhu University, Jinan, China, 2019.
- 46. Zhang, C.; Li, J.; Zhang, Y.; Li, L.; Duan, P.; Wei, J. Safety Analysis of Hydrogen-Blended Natural Gas Leakage in Comprehensive Pipe Gallery. *J. Xi'an Jiaotong Univ.* **2024**, *58*, 22–30.
- 47. Wang, X.; Pu, M.; Song, L.; Chen, J.; Guo, J.; Sun, J.; Xue, H. Analysis on the Comparison between Hydrogen and Natural Gas Long Distance Pipeline Design. *Pet. New Energy* **2022**, *34*, 21–26.
- 48. Wang, K.; Li, C.; Jia, W.; Chen, Y.; Wang, J. Study on multicomponent leakage and diffusion characteristics of hydrogen-blended natural gas in utility tunnels. *Int. J. Hydrog. Energy* **2024**, *50*, 740–760. [\[CrossRef\]](https://doi.org/10.1016/j.ijhydene.2023.06.262)
- <span id="page-18-19"></span>49. Zhu, H.; Li, J.; Chen, J.; Su, H.; Tang, T. Numerical simulation analysis of the spontaneous combustion process during the venting of hydrogen-mixed natural gas line pipes. *Nat. Gas Ind.* **2023**, *43*, 149–161.
- <span id="page-18-20"></span>50. Bagheri, M.; Sari, A. Study of natural gas emission from a hole on underground pipelines using optimal design-based CFD simulations: Developing comprehensive soil classified leakage models. *J. Nat. Gas Sci. Eng.* **2022**, *102*, 104583. [\[CrossRef\]](https://doi.org/10.1016/j.jngse.2022.104583)
- <span id="page-18-21"></span>51. Wang, Y. Spatial Expansion of Wind Speed in Chongqing Based on GIS. Master's Thesis, Nanjing Institute of Meteorology, Nanjing, China, 2004.
- <span id="page-18-22"></span>52. Liang, J. Research on Leakage Amount Estimation and Diffusion Characteristics for Buried Gas Pipeline. Master's Thesis, China University of Petroleum (East China), QingDao, China, 2019.
- <span id="page-18-23"></span>53. *GB/T 50493-2019*; Petrochemical Combustible Gas and Toxic Gas Detection and Alarm Design Standard. State Administration for Market Regulation, Ministry of Housing and Urban-Rural Development of the People's Republic of China: Beijing, China, 2019.
- <span id="page-19-0"></span>54. Su, Y.; Li, J.; Yu, B.; Zhao, Y. Numerical investigation on the leakage and diffusion characteristics of hydrogen-blended natural gas in a domestic kitchen. *Renew. Energy* **2022**, *189*, 899–916. [\[CrossRef\]](https://doi.org/10.1016/j.renene.2022.03.038)
- 55. Luo, Z. Study on Environmental Impact Ofleakage and Diffusion of Urbandirectly Buried Gas Pipeline. Master's Thesis, Harbin Institute of Technology, Harbin, China, 2021.
- <span id="page-19-1"></span>56. Liu, X. Numerical Simulation of Leakage and Diffusion Flow Field Ofurban Buried Gas Pipeline. Master's Thesis, Lanzhou University of Technology, Lanzhou, China, 2022.

**Disclaimer/Publisher's Note:** The statements, opinions and data contained in all publications are solely those of the individual author(s) and contributor(s) and not of MDPI and/or the editor(s). MDPI and/or the editor(s) disclaim responsibility for any injury to people or property resulting from any ideas, methods, instructions or products referred to in the content.