

Article

One-Stage Catalytic Oxidation of Adamantane to Tri-, Tetra-, and Penta-Ols

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Abstract: Tertiary tetraols of adamantane (C₁₀H₁₆, Tricyclo[3.3.1.1(3,7)]decan) have been widely used for the synthesis of highly symmetric compounds with unique physical and chemical properties. The methods for one-stage simultaneously selective, deep, and cheap oxidation of adamantane to tetraols of different structures have not yet been developed. In this research, chemically simple, cheap, and environmentally friendly reagents are used and that is the first step in this direction. The conditions, under which the impact of a hydrogen peroxide water solution on adamantane dissolved in acetonitrile results in full conversion of adamantane and formation of a total 72% mixture of its tri-, tetra-, and penta-oxygenated products, predominantly poliols, have been found. Conversion and adamantane oxidation depth are shown to depend on the ratio of components of the water-acetonitrile solution and the method of oxidizer solution introduction when using the dimer form of 1:1 dimethylglyoxime and copper dichloride complex as a catalyst. Under the conditions of mass-spectrometry ionization by electrons (70 eV), fragmentation across three C–C bonds of the molecular ions framework of adamantane tertiary alcohols Ad(OH)_n in the range $n = 0–4$ increases linearly with the rise of n .

Keywords: adamantane; catalytic oxidation; Cu(II), hydrogen peroxide; 1,3,5-trihydroxyadamantane; 1,3,5,7-tetrahydroxyadamantane; mass spectrometry



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1. Introduction

Adamantane (Tricyclo[3.3.1.1(3,7)]decane, Ad, **0**) (Scheme 1) can be oxidized to different compounds in different ways. In the general Scheme 1 and further in the numbering used in this paper, the numbers **0**, **1**, **2**, **3**, **4**, and **5** indicate the number of oxygen atoms in the composition of the chemical compound.

Medically, there is a certain interest in the oxidation of **0** since its derivatives are used to obtain drugs, the therapeutic effect of which and the composition of metabolites are described and systematized in the studies [1–5].

Oxidation of **0** can be considered from two points of view: positional selectivity and oxidation depth. The largest number of works is devoted to the oxidation of **0** to a mixture of monoxygenated (1O-Ad) products with a predominance of one of the following: 1-adamantanol (**1a**) [6–12], 2-adamantanol (**1b**) [13], and 2-adamantanone (**1c**) [14] (Scheme 1).

Tertiary alcohol **1a** can be oxidized to 1,2-, 1,3-, and 1,4-diols (**2a''**, **2a**, and **2a'**, respectively), of which **2a'** and **2a''**, containing secondary alcohol groups, are capable of further oxidation to keto-alcohols—5-hydroxy-adamantane-2-one (**2b**) (Scheme 1) [17] and to 1-hydroxy-adamantane-2-one (**2b'**) (not shown in Scheme 1), respectively [18].

Secondary alcohol **1b** is oxidized to ketone **1c** [17–20], to secondary diols, and then to their corresponding keto-alcohols and diketones (not shown in Scheme 1) [17].

Ketone **1c** is oxidized to **2b** and to 4-oxahomoadamantane-5-one (lactone **2c**) (Bayer-Williger reaction) [22,23].

Dehydration of **2a** with the opening of the **0** framework leads to 7-methylene bicyclo[3.3.1]nona-3-one (**1d**) (Scheme 1)—isomer **1c** [24,25]. The radical anion **1d**[•] is cyclized to form the noradamantane product and **1a** [26].

When **0** is oxidized to tri- and tetra-oxygenated products (3O-Ad and 4O-Ad, respectively), the composition of the product becomes even more complicated.

Therefore, even when using highly selective 3°-position biological oxidation methods (enzymes, bacteria, microbes, cells [27–37]) to obtain 1,3,5-adamantanetriol (**3a**), preference was given to sequential oxidation of **0**, **1a**, and **2a** with product isolation stages, so multi-stage synthesis was carried out [28–30].

Under the same conditions, the biooxidation of secondary alcohol **1b** and ketone **1c** does not occur selectively at the 2° and 3° positions [31,34]. Under other conditions, the biooxidation of ketone **1c** through the intermediate formation of two products **2b** and **2c** leads to one product—1-hydroxy-4-oxahomoadamantan-5-one (**3b**) (Scheme 1), but with a low yield [36].

Among the 3O-Ad and 4O-Ad products, the tertiary alcohols **3a** and 1,3,5,7-adamantantetraol (**4a**) are of the greatest practical importance.

Usually, **3a** and **4a** are synthesized as a precursor to obtaining derivatives of **3a(OR)** and **4a(OR)**, respectively, where R is represented by many classes of compounds [38–53].

Compounds **4a(OR)** by themselves and in copolymerization with other components are capable of producing stellate, reticular, and skeletal spatial structures that have numerous chemical and physical properties useful for technical applications [40–53].

1,3,5,7-aryladamantanes (**4a(Ar)**) are also synthesized from **4a** [49,54,55].

The crystal structure of **4a**, which has the same spatial structure as CsCl crystals, was determined in [56].

For the synthesis of **3a** and **4a**, the two-stage scheme was most used: (I) catalytic bromination of **0** to 1,3,5-tri- and 1,3,5,7-tetra-bromadamantane (**3a(Br)** and **4a(Br)**, respectively), (II) substitution of all Br atoms for alcohol groups (Scheme 1) [40–53].

It was shown that at stage (II), along with **4a**, a product of its dehydration was formed with the opening of the frame—1,5-dihydroxy-7-methylene-bicyclo[3.3.1]nona-3-one (**3c**) (Scheme 1), which can be separated from **4a** by dissolving in ethanol and using 50% H₂SO₄ converted into an additional amount of the target product **4a** [42].

The stage (II) using Ag₂SO₄/H₂SO₄(conc.) is general and can be applied to tertiary mono-, di- and tri-bromadamantanes, for which single-stage syntheses have been developed starting from **0** [50].

Secondary bromadamantanes may also be involved in this reaction (II). As an example, the synthesis of triol **3d** from **3d(Br)** is shown in Scheme 1 [48].

This synthesis scheme is quite expensive, which hinders the widespread synthetic use of compounds **3a** and **4a**.

With one-stage oxidation of **0** to **3a** and **4a**, the best results were obtained when methyl(trifluoromethyl)dioxirane O₂C(CF₃)CH₃ as an oxidizer was used, with which the sequential oxidation of **0** to **2a**, **3a**, and **4a** with high yields 93, 90, and 78% occurred in 40 min, 2 and 3 h, respectively [57]. The unique properties of this catalytic system during the oxidation of various substrates are systematized in the review [58].

For one-stage oxidation of **0** to **3a** with the use of hydrogen peroxide (H₂O₂), the best results (32%) were obtained by using a specially synthesized Fe(III) complex [59].

However, both of these one-stage schemes for the synthesis of **3a** and **4a** from **0** have not been widely used, possibly due to the peculiarities of the practical implementation of the oxidation process in the first case and the lack of availability of a catalyst in the second case.

In one-stage syntheses of **3a** and **4a**, as well as in multi-stage syntheses, in fact, the scheme of sequential oxidation of **0** is realized, but without the stages of isolation of intermediate products. For example, since **3a** is an intermediate product in the series **2a**, **3a**, **4a**, its synthesis using different chemical reagents means searching for optimal conditions in which the target product has the highest yield [49,57–63]. It was in this way that work was carried out to find the conditions for the oxidation of **0** to **3a** and **4a**.

In general, Scheme 1 shows all the types of **0** oxidation products described in the papers, the appearance of which was expected in the framework of this study.

At the same time, it should be noted that the products of tri- and tetra-oxygenation of **0** could include other compounds with a preserved and disclosed **0** frameworks, which will not be discussed further, since no evidence of their formation in the considered catalytic system was received.

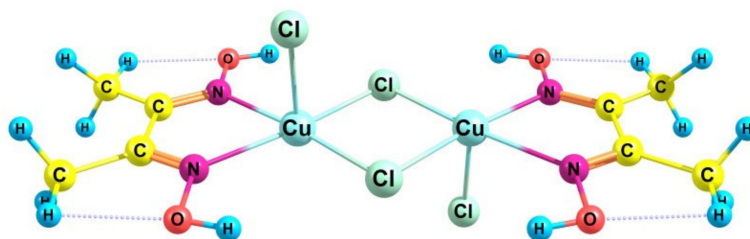
By analogy with the oxidation of cyclohexane [64–66], such compounds could include mono- and di- hydroperoxide groups in their composition. For example, a scheme for the oxidation of **0** with the participation of its primary and secondary hydroperoxides is proposed [66], the formation of thermally stable 1-adamantylhydroperoxide (**2d**) [67] and 2,2-dihydroperoxy-adamantane (**4a'**) is described [68,69].

Thus, to date, the problem of deep single-stage oxidation of **0** to **3a** and **4a** using a combination of an aqueous solution of H_2O_2 —a non-explosive, environmentally friendly, cheap oxidizer, and an affordable cheap catalyst—has not been solved.

The first results of the authors' efforts to solve this problem are reported in this paper.

As a catalyst, the $Cu_2Cl_4 \cdot 2DMG$ complex was used, where DMG—Butane-2,3-dione dioxime (dimethylglyoxime) (Scheme 2), in the presence of which, using an aqueous solution of H_2O_2 , cyclohexane was previously oxidized to adipic acid with a high yield of 53% (the main product) at a conversion of cyclohexane of 30% [70].

The $Cu_2Cl_4 \cdot 2DMG$ complex is a cheap, synthetically easily accessible reagent [71].



Scheme 2. The catalytic complex $Cu_2Cl_4 \cdot 2DMG$.

The catalytic activity of the $Cu_2Cl_4 \cdot 2DMG$ complex, although lower, is comparable to the best results obtained during the oxidation of cyclohexane and cyclohexene to adipic acid using aqueous solutions of hydrogen peroxide in the presence of metal complexes [72,73].

2. Results

2.1. Search for Optimal **0** Oxidation Conditions upon the Fast (~3 s) Method of Oxidizer Solution Introduction

With the volume of the oxidizing solution $V(H_2O_2) = 1$ mL and the mass of the catalyst $m = 30$ mg in the reaction temperature range $T = 40$ – 70 °C (10 °C–step) and reaction times $t = 5, 30,$ and 60 min, the composition of the **0** oxidation products does not depend on t and T . In the experiment, 92.5% of the total amount of identified products among n -oxygenation groups of **0** was divided as follows: mono- 26.4%, di- 36.5%, tri- 23.5%, and tetra- 6.1%. Unidentified products comprise 7.5%.

The dependence of the conversion $C = 81\text{--}89\%$ of the **0** initial hydrocarbon on T is transferred by the linear equation $C = -0.281 \cdot T + 100$ with the correlation coefficient $R^2 = 0.9874$ (Figure 1, $t = 30$ min). According to this equation, one could expect $C = 100\%$ at $T = 0$ °C. However, in the experiment carried out at $T = 0$ °C (single-wall reactor, mechanical mixing), the **0** oxidation products were not detected.

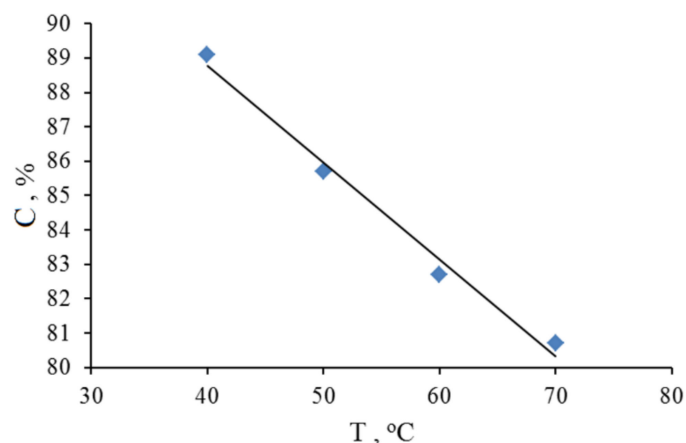


Figure 1. The dependence of the **0** conversion (C) on the reaction temperature T .

At $T = 0$ °C, the copper complex completely dissolved, and all **0** white flakes floated to the surface of the blue-green acetonitrile solution. At $T = 20$ °C, the taken amount of **0** was completely soluble, but oxidation was not carried out at this temperature. The maximum value of C , which, as it turned out, should have been at T less than 40 °C, and not more, was not determined.

At $V(\text{H}_2\text{O}_2) = 1$ mL and $T = 50$ °C in the range of $m = 5\text{--}50$ mg $\text{Cu}_2\text{Cl}_4 \cdot 2\text{DMG}$, the composition of the products and conversion of **0** depended on m at $t = 5$ min and ceased to depend on $t = 30$ and 60 min. The **0** K conversion at $t = 5$ min has a clearly pronounced inflection at $m = 10$ mg and a maximum of 92% at $m = 30$ mg (Figure 2).

Two groups of points: (I) $m = 0, 5, 10$ mg and (II) $m = 10, 20, 30, 40, 50$ mg with correlation coefficients $R^2 = 1$ are located along the trend lines, respectively, $C(\text{I}) = -0.14 m^2 + 3.1 m$ and $C(\text{II}) = -3 \cdot 10^{-5} m^4 + 0.0065 m^3 - 0.5525 m^2 + 18.4 m - 118$.

At $t = 5$ min, with an increase in the catalyst mass m up to 30 mg, the **0** oxidation depth increased, and after reaching this value, it remained unchanged. At $t = 30$ and 60 min, $C = 90\%$.

From the dependencies shown in Figure 2, two conclusions can be made. First, during the reaction time $t = 5$ min, the chemical composition of the catalyst changes in the system, since there is a clearly defined inflection on the curve C . Second, under the above-mentioned conditions, with increasing m , sequential oxidation occurs according to the scheme $0\text{O-Ad} \rightarrow 1\text{O-Ad} \rightarrow 2\text{O-Ad} \rightarrow 3\text{O-Ad} \rightarrow 4\text{O-Ad}$, and the starting compound and its oxidation products experience further parallel oxidation to an approximately equal extent.

At $m = 30$ mg and $T = 50$ °C, the **0** conversion and the composition of the products of its mono- (1O), di- (2O), tri- (3O), and tetra- (4O) oxygenation depend on $V(\text{H}_2\text{O}_2)$ (Figure 3), but within the error limits (10%) they are independent of t . Therefore, for each $V(\text{H}_2\text{O}_2)$, data are averaged for $t = 5, 30,$ and 60 min for four groups of **0** oxidation products.

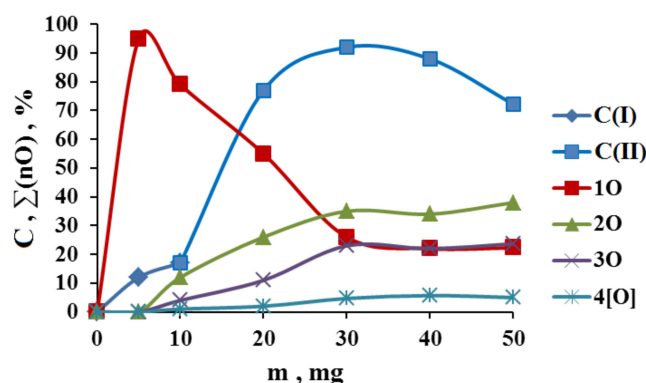


Figure 2. Dependencies of the C (C(I) (◆) and C(II) (■)) conversion and the sum of the products of 0 n -oxygenation, $n = 1-4$, on the mass m of the catalyst. $V(\text{H}_2\text{O}_2) = 1 \text{ mL}$, $T = 50 \text{ }^\circ\text{C}$, $t = 5 \text{ min}$.

The maximum C falls on the interval $V(\text{H}_2\text{O}_2) = 0.5-1.0 \text{ mL}$ (Figure 3). In the range $V(\text{H}_2\text{O}_2) = 0.5-2.0 \text{ mL}$, the content of intermediate 2O products remains approximately unchanged. In the range $V(\text{H}_2\text{O}_2) = 1.5-10.0 \text{ mL}$, with an increase in the volume of the oxidizing agent solution, the content of 1O-Ad products increases linearly, and the contents of 2O-, 3O-, and 4O-Ad products decrease linearly.

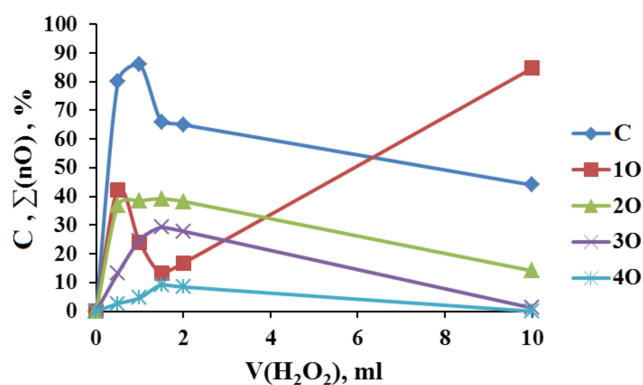
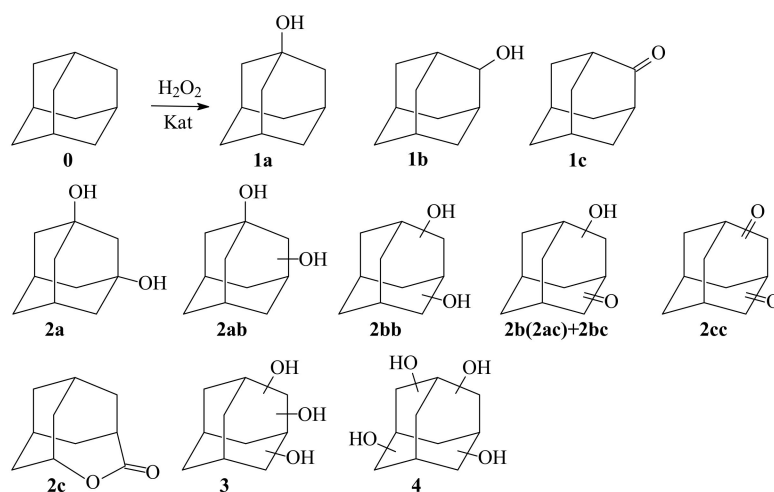


Figure 3. The 0 conversion (C) and the sum (Σ) of the products of its n -oxygenation, where $n = 1-4$, in dependence on the volume $V(\text{H}_2\text{O}_2)$ of the oxidizing solution.

In experiments on varying $V(\text{H}_2\text{O}_2) = 0.5-1.5 \text{ mL}$, alcohols were predominantly formed (Scheme 3). At 0.5, 1.0, and 1.5 mL, the ratio of products of the 1O-Ad group **1a:1b:1c** was equal to 2.8:3.2:1, 4.7:4.8:1, and 1.4:1.9:1, respectively.

At $V(\text{H}_2\text{O}_2) = 1 \text{ mL}$, the oxidation products of 0 were distributed in the following ratio: diols **2a** and **2ab**, 13.3 and 12.7%, respectively, compounds **2bb**, **2b (2ac) + 2bc**, **2cc**, **2c** in the amount of 12.5%, containing tertiary alcohol groups of triols **3a**–11.7%, other secondary triols and keto-alcohols in group **3**–13% and everything in the group of tetraols **4**–4.7%.

At $V(\text{H}_2\text{O}_2) = 10 \text{ mL}$, the main products of oxidation of 0 were **1a** (36.7%), **1b** (26.4%), and **1c** (21.6%), in total 84.7% in 1O-Ad products. The ratio of 3°:2° was 2.3. This value corresponds to the parallel course of several non-selective oxidation routes of 0 C–H bonds, mainly by the free radical mechanism [15,16]. Other products were: **2a** (5.3%), **2ab** (2.4%), **2bb** (5.5%), **2b (2ac) + 2bc** (0.4%), lactone **2c** (0.5%) and **3** (1.2%) (Scheme 3).



Scheme 3. Oxidation products of **0**.

2.2. Catalytic Activity of the $\text{Cu}_2\text{Cl}_4 \cdot 2\text{DMG}$ Complex and the Release of Molecular Oxygen upon the Fast (~ 3 s) Method of Oxidizer Solution Introduction

The reaction time $t = 5$ min at $m = 30$ mg and $T = 50$ °C, as well as for other values, was chosen based on visual observations. Around this time in the **0**/ H_2O_2 / $\text{Cu}_2\text{Cl}_4 \cdot 2\text{DMG}$ / CH_3CN system, gas began to be released, presumably it was molecular oxygen (O_2), the solution color was changing and precipitation was appearing.

The independence of C and output of **0** oxidation products of the time $t = 5, 30$ and 60 min at $m = 30$ mg and $T = 50$ °C (the averaged values are used in Figure 3) means that all the products of **0** n -oxygenation are formed in the initial stage of **0** oxidation during $t = 5$ min in the presence of the original form of the $\text{Cu}_2\text{Cl}_4 \cdot 2\text{DMG}$ catalyst. After the breakdown of this catalyst form, the formation of **0** oxidation products is terminated and the emission of gas on the other catalytic forms containing copper ions occurs.

2.3. Adamantane (**0**) Oxidation upon the Slow (60 min) Method of Oxidizer Solution Introduction

With a slow drop-by-drop method of introducing an oxidizer solution, $V(\text{H}_2\text{O}_2) = 1$ mL was used, at which earlier (see Figure 3), the highest **0** conversion was obtained. The search for optimal conditions (variation of m , t , and $V(\text{H}_2\text{O}_2)$) at a slow (60 min) method of introducing the oxidizer solution was not carried out.

T oxidation reactions with an interval of 10 °C varied from 30 to 80 °C. In all experiments, there was a 100% conversion of **0**. On the chromatograms of the total ion current of the mass detector, the oxidation products **0** are represented by the same set of overlapping narrow and wide peaks (Figure 4).

The ratio of these peaks strongly depends on T . During the transition from 50 to 60 °C, the proportion of narrow peaks sharply decreases, and the proportion of wide peaks increases. When moving from 70 to 80 °C, on the contrary, the wide peaks disappear and only the narrow peaks remain.

The following narrow peaks were identified from the mass spectra (MS) (retention times (min) according to the chromatogram with $T = 40$ °C): **1a** 11.91 (monool 1-Ad(OH)₁), **1c** 12.81, **1d** 12.74, **2a** 14.23 (diol 1,3-Ad(OH)₂), **2a'** 14.45, **2b** 14.78, **3a** 16.34 (triol 1,3,5-Ad(OH)₃), **4a** 18.16 (tetraol 1,3,5,7-Ad(OH)₄), **5a** 20.29 (pentaol 1,2,3,5,7-Ad(OH)₅) (Schemes 1, 4 and 5).

In Figure 4, the identified narrow peaks are mainly indicated only on one chromatogram of 40 °C, since at other T , these peaks are similarly located in the chromatograms.

The peaks of tertiary alcohols Ad(OH) _{n} , $n = 1$ – 5 , are the reference ones, since they were used to distinguish chromatograms into regions belonging to different groups of n -oxygenation of **0**.

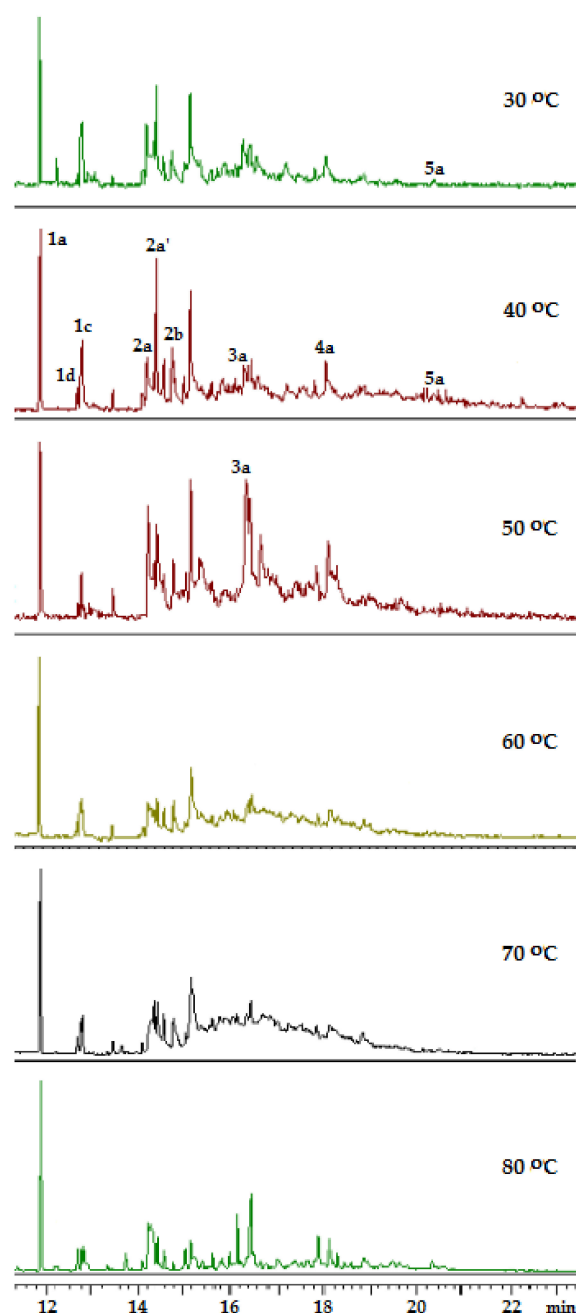


Figure 4. Chromatograms of diethyl ether extracts of reaction mixtures containing oxidation products of **0** obtained by slow drip addition of a 50% aqueous solution of H_2O_2 .

In the NIST/EPA/NIH 11,17 databases, reference MS of compounds **3a**, **4a**, and **5a** were absent [74]. In the two published MSs of **3a**, the intensity of the peak of the molecular ion with $m/z = 184$ ($\text{M}^{+\bullet}$) is 5–10%, the peak with $m/z = 111$ (31–46%), the peak with $m/z = 127$ (100%) [57,61]. There are no published MSs of **4a** and **5a**.

To find the location of peak **3a**, two (40 and 70 °C) chromatograms of the total ion current (Figure 4) were scanned when setting the $m/z = 127$ (Figure 5).

Two groups of peaks were found in the region of retention times of 16 and 18 min (Figure 5). Presumably, the first group of peaks is due to **0** triols, and the second—to **0** tetraols (Scheme 4). Polyols with tertiary positions of hydroxyl groups come out first. Scheme 4 also shows one of the most probable structures of **0** tri- and tetrapolyols, each containing one secondary hydroxy group, which are characterized by somewhat longer retention times.

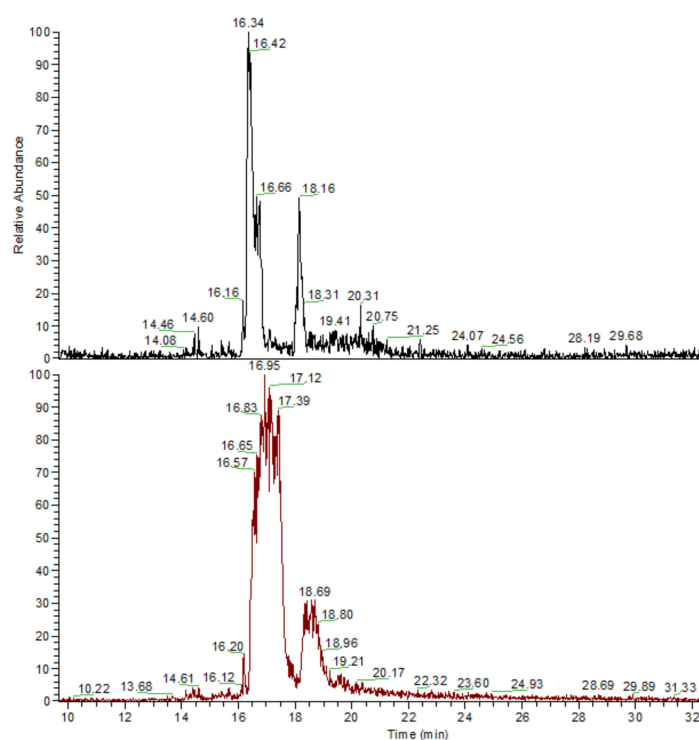
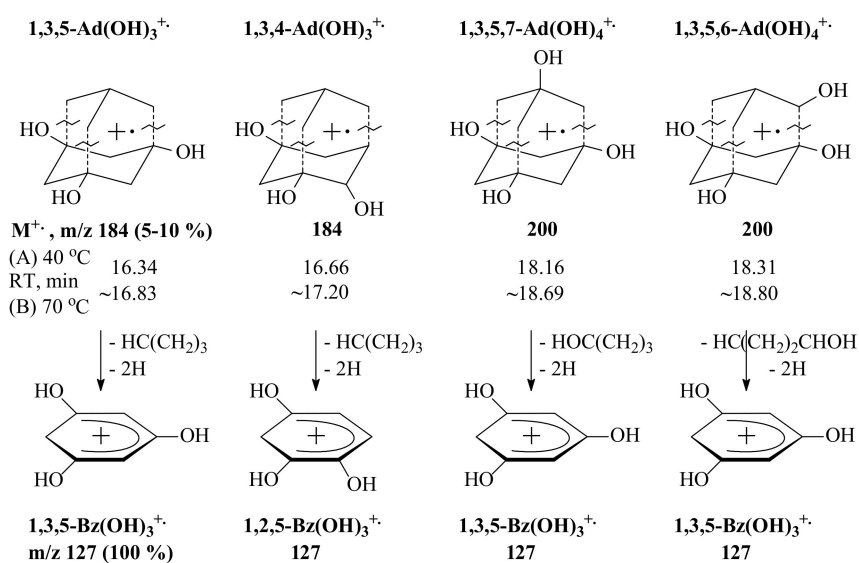
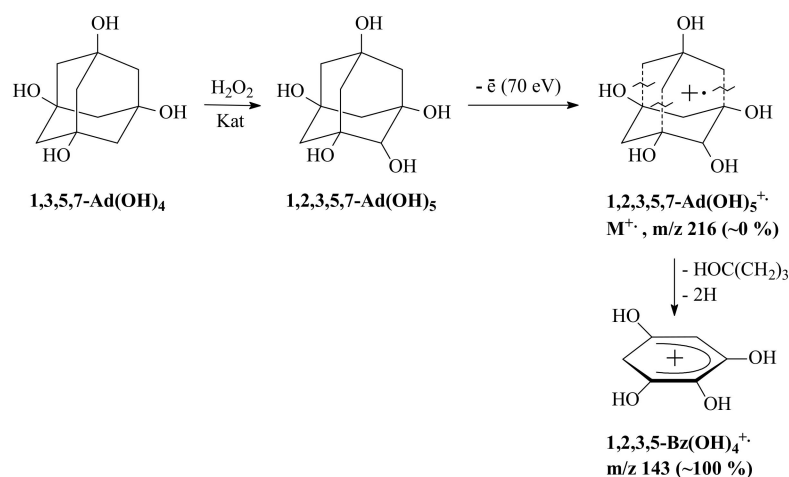


Figure 5. Selected ion (m/z 127) chromatograms: 40 °C (top), 70 °C (bottom).



Scheme 4. Fragmentation of molecular ions of **0** tri- and tetraols.

The tetraol $1,3,5,7\text{-Ad(OH)}_4$ (**4a**) molecule contains twelve equivalent secondary C–H bonds. In the complete absence of tertiary C–H bonds, this makes the **4a** molecule a unique object from the point of view of subsequent oxidation. The only hydroxy product of $1,3,5,7\text{-Ad(OH)}_4$ oxidation is pentaol $1,2,3,5,7\text{-Ad(OH)}_5$ (**5a**) (Scheme 5).



Scheme 5. Fragmentation of the molecular ion of **0** pentaol.

Upon fragmentation of radical cations $1,2,3,5,7\text{-Ad(OH)}_5^{\bullet+}$ ($m/z = 216$, the intensity of the molecular ion is about 0%), the formation of tetra-hydroxy-substituted benzenium cation $1,2,3,5\text{-Bz(OH)}_4^+$, $m/z = 143$ with the highest (100%) intensity, was expected (Scheme 5).

In order to search for such an ion, scanning with $m/z = 143$ of the two previously described chromatograms of the total ion current (see Figure 4) was set. A low-intensity peak with $m/z = 143$ was found in the chromatogram 40°C with a retention time of about 20 min (Figure 6) and was not detected in the chromatogram 70°C .

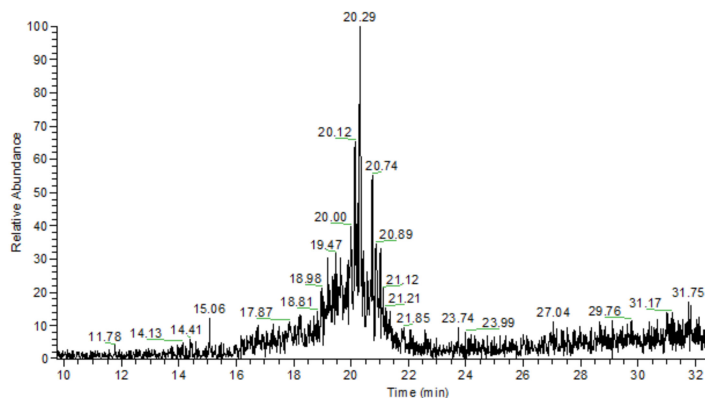


Figure 6. Selected ion ($m/z 143$) chromatogram 40°C .

Thus, at 40°C , the **0** oxidation proceeds more “ n -deeply” ($n = 5$) (Figure 6), but with lower yields of tri- and tetra-oles of **0**, than at 70°C (Figure 5).

As far as is known, this is the first example of the oxidation of **0** to pentaol.

To determine the composition of wide chromatographic peaks (15–21 min, Figure 4), including the regions of tri- and tetra-oles of **0**, they were scanned with different characteristic values of m/z . The analysis showed that these chromatographic peaks were formed by the superposition of several peaks, the exact identification of which is impossible.

Therefore, according to the retention times of the peaks of tertiary alcohols Ad(OH)_n , $n = 1\text{--}5$, all the chromatograms were divided into five regions belonging to different groups of n -oxygenation of **0**.

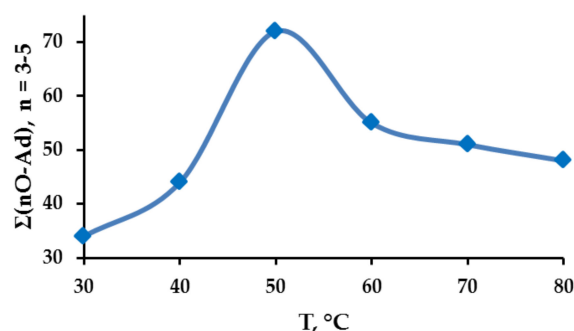
The highest values of the total outputs of $n\text{O-Ad}$ products, $n = 1\text{--}5$, are achieved at different T: 22% 1O-Ad at 80°C , 46% 2O-Ad at 30°C , 45% 3O-Ad and 25% 4O-Ad at 50°C , 7% 5O-Ad at 40°C (Table 1).

Table 1. The total yields of the five product groups nO-Ad, $n = 1-5$, at different reaction temperatures T.

n	T, °C					
	30	40	50	60	70	80
	%					
1	20	14	10	9	9	22
2	46	40	18	36	40	30
3	26	27	45	35	34	31
4	8	12	25	18	16	15
5	0	7	2	2	1	2

The content of **1a** was 10, 7, 5, 6, 6 and 16% at 30, 40, 50, 60, 70 and 80 °C, respectively. At 80 °C, there are no wide peaks, the content of narrow peaks **1a**, **2a**, **3a**, **4a**, and **5a** is 16, 3, 4, 4, and 1%, respectively, the total content of these tertiary alcohols is 28%.

Thus, when an oxidizer solution is introduced drop-by-drop in the catalytic system, **0** is oxidized to a mixture of n -oxygenated products with a significant content of tri-, tetra-, and penta-ols at its complete conversion. The total number of nO-Ad products, $n = 3-5$, reaches a maximum value of 72% at 50 °C (Figure 7).

**Figure 7.** The dependence of the sum of products $\Sigma(\text{nO-Ad})$, $n = 3-5$, on T.

If the envelopes of the wide peaks on the chromatogram of 50 °C are taken as the component of the wide peaks on the chromatogram of 70 °C (Figure 4), then at 50 °C, the content of the narrow peaks **1a**, **2a**, **3a**, **4a**, and **5a** is 5, 4, 10, 3 and 0%, respectively, the total content of these tertiary alcohols is 22% (Figure 4). Thus, at 50 °C, the highest yield of **3a** (10%) is observed.

3. Discussion

3.1. The Dependence of the Conversion (C) 0 on the Volume $V(\text{H}_2\text{O}_2)$ of the Fast Introduced Oxidizer Solution: Three Regions with Different Catalytic Activity and the Structure of the Solvent

The conversion C of **0** and the sums of the products $\Sigma(\text{nO-Ad})$, $n = 1-4$, depend on the volume $V(\text{H}_2\text{O}_2)$ of the oxidizer solution at a fast method of its introduction (Figure 3). The exact position of the maximum C, which was not experimentally established, was determined by the following method (Figure 8).

If you were to draw a straight line (a) $C = 160 \cdot V(\text{H}_2\text{O}_2)$ through two starting points (V (mL); C (%)): (0;0) and (0.5;80), then $C = 100\%$ will correspond to the value $V = 0.625$ mL. Three points (0.625;100), (1;86) and (1.5;66) fall exactly on the straight line (b) $C = -40 \cdot V(\text{H}_2\text{O}_2) + 126$, and three points (1.5;66), (2;65) and (10;44) fall exactly on the straight line (c) $C = -2.6044 \cdot V(\text{H}_2\text{O}_2) + 70.053$. Thus, the maximum value of $C = 100\%$ is reached at $V(\text{H}_2\text{O}_2) = 0.625$ mL, and the entire studied area is divided into three parts I, II, and III (Figure 8).

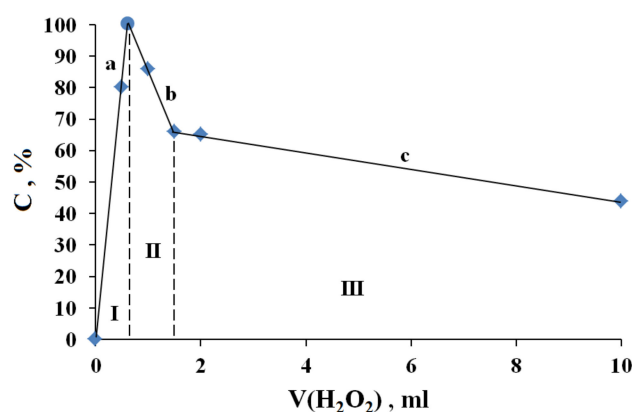


Figure 8. The dependence of C on V(H₂O₂), fast introduction.

Presumably, the presence of a maximum C at V(H₂O₂) = 0.625 mL is associated with greater stability of the initial Cu₂Cl₄·2DMG complex in region I than in region II.

A critical amount of H₂O is reached at V(H₂O₂) = 0.625 mL, above which H₂O begins to have a destabilizing effect on the initial Cu₂Cl₄·2DMG complex, apparently accelerating ligand exchange.

In this case, with an increase in V(H₂O₂) in region I, an increase in C can be associated with an increase in the concentration (amount) of the oxidant H₂O₂, and in region II with an increase in V(H₂O₂), a decrease in C can be associated with an increase in the rate of ligand exchange, as a result of which the contact time of 0 with the catalytic complex Cu₂Cl₄·2DMG and H₂O₂ decreases.

In region III, with an increase in V(H₂O₂), a further decrease in C may be associated with almost instantaneous destruction of the initial Cu₂Cl₄·2DMG catalytic complex.

It was found that the values of the maximum at V(H₂O₂) = 0.625 mL and the bend at V(H₂O₂) = 1.5 mL were not random, but were associated with a change in the structure of the solution, which occurs with an increase in the water component.

It is known that water-acetonitrile solutions have a number of unusual properties, which are manifested when analyzing the dependencies of various chemical and physical characteristics of solutions on the ratio of their components (from 100% H₂O to 100% CH₃CN) [75–78].

The presence of extreme points and bends on these dependencies indicates the ratios of the molecules of the two components, at which their sufficiently stable associates (complexes) are formed.

To compare the obtained results (Figure 8) with the data on the structure of binary solvents, the values of the characteristics of the three solutions used in these studies were calculated [75–78], based on the volume ratios of the oxidizer (Ox) and the solvent (An) (Table 2).

The maximum C at V(H₂O₂) = 0.625 mL (Figure 8) corresponds to the ratio of 4.4:1 molecules of acetonitrile and an aqueous solution of the oxidizer.

The formation of heteroassociates of CH₃CN and H₂O molecules of the composition 1:1, 2:1, and 4.5:1, respectively, at X(AN) = 50, 67, and 90 wt% of CH₃CN in binary solutions at 25 °C was established by ¹H NMR and chemometry methods in combination with quantum chemical calculations [76,77]. Based on quantum chemical calculations for a 4.5:1 heteroassociate, structural models of the association of one H₂O molecule with four and five CH₃CN molecules are proposed [77].

Table 2. The ratio of the main components of water-acetonitrile solutions of three reaction mixtures.

V, mL		X(AN), wt%	Y(AN), mol Fraction	N(AN): N(Ox), AN Molecules: Ox Molecules
Ox *	AN **			
0.625	8	91	0.81	4.4:1
1.5	8	80	0.65	1.8:1
10	10	43	0.25	1:2.9

* 50% H₂O₂, H₂O and H₂O₂ (1:1), d(Ox) ≈ d(H₂O) = 0.9881 g/cm³ at 50 °C, M(Ox) = 18.5 g/mol; ** CH₃CN, d(CH₃CN) = 0.7473 g/cm³ at 50 °C, M(CH₃CN) = 41 g/mol.

Thus, the achievement of the maximum C at V(H₂O₂) = 0.625 mL (Figure 8) can be associated with the formation of heteroassociates with a ratio of 4.4:1 of acetonitrile molecules and molecules of an aqueous solution of the oxidizer.

This means that water molecules introduced into the acetonitrile solution up to the value V(H₂O₂) = 0.625 mL remain in the solution and most of the time do not enter the coordination sphere of copper ions of the catalytic complex, which ensures its increased stability.

This assumption is consistent with the data on the solubility of CuCl₂ in aqueous acetonitrile solutions at 25 °C [78]. It was found that the entire studied range of values Y(AN) = 0–1 mol fraction was divided into four regions with different ratios of solvate components: (1) CuCl₂·2H₂O at Y(AN) = 0–0.15, (2) CuCl₂·2H₂O·CH₃CN at Y(AN) = 0.15–0.3, (3) CuCl₂·3H₂O·2CH₃CN at Y(AN) = 0.3–0.6 and (4) CuCl₂·1.5CH₃CN at Y(AN) = 0.6–1 [78].

Region I of this study completely falls into the region (4) [78], in which H₂O molecules are not part of the CuCl₂ solvate. The transition from region II to III occurs at Y(AN) = 0.65, which is close to Y(AN) = 0.6 transition from the region (4) to (3) [78], as a result of which H₂O molecules appear in the CuCl₂ solvate. With this transition, the relative amount of the H₂O molecule in the solvate immediately (abruptly) becomes one and a half times greater than the number of CH₃CN molecules.

At the transition point from region II to III, the value of N(AN):N(Ox) = 1.8:1 (50 °C) is close to the value of 2:1 of the 2CH₃CN·1H₂O heteroassociate, the formation of which at 25 °C was recorded at X(AN) = 67 wt% [76,77].

Taking into account rounding, one can assume that region III (Y(AN) = 0.25–0.65 mol fraction) of the study fully corresponds to the region (3) (Y(AN) = 0.3–0.6 mol fraction) of the study of solvates [78].

In all regions (I–III), the amounts of substrate and catalyst molecules are minimal compared to the amounts of solvent molecules and the added aqueous solution molecules of the oxidizer. After substitution of DMG molecules in the complex with CH₃CN molecules as a result of ligand exchange, one can obtain almost the same chemical system consisting of CuCl₂, H₂O (H₂O₂ ≈ H₂O), and CH₃CN as in the work on solvates [78]. The proximity of the chemical composition of the solutions explains the coincidence of the intervals Y(AN) of the two works.

Thus, the catalytic activity of the system under study and the type of dependence of C on V(H₂O₂) (Figure 8) is determined by the structure of the water-acetonitrile solution, which changes with an increase in the amount of V(H₂O₂) solution of the oxidizer introduced.

3.2. Comparison of the Results of the Authors' and Other Methods of 0 Oxidation Described in the Literature

Based on the above analysis, with a fast (~3 s) method of introducing an oxidizer solution into the reaction volume, the oxidation depth of 0 was small due to the impossibility of simultaneous implementation of two oppositely acting factors, each of which separately contributes to an increase in the oxidation depth.

The first factor: for the maximum possible contact time of **0** with the initial catalytic complex $\text{Cu}_2\text{Cl}_4 \cdot 2\text{DMG}$, the introduced amount of H_2O should be minimal. The second factor: the amount of the oxidizer H_2O_2 should be the maximum possible, but with its increase, the amount of water introduced increases (the oxidizer is a 50% aqueous solution of H_2O_2).

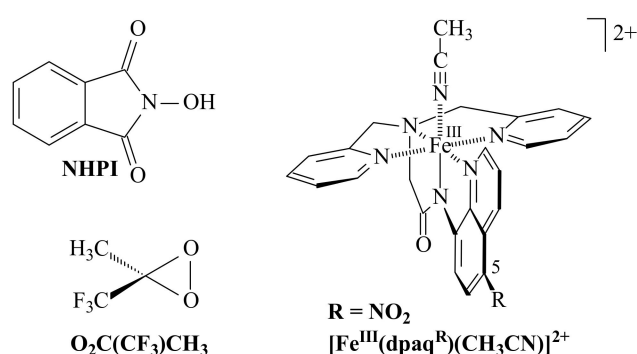
It is for the implementation of such conditions that a slow (60 min) drop-by-drop method of introducing the oxidizer solution was chosen. With this method of oxidation of **0**, the possible contact time of **0** with the initial catalytic complex $\text{Cu}_2\text{Cl}_4 \cdot 2\text{DMG}$ in combination with $V(\text{H}_2\text{O}_2) = 1 \text{ mL}$ from region II was maximized. The value $V(\text{H}_2\text{O}_2) = 1 \text{ mL}$ slightly exceeded the value $V(\text{H}_2\text{O}_2) = 0.625 \text{ mL}$ that was critical for the quick method of introducing the oxidizer solution.

The results achieved can be compared with the literature data (Table 3, Scheme 6) [57–63], [58]—review.

Table 3. One-stage synthesis of **3a** and **4a**.

Sub	Products, %				C, %	Ox	Cat	Sol	T, °C	t, h	Ref.
	1a	2a	3a	4a							
0	10	53			>99					6	
1a		76	18		95	O_2	NHPI/ $\text{Co}(\text{acac})_2$	AcOH	75	15	[60]
2a			85		46					24	
2a		42	56		100		+ MnO_2		60	30	[61]
0			42		n.r.		CrO_3	+ H_2SO_4	80	3	[62]
0			50 *		n.r.	AcOH		100	>1	[63]	
0			90		98	$\text{O}_2\text{C}(\text{CF}_3)\text{CH}_3$	$\text{CH}_2\text{Cl}_2/\text{TFP}$ (2:1)	−20	2	3	[57]
			78		n.r.						
0	2	12	32		46		$\text{Fe}(\text{III})^{**}$		25	5	[59]
0	5	4	10	3	100	H_2O_2	Cu_2Cl_4 2DMG	CH_3CN	50	1	***

* isolated product; ** $\text{Fe}^{\text{III}}\text{-dpaq}^{\text{R}}\text{-[D}_4\text{]}$, R = NO_2 ; *** this work.



Scheme 6. Oxidants and catalytic complex for one-stage synthesis of **3a** and **4a**.

The use of O_2 as an oxidizer does not allow the single-stage oxidation of **0** to **3a** and **4a**, but can be used for this purpose when implementing a multi-stage synthesis strategy [60,61].

CrO_3 is effective in single-stage oxidation of **0** to **3a** [62,63]. Apparently, this oxidizer can be used for deeper oxidation of **0** to **4a**.

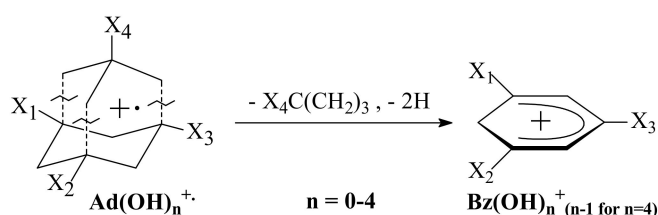
The oxidation of **0** with $\text{O}_2\text{C}(\text{CF}_3)\text{CH}_3$ demonstrates the unique properties of this system, which is out of competition, potentially capable of oxidizing **0** not only to **4a** but also to **5a** with high yields with an increase in reaction time [57,58].

The results obtained (**3a** 10%) are comparable to the yield of **3a** 32% under **0** oxidation conditions close to those discussed in this paper in the presence of a specially synthesized Fe(III) complex with increased stability when exposed to the H₂O₂ oxidizer [59].

It is interesting to note that in the last two works cited, oxidation with O₂C(CF₃)CH₃ and H₂O₂ was carried out with their slow gradual introduction into the reaction mixture, which, in the light of the above analysis, undoubtedly contributed to achieving high yields of the target products.

3.3. General Regularity in the Fragmentation of Molecular Ions Ad(OH)_n⁺, n = 0–4

In the Ad(OH)_n series (n = 0–4), the MS of **0** occupies a special position [57,61,74,79,80]. The molecular peak (M⁺•) with m/z = 136 has the highest (100%) intensity, and the peak of the benzenium cation (C₆H₇⁺ (Bz⁺)) (protonated benzene [81–84]) with m/z = 79 has the second highest (74%) intensity (Scheme 7, X_n = H, OH) [74].



Scheme 7. The main channel of fragmentation of **0**, **1a**, **2a**, **3a**, **4a** molecular ions.

The other eight most intense peaks also have a fairly high relative abundance in the MS of **0** (m/z (rel.int., %)): 136 (99.9), 135 (33.5), 94 (32.3), 93 (66.2), 80 (41.7), 79 (74.4), 77 (27.7), 67 (31.4), 41 (24.2), 39 (25.5) [74]. The pathways of fragmentation M⁺• **0** under MS conditions were analyzed in the studies [79,80].

Going from **0** to **1a** (Ad(OH)₁) in MS, the ratio of the intensities of the peaks with m/z = 152 (M⁺•) and the main fragmentation ion with m/z = 95 (Bz(OH)₁⁺) of 21%:100%, respectively, becomes opposite, and the intensities of the other eight most intense peaks become small (4–11%). In MS 1-ol **1a**, the ten most intense peaks are as follows (m/z (rel.int., %)): 152 (21.4 (M⁺•)), 109 (4.5), 96 (8.4), 95 (99.9), 94 (10.5), 79 (5.1), 77 (4.7), 67 (3.7), 41 (6.8), 39 (4.8) [74]. This indicates a high selectivity of one channel of fragmentation of the molecular ion Ad(OH)_n⁺• (n = 1) (Scheme 7).

The same selectivity of molecular ion fragmentation is retained for 1,3-diol **2a** (Ad(OH)₂) and 1,3,5-triol **3a** (Ad(OH)₃).

The MS of **2a** is as follows (m/z (rel.int., %)): 168 (14.1 (M⁺•)), 112 (14.4), 111 (99.9), 110 (8.7), 96 (10.8), 81 (8.8), 55 (10.7), 42 (8.9), 43 (26.1), 41 (17.1) [74].

The MS of **3a** was described in two papers in 1990 and 2015 as a set of m/z (rel.int., %) [57,61]. The first one reported that the MS of **3a** was: 184 (5 (M⁺•)), 128 (8), 127 (100), 111 (31), 110 (10), 109 (10), 85 (7), 69 (8), 55 (7), 43 (36), 41 (12), 39 (9), published for the first time [57]. In the second paper, the following MS of **3a** is given: 184 (10 (M⁺•)), 166 (6), 150 (50), 127 (100), 111 (46), 92 (28) [61].

In both published MSs of **3a**, the peak with m/z = 127 has the highest (100%) intensity, the peak with m/z = 111 (31–46%), and the intensity of the molecular ion with m/z = 184 is 5–10% (average 7.5%).

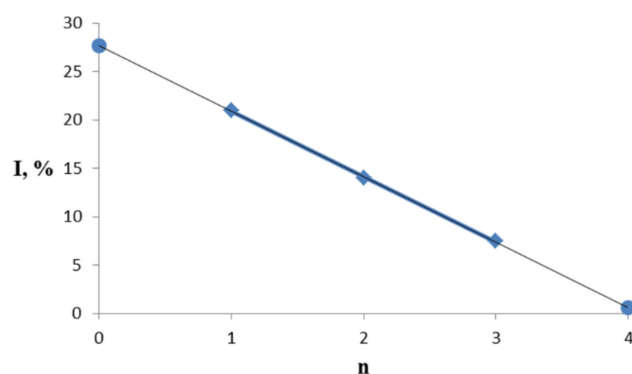
There is no published MS of 1,3,5,7-tetraol **4a** (Ad(OH)₄).

The intensities (I) of the peak of the molecular ion (M⁺•) relative to the intensities of the main fragment ions (100%) for the Ad(OH)_n compounds, where n = 1–3, decrease linearly with increasing n (Scheme 7, Table 4, Figure 9). The resulting equation I = –6.75n + 27.667, R² = 0.9995, allows making estimates I = 27.667 and 0.667%, respectively, for the values n = 0 and 4.

Table 4. Relative intensities of peaks of molecular and main fragmentation ions in electron ionization (70 eV) mass spectra of compounds Ad(OH)_n, n = 0–4 [57,61,74].

Ad(OH) _n		X ₁	X ₂	X ₃	X ₄	M ⁺		Bz(OH) _n ⁺	
No.	n					m/z	%	m/z	%
0	0	H	H	H	H	136	100 28 *	79	74 100 *
1a	1	OH	H	H	H	152	21	95	100
2a	2	OH	OH	H	H	168	14	111	100
3a	3	OH	OH	OH	H	184	7.5	127	100
4a	4	OH	OH	OH	OH	200	~1 **	127 ***	100 **

* The sum of the intensities of the nine most intense peaks of fragmentation ions given in the MS database is taken as 100% [74]. ** The authors' estimate by the equation $0.667 (M^{+\bullet})$ and 100% (Bz(OH)_n⁺), n = 4. *** Bz(OH)_{n-1}⁺ (see Scheme 7).

**Figure 9.** Correlation of the relative intensity I of the molecular ion Ad(OH)_n⁺• and the number n = 0–4 of hydroxyl groups introduced into the tertiary positions of **0**: experimental data for n = 1–3 and the authors' estimates for n = 0, 4.

Due to the high fragmentation selectivity of M⁺• (Ad(OH)_n⁺•, n = 1–4) in one channel (Scheme 7), the value of I can be considered as an indicator of the stability of M⁺•. Therefore, in the case of **0**, the indicator of the stability of M⁺• is its intensity (99.9%) relative to the sum of all fragment ions (356.9%). In terms of the accepted relative scale, this gives, respectively, the intensity I = 28% (M⁺•) relative to 100% of the sum of all fragment ions (Table 4, Figure 9).

The two estimates I = 27.667 and 28% made by different methods practically coincide, which indicates the unity of the mechanisms of fragmentation processes M⁺• Ad(OH)_n, where n = 0–4, in one channel (Scheme 7). The basis of this mechanism is the activation (weakening and lengthening) of three co-directed C–C bonds of the adamantane ring, which occurs upon single ionization of the starting compounds of this series (Scheme 7).

Since I and n are correlated, it can be assumed that both articles of 1990 and 2015 describe the MS of **3a**, and the differences are associated with the presence of impurities in the second case [57,61]. So in the article of 2015, in the MS of **3a** (m/z = 184 (10%, M⁺•)), there is a rather intense peak with m/z = 150 (50%). The appearance of such an ion cannot be associated with the fragmentation of M⁺• by the successive release of two OH radicals (m/z = 184 – 150 = 34 = 2·17), since such a process, even with the release of one OH radical, is not typical for **0** alcohols [74].

From the formal point of view, the peak with m/z = 150 (50%) can be associated either with the fragmentation of the hydroperoxide group in the secondary position (184 (M⁺•) – 34(H₂O₂) = 150) or with the fragmentation of **0** diol containing the secondary OH group (168 (M⁺•) – 18(H₂O) = 150). For example, in the MS of 2,4- and 2,6-adamantane diols (m/z = 168 (M⁺•)), the most intense peak is with m/z = 150 (100%) [74].

The authors believe that MS of **4a** is a single peak with $m/z = 127$ (100%), since the expected intensity I of the molecular ion ($m/z = 200$ ($M^{+\bullet}$)) peak is 0–1% and there is the only one highly selective channel of fragmentation $M^{+\bullet}$ -breaking the adamantane ring along its three codirectional C–C bonds, activated by a single ionization (Scheme 7).

4. Materials and Methods

The complex $\text{Cu}_2\text{Cl}_4 \cdot 2\text{DMG}$ of copper dichloride (CuCl_2) with dimethylglyoxime (DMG) was synthesized in ethanol according to the technique [71].

A 50% aqueous solution of H_2O_2 (Sigma-Aldrich, St. Louis, MI, USA) was used. **0** had a purity of at least 99% (Fluka, Buchs, Switzerland). Acetonitrile was qualified for HPLC (Sigma-Aldrich).

0 was oxidized in a glass thermostated reactor equipped with a jacket and reflux condenser with stirring on a magnetic stirrer. The reaction temperature was 50 °C unless otherwise specified. In all the experiments, the catalyst $\text{Cu}_2\text{Cl}_4 \cdot 2\text{DMG}$ was brought in immediately before adding the oxidizer solution.

Upon the fast method (~3 s) of oxidizer solution introduction, the following ratio of reagents was used: 8 mL of CH_3CN , 30 mg of $\text{C}_{10}\text{H}_{16}$, and 30 mg of $\text{Cu}_2\text{Cl}_4 \cdot 2\text{DMG}$, when varying the amount of 0.5–2 mL of an oxidizing solution—a 50% aqueous solution of H_2O_2 . Samples were taken after 5, 30, and 60 min of reaction time.

When the amount of H_2O_2 solution was increased to 10 mL, the ratio of components was used: 10 mL of CH_3CN , 100 mg of $\text{C}_{10}\text{H}_{16}$, and 20 mg of $\text{Cu}_2\text{Cl}_4 \cdot 2\text{DMG}$. The reaction time was 30 min.

0 conversion and the ratio of its oxidation products were calculated from the areas of chromatographic peaks obtained on a gas chromatograph (Chystallux 4000 M, Russia) equipped with a flame ionization detector. The column was 30 m long with an inner diameter of 0.25 mm, the stationary liquid phase SPB was OCTYL (Supelco), the carrier gas was helium. The temperature programming mode of column heating is as follows: isotherm at 60 °C–5 min, from 60 up to 260 °C—warming up with a speed of 5°/min, isotherm at 260 °C–10 min. To determine the conversion of **0**, a precisely measured amount of toluene was introduced into the sample.

Upon the slow method (drop-by-drop) of oxidizer solution introduction, the following ratio of reagents was used: 8 mL of CH_3CN , 30 mg of $\text{C}_{10}\text{H}_{16}$, and 30 mg of $\text{Cu}_2\text{Cl}_4 \cdot 2\text{DMG}$, 1 mL of a 50% aqueous solution of H_2O_2 . The total reaction time was 60 min: drop-by-drop adding of oxidizer solution—55 min, holding the reaction mixture—5 min. The reaction temperature was varied from 30 to 80 °C.

The structure and composition of the **0** oxidation products were determined in the diethyl extract using gas chromatography-mass spectrometry on a Finnigan MAT 95 XL instrument. A capillary column Varian VF-5ms was used: length 30 m, inner diameter 0.25 mm, phase thickness 0.25 μm , carrier gas—helium. Operating modes: injector temperature 270 °C; column temperature programming: 5 min isotherm at 30 °C, heating at a rate of 10 °C/min to 300 °C, then isotherm at 300 °C; energy of ionizing electrons 70 eV; source temperature 230 °C, scanning in the range of 20–800 Da at a speed of 1 s/decade of masses, resolution 1000.

For **0** products identification, its oxidation reference MS of the NIST 11,17 databases [74] and MS published in the scientific articles were used.

5. Conclusions

The distribution-group method of describing the composition of n -oxygenation products of **0**, where $n = 1–5$ is the number of oxygen atoms included in **0**, introduced as a characteristic of the oxidation depth of **0**, has shown its effectiveness in searching for conditions and factors contributing to deeper oxidation of **0**.

The catalytic system of 50% H_2O_2 / $\text{Cu}_2\text{Cl}_4 \cdot 2\text{DMG}$ / CH_3CN was able to deeply oxidize **0**, but positionally (3°:2°) not selectively, with the predominant formation of alcohol, rather than ketone groups.

At $T = 50\text{ }^{\circ}\text{C}$ and a fast ($\sim 3\text{ s}$) method of introducing an oxidizer solution into the reaction mixture, the conversion of **0** is determined by the structure of the water-acetonitrile solution, which is formed when different amounts of an aqueous solution of the oxidizer are added.

At $T = 50\text{ }^{\circ}\text{C}$ and a slow (for 60 min) drip method of introducing the oxidizer solution into the reaction mixture at full conversion, **0** is oxidized to a total amount of 72% of tri-, tetra- and penta-oxygenated products $n\text{O-Ad}$, $n = 3\text{--}5$, of which 10% fall on the tertiary triol 1,3,5-Ad(OH)₃.

A general pattern is found in the fragmentation of molecular ions of tertiary Ad(OH)_{*n*}⁺, where $n = 0\text{--}4$, which, as an example, can be useful for interpreting the MS of not only tertiary alcohols but also other n -oxygenation products of **0**.

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