



Article

Pt/C-TiO₂ as Oxygen Reduction Electrocatalysts against Sulfur Poisoning

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Abstract: Proton exchange membrane (PEM) fuel cells using Pt-based materials as electrocatalysts have achieved a decent performance, represented by the launched Toyota Mirai vehicle. The ideal PEM fuel cells consume stored pure hydrogen and air. However, SO₂, as a primary air contaminant, may be fed along with air at the cathode, leading to Pt site deactivation. Therefore, it is important to improve the SO₂ tolerance of catalysts for the stability of the oxygen reduction reaction (ORR). In this work, we develop the Pt/C-TiO₂ catalyst against SO₂ poisoning during ORR. Impressively, the hybrid Pt/C-TiO₂ catalyst with 20 mass % TiO₂ shows the best ORR and anti-toxic performance: the kinetic current density of ORR is 20.5% higher and the degradation rate after poisoning is 50% lower than Pt/C. The interaction between Pt and TiO₂ as well as the abundant hydroxyl groups on the surface of TiO₂ are both revealed to account for the accelerated removal of poisonous SO₂ on Pt surfaces.

Keywords: electrocatalysis; oxygen reduction reaction; sulfur dioxide; durability



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1. Introduction

The PEM fuel cell has been considered as one of the most promising automobile power supplies owing to its high energy efficiency and environmental benefits [1–3]. Delightfully, the first-generation Toyota Mirai has provided an excellent example, using PtCo as a cathode catalyst, achieving a max power with 114 kW and an endurance mileage of up to 502 km. However, the widespread implementation of PEM fuel cells is facing a greatly challenging poisoning/degradation problem caused by impurities such as SO₂ and NO_x in the air, which is ideally supplied directly to the cathodes [4,5]. In particular, SO₂ can strongly adsorb onto the Pt surface and deactivate the active sites for the oxygen reduction reaction (ORR), leading to the degradation of ORR performance [6–13]. For example, it has been reported that the continuous feeding of 2.5 ppm SO₂/air mixture for 45 h at the cathode significantly reduced the fuel cell performance by 53% and, importantly, the subsequent continuous clean air feeding for 20 h could not completely recover the performance [14]. This is because the widely accepted Pt/C catalysts are not efficient enough to remove the S_x species once the coverage is higher than 14%, where up to 95% of mass activity can be lost [15]. In addition, an extremely harsh potential range of 1.2 V~1.5 V is required to completely oxidize SO_x into water-soluble SO₄²⁻ and/or HSO₄⁻, which is much higher than the working potential of a PEM fuel cell (0.6 V~0.8 V) [6,16,17]. In this regard, the poisoning SO₂ species is almost irreversible under the normal operating conditions of a PEM fuel cell [18]. This fact triggers us to explore innovations in developing advanced anti-poisoning catalysts.

Numerous efforts have been made to prevent Pt-based catalysts from SO₂ poisoning [19]. For example, Baturina and coworkers [20,21] found that the adsorbed SO₂ is more easily oxidized and removed on Pt₃Co/C than Pt/C, although the alloying Pt₃Co/C catalyst is more sensitive to the poisoning (The same concentration of SO₂ has a more serious effect on the ORR performance of Pt₃Co/C). They found that H₂O is more likely to decompose into hydroxyl (-OH) on Pt₃Co/C, which is beneficial for accelerating the electro-oxidation of SO₂. In addition, Xu et al. [22] found that the SO₂-poisoned 5 mass % WO_x-Pt/C can cause a higher loss of SO₂ than commercial Pt/C after the first potential cycling up to 1.5 V, which might be due to the synergistic effect between WO_x and Pt. The OH group on the hydrophilic WO_x surface and the hydrogen spillover effect promote the electro-oxidation of sulfur-containing species. In their latter work, the Pt/CeO₂/C catalyst was prepared by one-pot synthesis, enhancing the oxygen migration and thus improving SO₂ electro-oxidation and ORR activity [23,24]. In our previous work, we found that Ru efficiently modified the electronic structure of Pt in PtRu alloy catalysts, leading to a weaker interaction between Pt and SO₂ [25]. In this work, we will focus on the effect of metal oxides to the ORR performance and SO₂ tolerance of Pt.

To tone-up the positive effects of oxidative hydroxyl and synergy, we herein develop a hybrid Pt/C-TiO₂ catalyst against SO₂ poisoning during ORR. The selection of TiO₂ is based on its high hydrophilicity and outstanding chemical and electrochemical stability, as well as strong interaction with the Pt component [26–33]. Importantly, based on the above discussions, the abundant hydroxyl groups (-OH) on the hydrophilic TiO₂ surface may benefit poisonous sulfur removal. Accordingly, the electro-oxidation of SO₂ is significantly accelerated on such a Pt/C-TiO₂ catalyst to reduce the SO₂ poisoning. To our knowledge, the effect of TiO₂ on suppressing SO₂ poisoning of Pt-based ORR catalysts has not been reported. In this work, our hybrid Pt/C-TiO₂ catalysts have higher ORR activity and better sulfur tolerance compared to traditional Pt/C.

2. Results and Discussion

2.1. Characterization of Catalysts

Figure 1 shows the X-ray diffraction (XRD) patterns of the as-prepared Pt/C, Pt/C-20TiO₂ catalysts and TiO₂ nanoparticles. For the Pt/C sample, the broad X-ray diffraction peak in the range of 20°–30° corresponds to the amorphous structure of XC-72 carbon black, while the peaks at 39.8°, 46.2°, 67.5°, and 81.3° correspond to Pt(111), (200), (220), and (311) facets, respectively (JCPDS No. 04-0802). The commercial TiO₂ sample shows sharp peaks, which can be indexed to the anatase TiO₂ (JCPDS No. 21-1272). The XRD pattern of Pt/C-20TiO₂ has the X-ray diffraction peaks of both Pt and TiO₂. The above facts demonstrate that the Pt/C and Pt/C-20TiO₂ were synthesized successfully.

As the high-resolution transmission electron microscopy (HRTEM) image in Figure 2a shows, the Pt nanoparticles are uniformly dispersed on the carbon supports with an average size of about 2.74 nm (Figure S1). A small Pt particle size and uniform dispersion potentially ensure good catalytic performance [34]. Figure 2b shows TEM images of the as-prepared Pt/C-20TiO₂ catalyst. The lattice fringes of 0.35 nm (red tags) and 0.22 nm (yellow tags) are assigned to the TiO₂ (101) plane and the Pt (111) plane, respectively. It can be seen that the TiO₂ and Pt particles are well contacted with each other.

2.2. Electrocatalytic Performance

The cyclic voltammogram (CV) and linear sweep voltammetry (LSV) curves of all pristine catalysts (before poisoning) are shown in Figure 3a,b, respectively. The electrochemical surface areas (ECSAs) of all the catalysts were calculated based on the H₂ adsorption/desorption region at 0–0.3 V in CV curves. All the relevant data recorded and calculated from electrochemical measurement are listed in Table 1.

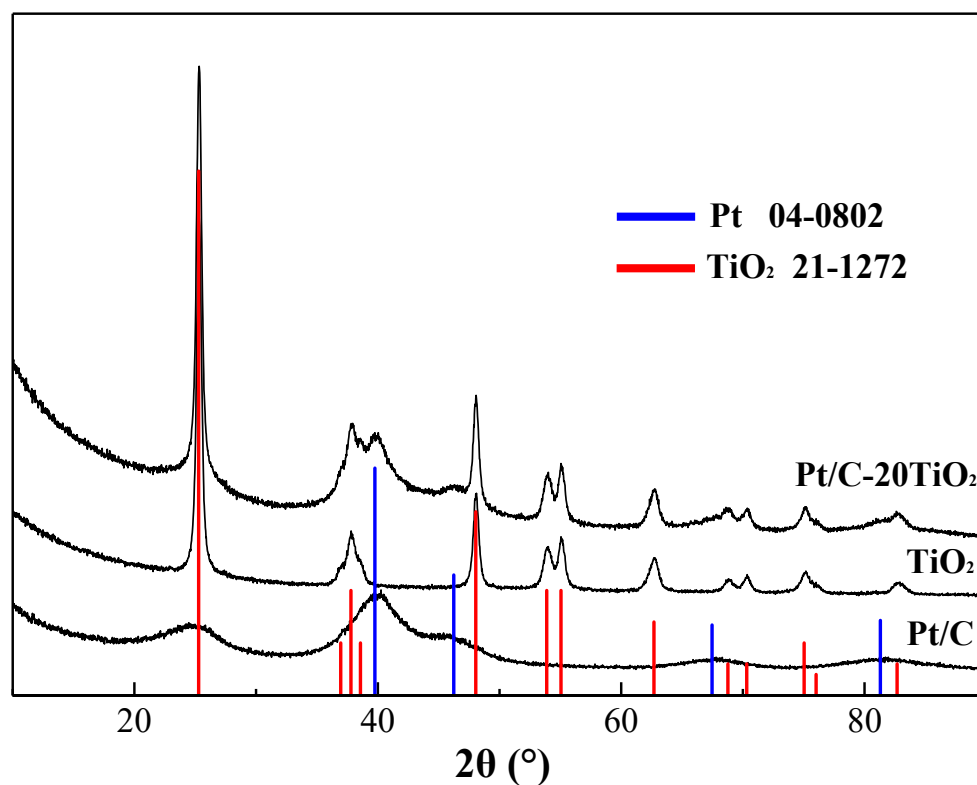


Figure 1. XRD patterns of Pt/C, commercial TiO₂ and Pt/C-20TiO₂ catalysts.

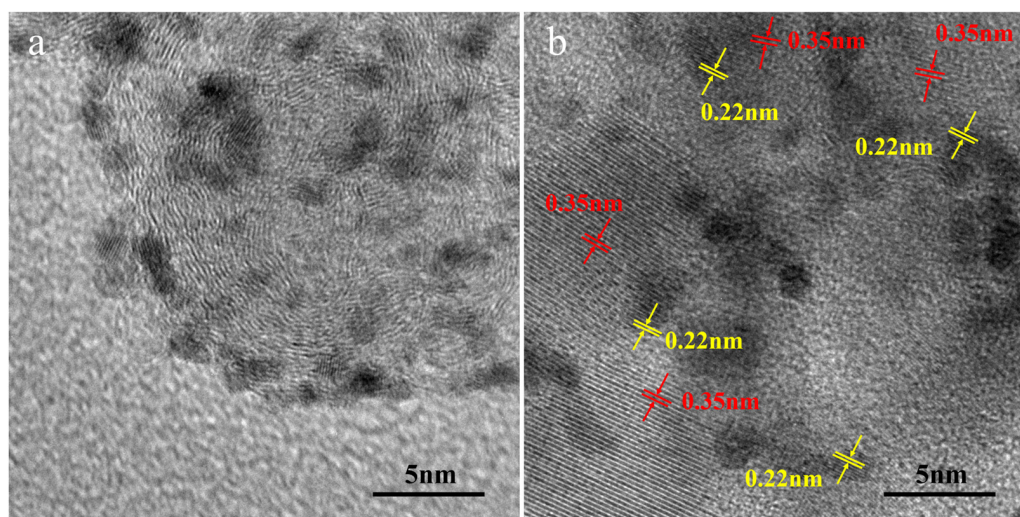


Figure 2. (a) TEM images of Pt/C and (b) Pt/C-20TiO₂ catalysts.

The results show that the addition of TiO₂ has little effect on the ECSA of the Pt/C catalyst. Compared with that of Pt/C, the current peak, representing the oxygen reduction of the Pt/C-TiO₂ catalysts, shifts positively when TiO₂ ≤ 30%; Pt/C-20TiO₂ has the most positive oxygen reduction peak, which likely indicates the best ORR activity, consistent with the LSV results in Figure 3b. The activity towards ORR is improved by increasing TiO₂ content and then started to decrease after reaching a maximum value, i.e., Pt/C-20TiO₂. Too much TiO₂ (≥30 mass %) hinders the ORR activity, which is due to the low electron conductivity of TiO₂. On the other hand, the half-wave potential ($E_{1/2}$) of Pt/C-20TiO₂ is 0.867 V, presenting an increase by 0.014 V compared with Pt/C (0.853 V), and the i_k @ 0.9 V is 2.337 mA/cm², 20.5% higher than Pt/C (1.939 mA/cm²). Based on the Koutechy–Levich (K–L) equation (see Section 3.3), the ORR polarization curves of Pt/C-20TiO₂ were

measured at different rotation speeds (Figure S2a). The charge transfer electrons (n) of Pt/C-20TiO₂ can be derived from the slopes of the liner K-L plot (Figure S2b), which are 3.89, 3.87, 3.87, and 3.86 at 0.75 V, 0.7 V, 0.65 V, and 0.6 V, respectively, indicating the four-electron reaction pathway of ORR. This fact demonstrates the positive effect of TiO₂ for ORR activity.

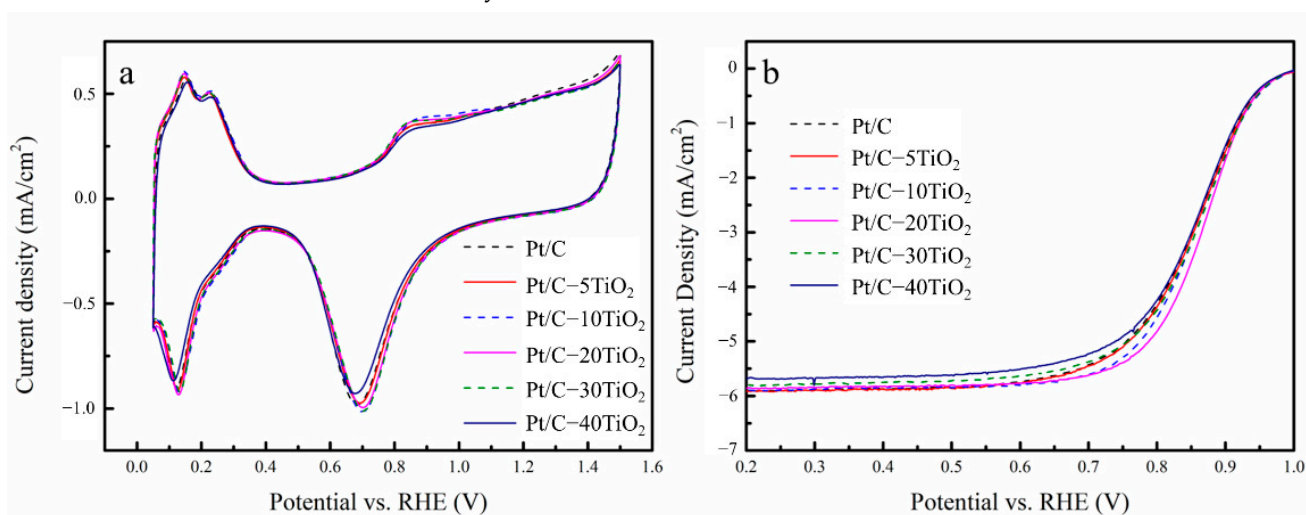


Figure 3. The (a) CV and (b) LSV curves of all pristine catalysts (before poisoning).

Table 1. Electrochemical data of all pristine (before poisoning) and SO₂-poisoned catalysts.

Sample	Pristine			SO ₂ Poisoned			Negative Shift of E _{1/2} after Poisoning (mV)	Loss of i_k @ 0.9 V after Poisoning
	ECSA (m ² g _{Pt} ⁻¹)	E _{1/2} (V)	i_k @ 0.9 V (mA cm ⁻²)	ECSA (m ² g _{Pt} ⁻¹)	E _{1/2} (V)	i_k @ 0.9 V (mA cm ⁻²)		
Pt/C	97.07	0.853	1.939	27.06	0.782	0.624	71	67.8%
Pt/C-5TiO ₂	97.84	0.855	2.042	26.55	0.800	1.175	55	42.5%
Pt/C-10TiO ₂	102.04	0.858	2.172	28.32	0.809	1.424	49	34.4%
Pt/C-20TiO ₂	101.46	0.867	2.337	25.99	0.814	1.517	53	35.1%
Pt/C-30TiO ₂	99.11	0.86	2.210	29.82	0.775	0.801	85	63.7%
Pt/C-40TiO ₂	95.11	0.855	1.884	26.81	0.736	0.716	119	62.0%

The first CV scans of each catalyst after poisoning in Ar-saturated 0.1 M HClO₄ solution are shown in Figure 4a, where the ECSA of all the catalysts decreases in a similar way because the strongly adsorbed SO₂ blocks the active site of Pt. In addition, clear oxidation peaks are observed in the potential range of 0.8 V~1.5 V, due to the electrochemical oxidation of SO₂. Notably, there is a negative shift in the SO₂ oxidation peak of Pt/C-TiO₂ catalysts compared with Pt/C, indicating the higher activity of Pt/C-TiO₂ catalysts to oxidize SO₂. Particularly, the Pt/C-20TiO₂ has the largest negative shift by about 50 mV in SO₂ oxidation, as shown in Figure 4b. The oxide reduction potential region of Figure 4b is magnified and shown in Figure 4c to compare the catalytic performance of Pt/C and Pt/C-20TiO₂ before and after poisoning. It is clear that the reduction peaks of Pt/C-20TiO₂ before or after poisoning all positively shift compared with the Pt/C catalyst, indicating that the Pt/C-20TiO₂ has a better electrocatalytic performance to reduce oxygen-bearing species than Pt/C at initial and after sulfur poisoning.

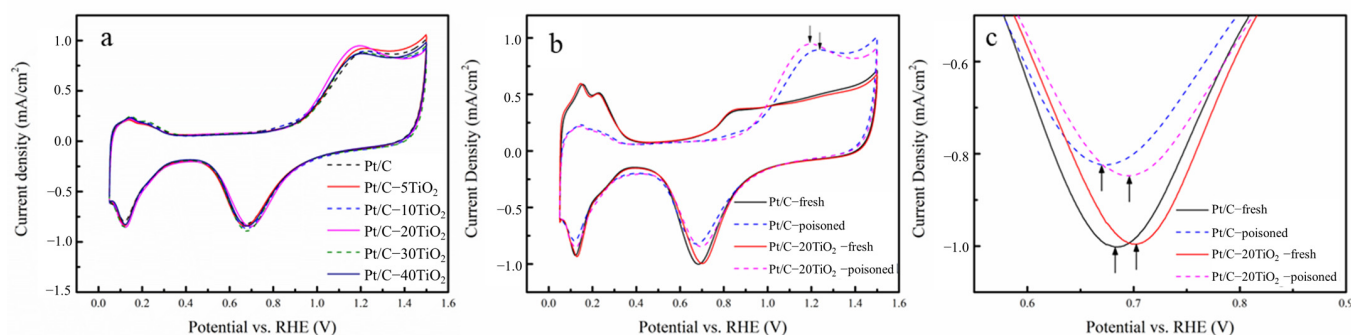


Figure 4. CV curves in Ar-saturated 0.1 M HClO₄ solution of (a) all catalysts after SO₂ poisoning, (b) Pt/C and Pt/C-20TiO₂ before and after poisoning, and (c) corresponding magnification at oxide reduction potential region.

The LSV curves of ORR after SO₂ poisoning are shown in Figure 5a. After SO₂ poisoning, the ORR activity of all catalysts is decreased, although the Pt/C-20TiO₂ catalyst still has the best ORR activity. The i_k @ 0.9 V comparison between the fresh and poisoned catalysts is shown in Figure 5b. With the addition of TiO₂, the decrease percentage of kinetic current density is significantly lowered. The Pt/C-10TiO₂ and Pt/C-20TiO₂ catalysts have the smallest activity decay by only 34.4% and 35.1%, respectively, in contrast to 67.8% for Pt/C. Table 1 shows that the $E_{1/2}$ of Pt/C-20TiO₂ went down by 53 mV negatively after poisoned, much lower than the 71 mV of Pt/C. All this indicates that the SO₂ tolerance of Pt/C-20TiO₂ is greatly improved than Pt/C.

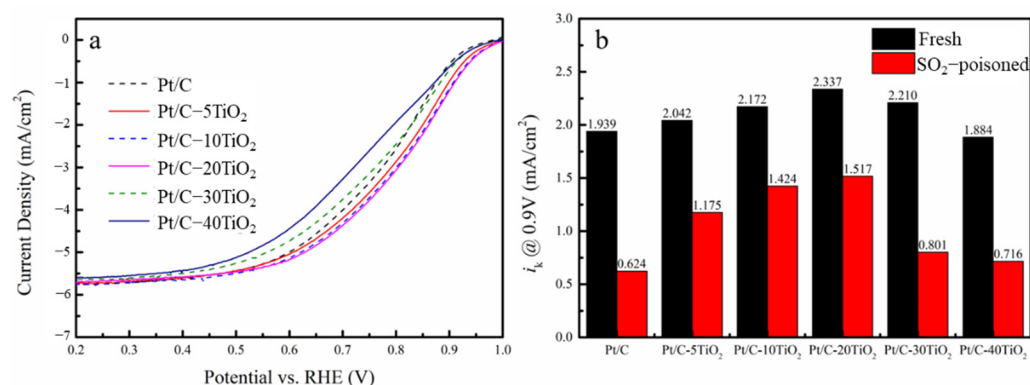


Figure 5. (a) The LSV ORR curves of SO₂ poisoned catalysts; (b) the kinetic current density at 0.9 V of fresh and SO₂-poisoned catalysts.

2.3. Mechanism of SO₂ Tolerance

The X-ray photoelectron spectroscopy (XPS) spectra of the O 1s, Ti 2p and Pt 4f regions in TiO₂, Pt/C, and Pt/C-20TiO₂ are shown in Figure 6. As shown in the O 1s region (Figure 6a), the peaks at 533.5 ± 0.1 eV, 532.2 ± 0.1 eV and 530.6 ± 0.1 eV are assigned to physically absorbed water (O1), chemisorbed OH species (O2), and lattice oxygen in TiO₂ and/or PtO (O3) [26,35]. In addition, it can be seen that the Ti 2p binding energy of Pt/C-20TiO₂ has a negative shift by 0.4 eV compared with Pt/C (Figure 6b). The Pt 4f regions for Pt/C and Pt/C-20TiO₂ can be fitted into three sets of doublets (Figure 6c). For the Pt/C, Pt 4f peaks at 71.4 eV and 74.7 eV are assigned to Pt (0), 72.8 eV and 76.1 eV to Pt (II) in PtO or Pt(OH)₂-like species, and 74.0 eV and 77.3 eV to Pt(IV) in PtO₂. Interestingly, the binding energy of the Pt/C-20TiO₂ catalyst is negatively shifted by 0.3 eV compared to the Pt/C catalyst, indicating an electronic interaction between Pt and TiO₂.

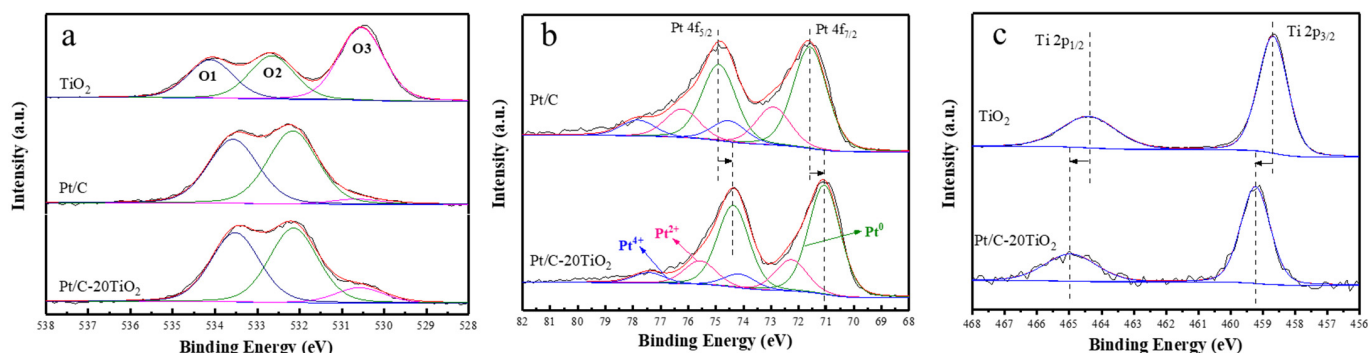


Figure 6. XPS spectra in (a) O 1s region of TiO₂, Pt/C and Pt/C–20TiO₂; (b) Ti 2p XPS of TiO₂ and Pt/C–20TiO₂; (c) Pt 4f XPS of Pt/C and Pt/C–20TiO₂.

The electron transfer from TiO₂ to Pt increases the electron density of Pt, which was reported as a necessity for effective ORR [36]. In addition, the binding energy between Pt and OH-like oxygen-containing species is weakened, which accelerates the reaction of O, OH, and H⁺ to generate H₂O and improves the ORR activity [37,38]. Jaksic et al. [39] found that in aqueous media, OH on the surface of metal oxides such as WO₃ and TiO₂ can be transferred to the Pt surface to form Pt-OH, which is the so-called spillover effect. Reasonably, such an OH spillover effect of TiO₂ will repel the OH groups on Pt, leading to decreased binding energy between OH and Pt and promoting ORR activity [40]. On the other hand, the electronic interaction between Pt and TiO₂ is able to weaken the adsorption of poisoning species on Pt surfaces [25,41]. At the same time, the spillover effect of oxidative OH on the TiO₂ surface plays a significant role in promoting the electro-oxidation (removal) of SO₂ [22]. Figure 7 is provided to illustrate this mechanism. For the Pt/C–TiO₂ catalyst: Pt provides electrocatalytic active sites for oxygen reduction; C supports Pt nanoparticles and conducts electrons; and TiO₂ modifies the electronic structure of Pt to enhance the ORR activity and SO₂ tolerance.

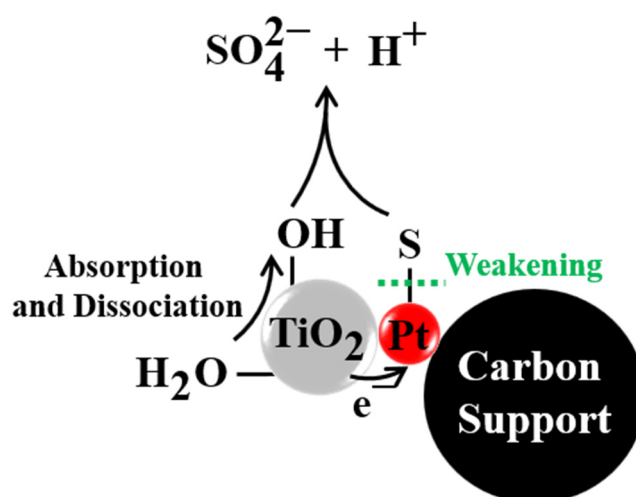


Figure 7. The schematic diagram of SO₂ electro-oxidation mechanism on Pt/C–TiO₂ catalysts.

3. Materials and Methods

3.1. Chemicals and Materials Characterization

Chloroplatinic acid (H₂PtCl₆, Sinopharm Chemical Reagent), Vulcan carbon XC-72 (Cabot Corp, Boston, MA, USA), TiO₂ nanoparticles (25 nm, anatase, Aladdin, Shanghai, China), perchloric acid (HClO₄, Aladdin, Shanghai, China), anhydrous sodium sulfite (Na₂SO₃, Dupont, Eleutherian Mills, DE, USA), and 5.0 wt % Nafion aqueous solution (Dupont, Eleutherian Mills, DE, USA) were of analytical grade and used as received if not

specified. Deionized water (18.2 M Ω cm, Mill-Q Corp, Darmstadt, Germany) was used in all of the experiments.

TEM and HRTEM images were taken on JEOL JEM-2100 with an acceleration voltage of 300 kV. The morphologies and crystal structure of the Pt/C, Pt/C-TiO₂ catalyst and TiO₂ nanoparticles were characterized by XRD (Netherlands, Panalytical X'PERT) using Cu K α radiation. XPS measurements were performed by a Physical Electronics PHI model 5700 instrument with an electron energy analyzer, with half-spherical precision using Al K α radiation (1486.6 eV). The binding energy of all samples was calibrated vs. the C 1s value of 284.6 eV.

3.2. Synthesis of Catalysts

The Pt/C catalyst (20 mass % Pt) was prepared by the microwave-assisted polyol reduction method [42]. Briefly, 40 mg Vulcan XC-72 carbon black was well-dispersed into 60 mL ethylene glycol (EG) and isopropanol ($V/V = 4:1$) under ultrasonic treatment for 2 h. Then H₂PtCl₆-EG solution was added to the slurry and stirred constantly for 2 h. Next, 1 mol/L NaOH-EG solution was dropped into the slurry under continuous stirring until the pH was stable at 12. Argon was injected into the slurry for 20 min to remove oxygen, which was then placed in a microwave oven (2450 MHz, 800 W) and heated for 2 min. After the solution was cooled down to room temperature, a certain amount of dilute nitric acid was added to pH = 3, followed by stirring for 12 h. After washing with plenty of boiling ultra-pure water (Milli-Q, 18 M Ω cm), the Pt/C catalyst was dried in a vacuum oven at 70 °C for 12 h.

The Pt/C catalyst ink was prepared by dispersing 5 mg Pt/C catalyst into a mixture of 5 μ L of 5 wt.% Nafion solution, 1.25 mL isopropanol, and 3.75 mL ultra-pure water. For the hybrid Pt/C-TiO₂ catalyst ink, a certain amount of TiO₂ nanoparticles were first dispersed in 3.75 mL ultra-pure water, prior to adding and dispersing 5 mg Pt/C, 5 μ L Nafion solution, and 1.25 mL isopropanol. The hybrid catalysts were labeled as Pt/C-5TiO₂, Pt/C-10TiO₂, Pt/C-20TiO₂, Pt/C-30TiO₂, and Pt/C-40TiO₂ using different TiO₂ contents of 5, 10, 20, 30, and 40 mass %.

3.3. Electrochemical Measurements

All electrochemical measurements were carried out in a three-electrode system with an electrolyte of 0.1 mol/L HClO₄ aqueous solution at room temperature, using the glassy carbon rotating-disk electrode (GC-RDE, 5 mm in diameter) as the working electrode, a saturated Ag-AgCl electrode as the reference electrode, and a piece of Pt foil (1 cm²) as the counter electrode. 10 μ L of catalyst ink was dropped onto the polished GC-RDE. Then the electrodes were air-dried at room temperature. The catalyst loading was about 10 μ g/cm².

The ECSA of the catalyst is calculated based on the charge number of H adsorption or desorption, as shown in Equation (1).

$$\text{ECSA} = \frac{Q_{\text{H}}}{0.21 \times 10^{-3} \times m_{\text{Pt}}} \quad (1)$$

where Q_{H} (C) represents the charge number of H adsorption or desorption and can be obtained by integrating the CV curve in Ar-saturated 0.1 mol L⁻¹ HClO₄ solution between 0.05 and 0.4 V; and m_{Pt} (g) is the Pt load in the catalyst. Assuming there is a one-to-one relationship between the Pt atom and H atom of the hydrogen monatomic layer on the Pt/C catalyst, the charge amount of the hydrogen monatomic layer on the Pt/C catalyst surface is 210 μ C cm⁻².

Before recording ORR activity, ultra-pure argon gas was injected into the electrolyte for 20 min to remove dissolved oxygen. CV scans were then performed at the scan rate of 50 mV s⁻¹ in a potential range of 0.05 V~1.5 V for 10 cycles at room temperature. The ORR activity of the catalyst was then measured by LSV from 0.05 V to 1 V at a scan rate of 10 mV s⁻¹ at 1600 rpm in O₂-saturated 0.1 mol/L HClO₄ solution. The kinetic current

density at 0.9 V and transferred electron number were calculated from the ORR polarization following the Koutechy–Levich (K–L) equation, Equation (2).

$$\frac{1}{i} = \frac{1}{i_k} + \frac{1}{i_d} = \frac{1}{i_k} + \frac{1}{0.62nFAD^{2/3}\omega^{1/2}\nu^{-1/6}c} \quad (2)$$

where i_k and i_d are the kinetic current density and limited diffusion current density, n is the number of electrons transferred, F is the Faraday constant ($96,487 \text{ C mol}^{-1}$), A is the geometric surface area of the RDE, c is the bulk concentration of O_2 ($2.64 \times 10^{-4} \text{ mol cm}^{-3}$), D is the diffusion coefficient of O_2 ($1.93 \times 10^{-5} \text{ cm}^2 \text{ S}^{-1}$), ν is the kinematic viscosity of the solution ($0.01 \text{ cm}^2 \text{ S}^{-1}$), and ω is the angular velocity. The half-wave potential ($E_{1/2}$) is read from the ORR curve of the catalyst, which is the potential corresponding to the half of the limited diffusion current density.

The poisoning of catalysts was carried out by immersing the working electrode at the potential of 0.65 V for 1 min in a 0.5 mmol/L Na_2SO_3 + 0.1 mol/L HClO_4 electrolyte. Then, the GC-RDE was rinsed with ultra-pure water and transferred to a fresh 0.1 mol/L HClO_4 electrolyte without SO_2 . The ORR activity of the poisoned electrode was evaluated in an O_2 -saturated 0.1 mol/L HClO_4 electrolyte using LSV at 1600 rpm. To investigate the oxidation behavior of adsorbed SO_2 , a CV scan was performed between 0.05 V and 1.5 V for 10 cycles at a sweep rate of 50 mV/s. All of the potentials were reported with respect to the reversible hydrogen electrode (RHE) in this work.

4. Conclusions

Hybrid Pt/C-TiO₂ catalysts were prepared by mixing Pt/C catalyst and TiO₂ nanoparticles. By adding TiO₂, the ORR performances of fresh and SO₂-poisoned catalysts were all improved compared to the Pt/C and the activity loss caused by SO₂ poisoning was remarkably reduced. Our detailed observations indicate that the improved SO₂ tolerance is due to the accelerated electro-oxidation of SO₂ in the presence of optimal TiO₂. We suggest that the electronic interaction between Pt and TiO₂ and the OH spillover effect on TiO₂ might be crucial for not only enhancing the ORR activity, but also removing the poisoning SO₂. These results indicate that the TiO₂ modified Pt/C catalyst is a desired ORR catalyst against sulfur poisoners in PEM fuel cells.

Supplementary Materials: The following supporting information can be downloaded at: <https://www.mdpi.com/article/10.3390/catal12050571/s1>, Figure S1: TEM images of Pt/C and particle size distributions; Figure S2: The ORR polarization curves of Pt/C-20TiO₂ measured at different electrode rotation speeds and the K-L plots from the polarization curve.

Author Contributions: Synthesis and characterization, Y.L. and J.Y.; electrocatalytic experiments, Y.L. and F.K.; supervision, L.D. and C.D.; project administration, G.Y. and P.Z.; writing, Y.L. and L.D.; proofread, G.Y. and L.D. All authors have read and agreed to the published version of the manuscript.

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Data Availability Statement: Data are available in the main text.

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Conflicts of Interest: The authors declare no conflict of interest.

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