

# Lanthanum–Cerium-Modified Nickel Catalysts for Dry Reforming of Methane

Mahmud S. Lanre, Ahmed E. Abasaheed \*, Anis H. Fakeeha, Ahmed A. Ibrahim \*, Abdulrahman S. Al-Awadi, Abdulrahman bin Jumah, Fahad S. Al-Mubaddel and Ahmed S. Al-Fatesh \*

Chemical Engineering Department, College of Engineering, King Saud University, P.O. Box 800, Riyadh 11421, Saudi Arabia; mahmudsofiu@gmail.com (M.S.L.); anishf@ksu.edu.sa (A.H.F.); alawadi@ksu.edu.sa (A.S.A.-A.); abinjahum@ksu.edu.sa (A.b.J.); falmubaddel@ksu.edu.sa (F.S.A.-M.)

\* Correspondence: abasaheed@ksu.edu.sa (A.E.A.); aididwhts2011@gmail.com (A.A.I.); aalfatesh@ksu.edu.sa (A.S.A.-F.); Tel.: +966-11-467-6856 (A.E.A.); +966-11-467-6856 (A.A.I.); +966-11-467-6859 (A.S.A.-F.)

**Citation:** Lanre, M.S.; Abasaheed, A.E.; Fakeeha, A.H.; Ibrahim, A.A.; Al-Awadi, A.S.; Jumah, A.b.; Al-Mubaddel, F.S.; Al-Fatesh, A.S. Lanthanum–Cerium-Modified Nickel Catalysts for Dry Reforming of Methane. *Catalysts* **2022**, *12*, 715. <https://doi.org/10.3390/catal12070715>

Academic Editors: Maria A. Goula

Received: 1 June 2022

Accepted: 27 June 2022

Published: 29 June 2022

**Publisher's Note:** MDPI stays neutral with regard to jurisdictional claims in published maps and institutional affiliations.



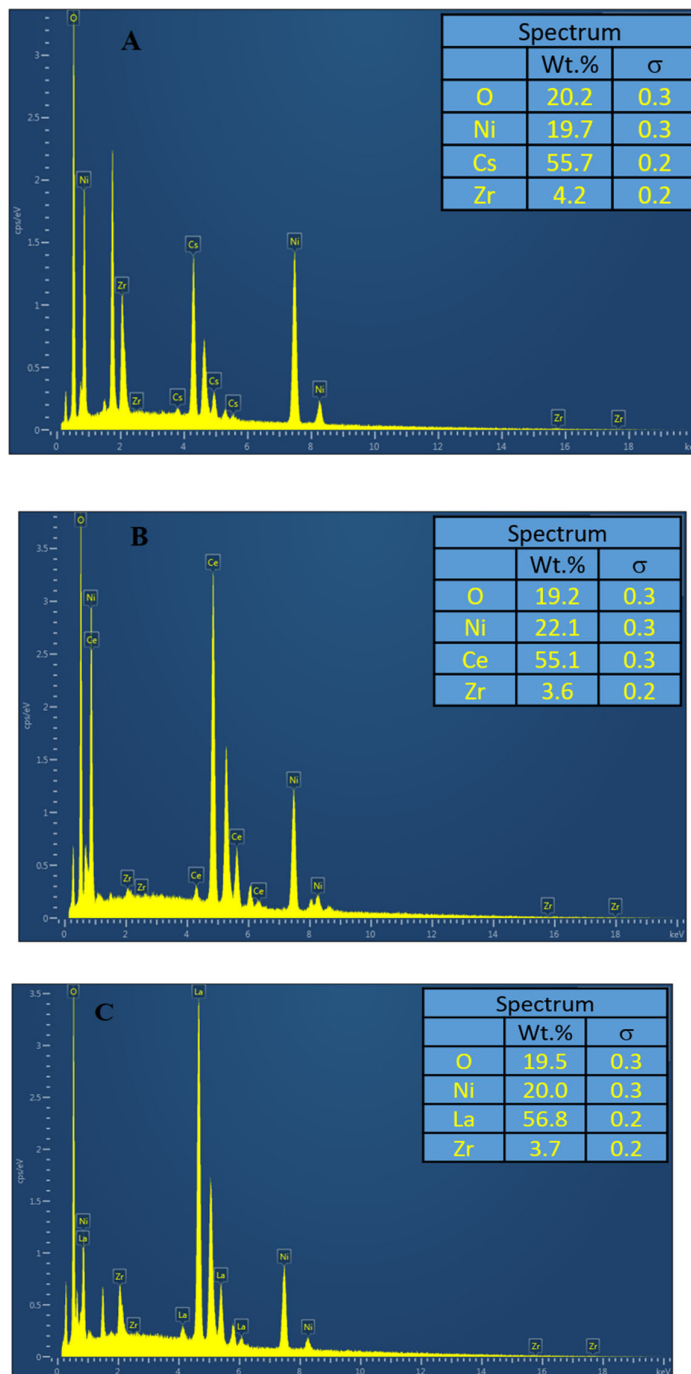
**Copyright:** © 2022 by the authors. Licensee MDPI, Basel, Switzerland. This article is an open access article distributed under the terms and conditions of the Creative Commons Attribution (CC BY) license (<http://creativecommons.org/licenses/by/4.0/>).

**Abstract:** The catalyst  $\text{MNi}_{0.9}\text{Zr}_{0.1}\text{O}_3$  ( $\text{M} = \text{La}$ ,  $\text{Ce}$ , and  $\text{Cs}$ ) was prepared using the sol–gel preparation technique investigated for the dry reforming of methane reaction to examine activity, stability, and  $\text{H}_2/\text{CO}$  ratio. The lanthanum in the catalyst  $\text{LaNi}_{0.9}\text{Zr}_{0.1}\text{O}_3$  was partially substituted for cerium and zirconium for yttrium to give  $\text{La}_{0.6}\text{Ce}_{0.4}\text{Ni}_{0.9}\text{Zr}_{0.1-x}\text{Y}_x\text{O}_3$  ( $x = 0.05, 0.07$ , and  $0.09$ ). The  $\text{La}_{0.6}\text{Ce}_{0.4}\text{Ni}_{0.9}\text{Zr}_{0.1-x}\text{Y}_x\text{O}_3$  catalyst's activity increases with an increase in yttrium loading. The activities of the yttrium-modified catalysts  $\text{La}_{0.6}\text{Ce}_{0.4}\text{Ni}_{0.9}\text{Zr}_{0.03}\text{Y}_{0.07}\text{O}_3$  and  $\text{La}_{0.6}\text{Ce}_{0.4}\text{Ni}_{0.9}\text{Zr}_{0.01}\text{Y}_{0.09}\text{O}_3$  are higher than the unmodified  $\text{La}_{0.6}\text{Ce}_{0.4}\text{Ni}_{0.9}\text{Zr}_{0.1}\text{O}_3$  catalyst, the latter having methane and carbon dioxide conversion values of 84% and 87%, respectively, and the former with methane and carbon dioxide conversion values of 86% and 90% for  $\text{La}_{0.6}\text{Ce}_{0.4}\text{Ni}_{0.9}\text{Zr}_{0.03}\text{Y}_{0.07}\text{O}_3$  and 89% and 91% for  $\text{La}_{0.6}\text{Ce}_{0.4}\text{Ni}_{0.9}\text{Zr}_{0.01}\text{Y}_{0.09}\text{O}_3$ , respectively. The BET analysis depicted a low surface area of samples ranging from 2 to  $9\text{m}^2/\text{g}$ . The XRD peaks confirmed the formation of a monoclinic phase of zirconium. The TPR showed that apparent reduction peaks occurred in moderate temperature regions. The TGA curve showed weight loss steps in the range 773 K–973 K, with  $\text{CsNi}_{0.9}\text{Zr}_{0.1}\text{O}_3$  carbon deposition being the most severe. The coke deposit on  $\text{La}_{0.6}\text{Ce}_{0.4}\text{Ni}_{0.9}\text{Zr}_{0.1}\text{O}_3$  after 7 h time on stream (TOS) was the lowest, with 20% weight loss. The amount of weight loss increases with a decrease in zirconium loading.

**Keywords:** dry reforming of methane; catalyst activity; oxygen vacancies; carbon deposit

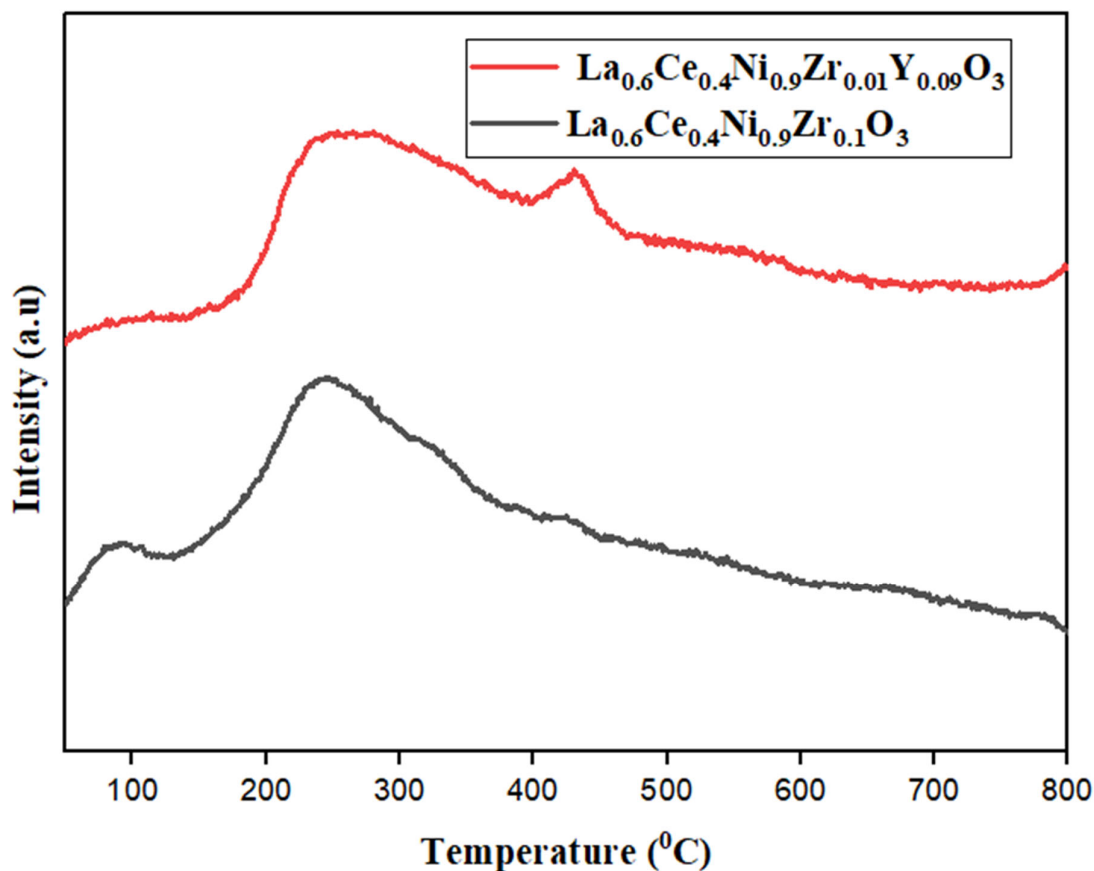
### Supplementary Characterization

Figure S1 illustrates the Energy Dispersive X-ray results of the catalyst samples. It denotes the qualitative elemental compositions of the freshly prepared samples. the percentage composition of elements corresponds to the computed composition during the synthesis.



**Figure S1.** The EDX analysis of fresh catalysts (A)  $\text{CsNi}_{0.9}\text{Zr}_{0.1}\text{O}_3$  (B)  $\text{CeNi}_{0.9}\text{Zr}_{0.1}\text{O}_3$  (C)  $\text{LaNi}_{0.9}\text{Zr}_{0.1}\text{O}_3$ .

Figure S2 displays the CO<sub>2</sub>-TPD results which highlight the basicity of different calcined samples. Apparently, there are two peaks in the profiles of the catalysts. The peaks around 100 °C and 250 °C can be ascribed to the weak basic sites of catalysts. Obviously, the addition of yttria has somewhat increased the content of weak basic sites. The peak at about 410 °C was attributed to the medium-strength basic sites.



**Figure S2.** CO<sub>2</sub>-TPD profiles of fresh catalysts:  $\text{La}_{0.6}\text{Ce}_{0.4}\text{Ni}_{0.9}\text{Zr}_{0.01}\text{Y}_{0.09}\text{O}_3$  and  $\text{La}_{0.6}\text{Ce}_{0.4}\text{Ni}_{0.9}\text{Zr}_{0.1}\text{O}_3$ .

The TPO analysis of  $\text{La}_{0.6}\text{Ce}_{0.4}\text{Ni}_{0.9}\text{Zr}_{0.01}\text{Y}_{0.09}\text{O}_3$  is shown in figure S3. The TPO profile exhibits only one distinct peak at around 600 °C indicating the formation of graphitic carbon type.

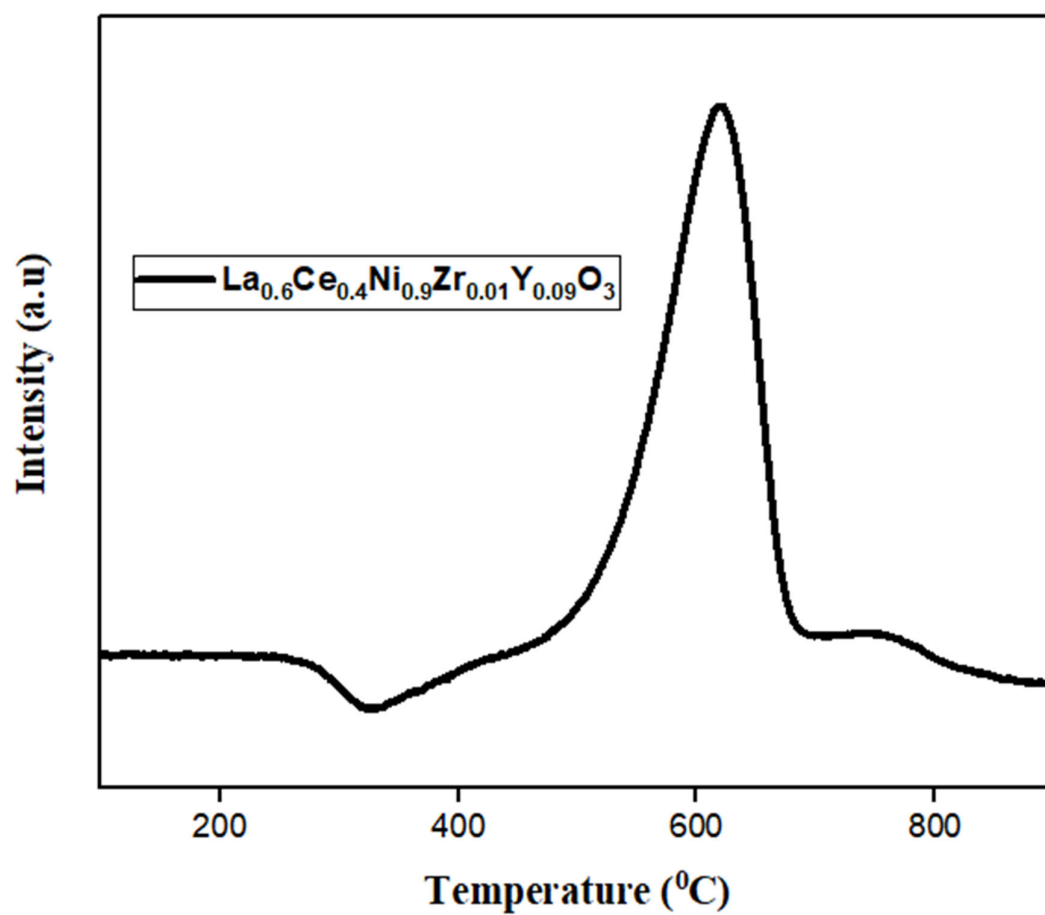


Figure S3. TPO profile of used catalysts:  $\text{La}_{0.6}\text{Ce}_{0.4}\text{Ni}_{0.9}\text{Zr}_{0.01}\text{Y}_{0.09}\text{O}_3$ .