

Supplementary Material

Performance of particulate and structured Pt/TiO₂-based catalysts for the WGS reaction under realistic high- and low-temperature shift conditions

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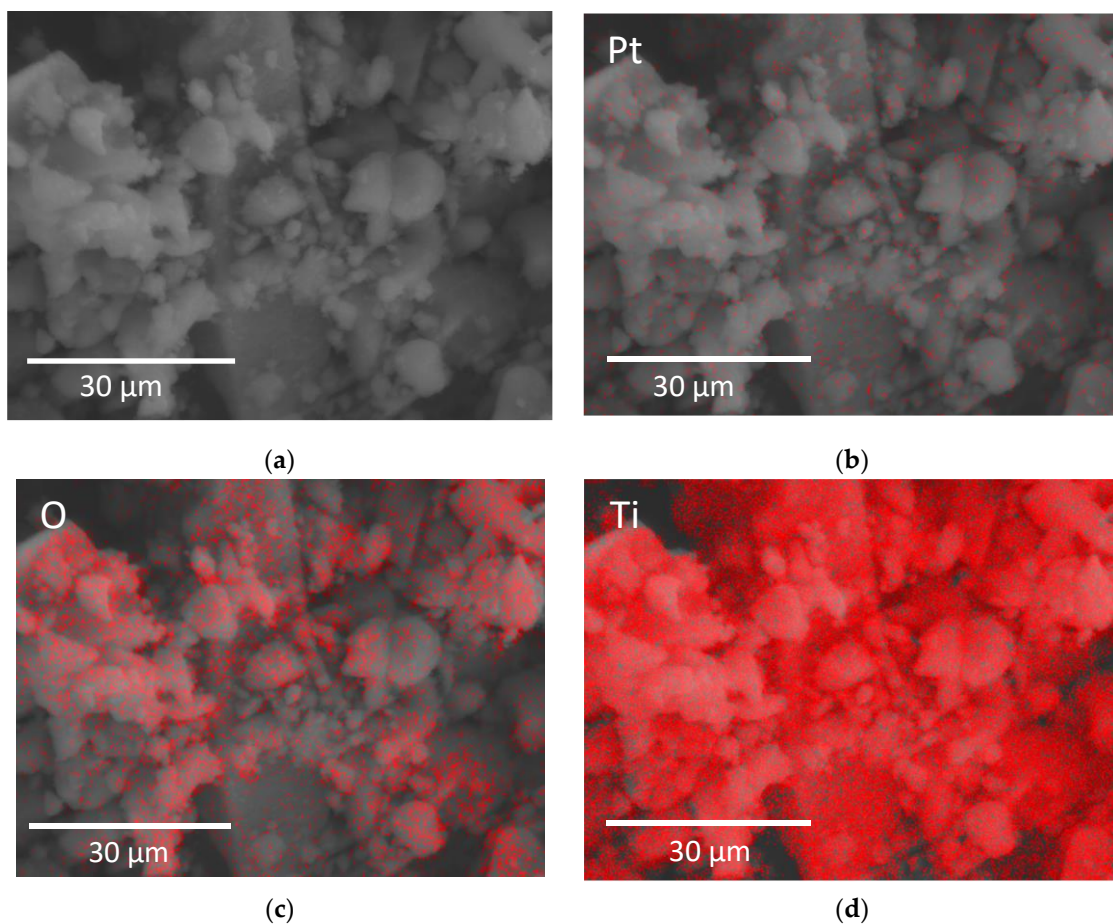


Figure S1. (a) SEM image of the as prepared Pt/TiO₂ catalyst, and EDS mapping results showing the distribution of (b) Pt, (c) O and (d) Ti elements.

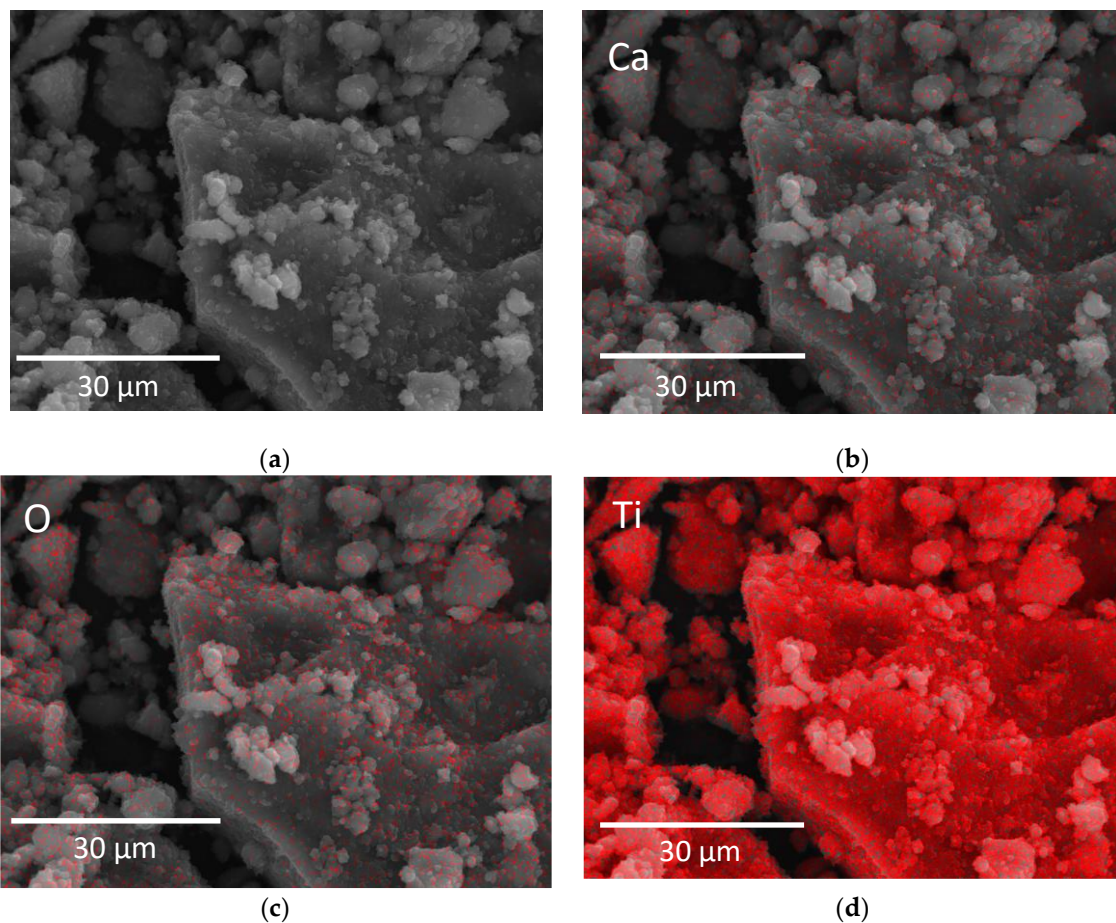


Figure S2. (a) SEM image of the as prepared $\text{TiO}_2(\text{Ca})$ support, and EDS mapping results showing the distribution of (b) Ca, (c) O and (d) Ti elements.

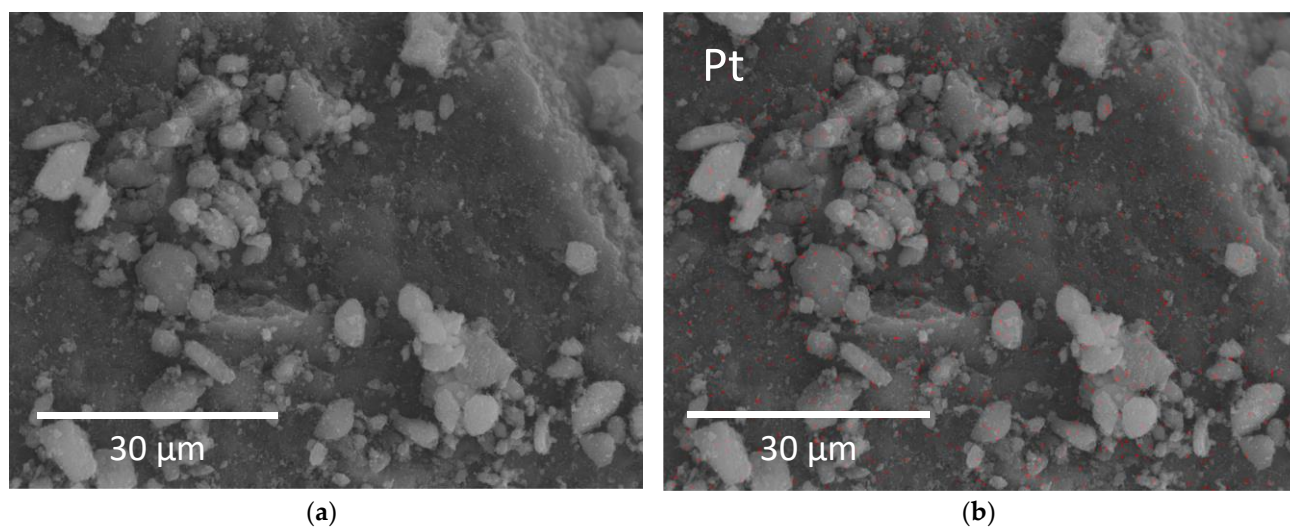


Figure S3. (a) SEM image of the $\text{Pt}/\text{TiO}_2(\text{Ca})$ catalyst and (b) EDS mapping results showing the distribution of Pt element.

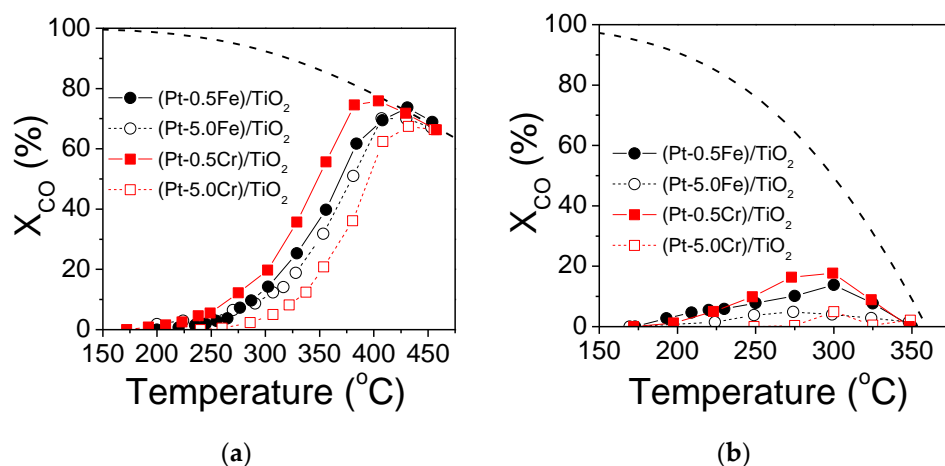


Figure S4. Effects of the metal content on the performance of bimetallic (0.5%Pt- x %M)/TiO₂ catalysts ($x=0.5$ or 5.0; M=Fe or Cr) under (A) HTS and (B) LTS conditions. Experimental conditions same as in Figure 3.

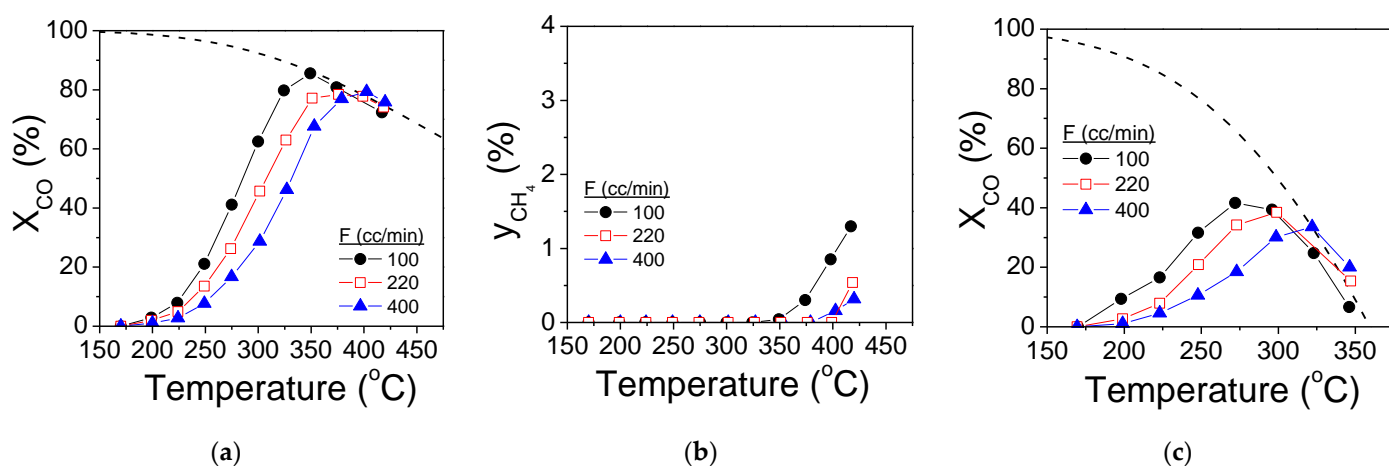


Figure S5. Effects of total flow rate on the performance of Pt/TiO₂(Ca) catalysts coated on the channels of the ceramic monolith: (A) Conversion of CO and (B) yield of CH₄ under HTS conditions. (C) Conversion of CO under LTS conditions. Other experimental conditions same as in Figure 5.

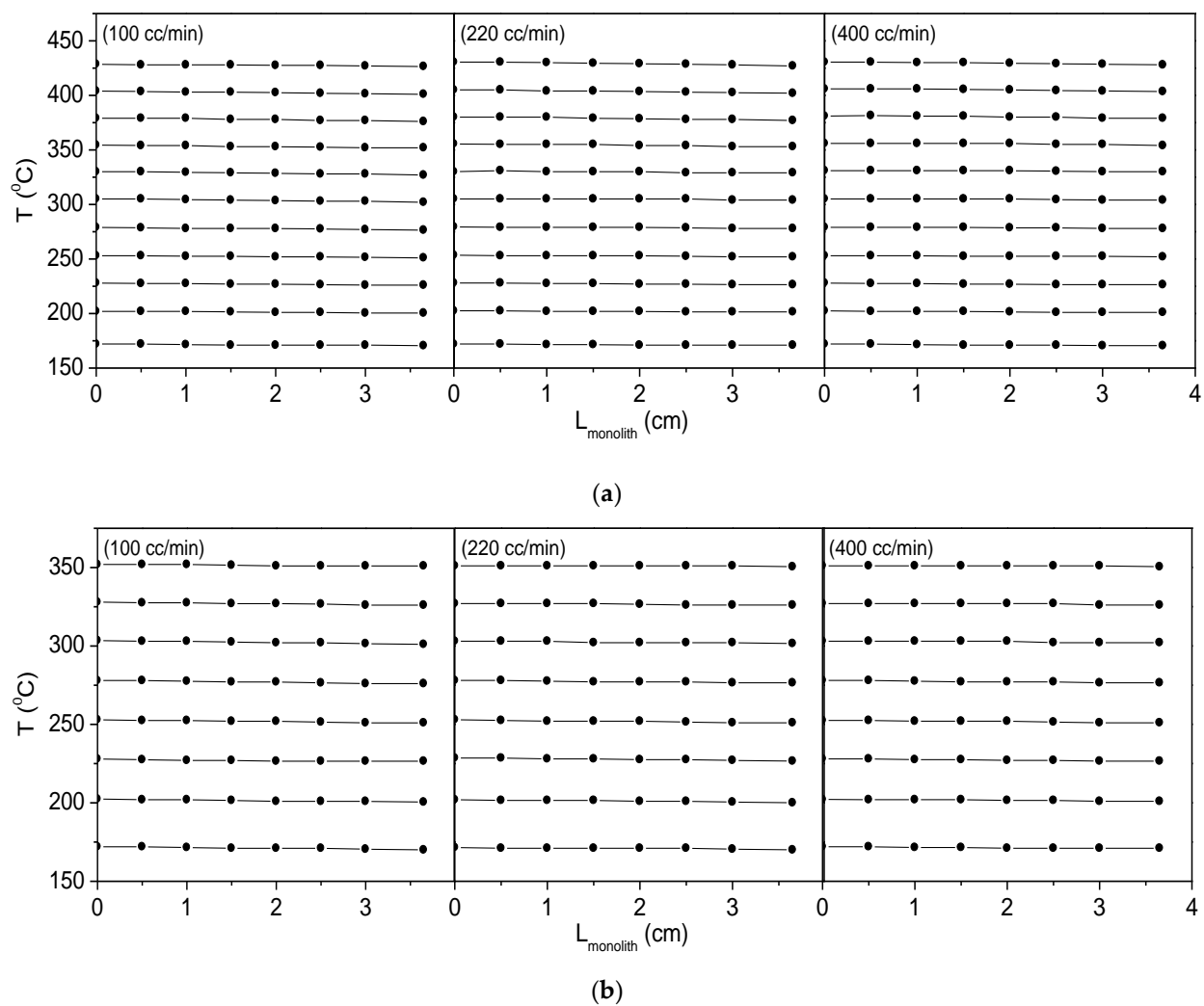
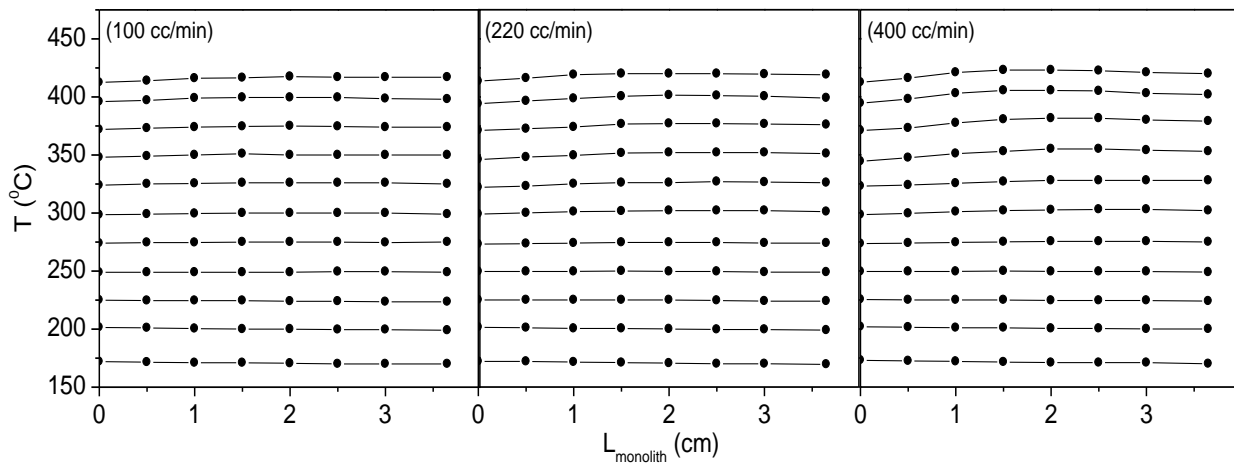
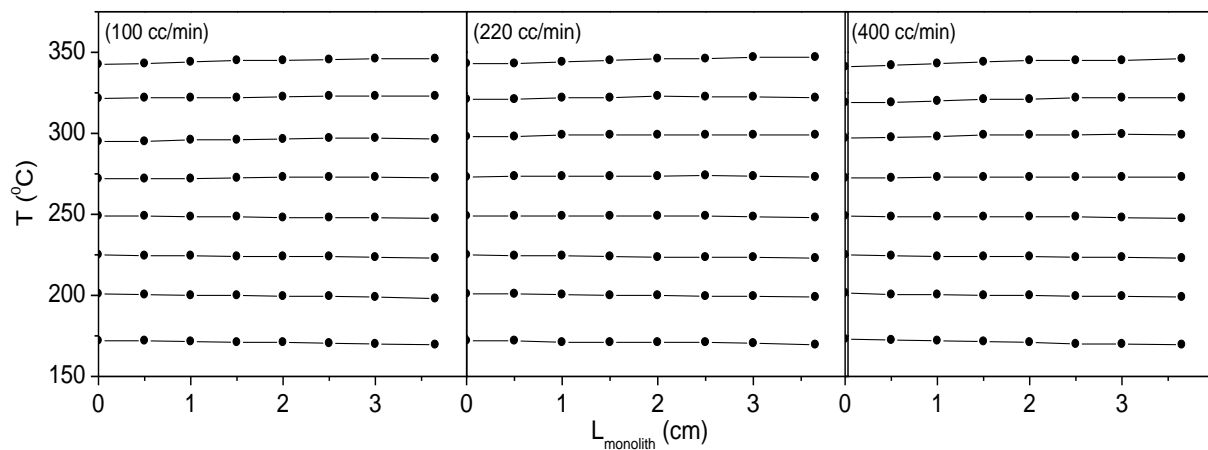


Figure S6. Temperature profile along the Pt/TiO₂(Ca)-coated metallic monolith (inlet at $L=0$) at the indicated total flow rates under the (a) HTS and (b) LTS reaction conditions shown in Figure 6.



(a)



(b)

Figure S7. Temperature profile along the Pt/TiO₂(Ca)-coated ceramic monolith (inlet at $L=0$) at the indicated total flow rates under the (a) HTS and (b) LTS reaction conditions shown in Figure 6.