

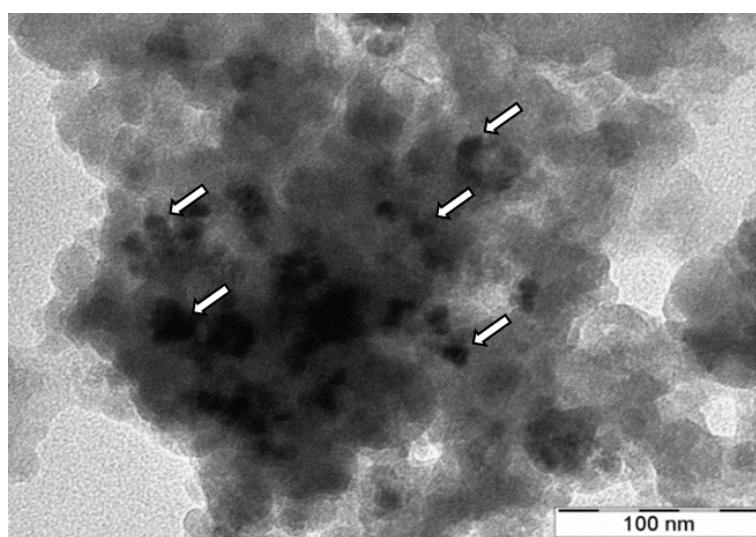
Supporting Information

# Reaction Pathways of Gamma-Valerolactone Hydroconversion over Co/SiO<sub>2</sub> Catalyst

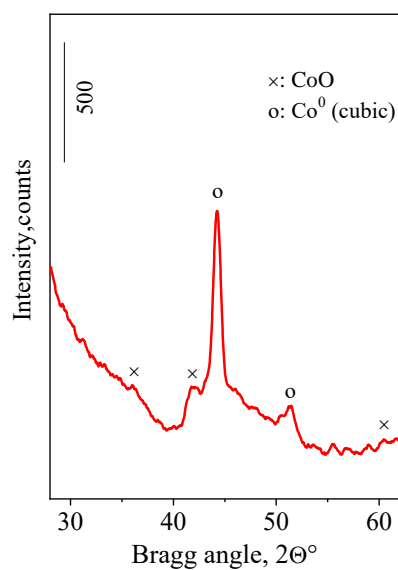
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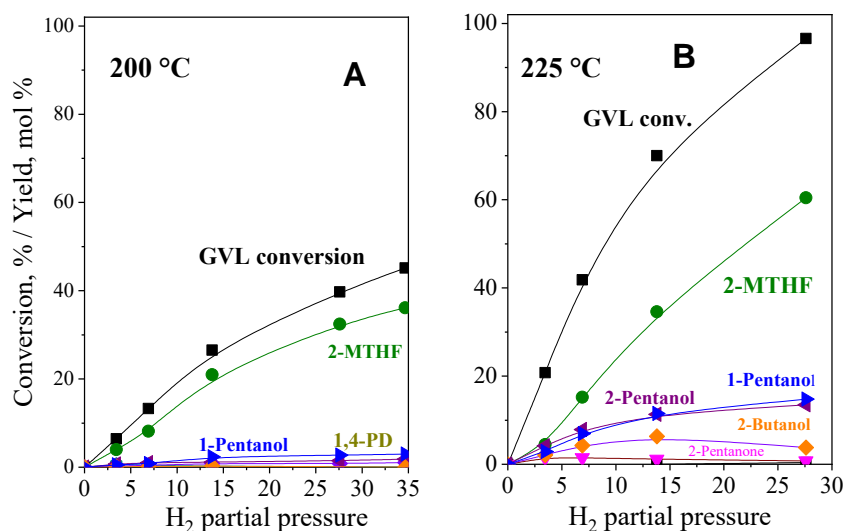


**Figure S1.** TEM image of the reduced Co/SiO<sub>2</sub> catalyst.



**Figure S2.** XRPD pattern of the used Co/SiO<sub>2</sub> catalyst. Sample was used in the hydroconversion of GVL to 2-MTHF for 58 h time-on-stream. Reaction conditions during the catalytic run were 225 °C, 30 bar, and space time of 1 g<sub>cat</sub>·g<sub>GVL</sub><sup>-1</sup>·h<sup>-1</sup>.

The TEM image of the Co/SiO<sub>2</sub> catalyst reduced in H<sub>2</sub> at 450 °C (Fig. S1) presents relatively homogeneously distributed spherical Co particles and agglomerates with a mean diameter of 20–30 nm.



**Figure S3.** GVL hydroconversion and product yields over Co/SiO<sub>2</sub> catalysts as a function of H<sub>2</sub> partial pressure at 200 °C (A) and 225 °C (B) and 1 g<sub>cat</sub>·g<sub>GVL</sub><sup>-1</sup>·h space time. The partial pressure of GVL was kept constant at 2.3 bar. 2-MTHF: 2-methyltetrahydrofuran; 1,4-PD: 1,4-pentanediol.

To adjust the H<sub>2</sub> partial pressure (Fig. S3) the flow rate of H<sub>2</sub> was changed, whereas the partial pressure of the GVL reactant was kept at 2.3 bar by simultaneously adjusting the total pressure. The conversion of GVL and the yield of the main products seem to reach the highest level at an H<sub>2</sub> partial pressure of 27.7 bar and H<sub>2</sub>/GVL molar ratio of 12. Under these reaction conditions the coverage of the catalyst surface by activated GVL and H<sub>2</sub> is considered to be well balanced for attaining the highest rate of the reaction.

**Table S1.** GVL conversion over SiO<sub>2</sub> support at different reaction temperatures.

Support	Temperature, °C	Conversion, %	Yield (mol %)		
			PE	PA	Others
SiO <sub>2</sub>	225	-	-	-	-
	250	0.6	-	-	0.6
	275	1.4	0.7	-	0.7
	300	1.7	0.7	0.2	0.8

The support was activated at 450 °C in He flow for 2 hours. Reaction conditions: 1 g<sub>cat</sub>·g<sub>GVL</sub><sup>-1</sup>·h space time, 30 bar total pressure, H<sub>2</sub>/GVL molar ratio of 12, time-on-stream 3 h. PE: pentenoic acid, PA: pentanoic acid.

The neat SiO<sub>2</sub> support material show negligible catalytic activity in the conversion of GVL.

**Table S2.** Weisz-Prater criterion and Thiele modulus <sup>a</sup> for the HDO reaction of GVL on Co/SiO<sub>2</sub> at 2.3 bar GVL partial pressure and 225 °C at increasing contact times.

<b>Contact time, h</b>	<b>-r'<sub>GVL(obs.)</sub> mol·g<sup>-1</sup>·s<sup>-1</sup></b>	<b>C<sub>WP</sub></b>	<b>ϕ</b>
0.10	7.5E-8	8.0E-5	0.009
0.25	4.5E-7	4.8E-4	0.022
0.50	1.3E-6	1.4E-3	0.037
1.00	2.8E-6	2.9E-3	0.054

<sup>a</sup> See Ref. [40] and [41] in the main text.

The low C<sub>WP</sub> values (<<0.3) and Thiele modulus values (ϕ<<3) clearly indicate the absence of diffusion limitations for the particle size range used in the present study (0.315-0.63 mm) under the applied reaction conditions.