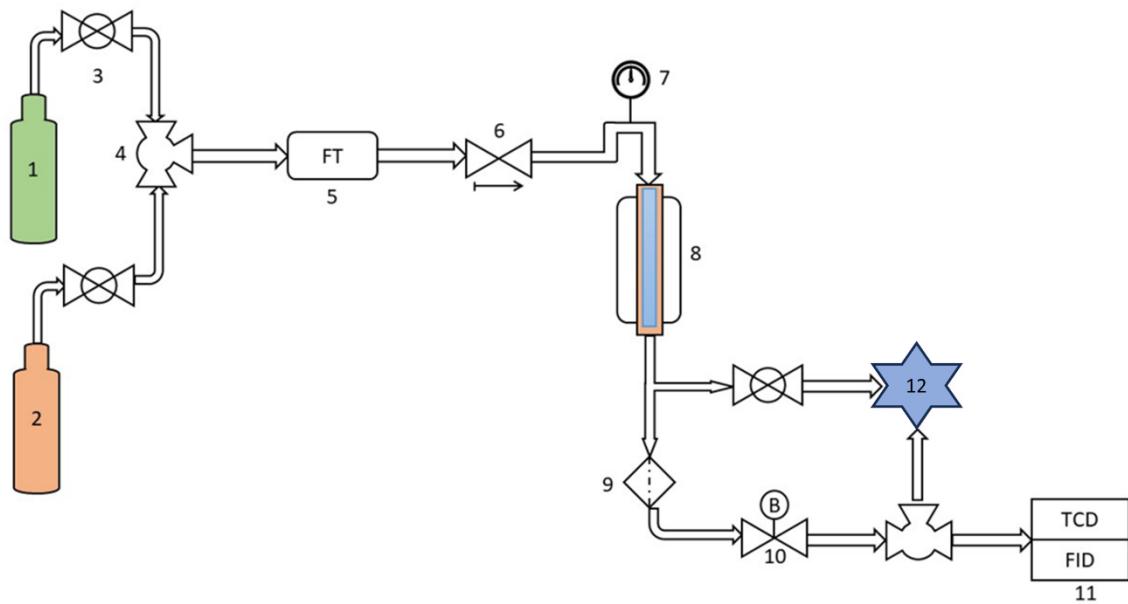


## Supplementary Material



1.Reduction gas bottle 2.Raw gas bottles 3.Two way valve 4.Three way valve 5.Mass flow meter 6.Check valve  
7.Pressure gauge 8.Fixed bed reactor 9.Filter 10.Back pressure valve 11.Gas chromatograph 12.Venting valve

**Figure S1.** Schematic diagram of the reaction apparatus for CO<sub>2</sub> hydrogenation to methanol.

**Table S1.** Peak area parameters of the different Cu-ZnO-ZrO<sub>2</sub> catalysts.

Catalyst	$A_{\beta}/(\text{a.u.})$	$A_{\gamma}/(\text{a.u.})$
CZZ-1	17753	9504
CZZ-3	18965	9529
CZZ-6	27823	10977
CZZ-12	12111	18753

**Table S2.** XPS parameters of the different Cu-ZnO-ZrO<sub>2</sub> catalysts.

Catalyst	BE (eV)			Relative metal content (at%)		
	Cu2p <sub>3/2</sub>	Zn2p <sub>3/2</sub>	Zr3d <sub>5/2</sub>	Cu	Zn	Zr
CZZ-1	calcined	933.1	1021.4	29.5	41.5	29.0
	reduced	932.0	1021.4	31.9	38.8	29.3
CZZ-3	calcined	933.2	1021.3	181.8	29.5	20.3
	reduced	931.7	1021.3	181.9	28.5	50.2
CZZ-6	calcined	933.1	1021.3	181.8	24.9	21.2
	reduced	931.7	1021.3	181.9	23.3	53.9
CZZ-12	calcined	933.2	1021.5	181.8	20.0	46.7
	reduced	931.9	1021.3	181.7	21.7	33.3

**Table S3.** Comparison of the activity of Cu-Zn-Zr catalysts.

Composition	Preparation method	Reaction conditions	Catalytic performance	Ref.
Cu/Zn/Zr = 6:3:1 molar ratio	co-precipitation	T = 250 °C, H <sub>2</sub> /CO <sub>2</sub> = 3 (v/v), P = 5 MPa, GHSV = 4600 h <sup>-1</sup>	CO <sub>2</sub> conv. = 21.0%, S <sub>MeOH</sub> = 59.4%, Y <sub>MeOH</sub> = 12.5 %	[12]
Cu/Zn/Zr = 5:2:3 molar ratio	combustion	T = 240 °C, H <sub>2</sub> /CO <sub>2</sub> = 3 (v/v), P = 3 MPa, GHSV = 3600 h <sup>-1</sup>	CO <sub>2</sub> conv. = 12.0%, S <sub>MeOH</sub> = 71.1%, Y <sub>MeOH</sub> = 8.5%	[21]
Cu/Zn/Zr = 6:3:1 molar ratio	complexation by citric acid	T = 240 °C, H <sub>2</sub> /CO <sub>2</sub> = 3 (v/v), P = 3 MPa, GHSV = 10000 mL·g <sub>cat</sub> <sup>-1</sup> ·h <sup>-1</sup>	CO <sub>2</sub> conv. = 12.5%, S <sub>MeOH</sub> = 51.8%, Y <sub>MeOH</sub> = 6.5%	[11]
Cu/ZnO/ZrO <sub>2</sub>	co-precipitation	T = 250 °C, H <sub>2</sub> /CO <sub>2</sub> = 3	CO <sub>2</sub> conv. = 19.4%, S <sub>MeOH</sub>	[46]

50/40/10 wt%		(v/v), P = 3 MPa, GHSV = 3000 h <sup>-1</sup>	= 29.3%, S <sub>MeOH</sub> = 5.7%	
Cu/Zn/Zr = 6:3:1 molar ratio	oxalate-gel coprecipitation	T = 200 °C, H <sub>2</sub> /CO <sub>2</sub> = 4 (v/v), P = 3 MPa,, WHSV = 48,000 cm <sup>3</sup> h <sup>-1</sup> g <sub>cat</sub> <sup>-1</sup> .	CO <sub>2</sub> conv. = 4.5%, S <sub>MeOH</sub> = 85.0%, Y <sub>MeOH</sub> = 3.8%	[47]
Cu/Zn/Zr = 4:3:3 molar ratio	reverse co- precipitation	T=240 °C, H <sub>2</sub> /CO <sub>2</sub> =3, P = 2 MPa, GHSV=14400 mLg <sub>cat</sub> <sup>-1</sup> h <sup>-1</sup>	CO <sub>2</sub> conv. = 13.2%, S <sub>MeOH</sub> = 32.3%, Y <sub>MeOH</sub> = 4.3%	[7]
CuO/ZnO/ZrO <sub>2</sub> = 37.5/41/21.5 wt%	micro-fluidic continuous coprecipitation	T = 240 °C, H <sub>2</sub> /CO <sub>2</sub> = 3.89 (v/v), P = 50 bar, GHSV = 10000 h <sup>-1</sup>	CO <sub>2</sub> conv. = 9.3%, S <sub>MeOH</sub> = 47.0%, Y <sub>MeOH</sub> = 4.4%	[48]
Cu/Zn/Zr = 6:3:1 molar ratio	co-precipitation	T = 240 °C, H <sub>2</sub> /CO <sub>2</sub> = 3 (v/v), P = 3 MPa, GHSV = 10000 mL·g <sub>cat</sub> <sup>-1</sup> ·h <sup>-1</sup>	CO <sub>2</sub> conv. = 16.0%, S <sub>MeOH</sub> = 48.7%, Y <sub>MeOH</sub> = 7.8%	[11]
CuO/ZnO/ZrO <sub>2</sub> = 15.1/41.8/43.1 wt%	reverse co- precipitation	T = 240 °C, H <sub>2</sub> /CO <sub>2</sub> = 3 (v/v), P = 3 MPa, GHSV = 4400 mL·g <sub>cat</sub> <sup>-1</sup> ·h <sup>-1</sup>	CO <sub>2</sub> conv. = 17.5%, S <sub>MeOH</sub> = 48.4%, Y <sub>MeOH</sub> = 8.5%	[49]
Cu/Zn/Zr = 6:3:1 molar ratio	reverse co- precipitation	T = 260 °C, H <sub>2</sub> /CO <sub>2</sub> = 3 (v/v), P = 4 MPa, WHSV = 5400 mL·g <sub>cat</sub> <sup>-1</sup> ·h <sup>-1</sup>	CO <sub>2</sub> conv. = 22.0%, S <sub>MeOH</sub> = 30.0%, Y <sub>MeOH</sub> = 6.6%	[50]
Cu/Zn/Zr = 45:45:10 molar ratio	gel-oxalate coprecipitation	T = 240 °C, H <sub>2</sub> /CO <sub>2</sub> = 3 (v/v), P = 2 MPa, GHSV = 3600 h <sup>-1</sup>	CO <sub>2</sub> conv. = 18.5%, S <sub>MeOH</sub> = 38.4%, Y <sub>MeOH</sub> = 7.1%	[51]
Cu/Zn/Zr = 6:3:1 molar ratio	gel-oxalate coprecipitation	T = 240 °C, H <sub>2</sub> /CO <sub>2</sub> = 3 (v/v), P = 3 MPa, GHSV = 10000 mL·g <sub>cat</sub> <sup>-1</sup> ·h <sup>-1</sup>	CO <sub>2</sub> conv. = 18.0%, S <sub>MeOH</sub> = 51.2%, Y <sub>MeOH</sub> = 9.2%	[11]
Cu/Zn/Zr = 5:2:3 molar ratio	CTAB assisted co-precipitation	T = 240 °C, CO <sub>2</sub> :H <sub>2</sub> = 1:3 (v/v), P = 3.0 MPa, GHSV = 3600 h <sup>-1</sup>	CO <sub>2</sub> conv. = 12.1%, S <sub>MeOH</sub> = 54.1%, Y <sub>MeOH</sub> = 6.5%	[52]
Cu/Zn/Zr = 30/15/55 wt%	P123 assisted co-precipitation	T = 250 °C, CO <sub>2</sub> :H <sub>2</sub> = 1:3 (v/v), P = 3.0 MPa, GHSV = 6000 mL·g <sub>cat</sub> <sup>-1</sup> ·h <sup>-1</sup>	CO <sub>2</sub> conv. = 23.0%, S <sub>MeOH</sub> = 34.0%, Y <sub>MeOH</sub> = 7.8%	[53]
Cu/Zn/Zr = 5:2:3 molar ratio	microwave assisted	T = 240 °C, CO <sub>2</sub> :H <sub>2</sub> = 1:3 (v/v), P = 3.0 MPa, GHSV =	CO <sub>2</sub> conv. = 17.4%, S <sub>MeOH</sub> = 37.5%, Y <sub>MeOH</sub> = 6.5%	[24]

	hydrothermal	2400 mL·g <sub>cat</sub> <sup>-1</sup> ·h <sup>-1</sup>		
Cu/Zn/Zr = 5:2:3 molar ratio	polymeric precursor	T = 240 °C, CO <sub>2</sub> :H <sub>2</sub> = 1:3 (v/v), P = 3.0 MPa, GHSV = 2400 mL·g <sub>cat</sub> <sup>-1</sup> ·h <sup>-1</sup>	CO <sub>2</sub> conv. = 16.8%, S <sub>MeOH</sub> = 41.4%, Y <sub>MeOH</sub> = 7.0%	[15]
Cu/Zn/Zr = 4:5:1 molar ratio	solid-state	T = 240 °C, H <sub>2</sub> /CO <sub>2</sub> = 3 (v/v), P = 3 MPa, GHSV = 7000 h <sup>-1</sup>	CO <sub>2</sub> conv. = 11.9%, S <sub>MeOH</sub> = 93.5%, Y <sub>MeOH</sub> = 11.1%	[54]
Cu/Zn/Zr = 5:2:3 molar ratio	solvothermal	T = 240 °C, CO <sub>2</sub> :H <sub>2</sub> = 1:3 (v/v), P = 3.0 MPa, GHSV = 2400 mL·g <sub>cat</sub> <sup>-1</sup> ·h <sup>-1</sup>	CO <sub>2</sub> conv. = 15.6%, S <sub>MeOH</sub> = 46.1%, Y <sub>MeOH</sub> = 7.2%	this work