

Supplementary information

Table S1. Nickel catalysts reported for CO₂ hydrogenation at atmospheric pressure.

Catalyst	Molar ratio H ₂ :CO ₂ :N ₂ *	Temp. °C	GHSV	x _{CO2} %	S _{CH4} %	Ref.
5%Ni/SiO ₂	4:1:1.1	350	11,000 h ⁻¹	38	90.0	[2]
5%Ni/CZ _{imp}	4:1:1.1	350	43,000 h ⁻¹	60	97.3	
5%Ni/CZ _{sol-gel}	4:1:1.1	350	43,000 h ⁻¹	80	90.0	
5%NiUSY _{imp}	4:1:1.1	400	43,000 h ⁻¹	24.7	61.4	[3]
4%Ni3%CeUSY _{imp}	4:1:1.1	400	43,000 h ⁻¹	37.7	72.1	
4%Ni7%CeUSY _{imp}	4:1:1.1	400	43,000 h ⁻¹	44.3	75.5	
5%Ni15%CeUSY _{imp}	4:1:1.1	400	43,000 h ⁻¹	55.0	86.2	
10%NiUSY _{imp}	4:1:1.1	400	43,000 h ⁻¹	47.9	78.8	
8%Ni7%CeUSY _{imp}	4:1:1.1	400	43,000 h ⁻¹	51.7	85.6	
14%NiUSY _{imp}	4:1:1.1	400	43,000 h ⁻¹	65.5	94.2	
14%Ni7%CeUSY _{imp}	4:1:1.1	400	43,000 h ⁻¹	68.3	95.1	
5%Ni/80Ce ₂₀ Zr	4:1:1.1	350	43,000 h ⁻¹	71.5	98.5	[5]
5%Ni/60Ce ₄₀ Zr	4:1:1.1	350	43,000 h ⁻¹	79.7	99.3	
5%Ni/20Ce ₈₀ Zr	4:1:1.1	350	43,000 h ⁻¹	73.0	99.0	
(5%Ni-0.5%Rh)/ 80Ce ₂₀ Zr	4:1:1.1	350	43,000 h ⁻¹	77.8	99.2	
15%Ni/Al ₂ O ₃	4:1:0	350	15,000 ml g ⁻¹ h ⁻¹	45.0	100.0	[6]
15%Ni-0.3%CeO ₂ /Al ₂ O ₃	4:1:0	350	15,000 ml g ⁻¹ h ⁻¹	55.0	98.0	
15%Ni-0.5%CeO ₂ /Al ₂ O ₃	4:1:0	350	15,000 ml g ⁻¹ h ⁻¹	65.0	99.0	
15%Ni-2%CeO ₂ /Al ₂ O ₃	4:1:0	350	15,000 ml g ⁻¹ h ⁻¹	71.0	100.0	
15%Ni-4%CeO ₂ /Al ₂ O ₃	4:1:0	350	15,000 ml g ⁻¹ h ⁻¹	73.0	98.0	
15%Ni-6%CeO ₂ /Al ₂ O ₃	4:1:0	350	15,000 ml g ⁻¹ h ⁻¹	67.0	97.0	
15%Ni/SiC	4:1:0	360	12,000 h ⁻¹	79	99.6	[7]
15%Ni-5%La/SiC	4:1:0	360	12,000 h ⁻¹	85	99.6	
5%Ni/MOF-5	4:1:0	280	2,000 h ⁻¹	16.5	---	[8]
7.5%Ni/MOF-5	4:1:0	280	2,000 h ⁻¹	20.0	---	
10%Ni/MOF-5	4:1:0	280	2,000 h ⁻¹	47.2	---	
12.5%Ni/MOF-5	4:1:0	280	2,000 h ⁻¹	45.1	---	
10%Ni/MOF-5	4:1:0	360	2,000 h ⁻¹	75.1	100	
5%Ni/ Ce _{0.72} Zr _{0.28} O ₂	4:1:1.1	350	43,000 h ⁻¹	71.5	98.5	[9]
10%Ni/ Ce _{0.72} Zr _{0.28} O ₂	4:1:1.1	350	43,000 h ⁻¹	83.4	99.7	
15%Ni/ Ce _{0.72} Zr _{0.28} O ₂	4:1:1.1	350	43,000 h ⁻¹	80.3	99.5	

Catalyst	Molar ratio H ₂ :CO ₂ :N ₂ *	Temp. °C	GHSV	x _{CO2} %	S _{CH4} %	Ref.
LaNiO ₃ (Act 400°C)	4:1:0	300	7,500 ml g ⁻¹ h ⁻¹	55.4	98.7	
LaNiO ₃ (Act 500°C)	4:1:0	300	7,500 ml g ⁻¹ h ⁻¹	77.7	99.4	
LaNiO ₃ (Act 600°C)	4:1:0	300	7,500 ml g ⁻¹ h ⁻¹	71.7	99.3	[10]
LaNiO ₃ (Act 700°C)	4:1:0	300	7,500 ml g ⁻¹ h ⁻¹	59.7	99.2	
5%Ni/La ₂ O ₃ CO ₃	4:1:0	300	7,500 ml g ⁻¹ h ⁻¹	40.3	88.9	
23%Ni/CaO-Al ₂ O ₃	4:1:3.3	400	15,000 h ⁻¹	81	98	[11]
10%Ni/CeO ₂	4:1:0	350	10,000 h ⁻¹	92	100	
10%Ni/MgO	4:1:0	450	10,000 h ⁻¹	69	97	
10%Ni/TiO ₂	4:1:0	450	10,000 h ⁻¹	78	98	[12]
10%Ni/Al ₂ O ₃	4:1:0	450	10,000 h ⁻¹	81	99	
(10%Ni-0.1%Ru)/SiC	4:1:1.1	400	10,000 h ⁻¹	76.2	98.4	
(10%Ni-0.1%Ru)/Ce ₂ Zr ₂ O ₈	4:1:1.1	400	10,000 h ⁻¹	82.2	99.3	
(10%Ni-0.1%Ru)/SiC _{foam}	4:1:1.1	400	10,000 h ⁻¹	69.9	93.9	
(2.5%Ni-0.025%Ru)/SiC _{foam}	4:1:1.1	400	10,000 h ⁻¹	37.5	76.6	
(2.5%Ni-0.025%Ru)/ (15%CNF-SiC _{foam})	4:1:1.1	400	10,000 h ⁻¹	48.6	86.5	
(2.5%Ni-0.025%Ru)/ (1%Ce ₂ Zr ₂ O ₈ -SiC _{foam})	4:1:1.1	400	10,000 h ⁻¹	46.4	92.3	[13]
(2.5%Ni-0.025%Ru)/ (27%Ce ₂ Zr ₂ O ₈ -SiC _{foam})	4:1:1.1	400	10,000 h ⁻¹	59.8	96.4	
(2.5%Ni-0.025%Ru)/ (1%Ce ₂ Zr ₂ O ₈ -15%CNF-SiC _{foam})	4:1:1.1	400	10,000 h ⁻¹	65.1	96.2	
Ni(100)/Al ₂ O ₃	4:1:0	400	500 mL g ⁻¹ h ⁻¹	17.8	---	
Mn/Ni(40:60)/ Al ₂ O ₃	4:1:0	400	500 mL g ⁻¹ h ⁻¹	20.1	---	
Mn/Ni(20:80)/ Al ₂ O ₃	4:1:0	400	500 mLg ⁻¹ h ⁻¹	21.3	---	
Pd/Mn/Ni(5:35:60)/Al ₂ O ₃	4:1:0	400	500 mL g ⁻¹ h ⁻¹	21.0	---	
Ru/Mn/Ni(5:35:60)/Al ₂ O ₃	4:1:0	400	500 mL g ⁻¹ h ⁻¹	99.7	72.36	[14]
Pd/Mn/Ni(5:15:80)/ Al ₂ O ₃	4:1:0	400	500 mL g ⁻¹ h ⁻¹	13.0	---	
Ru/Mn/Ni(5:15:80)/ Al ₂ O ₃	4:1:0	400	500 mL g ⁻¹ h ⁻¹	51.0	---	
5%Ni/Zr/CNT-SEQ	5:1:94	400	75,000 mL g ⁻¹ h ⁻¹	55	98	
5%Ni/CNT	5:1:94	450	75,000 mL g ⁻¹ h ⁻¹	48	30	[17]
5%Ni/Zr/CNT-COI	5:1:94	500	75,000 mL g ⁻¹ h ⁻¹	47	12	
15%Ni/ZrO ₂	4:1:0.55	300	48,000 mL g ⁻¹ h ⁻¹	60	98	[18]
40Ni-Ce _{0.9} Zr _{0.1} O	4:1:0	275	3,000 mL g ⁻¹ h ⁻¹	98	100	[19]
15%Ni/ZrO ₂ -O	4:1:0.55	400	50,000 mL g ⁻¹ h ⁻¹	80	100	
15%Ni/ZrO ₂	4:1:0.55	400	50,000 mL g ⁻¹ h ⁻¹	75	100	[20]

Catalyst	Molar ratio H ₂ :CO ₂ :N ₂ *	Temp. °C	GHSV	x _{CO2} %	S _{CH4} %	Ref.
20%Ni/ZrO ₂ -COP	4:1:5	400	126,000 mL g ⁻¹ h ⁻¹	55	100	This work
20%Ni/ZrO ₂ -COP	4:1:5	400	43,500 mL g ⁻¹ h ⁻¹	50	100	This work

* Molar ratio for H₂ and N₂ are calculated on CO₂ mole basis.

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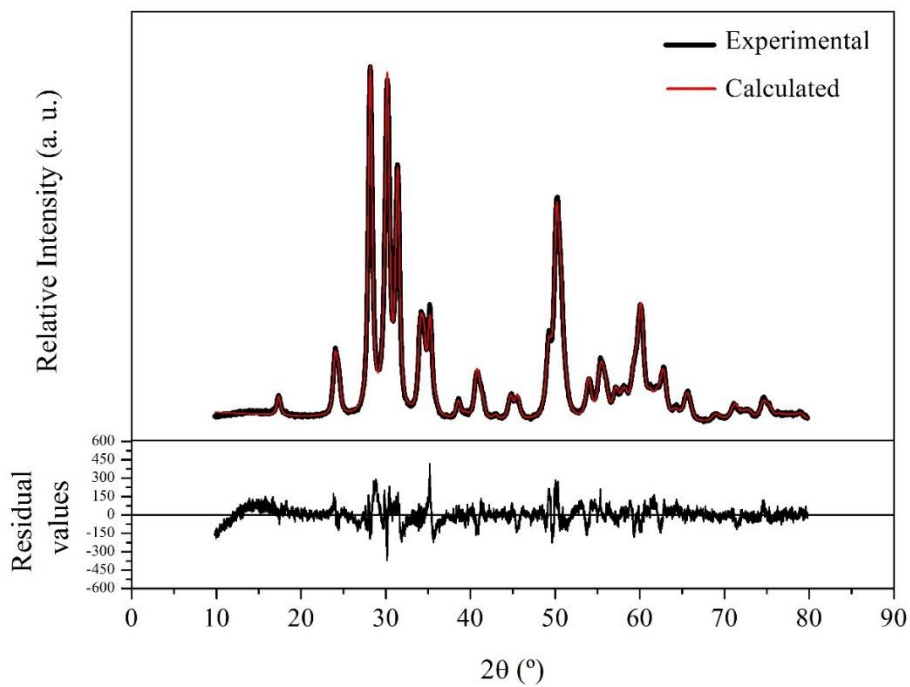


Figure S1. Rietveld simulation for the sol-gel ZrO₂ support.

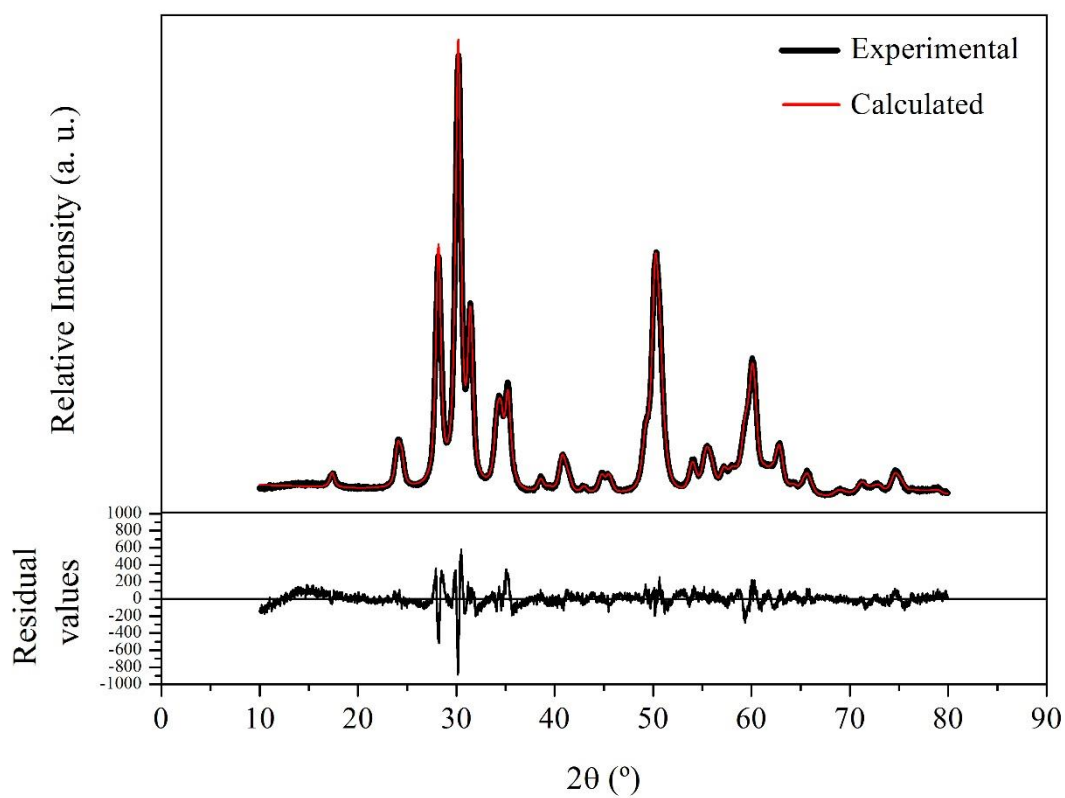


Figure S2. Rietveld simulation for the co-precipitation ZrO₂ support.

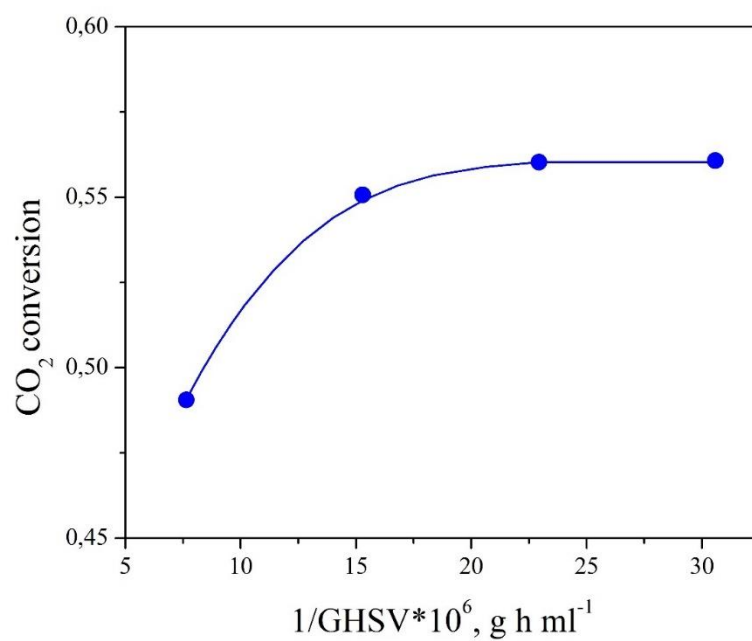


Figure S3. Effect on GHSV on CO₂ conversion with the 20%Ni/ZrO₂-COP catalyst. Reaction conditions: 400 °C, 0.1 MPa.

20%Ni/ZrO₂-COP (Fresh)

20%Ni/ZrO₂-COP (Spent)

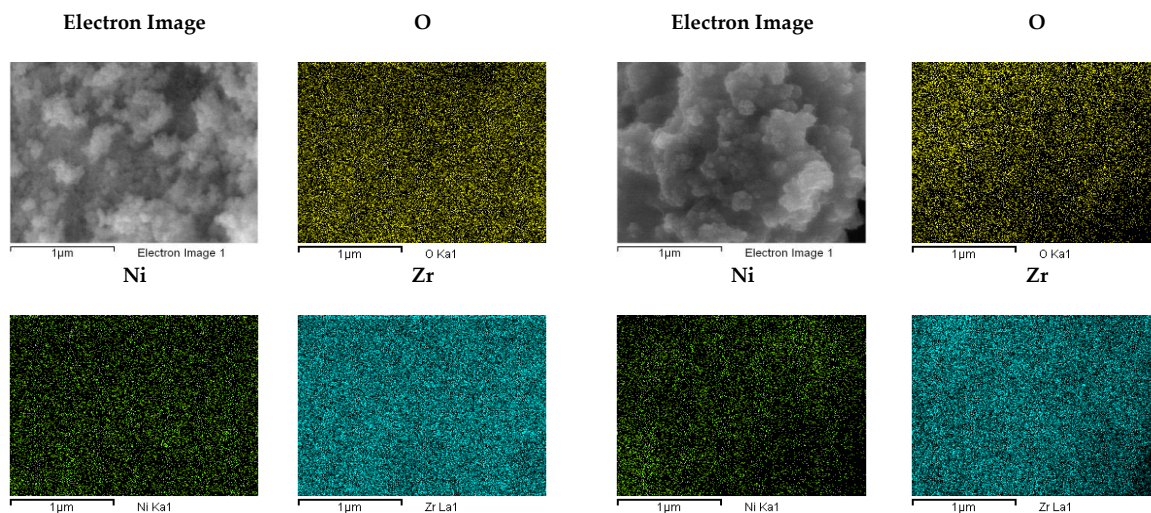


Figure S4. SEM images of 20%Ni/ZrO₂-COP catalysts.

Table S2. SEM microanalysis.

wt%	Catalyst	
	20%Ni/ZrO ₂ -COP-F	20%Ni/ZrO ₂ -COP-S
O	28.6	28.1
Ni	18.4	20.2
Zr	53.0	51.6

Catalyst dispersion calculations**Table S3.** Peak areas of the hydrogen chemisorption analysis.

Injection #	Peak Area	Peak Area
	20%Ni/ZrO ₂ -COP Fresh catalyst <i>m</i> =0.052 g	20%Ni/ZrO ₂ -COP Spent catalyst <i>m</i> =0.012 g
1	7.34	144.62
2	17.74	154.02
3	28.40	154.15
4	41.00	157.43
5	59.08	158.50
6	80.74	160.49
7	112.86	162.19
8	114.92	166.47
9	113.47	161.75
10	121.85	161.90
11	121.40	163.67
12	125.05	165.25
13	129.51	165.54
14	131.09	164.49
15	132.01	167.61

$$\%D = \left[n \left(\frac{V_{ads}}{V_g} \right) \left(\frac{MW}{M} \right) 100 \right] 100$$

$\%D$ = metal dispersion, %.

n = stoichiometry factor = 2

V_{ads} = volume of the active gas adsorbed, cm³/g

V_g = molar volume gas at STP = 22414 cm³/mol

MW = molecular weight of nickel = 58.693 g/mol

M = % of metal loading = 20%

$$V_{ads}(STP) = \frac{V_{inj}}{m} \sum_{i=1}^n \left(1 - \frac{A_i}{A_f} \right)$$

m = mass of the sample, g

A_i = Area of the peak i

A_f = area of the last peak

$$V_{inj}(STP) = V_{loop} \left(\frac{T_{std}}{T_{room}} \right) \left(\frac{P_{room}}{P_{std}} \right) \left(\frac{A}{100} \right)$$

V_{inj} = Volume of the active gas injected, cm³

V_{loop} = Volume of the loop, cm³

T_{room} = room temperature, K

P_{room} = room pressure, mmHg

T_{std} = standard temperature = 273.15 K

P_{std} = standard pressure = 760 mmHg

A = % of active gas in the gas-mixture