



# *Article* **Effect of Synthetic Quadripolymer on Rheological and Filtration Properties of Bentonite-Free Drilling Fluid at High Temperature**

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**Abstract:** High temperature would dramatically worsen rheological behaviors and increase filtration loss volumes of drilling fluids. Synthetic polymers with high temperature stability have attracted more and more attention. In this paper, a novel quadripolymer was synthesized using 2-acrylamido-2-methylpropanesulfonic acid (AMPS), acrylamide (AM), sodium styrene sulfonate (SSS), and dimethyl diallyl ammonium chloride (DMDAAC). Firstly, the molecular structure was studied by Fourier transform–infrared spectroscope (FT-IR) and nuclear magnetic resonance (<sup>1</sup>H-NMR) analysis. It was shown that the synthetic polymer contained all the designed functional groups. Moreover, the effect of temperature and the quadripolymer concentration on the rheological behavior and filtration loss of the bentonite-free drilling fluid were investigated. It was experimentally established that when the adding amount of the quadripolymer was 0.9 wt%, the prepared drilling fluid systems exhibited relatively stable viscosities, and the filtration losses could be controlled effectively after hot rolling aged within 180  $°C$ . Further, it was confirmed that the bentonite-free drilling fluid containing the synthesized quadripolymer had good reservoir protection performance. In conclusion, the synthetic quadripolymer is a promising rheology modifier and a filtrate reducer for the development of the bentonite-free drilling fluid at high temperature.

**Keywords:** synthetic polymer; high temperature; bentonite-free drilling fluid; rheology; filtration

## **1. Introduction**

Drilling fluid is indispensable in oil and gas drilling engineering to maintain wellbore stability, carry and transport drilled cuttings, and reduce water loss. It is divided into water-based drilling fluid system (WBDF), oil-based drilling fluid system (OBDF), and gas-based drilling fluid system (GBDF) [\[1\]](#page-11-0). Among them, a water-based working fluid is the most commonly used one because of its environmental friendliness and low cost, and it is mainly composed of bentonite clay and different functional polymer treating agents [\[2](#page-11-1)[–4\]](#page-12-0). Bentonite as the most essential component in drilling fluid exhibits incomparable advantages in viscosity and filtration loss control [\[5,](#page-12-1)[6\]](#page-12-2). Furthermore, clay particles can plug pores and fractures in the near wellbore area and form a thin and low-permeability filtration cake. However, as the number of deep and ultra-deep wells increases, one of the inevitable problems is that drilling fluid must endure high temperatures [\[7\]](#page-12-3). It is worth noting that high bentonite content of water-based drilling fluids at high temperatures would give rise to serious detrimental effects [\[8–](#page-12-4)[10\]](#page-12-5), for example, deterioration of rheological behavior, increase in filtration volume seeping into formation, particularly formation damages caused by dispersive clay particles. Thus, less or no bentonite in drilling fluids capable of providing necessary performance in harsh operating conditions should be contained to



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maintain the desired properties [\[11\]](#page-12-6). Xiao et al. prepared a bentonite-free drilling fluid with amphoteric polymer (FA367) as the main treating agent, and the filed application results in the shallow formations of Anpeng oilfield showed that the drilling speed greatly increased, and the complex conditions such as leakage and sticking were effectively alleviated [\[12\]](#page-12-7).

In order that a drilling fluid with low or no bentonite could be appropriate for deep well drilling project, one or more polymers are required to take place of bentonite and provide satisfactory performance, such as proper rheological parameters, low filtration loss volume, and good salt tolerance at high temperature conditions [\[13–](#page-12-8)[15\]](#page-12-9). However, one disadvantage of polymers is related to the thermal degradation at elevated temperatures (above 150 °C) [\[16](#page-12-10)[,17\]](#page-12-11), which gives rise to the rheology and filtration loss being difficult to meet the demands of field application. Thus, it is necessary to develop novel polymers with high temperature resistance to contribute to rheological stability and low filtration loss for bentonite-free drilling fluids.

Synthetic polymers have attracted researchers' attentions for a long time. Water soluble polymers are universally used in water based drilling fluids. The rheological behavior and filtrates of drilling fluid can be adjusted primarily by adding them However, with the increase of well depth, one disadvantage of natural polymer is related to the thermal degradation and oxidation under high temperature (150 ◦C) [\[18](#page-12-12)[,19\]](#page-12-13) which could not control the rheology and filtration loss to meet the demands of the field application. Thus, regarding these disadvantages of natural polymer, some researchers were directed to synthetic polymer that could contribute to rheological stability and low fluid loss in water based fluids at HTHP conditions. Perricone et al. used acrylamido-methylpropanesulfonic acid (AMPS), acrylamide (AM), and alkyl acrylamide monomers to synthesize a copolymer (named COP) through inverse micro-emulsion polymerizations [\[20\]](#page-12-14). In the field application, the drilling fluid with this synthetic product showed good high temperature resistance. Furthermore, Tao et al. (2011) synthesized a terpolymer of AM/acrylic acid/sodium styrene sulfonate (SSS) and evaluated its high temperature and high pressure rheological property with various salt concentrations [\[21\]](#page-12-15). Wu et al. synthesized AM/AMPS/itaconic acid (IA)/N-vinyl caprolactam (NVCap) by solution polymerization. It is reported that drilling fluid containing this terpolymer could control fluid loss and rheological properties after aging at 220 ◦C [\[22\]](#page-12-16). Some other synthetic polymers were developed and were used as rheology modifiers and filtrate reducers, which indicated that the sulfonate structure can be resistant to high temperature and salt [\[23–](#page-12-17)[25\]](#page-12-18). The excellent performance of the drilling fluid decides the formation protection and drilling efficiency in deep wells [\[26\]](#page-12-19).

In this paper, a new quadripolymer was synthesized with monomers of AMPS, AM, DMDAAC, and SSS by aqueous solution polymerization. Among these, amide group provided by AM monomer is mainly responsible for forming the main chain structure. The sulfonic acid group of AMPS plays a role of hydration, and the side group  $-(CH_3)_2CH_2SO_3Na$ can enhance the rigidity of the molecular chain, thus improving the thermal stability of the product. The rigid group of benzene ring contained in SSS monomer has a strong hindering effect [\[27](#page-12-20)[,28\]](#page-12-21). Then, two double bonds in the molecule of DMDAAC contribute to form mesh structure. Thus, such a quadripolymer was characterized with Fourier transform infrared spectroscopy and nuclear magnetic resonance. Firstly, the ability of the quadripolymer in adjusting rheological and filtration performance of bentonite-free fluids at elevated temperatures were studied by thermal aging test. Meanwhile, the salt tolerance of the bentonite-free drilling fluid was evaluated through an investigation of the viscosity change of the fluid system in different salinity of sodium chloride solution. Additionally, the reservoir protection performance of the bentonite-free drilling fluid containing the quadripolymer was evaluated experimentally.

## **2. Materials and Methods**

## *2.1. Materials and Experiment Instruments*

Acrylamide(AM), 2-acrylamido-2-methylpropanesulfonic acid (AMPS), dimethyl diallyl ammonium chloride(DMDAAC), sodium styrene sulfonate (SSS), chemical grade,

were purchased from Aladdin Reagent Co., Ltd. (Shanghai, China); Ammonium persulfate  $((NH_4)_2S_2O_8)$  and sodium hydrogen sulfite (NaHSO<sub>3</sub>), sodium hydroxide (NaOH), sodium carbonate (Na<sub>2</sub>CO<sub>3</sub>), analytical grade, were employed without further purification.

Drispac and HE150 were purchased from Chevron Phillips Chemical Company, Texas, America; 80A51, PAM, LOCKSEAL, PAC-LV and sized CaCO<sub>3</sub> were collected from Jiahua Technology Co., Ltd., Jingzhou City, China. The experiment instruments used for this study are listed in Table [1.](#page-2-0)

<span id="page-2-0"></span>**Table 1.** Experiment instruments and the providers.



## *2.2. Methods*

## 2.2.1. Synthesis of Quadripolymer

The quadripolymer of AM, AMPS, SSS, DMDAAC was synthesized by solution free radical polymerization. The effect of molar ratio of four monomers, dosage of initiator, pH and reaction temperature on optimizing the best synthesis condition was determined (AM: AMPS: SSS: DMDAAC is 10:3:3:2, redox initiator dosage( $(NH_4)_2S_2O_8$ ) is 0.2 wt%, temperature is 80  $\degree$ C and reactants system pH is 7) by dosage experiment.

Firstly, a desired amount of mixture monomers was mixed well in a reaction flask and deoxygenated with nitrogen. Secondly, sodium hydroxide was used to adjust the  $pH$  value ( $pH = 7$ ) of the reaction system. The whole reaction process took place in a constant temperature oil bath. Next, a redox initiator  $((NH_4)_2S_2O_8)$  dosage of 0.2 wt% was added into the above solution with a constant stirring speed of 200 r/min. After 5 h of reaction time, the white product was filtered off and extracted with acetone and methanol for three times, and finally dried powders were obtained.

## 2.2.2. Characterization of Molecular Structure

FT-IR spectrum of the quadripolymer was recorded on a Nicolet 6700 Fourier Transform Infrared Spectrometer. A pellet sample made from a mixture of 1 mg quadripolymer and about 100 mg of potassium bromide (KBr) was prepared under a pressure of 100 psi and tested in the optical range of 400–4000  $cm^{-1}$ .

 $1H$  NMR spectrum of the quadripolymer was measured by Angilent 400 MHz Nuclear magnetic resonance spectrometer. Mass of 10 mg of sample powder was dissolved into a test tube containing 0.65 mL D<sub>2</sub>O, and then transferred to a sample cavity. <sup>1</sup>H NMR spectrum measurement was carried out with controlled heating and cooling steps.

Thermal stability: The thermal stability of the quadripolymer was tested with HCT-1 Differential Thermobalance analyzer (Beijing Henven Instrument Plant, Beijing, China) in nitrogen gas atmosphere. The heating rate was  $10\degree C/min$ , and the temperature was in the range of  $30-600$  °C.

## 2.2.3. Sample Preparation

Base formula of bentonite-free drilling fluid (marked as formula1#) was prepared as follows: 1000 mL deionized water, 0.1 wt% NaOH, 0.15 wt%  $Na<sub>2</sub>CO<sub>3</sub>$ , desired amount of polymer (the quadripolymer or Drispac), 2 wt% PAC-LV, 2 wt% LOCK-SEAL, 4 wt% super-fine  $CaCO<sub>3</sub>$ , 0.5 wt% Na<sub>2</sub>SO<sub>3</sub> were weighted and added sequentially at high speed stirring for 20 min with a GJSS-B12K multi-spindle mixer, and then the solution was stood still for 24 h at room temperature for complete dissolution.

## 2.2.4. Drilling Fluid Performance Measurements

Rheological and filtration properties of bentonite-free drilling fluid were evaluated according to the American Petroleum Institute test program [\[29\]](#page-12-22), Formulas (1)–(3) were applied to calculate the rheological parameters, including apparent viscosity (*AV*), plastic viscosity (*PV*) and yield point (*YP*), for the fluid system. The readings at 600 rpm and 300 rpm obtained with a ZNN-D6 six-speed rotational viscometer were marked as Φ600 and Φ300, respectively. The initial and final gel strength were also measured and marked as *G*<sup>1</sup> and *G*2. Before thermal stability evaluation, the bentonite-free drilling fluid was required to be heated at a given temperature for 16 h with a XGRL-4A hot roller oven and then cooled to ambient temperature.

$$
AV (Appendiv is \text{cosity}) = \Phi 600/2, mPa·s,
$$
\n(1)

$$
PV (Plastic viscosity) = \Phi 600 - \Phi 300, mPa·s,
$$
\n(2)

$$
YP (Yield point) = 0.511(\Phi 300 - PV), Pa,
$$
\n(3)

$$
K = \frac{Q\mu l}{\Delta p A}.\tag{4}
$$

API filtration loss  $(FL_{\text{API}})$  was determined by a SD-4 API filtration apparatus with a pressure difference of 100 psi at ambient temperature for 30 min. HTHP filtration loss (*FL*HTHP) was measured with a GCS71-A HTHP filtration apparatus at 150 ◦C and 500 psi for 30 min. After the test, the filtrate was collected into the measuring cylinder and the volume was recorded.

HTHP rheology test: After placing the drilling fluid inside the rheometer, the sample was heated up to the desired temperature and meanwhile pre-shear at 100 s<sup> $-1$ </sup> was performed before rheological measurement. The pressure was adjusted to 500 psi and the shear stress was measured at the shear rate of 511  $\rm s^{-1}.$ 

Reservoir protection test: The core original kerogen permeability  $K_0$  was measured as follows, Formula (4), wherein, Q, flow rate;  $\mu$ , Kerosene viscosity; l, Core length;  $\Delta p$ , Differential pressure before and after flow through the core; A, core, end surface area.

In step 1, the core saturated with simulated groundwater is placed into the core holder and repelled with filtered and dewatered kerosene at 0.4 times the critical flow rate; subsequently, repelled at 0.8 times the critical flow rate until no water flows out and the pressure is stable. According to the above formula,  $K_0$  can be calculated.

In step 2, the core tested for  $K_0$  is quickly loaded into the core holder of JHDS high temperature and high pressure dynamic water loss instrument, and the formulation drilling fluid is injected in the reverse direction at 90  $^{\circ}$ C and 3.5 MPa differential pressure, and cycled at a shear rate of 300 s<sup>-1</sup> for 125 min. The core is loaded into the gripper and repelled at the same flow rate as in step 1, and the contaminated permeability  $K_1$ , is calculated after the pressure and flow rate are stabilized.

In step 3, the end face of the core contaminated by drilling fluid in step 2 is cut off for about 1 cm, and step 2 is repeated to obtain the core permeability *K*2.

## **3. Results and Discussion** 3. Results and Discussion

## *3.1. Characteristic* 3.1. Characteristic

The quadripolymer used in this study was milky white dispersion. The scanning elec-The quadripolymer used in this study was milky white dispersion. The scanning tron microscopy (SEM) pict[ur](#page-4-0)e is shown in Figure 1. The microstructure of the quadripolymer had the following characteristic: irregular shapes, different sizes (Fig[ur](#page-4-0)e 1a), and smooth surface (Fig[ure](#page-4-0) 1b) of the particles were easily recognizable. Among them, the particle size is relatively widely distributed. The largest is around 200 microns and the smallest is just under 10 microns. smallest is just under 10 microns.

about 1 cm, and step 2 is repeated to obtain the core permeability  $K^2$ . The core permeability  $K^2$ 

<span id="page-4-0"></span>

Figure 1. Microscopic images of the quaripolymer particles: (a) 200 times, (b) 1500 times.

The FT-IR spectrum of [th](#page-4-1)e quadripolymer is presented in Figure 2. Moreover, 3444  $cm^{-1}$ and 3300 cm<sup>-1</sup> are assigned to the N-H stretching vibration of AM and AMPS, respectively. The absorbency at 2935 cm<sup>-1</sup> results from the characteristic peak of the methyl group. The The absorbency at 2955 cm  $\sim$  results from the characteristic peak of the metrivi group. The stretching vibration of C=O at 1699 cm<sup>-1</sup> is attributed to AM and AMPS. The absorption peak observed at  $1454 \text{ cm}^{-1}$  is due to the C-H bending vibration from DMDAAC unit. Bands recorded at 1185 cm<sup>-1</sup> and 1044 cm<sup>-1</sup> assigned to S=O stretching vibration in the sulfonic group correspond to SSS unit. The absorption peaks at 766 cm<sup>-1</sup> reveal the bending<br>vibration of a bongane ring of the SSS unit. vibration of a benzene ring of the SSS unit.

<span id="page-4-1"></span>

Figure 2. FT−IR spectrum of quadripolymer (AM/AMPS/DMDAAC/SSS). **Figure 2.** FT−IR spectrum of quadripolymer (AM/AMPS/DMDAAC/SSS).

The  ${}^{1}$ H-NMR spectrum of the quadripolymer is shown in Figure 3. Bands recorded at 7.48 ppm (a<sub>1</sub>) and 7.24 ppm (a<sub>2</sub>) indicate the chemical shift in the benzene ring of SSS<br>peaks The MALI sortion from 5.97 to 5.92 ppm (b) are related to AM. The mode between units. The N-H proton from 5.87 to 5.92 ppm (b) are related to AM. The peaks between  $5.51$  and  $5.63$  ppm (c) are due to the N-H proton vibration of AMPS. The characteristic peak at 4.79 ppm belongs to the chemical shift of D<sub>2</sub>O protons. Broad peaks between 3.45 and 3.53 ppm (d) are assigned to N-C proton of DMDAAC. Respectively, the peaks at 2.76 ppm and 1.45 ppm and and 1.65 ppm correspond to the chemical shift of  $-CH<sub>2</sub>$  and  $-CH<sub>3</sub>$  of AMPS (e). The board peak at 2.93 ppm and 1.45 ppm are related to the -CH- linked with the benzene ring and the main chain of SSS, respectively (f). Combined with the FT-IR spectrum, the quadripolymer molecular structure is consistent with the designed one.

<span id="page-5-0"></span>

Figure 3. 1H−NMR spectrum of quadripolymer(AM/AMPS/DMDAAC/SSS). **Figure 3.** <sup>1</sup>H−NMR spectrum of quadripolymer (AM/AMPS/DMDAAC/SSS).

degradation process, first stage, the quadripolymer has 8.5% of mass losses before 260 °C,<br>in directive all debtathermal degree define form algebra since  $\Gamma$  accound the set form 260 °C, to 319.5 °C, apparent mass loss of the quadripolymer occurs (27.71%) in the TG curve and the fastest mass loss temperature emerges at 300.5 °C in the DSC curve. The third stage is from 319.5 °C to 528.5 °C, the mass loss declines constantly (35.43%). the release of the nonby the darly divided formation dery he detailed repeat date of the editiony he detail pendului group.<br>Moreover, accordingly, there is no significant fluctuation on the DSC curve. The last stage is from 528.5 °C to 600 °C, 28.36% mass is left. This might be due to the thermal degradation of C=C decomposition in the main chain of AM and SSS segments and the breakage of the quadripolymer is not obvious before 260 °C and only 27.7%, which demonstrates the quadripolymer has strong heat-resistance ability. From the TG curve (Figure [4\)](#page-6-0), it can be found that the four stages of the thermal indicating slightly thermal degradation from chain scissionThe second stage is from 260 ◦C cyclic anhydrides formation acrylic acid repeat unit or the carboxylic acid pendant group. benzene ring in SSS monomers. From the above analysis, the thermal degradation of

<span id="page-6-0"></span>

Figure 4. TG- DSC curve. **Figure 4.** TG- DSC curve.

lar structure of the quadripolymer. The weight-average molecular weight is  $1161,000 g/mol,$ and the number-average molecular weight is  $684,000$  g/mol. Besides, the viscosity-average molecular weight is  $684,000$  g/mol. Besides, the viscosity-average molecular weight is 1090,000 g/mol. Calculated with Mark-Tiouwink-Sakurada equation<br>(Mη = 802\*[η]1.25), among which the η value is 3.236 dL/g measured by Ubbelohdo viscometer (the flowing time of 0.1 wt% quadripolymer solution). Moreover, the molecular weight distribution index PDI is 1.6974, indicating that the quadripolymer has narrow molecular weight distribution. The data of quadripolymer molecular weight is follow in Table [2.](#page-6-1) Based on the molecumolecular weight is 1090,000 g/mol calculated with Mark–Houwink–Sakurada equation

<span id="page-6-1"></span>Table 2. Molecular weight indexed of copolymer.



# 3.2. Performance Evaluation of Bentonite-Free Drilling Fluid with the Quadripolymer

## 3.2.1. Rheological Behavior

gel strength, and high yield point) will provide good cuttings transportation efficiency in<br>drilling aporation. To investigate the influence of the quadripolymer on the rheelecieel behavior of the bentonite-free drilling fluid, various amount (from 0.3 to 0.9 wt%) of  $\mu$  drilling wele added to the base formula and the meological parameters, such as the apparent viscosity (*AV*), plastic viscosity (*PV*), and yield point (*YP*), were measured and compared. A drilling fluid having good rheological properties (low plastic viscosity value, suitable drilling operation. To investigate the influence of the quadripolymer on the rheological two polymers were added to the base formula and the rheological parameters, such as and compared.

As illustrated in Table 3, the two polymer drilling fluids display a remarkable increase in rheological parameters (*AV*, *PV*, and *YP*), as the concentration of polymer increases in the range from 0.3 to 0.9 wt%, which is mainly because that polymer contributes to forming It is the visit of declare of malastical consequently improving the incregation properties.<br>Compared with Drispac, *PV* values of the quadripolymer containing bentonite-free fluid system are relatively lower at the same polymer concentrations on the whole, while *YP* show relatively higher values. Moreover, the quadripolymer system exhibits a dynamic ratio (*YP*/*PV*) of up to 0.80, significantly larger than that of Drispac, at polymer concentration of 0.9 wt%, indicating that the quadripolymer has good shear thinning property. Lastly,<br>col strength of drilling fluid describes the sepecity to system d the drilling suttings when the pump is shut down. It can be observed that the increase in concentration of the quadripolymer contributes to a more dramatic increase than Drispac in *G*<sub>1</sub> and *G*<sub>2</sub>. The enhanced gel strength is attributed to the interactions among polymer molecules. Therefore, the bentonite-free drilling fluid with the quadripolymer has excellent cuttings suspending and carrying capacity. the network structure of fluids and consequently improving the rhelogical properties. gel strength of drilling fluid describes the capacity to suspend the drilling cuttings when and carrying capacity.



<span id="page-7-0"></span>**Table 3.** Influence of polymer concentration on rheological behavior of base formula.

## 3.2.2. Salt Resistance

It is shown from Table [4](#page-7-1) that all bentonite-free polymer drilling fluids with NaCl have lower rheological parameters than that without salt. Furthermore, as the salt content increases, all the rheological parameters display a remarkable decreasing trend. This is mainly because of charge shielding effect.  $Na<sup>+</sup>$  has strong ability to compress electric double layer of polymer and neutralize negative charge on ionized polymer, which could reduce an electrostatic repulsion force between particles to lower viscosity values, thus destroying network structure between polymer molecules. Furthermore, with a further increase in salt, large amount of Na<sup>+</sup> will increase the polarity of solution and enhance the hydrophobic associate effect, which can compensate the decrease of viscosity to a certain extent [\[30\]](#page-12-23). However, it could be seen clearly that compared with Drispac containing fluids, the quadripolymer shows a less variation in rheological parameters and has higher YP and gel strength values at the same salt concentration of  $5 \text{ wt}$ % and  $10 \text{ wt}$ %, respectively, suggesting that the quadripolymer has better salt resistance than Drispac.



<span id="page-7-1"></span>**Table 4.** Influence of salt concentration on rheological behavior of bentonite-free drilling fluid.

Note:  $2\text{#}$ : formula  $1\text{#} + 0.9$  wt% quadripolymer;  $3\text{#}$ : formula  $1\text{#} + 0.9$  wt% Drispac.

#### 3.2.3. Filtration Property

For filtration property, the API filtration (*FL*API) experiments were performed under a pressure of 100 psi and room temperature. The effect of salinity and polymers on filtration performance of bentonite-free drilling fluid is presented in Figure [5.](#page-8-0)

<span id="page-8-0"></span>

Figure 5. Effect of salinity and polymers on filtration property of bentonite-free drilling fluid. **Figure 5.** Effect of salinity and polymers on filtration property of bentonite-free drilling fluid.

Dramatic decreases in *FL*<sub>API</sub> of both fresh and salt fluid samples are seen as the dosage of polymer increases from 0 to 0.9 wt%. Firstly, in deionized water, *FL*<sub>API</sub> of the bentonite-free fluids with 0.9 wt% quadripolymer and Dispac decrease to 3 mL and 3.5 mL, respectively. The two polymers have approximately equal ability to control the filtration loss in fresh water environment. Similarly, in electrolyte solution, the filtration loss variations also present a declining trend with increasing polymer concentration, but the volumes are considerably higher than those in fresh water solution. This is mainly because that the molecular chains of polymer cannot be fully stretched in salt water, and subsequently the repulsive forces between molecular reduce and a high permeable filtration cake is formed. For all that, compared with *FL*<sub>API</sub> of Drispac containing salt system (18 mL), at 0.9 wt%, *FL*<sub>API</sub> of bentonite-free drilling fluid with the quadripolymer can be controlled within 12.5 mL, which demonstrates that the quadripolymer has better filtration loss control in brine drilling fluid. property in brine drilling fluid.

## 3.2.4. Thermal Stability 3.2.4. Thermal Stability

In petroleum industry, it is well known that high temperature would dramatically worsen rheological property and increase filtration volume loss of drilling fluids. Therefore, worsen rheological property and increase initiation volume loss of drilling fluids. Therefore, common used polymers PAM, 80A51, HE150 were compared with the quadripolymer to fore, common used polymers PAM, 80A51, HE150 were compared with the quadripoly-investigate their high temperature resistance. The initial viscosity was recorded as *V*<sup>1</sup> when polymer solutions were prepared at 0.9 wt%. Then, the polymer solutions were hot rolling polymer solutions were prepared at 0.9 wthen then, the polymer solutions were not roung<br>aged at different temperatures for 16 h, and the residual viscosity was marked as  $V_2$ . The  $h_{\text{in}}$  rolling and the rolling and the residual viscosity residual viscosity residual viscosity was matter  $\beta$  at different temperatures are shown in Eigure 6. viscosity retention rates  $R_v$  at different temperatures are shown in Figure [6.](#page-9-0) In petroleum industry, it is well known that high temperature would dramatically

$$
R_v = \left(\frac{V_1 - V_2}{V_1}\right) \times 100\% \tag{5}
$$

<span id="page-9-0"></span>

Figure 6. Viscosity retention rate of polymers at different aging temperature. **Figure 6.** Viscosity retention rate of polymers at different aging temperature.

rates of different polymers generally show downward trends, but the change degree varies. As illustrated in Figure 6, as the aging temperature increases, the viscosity retention after aging at 140 °C. In contrast, HE150 and the quadripolymer have higher viscosity retention rates at the same temperature, especially for the quadripolymer, the viscosity retention rate is as high as 40% even when the aging temperature reaches to 180 °C, and nearly 10% at 200 °C. Therefore, compared with other three polymers commonly used in drilling fluids, the quadripolymer has better temperature resistance. Among them, the viscosity of the two polymers, PAM and 80A51, has been basically lost

In order to further study the effect of the quadripolymer on the thermal stability of the bentonite-free drilling fluid, the rheological and filtration properties were evaluated before and after hot rolling aging at various temperatures (25 °C, 100 °C, 120 °C, 140 °C, 160 °C, 180 °C, 200 °C), and the results are shown in Table [5.](#page-9-1)

T,	PV,	YP,	$G_1/G_2$ ,	$FL_{API}$	$FL_{\rm HTHP}$
$^{\circ}C$	mPa·s	Pa	Pa/Pa	mL	mL
25	27	21.5	4.5/5.5	3.0	
100	25	14.3	4.0/5.0	4.2	14.6
120	24	14.3	3.5/4.5	5.4	17.8
140	23	13.3	3.5/4.0	6.6	19.7
160	22	10.4	2.5/3.5	7.4	21.6
180	20	8.2	1.5/2.5	8.6	24.8
200	12	2.0	0.5/0.5	12.4	46.4

<span id="page-9-1"></span>Table 5. Influence of thermal aging temperature on performance of bentonite-free drilling fluid.

Note: bentnoite-free drilling fluid formulation: deionized water + 0.1 wt% NaOH + 0.15 wt% Na<sub>2</sub>CO<sub>3</sub> + 0.9 wt% quadripolymer + 2 wt% PAC–LV + 2 wt% LOCKSEAL + 4 wt% CaCO $_3$  + 0.5 wt% Na<sub>2</sub>SO<sub>3.</sub>

180 20 8.2 1.5/2.5 8.6 24.8 As shown in Table [5,](#page-9-1) it can be clearly observed that in the aging temperature range of 100–180 °C, all parameters variation are within the acceptable range, showing a good thermal stability. *PV* value of the quadripolymer bentonite-free drilling fluid still remains at 20 mPa·s after aging at 180 °C. Meanwhile, *FL*<sub>API</sub> and *FL*<sub>HTHP</sub> are controlled within 8.6 mL and 24.8 mL, respectively. However, when the aging temperature rises to 200  $^{\circ}$ C, the rheological parameters of the bentonite-free drilling fluid with the quadripolymer

show an obvious decreasing trend, and the amount of filtration loss markedly increases, indicating that the comprehensive properties of drilling fluid are out of control. Based on the above analysis, it can be demonstrated that the bentonite-free drilling fluid prepared by the quadripolymer possesses excellent ability to maintain viscosity and filtration loss at the temperature of 180 °C.  $\mathbf{t}$ 

thermal stability. PV value of the quadripolymer bentonite-free drilling fluid still remains

## 3.2.5. HTHP Rheology

In order to determine the rheological characteristics of the synthetic quadripolymer In order to determine the rheelogical characteristics of the synthetic quadripolymerature in the synthetic quadripology test of four common high temperature resistant polymers were performed. A constant shear rate (511 s<sup>-1</sup>) was applied at different temperatures. Moreover, the curves of viscosity changing with temperature are presented in Figure [7.](#page-10-0) with temperature are presented in Figure 7. under high temperature and high pressure environment, the HTHP rheology test of four

<span id="page-10-0"></span>

Figure 7. HTHP rheology curves of different polymer solutions. **Figure 7.** HTHP rheology curves of different polymer solutions.

As shown in Figure [6,](#page-9-0) heating causes the rapid drop in the viscosity of polymer solutions, especially for PAM, 80A51 and HE150. Among the four polymers, the viscosity reduction rates of the three polymers mentioned above are much higher than that of quadripolymer. When temperature rises to 180 °C, the viscosities of the PAM and 80A51 solution are close to 0. In contrast, the quadripolymer has higher viscosity values at each temperature point than those of the other three polymers in the temperature range of 200 ◦C, which further suggests that the quadripolymer has good temperature resistance at high temperatures.

### 3.2.6. Reservoir Protection Performance

ZDY50–180 core flow tester and oil reservoir cores taken from Well TK10 at the depth of 5298.83–5299.50 m, were used for reservoir protection evaluation of the bentonite-free drilling fluid with the new quadripolymer.

The degree of reservoir damage caused by drilling fluid can be characterized by the change of permeability before and after core contamination by drilling fluid, i.e., the lower permeability of core contamination means the higher degree of reservoir damage. It is clear

that the permeability of both cores (sample a and sample b) after contamination is restored to more than 85% (Table [6\)](#page-11-2). Moreover, the permeability recovery rate of two cores are obviously improved and reaches up as high as 95.7% and 94.2%, respectively, after cutting off 1 cm of contaminated core section, which indicates that the bentonite-free drilling fluid has a good protective effect on reservoir.



<span id="page-11-2"></span>**Table 6.** Reservoir protection performance test for bentonite-free polymer drilling fluid.

Note:  $K_1$  is the initial permeability of cores;  $K_2$  is the permeability of contaminated cores.

## **4. Conclusions**

A novel hydrophilic polymer was prepared with AM, AMPS, DMDAAC, and SSS monomers via a method of free radical polymerization in aqueous solution. The new polymer was characterized by  ${}^{1}H$  NMR and FT-IR analysis. Results indicated the quadripolymer molecular structure was consistent with the designed one. Moreover, the rheological and filtration properties of the bentonite-free drilling fluid containing the quadripolymer and Drispac were examined in deionized and salt water at various temperatures. As a result, the rheological parameters regularly increased with increasing dosage of polymers. Simultaneously, the viscosity of the salt water fluid system was explicit smaller than that of the fresh water system. Additionally, when the adding amount was 0.9 wt%, it was confirmed that *FL*<sub>API</sub> of two polymers drilling fluid systems decreased to 3 mL and 3.5 mL, respectively, which are in acceptable range. The thermal stability test of bentonite-free drilling fluid showed that the quadripolymer drilling fluid could maintain a certain viscosity value, and *FL*API and *FL*HTHP were also controlled within 8.6 mL and 24.8 mL, respectively. In HTHP rheology test, the synthetic polymer showed superior resistance to high temperature than commonly used polymers. As for its damage to the reservoir, the permeability recovery of cores reached more than 95.72%. In general, the synthesized polymer has good properties of high temperature resistance and salt tolerance in controlling rheology and filtration loss of the bentonite-free drilling fluid system.

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