



Supplementary Materials

Mitigation of membrane fouling using an electroactive polyether sulfone membrane

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Supplementary Materials: 2 tables and 8 figures.





Materials and methods:

Static protein adsorption experiment.

BSA-FITC solution was used to measure the protein adsorption behavior of Car-PES membranes. The flow channel was filled with staining fluid at room temperature for 1 h in the dark in order to stain the BSA on the membrane. It was then rinsed with 0.5 mg/mL potassium phosphate buffer solution (PBS) to reduce the interference due to background fluorescence. The adsorption was imaged by a fluorescence microscope (ZIESS A1, Carl Zeiss AG, Germany) equipped with an excitation filter of 495 nm and an emission filter of 525 nm.

Filtration velocity method

According to the Guerout-Elford-Ferry equation, mean pore radius D could be experimentally determined by [1]:

$$D = \sqrt{\frac{(2.90 - 1.75\varepsilon) \times 8\eta\ell Q}{\varepsilon \times A \times \Delta P}} \times 2 \tag{1}$$

where η is the water viscosity (8.9 × 10⁻⁴ Pa·s), ℓ is the membrane thickness (nm), Q is the volume of the permeate water per unit time (m³·s⁻¹), ϵ is the membrane porosity, A is the membrane effective area (m²) and Δ P is the operational pressure (0.1 MPa).

Table S1. Properties of the PES and Car-PES membrane.

membrane	electrical conductivity	pore size (nm)	flux of deionized water (LMH)	R₄(nm)
PES	∞	77.0±4.3	421.5±44.6	77.07
Car-PES	5±2.1 Ω·cm	65.1±5.8	374.0±20.1	41.26

Table S2. Properties of the four foulants.

foulant	diameter	Zeta potential	specific value
		(mV)	(mV/nm)
BSA	5.4±0.6 nm	-11.6	2.150
SA	346.2±34.7 nm	-26.5	0.080
yeast	3.3± 0.4 μm	-11.2	0.003
Emulsified oil	13.6±14.5 μm	-56.3	0.004

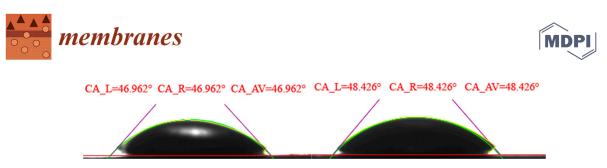


Figure S1. Contact angle images: (**a**) PES membrane with contact angle of 46.9°, (**b**) Car-PES membrane with contact angle of 48.4°.

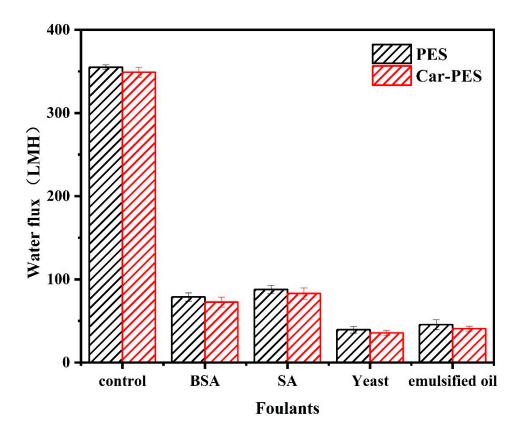


Figure S2. Water fluxes through PES and Car-PES membranes over 24h. (Conditions: (BSA)_{in}=10 mg/L, (SA)_{in}=10 mg/L, (yeast)_{in}=10 mg/L, (emulsified oil)_{in}=10 mg/L, (cross-flow velocity)=6.1 cm/s, (time)=24 h, and (pressure)= 0.1 bar).





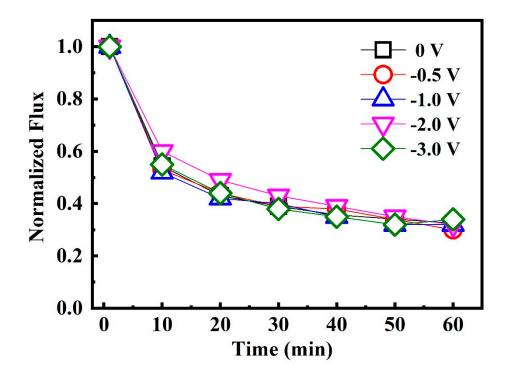


Figure S3. Normalized flux through a PES membrane in comprehensive anti-fouling experiments with different negative voltages applied (Conditions: (SA)in= 10 mg/L, (Na₂SO₄)= 10 mM, (cross-flow velocity)= 6.1 cm/s, and (pressure)= 0.1 bar).





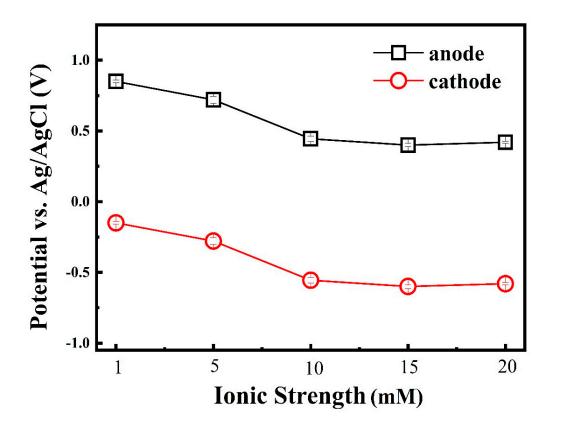


Figure S4. Anode/cathode potential distribution as a function of total cell potential at different ionic strengths: (Conditions: Car-PES memebrane cathode, titanium plate anode, and silver/silver chloride (Ag/AgCl) contrast electrode, (SA)_{in}= 10 mg/L).

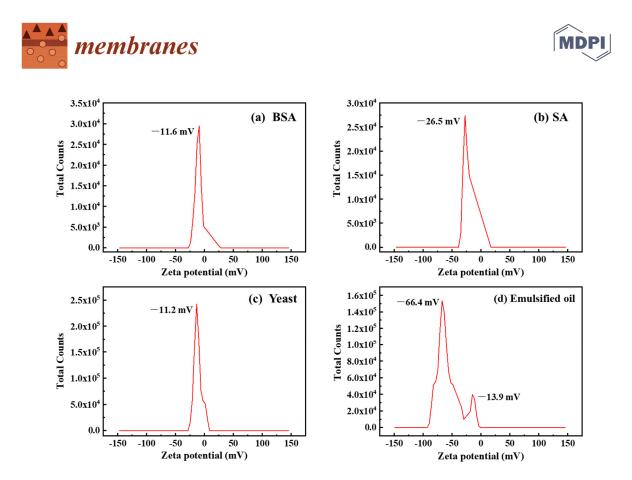


Figure S5. Zeta potential: (**a**) BSA, (**b**) SA, (**c**) yeast, (**d**) emulsified oil. (Conditions: (BSA)_{in}= 10 mg/L, (SA)_{in}= 10 mg/L, (yeast)_{in}= 10 mg/L, (emulsified oil)_{in}= 10 mg/L, PH= 7.2).





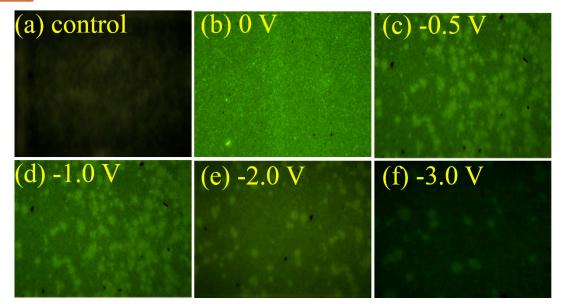


Figure S6. Protein adsorption of at different initial electric fields: (**a**) Control, (**b**) 0 V, (**c**) -0.5 V, (**d**) -1 V, (**e**) -2 V, (**f**) -3 V.





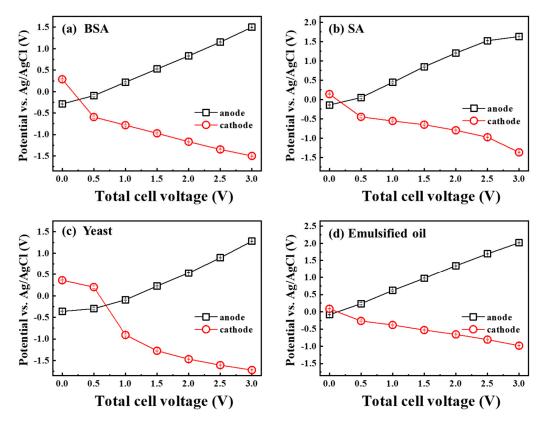


Figure S7. Anode/cathode potential distribution as a function of total cell potential: (**a**) BSA, (**b**) SA, (**c**) yeast, (**d**) emulsified oil. (Conditions: Car-PES memebrane cathode, titanium plate anode, and silver/silver chloride (Ag/AgCl) contrast electrode, (BSA)_{in}= 10 mg/L, (SA)_{in}= 10 mg/L,(yeast)_{in}= 10 mg/L, (emulsified oil)_{in}= 10 mg/L).





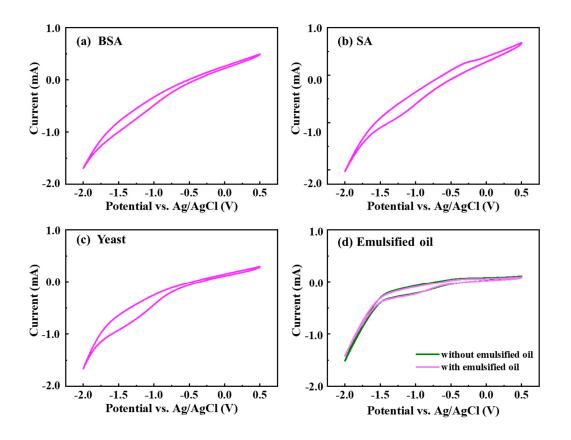


Figure S8. Cyclic voltammetry of the conductive Car-PES membrane with a scan rate of 100 mV·s⁻¹: (**a**) BSA, (**b**) SA, (**c**) yeast, (**d**) emulsified oil. (Conditions: Car-PES memebrane cathode, titanium plate anode, and silver/silver chloride (Ag/AgCl) contrast electrode, (BSA)_{in}= 10 mg/L, (SA)_{in}= 10 mg/L, (yeast)_{in}= 10 mg/L, (emulsified oil)_{in}= 10 mg/L).

Reference

 Basri, H.; Ismail, A.F.; Aziz, M. Polyethersulfone (PES)–silver composite UF membrane: Effect of silver loading and PVP molecular weight on membrane morphology and antibacterial activity. *Desalination* 2011, 273, 72-80, doi:https://doi.org/10.1016/j.desal.2010.11.010.



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