



Syngas Production via Oxidative Reforming of Propane Using a CO₂- and O₂-Permeating Membrane

José A. Fabián-Anguiano ¹, Lorena G. Cuéllar-Herrera ¹, José A. Romero-Serrano ¹, Issis C. Romero-Ibarra ², Antonieta García-Murillo ³, Felipe Carrillo-Romo ³ and José Ortiz-Landeros ^{1,*}

¹ Instituto Politécnico Nacional, Escuela Superior de Ingeniería Química e Industrias Extractivas, Departamento de Ingeniería en Metalurgia y Materiales, UPALM-Zacatenco, IPN Avenue, Mexico City 07738, Mexico

² Instituto Politécnico Nacional, Unidad Profesional Interdisciplinaria en Ingeniería y Tecnologías Avanzadas, IPN Avenue, Mexico City 07340, Mexico

³ Instituto Politécnico Nacional, Centro de Investigación e Innovación Tecnológica, Cerrada de Cecati S/N, Santa Catarina, Azcapotzalco, Mexico City 02250, Mexico

* Correspondence: jortizla@ipn.mx; Tel.: +52-5557296000 (ext. 54267)

Based on the chromatography analysis, the conversion rate of C₃H₈, CO₂, and O₂ can be estimated by Eqs. (S1), (S2) and (S3).

$$X_{C_3H_8} = \frac{F_{C_3H_8(in)} - F_{C_3H_8(out)}}{F_{C_3H_8(in)}} \times (100) \quad (S1)$$

$$X_{CO_2} = \frac{J_{CO_2} - J_{CO_2(unconsumed)}}{J_{CO_2}} \times (100) \quad (S2)$$

$$X_{O_2} = \frac{J_{O_2} - J_{O_2(unconsumed)}}{J_{O_2}} \times (100) \quad (S3)$$

In Eq. (S1), $F_{C_3H_8(in)}$ and $F_{C_3H_8(out)}$ are the propane flow rate at the sweep in and the sweep out of the membrane reactor, while in Eq. (S2) and (S3) J_{CO_2} , J_{O_2} correspond to the permeated concentration of species through the membrane and J_{CO_2} , $J_{O_2(unconsumed)}$ represent the unreacted flux of CO₂ and O₂.