



Supplementary Materials

TiO₂-Supported Pd as an Efficient and Stable Catalyst for the Mild Hydrotreatment of Tar-Type CompoundsZaher Raad ^{1,2}, Joumana Toufaily ², Tayssir Hamieh ² and Marcelo E. Domine ^{1,*}¹ Instituto de Tecnología Química (UPV-CSIC), Universitat Politècnica de València, Consejo Superior de Investigaciones Científicas, Avda. de los Naranjos s/n, 46022 Valencia, Spain; zaraa@upvnet.upv.es² Laboratoire de Matériaux, Catalyse, Environnement et Méthodes Analytiques (MCEMA-CHAMSI), EDST, Université Libanaise, Campus Hariri, Hadath, 1003 Beyrouth, Lebanon; joumana.toufaily@ul.edu.lb (J.T.); tayssir.hamieh@ul.edu.lb (T.H.)

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Preliminary catalytic screening:

Table S1. Catalytic activity (Conversion and selectivity to the different groups of products) of carbon-supported Pd, Pt and Ru commercial catalysts (comparison at 50–60% conversion).^a

Catalyst	Conv. (mol%)	TON ^b	Product selectivity (mol%) ^c							
			MonoAr	Tetralin	Decalin	Ace	HAce-1	HPhe-1	HPhe-2	HAce-2 /HPhe-3
5wt%Pd/C	71	21	2	32	0	4	42	18	2	0
5wt%Pt/C	55	30	2	29	0	34	13	21	1	0
5wt%Ru/C	52	15	2	32	0	35	14	16	1	0

^a Reaction conditions: 0.5 g of tars-type compounds, 4 g of n-hexadecane, 0.2 g of catalyst, at 250 °C and 30 bar of H₂ during 7 h. ^bTON = mols of products / mols of metal. ^c Liquid phase composition; Selectivity = mol of product (t) × 100 / total mol of identified products (t).

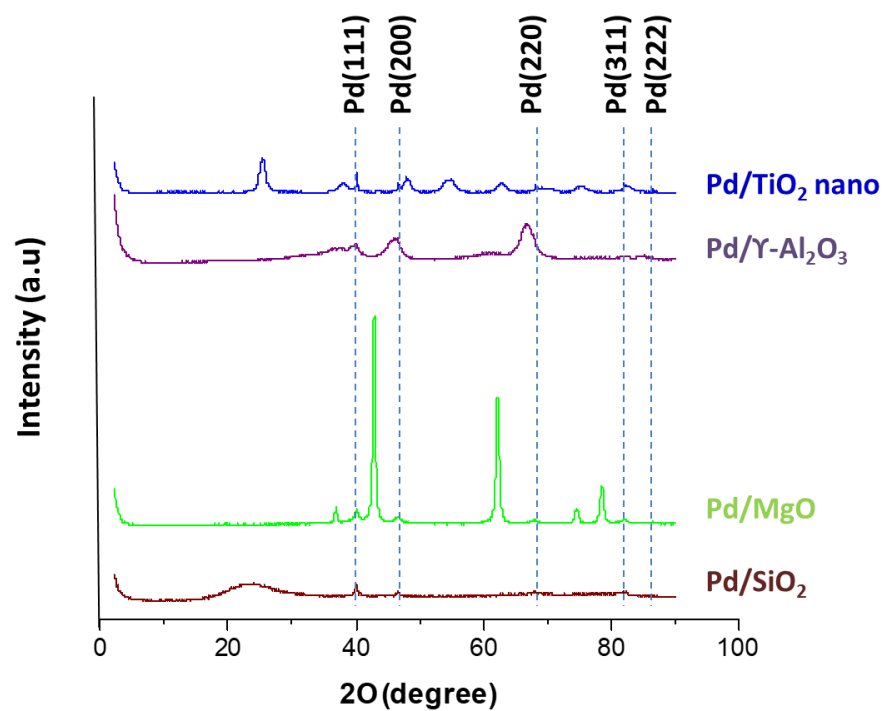


Figure S1. XRD patterns for different metal oxides-supported Pd catalysts.

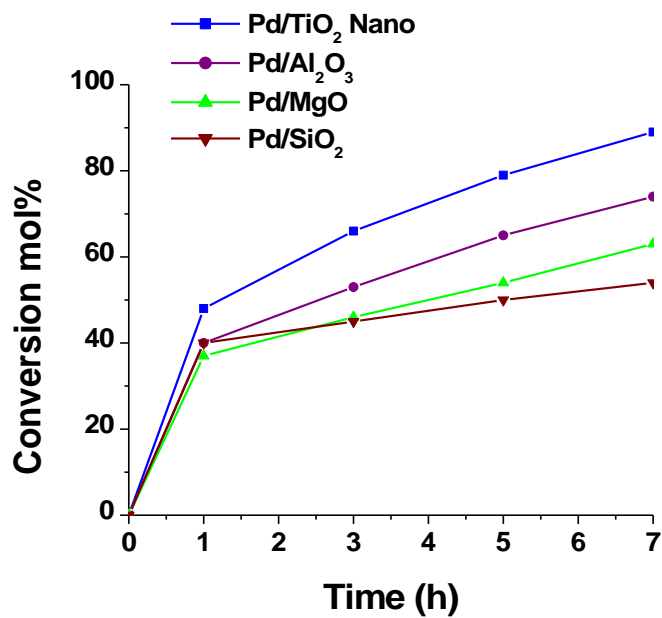


Figure S2. Conversion vs time for different metal oxides-supported Pd catalysts. Reaction conditions: 0.5 g of tar-type compounds, 4 g of n-hexadecane at 250 °C and 30 bar of H₂ during 7 h.

Effect of Pd content in Pd/TiO₂ (Nano) catalysts:

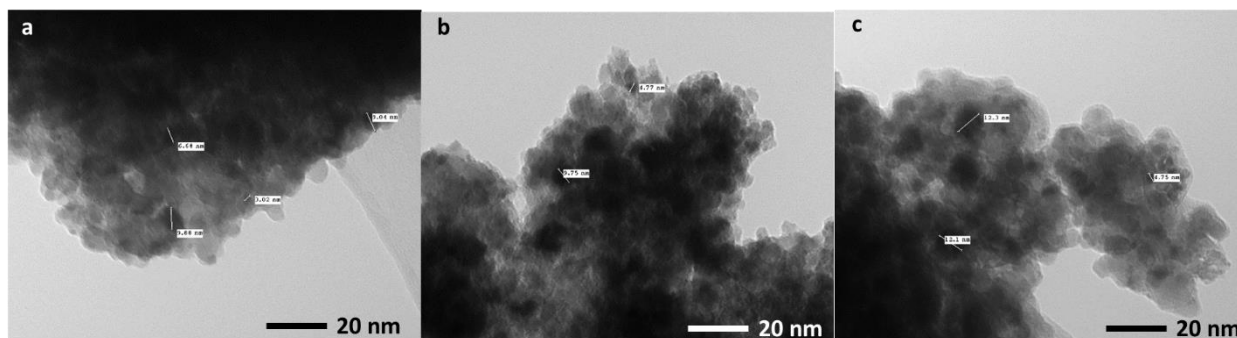


Figure S3. TEM images of (a) 0.8wt%Pd/TiO₂ (4–7 nm), (b) 1.3wt%Pd/TiO₂ (5–9 nm), and (c) 2.2wt% Pd/TiO₂ (6–12 nm).

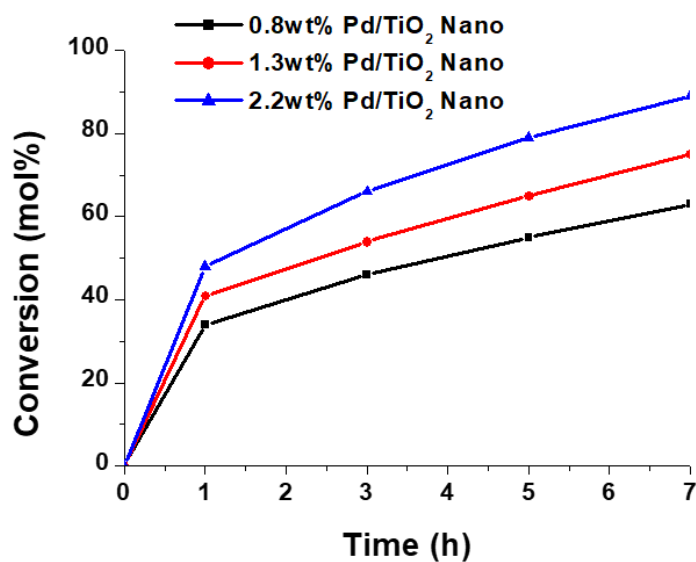


Figure S4. Conversion vs time for Pd/TiO₂ Nano catalysts with different Pd loadings. Reaction conditions: 0.5 g of tars-type compounds, 4 g of n-hexadecane, 0.2 g of catalyst, at 250 °C and 30 bar of H₂ during 7 h.

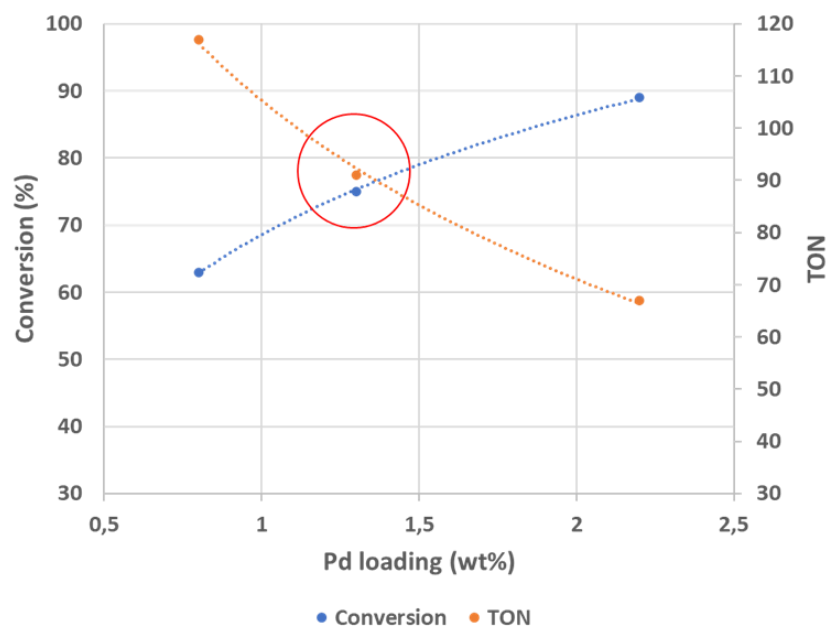


Figure S5. Conversion and TON (mols prod. / mols of Pd in solid) vs Pd loading for Pd/TiO₂ nano catalysts. Reaction conditions: 0.5 g of tars-type compounds, 4 g of n-hexadecane, 0.2 g of catalyst, at 250 °C and 30 bar of H₂ during 7 h.

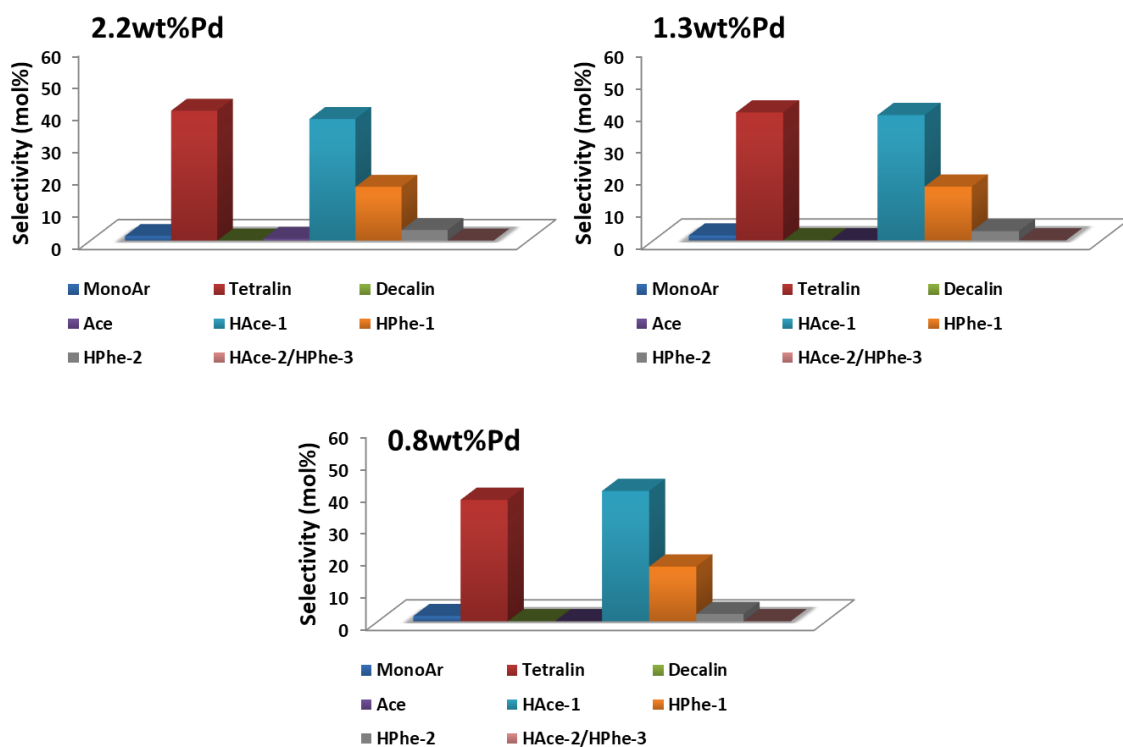


Figure S6. Selectivity to the different groups of products for Pd/TiO₂ Nano catalysts compared in the range 63-65% of conversion. Reaction conditions: 0.5 g of tars-type compounds, 4 g of n-hexadecane, 0.2 g of catalyst, at 250 °C and 30 bar of H₂ during 7 h.

Table S2. Pd/TiO₂ Nano catalysts prepared by using different Pd precursors and their catalytic results in tars mild hydrotreatment.^a

Pd Precursor	Pd (wt%)^b	Conversion (mol%)	TON^c
Pd(NH ₃) ₄ .Cl ₂ .H ₂ O	1.3	75	91
Pd(NO ₃) ₂ .2H ₂ O	1.3	79	90
Pd(NO ₃) ₂ .4NH ₃	0.8	68	127
Pd(NH ₃) ₄ .Cl ₂ .H ₂ O	0.8	63	117

^a Reactions conditions: 0.5 g of tars -type compounds, 4 g of n-hexadecane, at 250 °C, 30 bar of H₂, 0.2 g catalyst during 7 h. ^b

Measured by ICP; ^c TON = mols of products / mols of metal in solid.

Effect of TiO₂ crystalline phase used as support

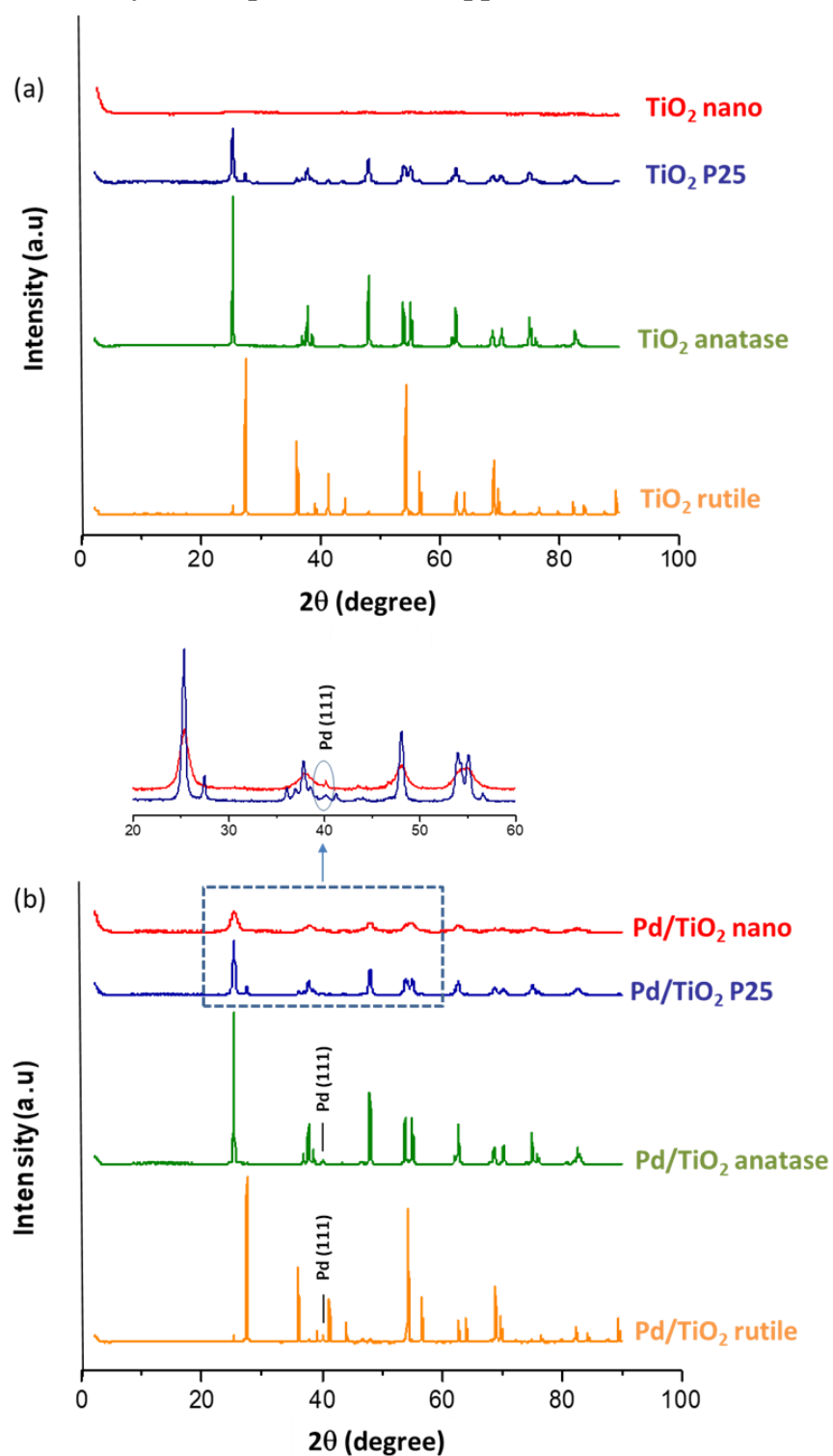


Figure S7. XRD patterns of different (a) pure TiO₂ supports and (b) TiO₂-supported Pd catalysts (Inset showing a zoom of 20-60° 2θ region for Pd/TiO₂ nano and Pd/TiO₂ P25).

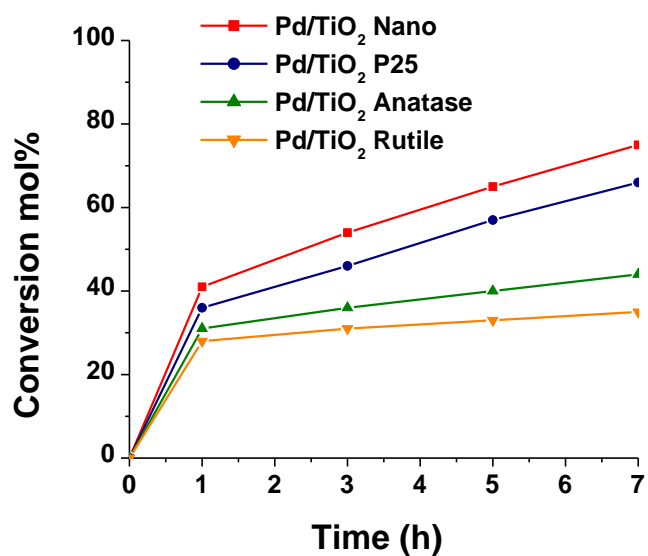


Figure S8. Conversion vs time for different TiO₂-supported Pd catalysts in tars mild hydrotreatment. Reaction conditions: 0.5 g of tars-type compounds, 4 g of n-hexadecane, at 250 °C and 30 bar of H₂ during 7 h.

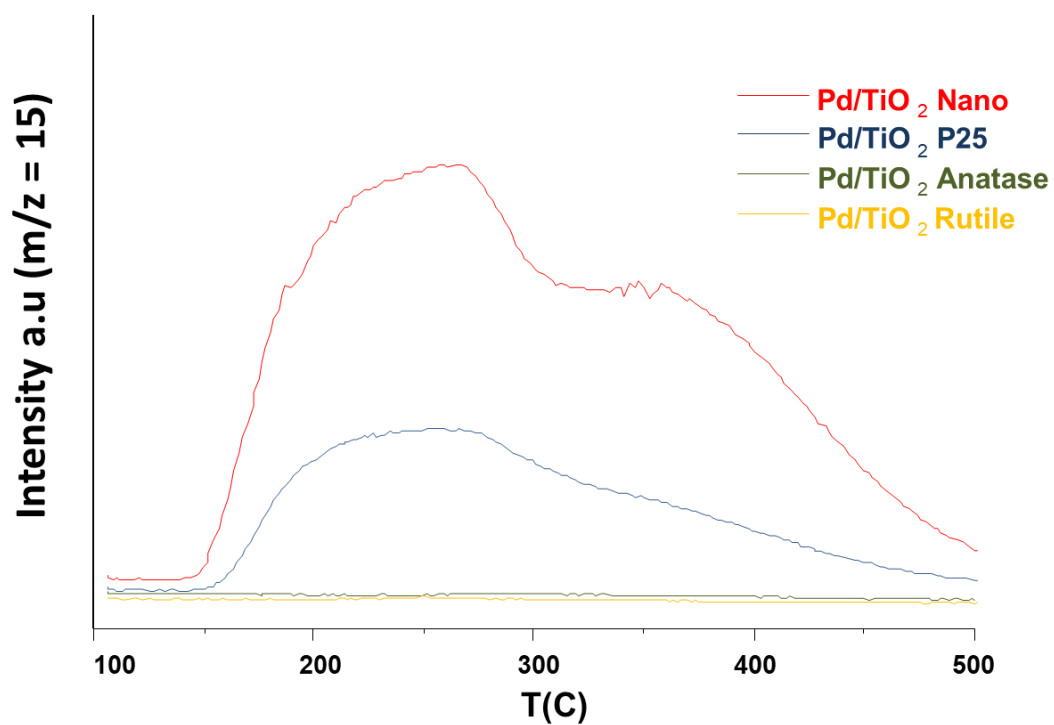


Figure S9. NH₃-TPD profiles for different TiO₂-supported Pd catalysts.

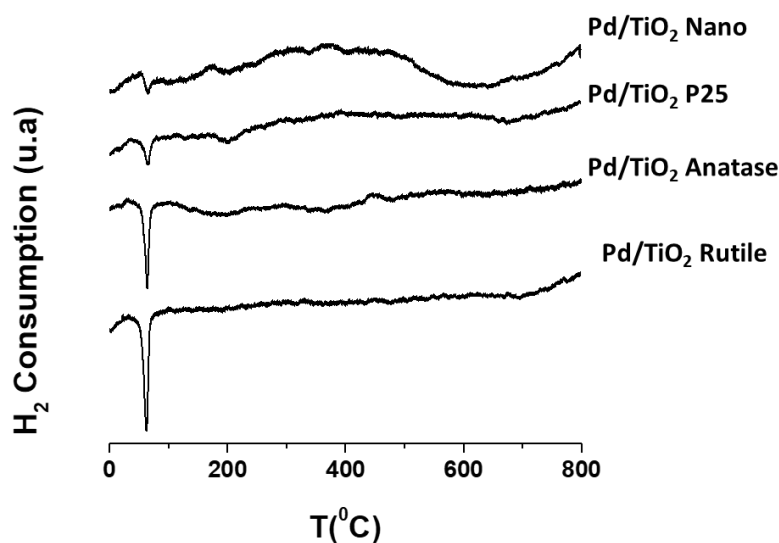


Figure S10. H₂-TPR profiles for different TiO₂-supported Pd catalysts.

Effect of reaction conditions for Pd/TiO₂ Nano catalyst

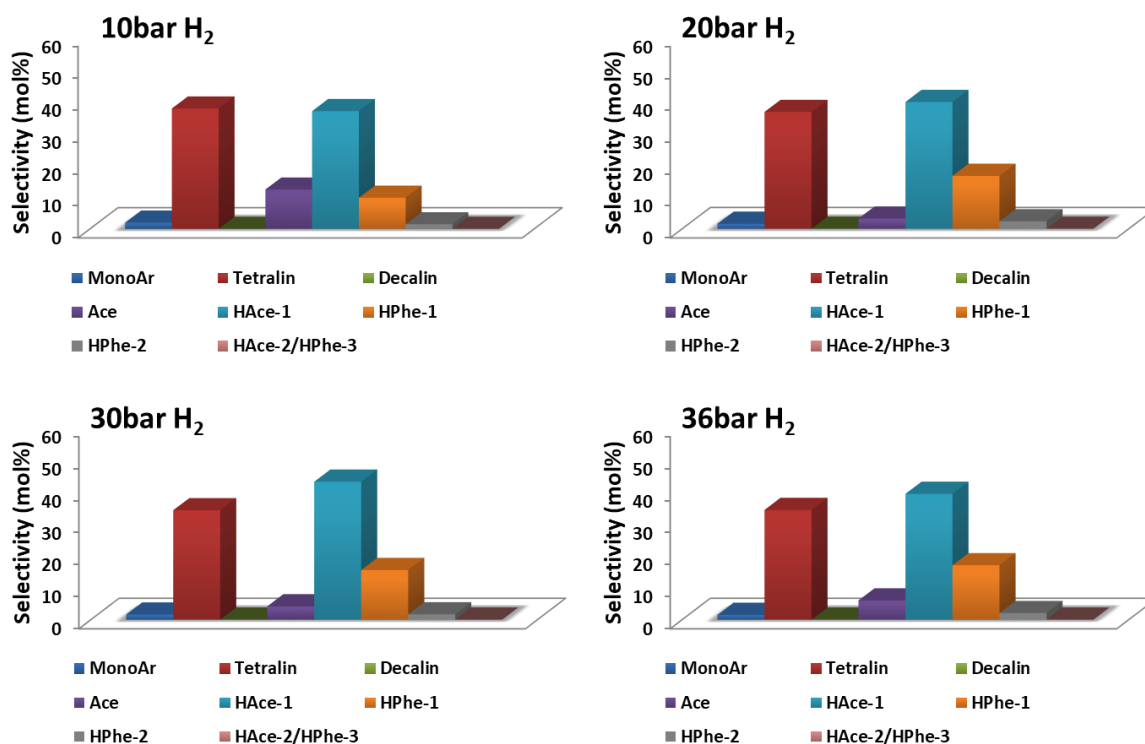


Figure S11. Selectivity to the different groups of products (compared at ≈53% conversion) for 1.3wt%Pd/TiO₂ Nano catalyst by using different H₂ pressures. Reaction conditions: 0.5 g of tars-type compounds, 4 g of n-hexadecane, 0.2 g of catalyst, at 275 °C during 7 h.

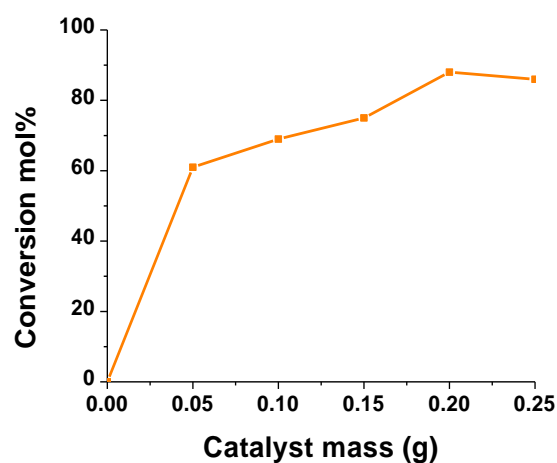


Figure 12. Catalyst loading optimization in tars mild hydrotreatment over 1.3wt%Pd/TiO₂ Nano. Reaction conditions: 0.5 g of tars-type compounds, 4 g of n-hexadecane, at 275 °C and 30 bar of H₂ during 7 h.

Reusability tests

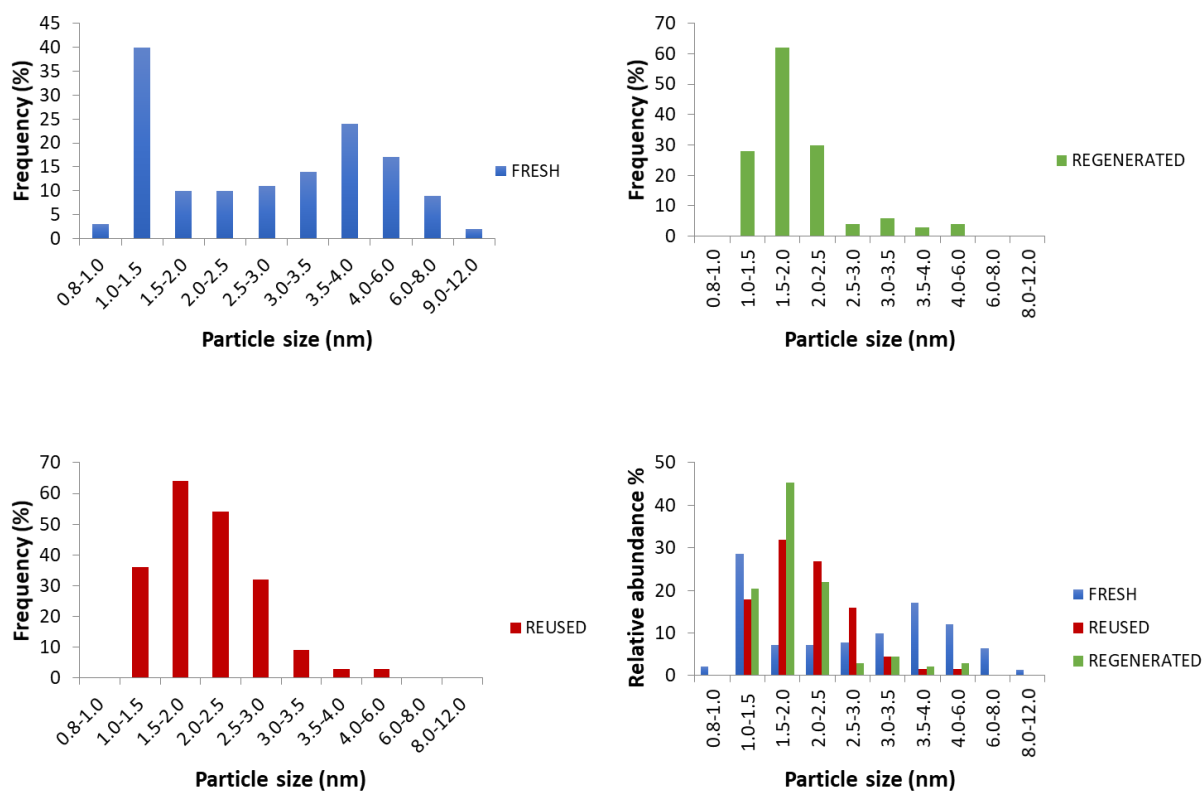


Figure S13. Pd particle size distribution of fresh, reused and regenerated samples of Pd/TiO₂ Nano catalyst.

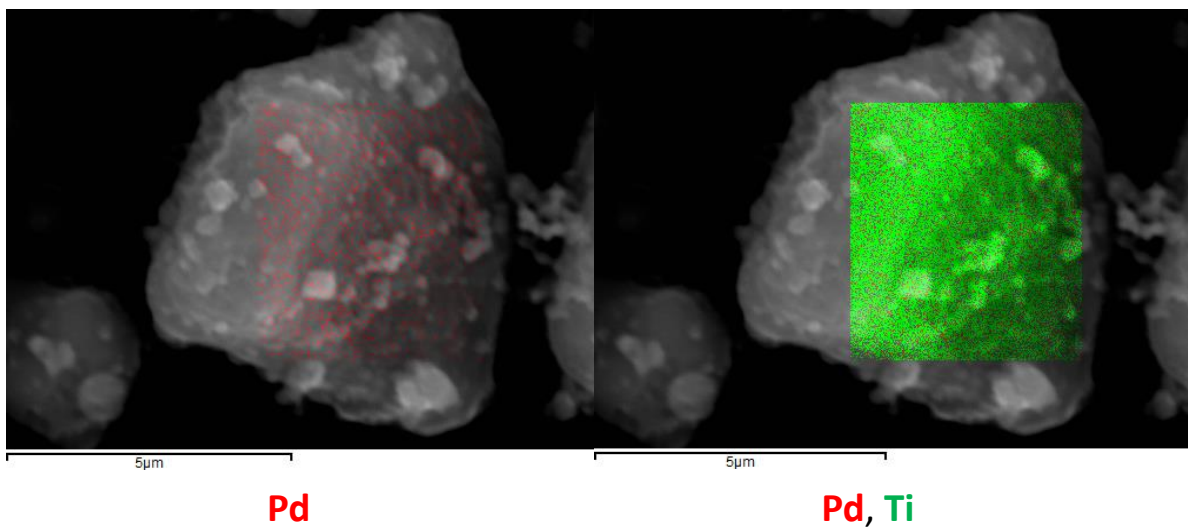


Figure S14. SEM-EDX for the fresh sample of Pd/TiO₂ Nano catalyst.

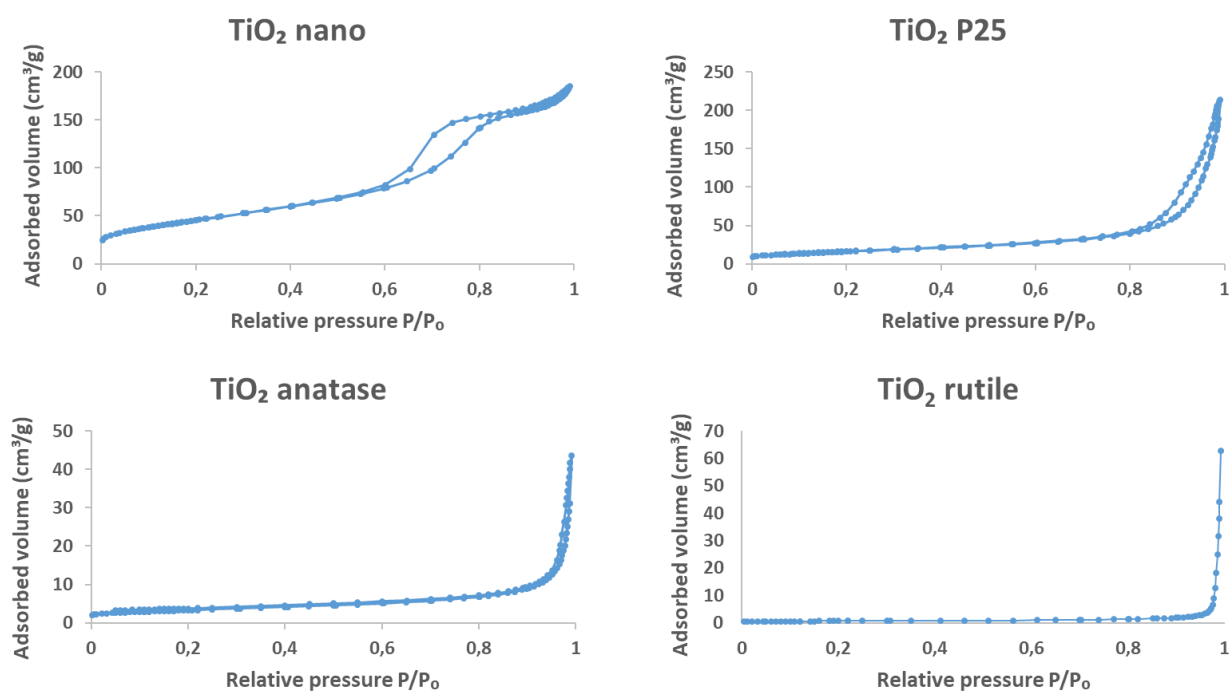


Figure S15. Nitrogen adsorption-desorption isotherms for different TiO₂ materials.

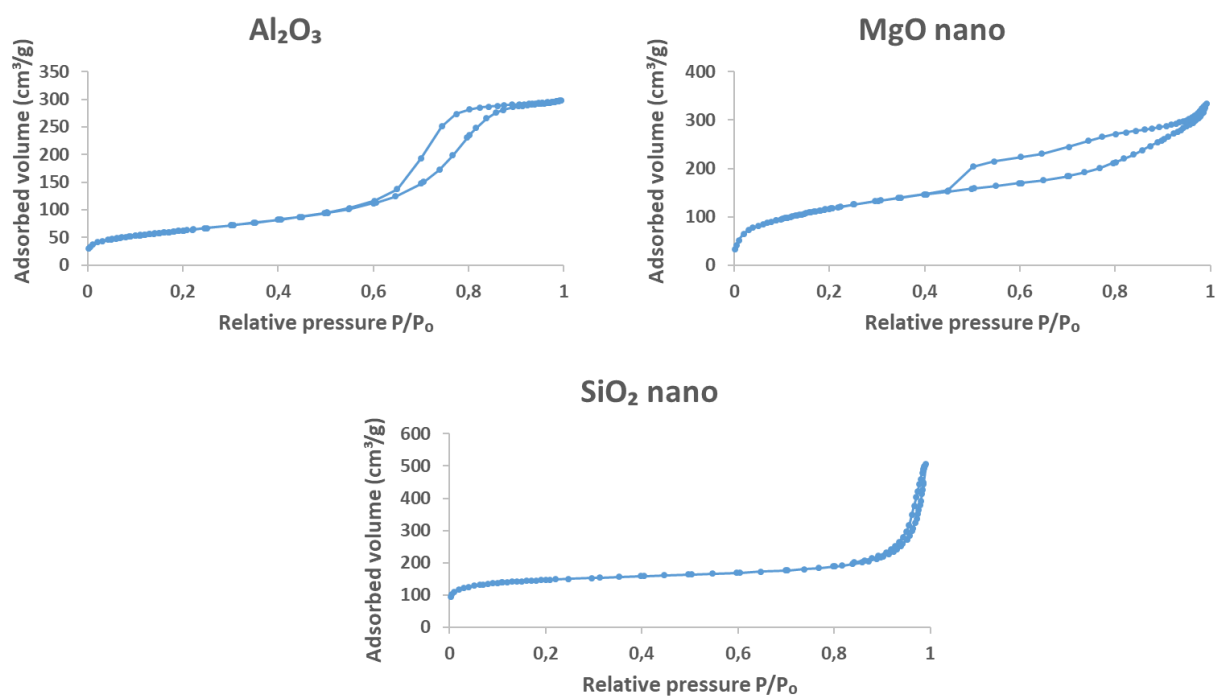


Figure S16. Nitrogen adsorption-desorption isotherms for different metal oxides materials.