



Flow behavior of nanoparticle agglomerates in a fluidized bed simulated with porous-structure-based drag laws

Shaowei Wang^{1,*}, Xiaobing Hu¹, Niannian Liu² and Huanpeng Liu³

¹ Energy and Power Engineering Institute, Henan University of Science and Technology, Luoyang, Henan 471003, PR China

² Department of Engineering Mathematics, University of Bristol, Bristol, United Kingdom

³ School of Energy Science and Engineering, Harbin Institute of Technology, Harbin, Heilongjiang 150006, PR China

* Correspondence: 9906235@haust.edu.cn; Tel.: 0086-379-64231480

Section S1. Governing equations for gas/solid flows.

Mass conservation for phase i ($i = g$ for gas and s for solid):

$$\frac{\partial(\varepsilon_i \rho_i)}{\partial t} + \nabla \cdot (\varepsilon_i \rho_i \vec{v}_i) = 0$$

Linear momentum balance for gas and solid phases:

$$\frac{\partial(\varepsilon_g \rho_g \vec{v}_g)}{\partial t} + \nabla \cdot (\varepsilon_g \rho_g \vec{v}_g) = -\varepsilon_g \nabla p_g + \nabla \cdot \bar{\tau}_g + \beta_{gs} |\vec{v}_s - \vec{v}_g| + \varepsilon_g \rho_g \vec{g}$$

$$\frac{\partial(\varepsilon_s \rho_s \vec{v}_s)}{\partial t} + \nabla \cdot (\varepsilon_s \rho_s \vec{v}_s) = -\varepsilon_s \nabla p_s + \nabla \cdot \bar{\tau}_s + \beta_{gs} |\vec{v}_s - \vec{v}_g| + \varepsilon_s \rho_s \vec{g}$$

Transport equation for the solid phase granular temperature:

$$\frac{3}{2} \left[\frac{\partial}{\partial t} (\varepsilon_s \rho_s \Theta_s) + \nabla \cdot (\varepsilon_s \rho_s \vec{v}_s \Theta_s) \right] = (-p_s \bar{I} + \bar{\tau}_s) \cdot \nabla \vec{v}_s + \nabla \cdot (k_{\Theta_s} \nabla \Theta_s) - \gamma_{\Theta_s} + \Phi_{gs}$$

Section S2. Constitutive equations of gas-solid flow.

Gas stress tensor:

$$\bar{\tau}_g = \varepsilon_g \mu_g [\nabla v_g + \nabla v_g^T] - \frac{2}{3} \varepsilon_g \mu_g \nabla \cdot v_g \vec{I}$$

Solid stress tensor:

$$\bar{\tau}_s = \mu_s [\nabla v_s + \nabla v_s^T] - \frac{2}{3} \mu_s \nabla \cdot v_s \vec{I}$$

where solid shear viscosity is:

$$\mu_s = \mu_{s,col} + \mu_{s,kin} + \mu_{s,fr}$$

The collisional contribution to shear viscosity is:

$$\mu_{s,col} = \frac{4}{5} \varepsilon_s \rho_s g_{0,ss} (1 + e_{ss}) \sqrt{\frac{\theta_s}{\pi}}$$

The kinetic contribution to shear viscosity:

$$\mu_{s,kin} = \frac{10 d_s \rho_s \sqrt{\theta_s \pi}}{96 \varepsilon_s g_{0,ss} (1 + e_{ss})} [1 + \frac{4}{5} \varepsilon_s g_{0,ss} (1 + e_{ss})]^2$$

The frictional contribution to shear viscosity [1]:

$$\mu_{s,fr} = p_f \sin(\varphi) / 2 \sqrt{I_{2D}}$$

Solid phase bulk viscosity:

$$\lambda_s = \frac{4}{3} \varepsilon_s d_s \rho_s g_{0,ss} (1 + e_{ss}) \sqrt{\frac{\theta_s}{\pi}}$$

Collision dissipation energy [2]:

$$\gamma_\theta = \frac{12(1 - e_{ss}^2) g_{0,ss}}{d_s \sqrt{\pi}} \rho_s \varepsilon_s^2 \theta_s^{3/2}$$

Solids pressure:

$$p_s = \varepsilon_s \rho_s \theta_s + 2 \rho_s (1 + e_{ss}) \varepsilon_s g_{0,ss}$$

Thermal energy diffusion coefficient:

$$k_\theta = \frac{25 d_s \rho_s \sqrt{\theta_s \pi}}{64 g_{0,ss} (1 + e_{ss})} [1 + \frac{6}{5} \varepsilon_s g_{0,ss} (1 + e_{ss})]^2 + 2 \rho_s \varepsilon_s^2 d_s g_{0,ss} (1 + e_{ss}) \sqrt{\frac{\theta_s}{\pi}}$$

Radial distribution function:

$$g_{0,ss} = [1 - (\frac{\varepsilon_s}{\varepsilon_{s,max}})^{1/3}]^{-1}$$

Dissipation of granular temperature by gas damping:

$$\Phi_{gs} = -3\beta\theta_s$$

Section S3. The drag model used in this work.

Huilin-gidaspow drag model [3]:

Huilin-gidaspow drag model is a combination of the previous drag models proposed by Wen and Yu [4] and Ergun [5]. It introduces a transition function to smoothly switch the drag coefficients at the bed porosity of 0.8. The pressure drop due to friction between gas and particles is described by the Ergun equation [5] as the bed porosity is less than 0.8 and Wen and Yu equation as the bed porosity is larger than 0.8.

$$\beta_1 = 150 \frac{\varepsilon_s(1-\varepsilon_g)\mu_g}{\varepsilon_g d_a^2} + 1.75 \frac{\rho_g \varepsilon_s |\vec{v}_s - \vec{v}_g|}{d_a} \quad (\varepsilon_g \leq 0.8)$$

$$\beta_2 = \frac{3}{4} C_d \frac{\varepsilon_s \varepsilon_g \rho_g |\vec{v}_s - \vec{v}_g|}{d_a} \varepsilon_g^{-2.65} \quad (\varepsilon_g > 0.8)$$

$$\beta_{gs} = \beta_1 \quad (\varepsilon_g < 0.8)$$

$$\beta_{gs} = \varphi \beta_1 + (1 - \varphi) \beta_2 \quad (\varepsilon_g > 0.8)$$

$$\varphi = \frac{1}{2} + \frac{\arctan(262.5(\varepsilon_s - 0.2))}{\pi}$$

where drag coefficient is:

$$C_d = \frac{24}{Re_s} [1 + 0.15(Re_s)^{0.687}] \quad (Re_s < 1000)$$

$$Re_s = \frac{\rho_g d_a |\vec{v}_s - \vec{v}_g|}{\mu_g}$$

References

1. Johnson P C, Jackson R. Frictional-collisional constitutive relations for granular materials, with application to plane shearing. *Journal of Fluid Mechanics*, 1987, 176.
2. Gidaspow D. Multiphase Flow and Fluidization: Continuum and Kinetic Theory Description. *Journal of NonNewtonian Fluid Mechanics*, 1994, 55(2):207-208.
3. Huilin Lu, Gidaspow D, Bouillard J, et al. Hydrodynamic simulation of gas-solid flow in a riser using kinetic theory of granular flow. *Chemical Engineering Journal*, 2003, 95(1-3):1-13.
4. Wen C, Yu Y. A Generalised Method for Predicting Minimum Fluidization Velocity. *AIChE Journal*.1966, 12.
5. Ergun S. Fluid Flow through Packed Columns. *Chemical Engineering Progress*, 1952, 48:89-94.