

1 *Supporting Information*

2 **Porous carrageenan-derived carbons for efficient**  
 3 **ciprofloxacin removal from water**

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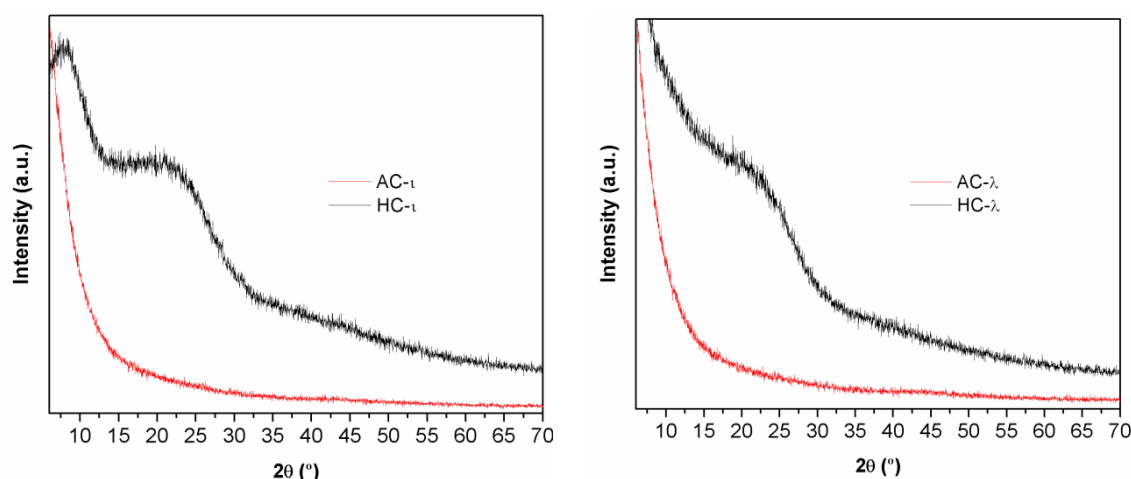
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13 **A. Characterization of carbon materials**



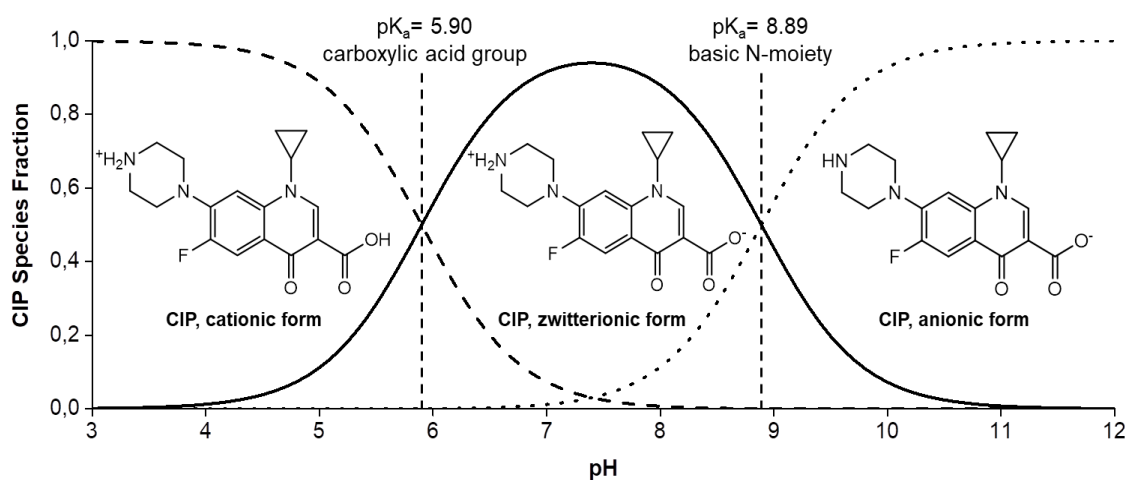
14 **Figure S1.** Powder XRD pattern of carrageenan ( $\iota$ - and  $\lambda$ -type; left and right, respectively) derived  
 15 carbons before (HC) and after activation (AC).

16 **Table S1.** Selected infrared bands ( $\text{cm}^{-1}$ ) for the materials and respective assignments<sup>a</sup>.

Assignment	Hydrothermal carbons			Activated carbons		
	HC- $\kappa$	HC- $\iota$	HC- $\lambda$	AC- $\kappa$	AC- $\iota$	AC- $\lambda$
$\nu(\text{O-H})$	3273 (vs)	3221 (vs)	3315 (vs)	--	--	--
$\nu(\text{C-H})$ aliphatic	2926 (s)	2922 (s)	2926 (s)	--	--	--
	2879 (s)	2879 (s)	2879 (s)	--	--	--
$\nu(\text{C=O})$	1693 (s)	1695 (s)	1695 (s)	--	--	--
$\nu(\text{C=C})$	1606	1606	1606	1560-1520	1560-1520	1560-1520
aromatic	(vs)	(vs)	(vs)	(vs)	(vs)	(m)
$\delta(\text{C-O})$	1290 (vs)	1292 (vs)	1298 (vs)	--	--	--
C-H aromatic	798 (s)	798 (s)	798 (s)	--	--	--

17 <sup>a</sup> vs – very strong; s – strong; m– medium;  $\nu$  – stretching vibration;  $\delta$  – deformation vibration

## 18 B. CIP Adsorption Modelling



19 Figure S2. Speciation of CIP [1,2]

20 Table S2. Isotherm models and parameters [3–6].

Model	Equation (non-linear form)	Parameters
Langmuir	$q_e = \frac{q_L K_L C_e}{1 + K_L C_e}$	$q_L$ is the monolayer adsorption capacity ( $\text{mg}\cdot\text{g}^{-1}$ ) $K_L$ is the Langmuir isotherm constant ( $\text{L}\cdot\text{mg}^{-1}$ ), related to the affinity of binding sites.
Freundlich	$q_e = K_F C_e^{\frac{1}{n}}$	$K_F$ is the Freundlich constant ( $\text{mg}^{(1-1/n)}\cdot\text{L}^{(1/n)}\cdot\text{g}^{-1}$ ) $1/n$ is the heterogeneity factor; $n$ is usually between 1 and 10 (dimensionless)
Sips	$q_e = \frac{N_T a C_e^m}{1 + a C_e^m}$	$N_T$ is the total number of binding sites ( $\text{mg}\cdot\text{g}^{-1}$ ) $a$ is related to the median binding affinity $k$ ( $a=k^m$ ) $m$ is the heterogeneous index (dimensionless, $0 < m < 1$ )

21

22 Table S3. Kinetic models and parameters.  $q_t$  and  $q_e$  ( $\text{mg}\cdot\text{g}^{-1}$ ) are the adsorption capacity at time  $t$  and  
23 equilibrium time, respectively [7,8].

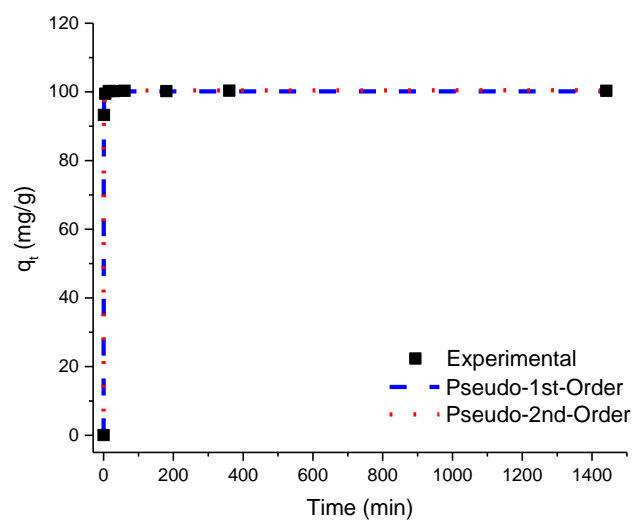
Model	Equation (non-linear form)	Parameters
Pseudo 1 <sup>st</sup> order	$q_t = q_e(1 - e^{-k_1 t})$	$k_1$ - equilibrium rate constant of pseudo 1 <sup>st</sup> order adsorption ( $\text{min}^{-1}$ ).
Pseudo 2 <sup>nd</sup> order	$q_t = \frac{k_2 q_e^2 t}{1 + k_2 q_e t}$	$k_2$ - equilibrium rate constant of pseudo 2 <sup>nd</sup> order adsorption ( $\text{g}\cdot\text{mg}^{-1}\cdot\text{min}^{-1}$ ).

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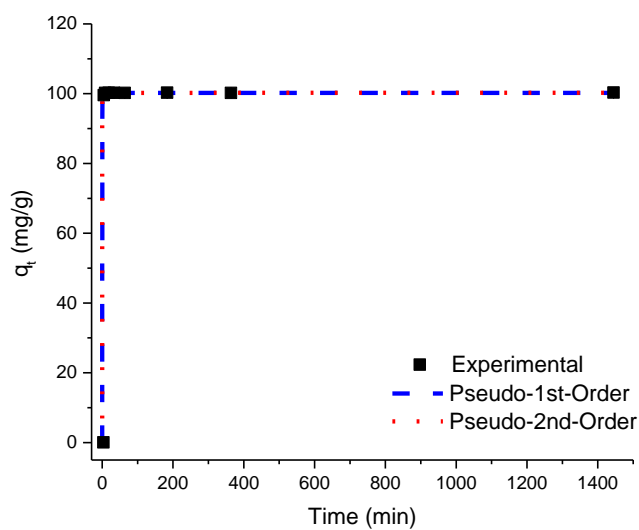
25 The goodness of the fittings was determined based on the calculation of the correlation  
26 coefficient ( $R^2$ ) (S1) and Chi-square test value ( $\chi^2$ ) (S2), expressed by the following equations  
27 respectively:

$$R^2 = 1 - \frac{\sum_{i=1}^n (y_i - \hat{y}_i)^2}{\sum_{i=1}^n (y_i - \bar{y})^2} \quad (\text{S1}) \quad \chi^2 = \sum_{i=1}^n \frac{(y_i - \hat{y}_i)^2}{\hat{y}_i} \quad (\text{S2})$$

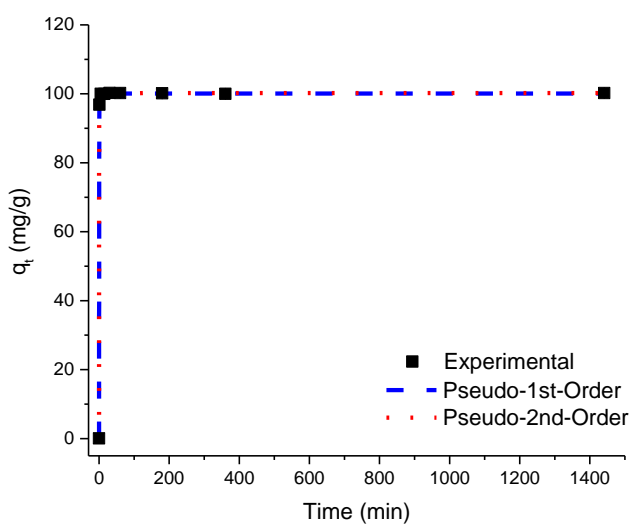
28 where  $y_i$  and  $\hat{y}_i$  are the experimental and model predicted values respectively,  $\bar{y}$  is the mean of the  
29 experimental data and  $n$  is the sample size.



(a)



(b)



(c)

30  
31

**Figure S3.** Time profile of CIP adsorption capacity over 24h and corresponding kinetic model fitting using pseudo 1<sup>st</sup> and pseudo 2<sup>nd</sup> order equations: AC-κ (a), AC-ι (b), AC-λ (c).

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53

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