

Article



## Broken Riceberry (BR) Powder Production Using a Double Drum Dryer and Its Utilization in the Development of Instant Beverages

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**Abstract:** This study was designed to examine broken riceberry (BR) powder production through the use of a double drum dryer. There were two stages involved: (1) to study the optimized drum drying conditions for BR powder using response surface methodology (RSM), and (2) to utilize BR powder for the development of instant beverages. According to the results, the optimum drum drying condition was a drum temperature of 125 °C and drum speed of 1.0 rpm. Under these conditions, BR powder contained moisture = 5.81%, water activity = 0.494, total color difference 15.45, DPPH scavenging activity = 73.93%, water solubility index (WSI) = 52.33%, and water absorption index (WAI) = 10.52. For the utilization of BR powder for developing instant beverages, the product quality was light purple in color, water activity = 0.354, DPPH scavenging activity = 45%, WSI = 65.75%, and WAI = 12.25. The developed instant beverage contained 4.28% moisture, 13.89% protein, 12.42% fat, 4.23% fiber, and 2.23% ash. The microbial properties were <10 CFU/g for aerobic plate count and yeast and mold. The overall liking score was 'like moderately'. This study indicated that the BR powder is of good quality and has potential in the beverage industry.

**Keywords:** broken riceberry powder; double drum dryer; product development; instant beverage; utilization; response surface methodology; optimization; antioxidant activity; sensory attributes

## 1. Introduction

Riceberry is one of the more valuable rice varieties in Thailand, with high antioxidant properties and other significant constituents offered to the consumers [1]. The consumption of riceberry is increasing because of its health benefits. Riceberry, or *Oryza sativa*, is a cross-bred rice strain with a deep purple appearance. Its origins involve the Jao Hom Nin variety of non-glutinous purple rice, noted for its antioxidant qualities, and the Khao Dawk Mali 105 variety of rice, noted for its fragrance [2]. Riceberry was original first produced by Kasetsart University in Thailand, at its dedicated Rice Science Center [3].

During the riceberry rice milling process, about 20–30% of rice grains break and become the major by-product known as rice grits or broken rice. A high proportion of broken riceberry (BR) is sold as raw material for animal feed or ingredients for food products at very low prices [4]. The principal by-products of rice production include rice bran, rice husk, and broken rice. These by-products each offer potential benefits as nutrients or through their medicinal properties. Although they are typically discarded during the process of milling, these by-products, especially the edible broken rice, can be used to create products such as rice flour, rice milk, rice starch, rice puddings, rice cakes, rice glue, and so forth. This is an important consideration given that it is anticipated that rice demand levels will remain high in the future as populations continue to rise in countries where rice is a staple [5].



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**Copyright:** © 2022 by the authors. Licensee MDPI, Basel, Switzerland. This article is an open access article distributed under the terms and conditions of the Creative Commons Attribution (CC BY) license (https:// creativecommons.org/licenses/by/ 4.0/). One key process employed to alter flour or starch to enhance its solubility and capacity to absorb water is pregelatinization. The procedure also improves the pasting property and makes storage more reliable, and so the technique allows the starch or flour to be used in various food products. The procedure requires heat which comes from a spray dryer or drum dryer, or in some cases an extruder [6]. Following the process of pregelatinization, there is a clearly notable change in the flour or starch in terms of its physicochemical and functional properties. It can be observed, for example, that after pregelatinization, the level of water absorption is enhanced along with the cold-water solubility when compared to the original starch or flour form [6]. A number of pregelatinization techniques exist, but the cheapest and simplest involves drum drying [7].

In the food sector, a double drum dryer is more commonly employed because of its greater suitability when used with different types of materials. This technique is highly suitable when used with liquid feedstock forms such as slurries, pastes, or solutions, and can help to create the finished product in the form of flakes or powders, making the approach different to other drying methods [8,9]. The resulting pregelatinized flour therefore has physicochemical properties which are governed by the raw material source and the parameters applied for the process of drum drying [6]. The applicable parameters comprised film thickness, feed rate, the surface temperature and speed of the drum, as well as the gap.

The outcomes when the drying temperature of the drum was altered in the range of 115–135 °C were investigated by Supprung and Noomhorm [10], who also conducted tests when varying the holding time (14–84 s) as well as the solid content of the slurry (20–40%) to assess the physicochemical properties of rice flour and starch obtained from Khao Dawk Mali 105 rice. It was discovered that with increasing solid content in the slurry, the rice flour and starch showed a decline in gelatinization degree, water absorption index, and the initial peak viscosity, whereas there was a rise in both the moisture content and water solubility index. When the holding times were extended, the degree of gelatinization also increased, but no significant influence in any variable was recorded in response to changes in the drum drying temperature.

Further work conducted by Ruttarattanamongkol et al. [11] used flours from orangeand purple-flesh sweet potato in testing their quality at different drum drying temperatures (80 °C, 95 °C, 110 °C) and speeds (3 rpm, 5 rpm, 7 rpm). The findings revealed a decline in both flour types' moisture content at lower drum speeds and higher drying temperatures. In the case of samples of sweet potato flour for which the drum speed was 3 rpm and the drying temperature was 95 °C, the highest levels of antioxidant activity and phenolic content were recorded. However, further increasing the drying temperature to 110 °C resulted in a significant drop in both antioxidant activity and phenolic content, potentially as a consequence of phenolic compound degradation which normally takes place at higher temperatures.

Wiriyawattana et al. [12] made similar findings when assessing the influence of the drum drying process upon pregelatinized riceberry flour in terms of the antioxidant properties and other physical qualities. When the drum dryer was employed to produce the pregelatinized riceberry flour, the color was then darker and the WAI (water absorption index) and SP (swelling power) values increased, although the viscosity was found to be lower than was the case for the unheated riceberry flour. As the drum drying temperatures were further increased (110–130 °C), these changes became more apparent, although it was also noted that there is also a reduced capacity for pregelatinized riceberry flour, a drum drying temperature of 110 °C brought about smaller decreases in total phenolic content and antioxidant activity than was the case at greater temperatures of 120 °C and 130 °C.

This current research sought to produce a novel instant beverage based on riceberry powder. This first required the riceberry to be milled to produce the powder prior to drum drying for pregelatinization. The resulting pregelatinized riceberry flour could then be employed to create the instant beverage. At different drum drying temperatures and drum speeds, the heat involved would affect the physical properties of the riceberry powder along with its antioxidant qualities to varying extents. This study aimed to establish with greater precision the effects of the drum drying process when varying the drum speeds or temperatures because the literature contains little information in this area, especially in the context of developing instant beverages.

## 2. Materials and Methods

### 2.1. Materials

In this study, the broken riceberry (BR) was supplied by the Allricesurin Brand, located in Surin Province, Thailand. Full fat milk powder, fiber creamer, cocoa powder, vanilla powder, and pandan powder were purchased from local markets in Prachinburi province. Erythritol and sucralose were purchased from Krungthepchemi Co., Ltd., Bangkok, Thailand.

### 2.2. Reagents

Sigma-Aldrich (St. Louis, MO, USA) supplied the 1,1-diphenyl-2-picrylhydrazyl (DPPH) employed in this research, while the remainder of the chemicals used were all of analytical grade.

# 2.3. Study of the Optimal Process Conditions of Broken Riceberry (BR) Powder Using a Double Drum Dryer

The process for preparing BR powder (Figure 1) involved washing and soaking the BR in the ratio of rice to water of 1:2 w/w for 4 h, then draining off the water. The BR was then blended with water (ratio of BR to water, 1:10) using a food processor (Sharp, EM-ICE2, Samutprakarn, Thailand) for 5 min at a speed of 17,000 rpm. It was then heated to 80 °C for 40 min with a 1700-W electric hot plate (Imarflex, IF-404, Bangkok, Thailand) before subsequently drying using a double drum dryer (electric heating, DD-D6L12-HT-INV, Bangkok, Thailand). A centrifugal mill was then used for the milling process (Retsch, ZM 200, Haan, Germany) prior to sieving using No.140 mesh to achieve particle sizes of 105  $\mu$ m.

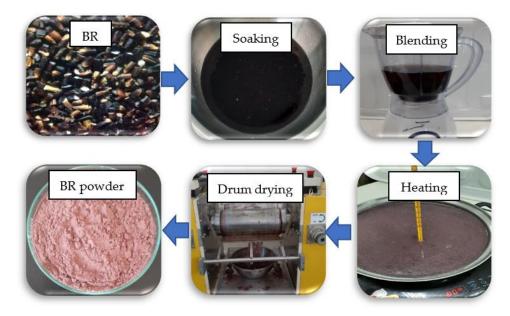


Figure 1. The process of preparing BR powder and its product.

A full factorial design consisting of three levels with two variables  $(3^2)$  was used to measure the effects upon the process conditions of the drum temperature and rotation speed, making use of three central point replicates. Replicate center points are useful (1) to estimate pure error for a lack-of-fit test, (2) to provide a measure of process stability and inherent variability, and (3) to check for curvature in the response model [13]. The

independent variables were the drum temperature (120 °C, 125 °C, 130 °C) and the drum rotation speed (0.6, 0.8, 1.0 rpm), while the spacing between the two rollers was 0.10 mm.

The quality analysis of BR powder was conducted. Evaluation of the moisture content (AOAC 925.10) calculated based on weight loss after oven-drying at 130 °C followed the guidelines established by the Association of Official Analytical Chemistry [14]. The product water activity was measured with a water activity meter (AQUA LAB Model series 3TE) obtained from Meter Group, Inc. (Pullman, WA, USA). The color was evaluated using a colorimeter (Hunter Lab Model Colorflex 45/0) from Konica Minolta (Vienna, VA, USA) in the CIE Lab system using CIE Standard Illuminate D65, di:8, and CIE:2 Standard Observer, where L\* indicates lightness; a\* and b\* show opposing color coordinates, whereby negative a\* is green and positive a\* is red; and negative b\* represents blue and positive b\* represents yellow. It is then possible to calculate the total color difference ( $\Delta E$ ) to compare the color ( $L_1^*$ ,  $a_1^*, b_1^*$ ) of BR prior to drying with the color ( $L_2^*$ ,  $a_2^*, b_2^*$ ) of BR after drying by following Equation (1):

$$\Delta E = \sqrt{\left[ \left( L_2^* - L_1^* \right) + \left( a_2^* - a_1^* \right) + \left( b_2^* - b_1^* \right) \right]} \tag{1}$$

Performance of the DPPH scavenging assay followed the approach of Daiponmak et al. [15], while the guidelines offered by Anderson et al. [16] were used to determine WSI (water solubility index) and WAI (water absorption index).

The response variables (moisture content ( $Y_1$ ), water activity ( $Y_2$ ), total color difference ( $\Delta E$ ) ( $Y_3$ ), DPPH scavenging activity ( $Y_4$ ), WSI ( $Y_5$ ), and WAI ( $Y_6$ )) are represented using the second-degree polynomial shown in Equation (2) as follows:

$$Y_{i} = \beta_{0} + \sum_{i=1}^{2} \beta_{i} x_{i} + \sum_{i=1}^{2} \beta_{ii} x_{i}^{2} + \sum_{i< j}^{2} \beta_{ij} x_{i} x_{j}$$
<sup>(2)</sup>

where  $Y_i$  is the response variable  $(Y_1-Y_6)$ ,  $\beta_0$  is a constant,  $\beta_i$  are regression coefficients associated with linear effects,  $\beta_{ij}$  are regression coefficients associated with interaction effects, and  $\beta_{ii}$  are regression coefficients associated with quadratic effects. Meanwhile, the coded levels of  $X_i$  and  $X_j$  show the drum temperature (X<sub>1</sub>) and drum rotation speed (X<sub>2</sub>) as recorded in the experiments. Minitab Statistical software (Minitab Pty Ltd., Inc., Sydney, Australia) was used to design the experiments and to use the second-order polynomial equations to develop the response surface graphs on the basis of the experimental data. The desirability function was then used in the simultaneous optimization procedure so as to emphasize water activity < 0.6 and moisture content < 7% in line with Thai Industrial Standard No. 315-2005. In addition, the optimization of drum drying conditions was considered for high antioxidant activity, WSI, and WAI with a low total color difference indicating good BR powder quality. The suitability of the second-order polynomial model fit was demonstrated through a contour plot, revealing the associations between experimental levels and responses in the case of each of the study variables.

The BR powder sample was produced in three replicates. The product analyses were conducted in triplicate (n = 3). Analysis of variance and significant differences among means and correlation analysis were performed with one-way ANOVA. The significant level was based on the total error criteria with a confidence level of 95%.

## 2.4. Study of the Utilization of Broken Riceberry (BR) Powder for the Development of Instant Beverages

The utilization of BR powder was applied in instant beverages as a food model. The basic formulation of the instant beverage was selected as described by Yuthavisuthi et al. [17]. Jasmine brown rice powder and Job's tears powder were substituted by BR powder. Non-dairy creamer was substituted by fiber creamer. Three flavors (cocoa powder, vanilla powder, and pandan powder) were developed in formulations (Table 1). The prototypes of instant beverages using BR powder were prepared by mixing all dried ingredients using a cubic mixer (SEG, NANA-191940, Bangkok, Thailand). They were then tested by 50 untrained panel members, who were asked to rate the formulas by allocating scores on a 9-point hedonic scale (1 = extreme dislike to 9 = extreme like) in terms of color,

odor, flavor, and overall liking score [18]. Each instant beverage (in a sachet) was brewed with hot water (ratio of instant beverage to hot water = 25 g/120 mL) and subsequently an amount of 20 mL was poured into a 1 oz. plastic cup with a lid. Three different instant beverage sample types were prepared and then coded with a three-digit random number and served to each panelist at 65–75 °C [17].

Ingredient	Formulation A (%)	Formulation B (%)	Formulation C (%)
BR powder	52.50	52.50	52.50
Full fat milk powder	16.00	16.00	16.00
Fiber creamer	29.55	29.55	29.55
Erythritol	3.50	3.50	3.50
Sucralose	0.05	0.05	0.05
Cocoa powder	1.30	-	-
Vanilla powder		1.30	-
Pandan powder		-	1.30

Table 1. Instant beverage formulations from BR powder in various flavors.

Data were analyzed with SPSS<sup>®</sup> version 26.0 (SPSS Inc. and IBM Co., Chicago, IL, USA) based on one-way ANOVA procedure. Results are displayed as mean  $\pm$  standard deviation.

## 2.5. Quality Analysis of the Developed Instant BR Beverage

The qualities of the developed instant BR beverage were determined in terms of water activity (AQUA LAB Model series 3TE), color values (CIE, L\* a\* b\* values), water solubility index (WSI), and water absorption index (WAI) [16]. Proximate analysis (moisture, crude fat, crude ash, crude protein, crude fiber) was carried out in line with the guidelines of the Association of Official Analytical Chemistry [14]. To determine moisture content (AOAC 925.10), samples were dried using oven-drying at 130 °C to constant weight. Crude fat (AOAC 948.15) was determined using the Soxhlet extraction method with diethyl ether as solvent using Soxhlet extraction apparatus (Gerhardt, EV16, Konigswinter, Germany). Crude ash (AOAC 923.03) was determined using incineration in muffle furnace at 550 °C (Carbolite, AAF1100, Neuhausen, Germany). Crude protein (AOAC 920.87) was determined using the Kjeldalh method using distillation unit (Gerhardt, Vapodest 30s, Konigswinter, Germany). Crude fiber (AOAC 978.10) was determined as the organic residue after sequential digestion with 1.25% H<sub>2</sub>SO<sub>4</sub> and with 1.25% NaOH using fiber extraction unit (Gerhardt, EV1, Konigswinter, Germany). The equation given below was then employed to determine the carbohydrate content:

Carbohydrate (%) = 100 - (moisture % + crude fat % + crude protein % + crude fiber % + crude ash %) (3)

The product quality was evaluated by microbial aerobic total plate count, yeast, and mold following the Bacteriological Analytical Manual methods [19]. Percentage of inhibition for antioxidant activity was evaluated using the DPPH scavenging assay in line with the approach of Daiponmak et al. [15].

## 3. Results and Discussion

## 3.1. Model Fitting

The mean value of moisture content, water activity ( $a_w$ ), total color difference ( $\Delta E$ ), DPPH, WSI, and WAI of the 11 process conditions, with triplicates in the central point of the independent variables, varied from 4.55–8.43%, 0.232–0.549, 13.60–18.58, 58.62–80.26, 32.10–53.09, and 6.25–11.55, respectively (Table 2). The coefficients of the second-degree polynomial equation (Table 3) were determined on the basis of the data obtained through the experiments, while the R<sup>2</sup> value for the moisture content response, water activity ( $a_w$ ), total color difference, DPPH, WSI, and WAI were 0.955, 0.972, 0.943, 0.892, 0.965, and 0.941, respectively. Joglekar and May [20] suggested that for a good fit of a model, R<sup>2</sup> should be

at least 0.80. This would mean that the model could be used to predict the response. In the case of a high regression coefficient and small *p*-value, it can be argued that the effect upon the response variable in question would be of greater significance [21]. To determine the model suitability for each of the different responses, a lack-of-fit test was carried out. The resulting *p*-value was found to be greater than the 0.05 threshold, thus demonstrating that an adequate fit was offered for the experimental data by the model, as can be observed in Table 3.

**Table 2.** Structure of the factorial design and the dependent variable responses under drum drying process conditions (independent variables).

	Independent Variables			Dependent Variables <sup>b</sup>				
Test Run <sup>a</sup> No.	Drum Temp. (°C)	Drum Speed (Min)	Moisture Content (%)	a <sub>w</sub>	(Δ <i>E</i> )	DPPH (%Inhibition)	WSI (%)	WAI
	X1	X <sub>2</sub>	Y <sub>1</sub>	Y <sub>2</sub>	Y <sub>3</sub>	Y <sub>4</sub>	Y <sub>5</sub>	Y <sub>6</sub>
1	120	0.6	5.55	0.241	16.00	70.55	32.10	6.25
2	120	0.8	7.35	0.427	15.32	71.57	40.38	8.01
3	120	1.0	8.43	0.435	13.60	80.26	46.72	8.79
4	125	0.6	5.14	0.232	17.25	65.19	35.07	7.53
5	125	1.0	6.02	0.509	15.16	72.47	51.76	10.29
6	130	0.6	4.55	0.244	18.58	58.62	35.64	7.76
7	130	0.8	4.73	0.402	18.21	65.21	39.98	9.09
8	130	1.0	5.21	0.549	18.40	71.84	53.09	11.55
9	125	0.8	5.25	0.449	15.93	72.51	39.38	7.80
10	125	0.8	5.44	0.422	15.45	72.19	39.77	7.63
11	125	0.8	4.93	0.445	15.00	73.79	38.07	8.23

Note: <sup>a</sup> Test runs were carried out randomly. <sup>b</sup> Based on triplicate measurements. Standard deviation (SD) range was 0.001–1.23.

	Table 3. ANOVA (a	analysis of	variance)	of the de	pendent varia	ole predictive	e regression mod	lel.
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Predictive Regression Model of Responses	R <sup>2</sup>	Source of Variation	<i>p</i> -Value
Y <sub>1</sub> : Moisture content =340.7930 - 5.5998X <sub>1</sub> + 68.1952X <sub>2</sub> + 0.02326X <sub>1</sub> <sup>2</sup> + 3.0395X <sub>2</sub> <sup>2</sup> - 0.5550X <sub>1</sub> X <sub>2</sub>	0.955	Model Lack of fit	0.002 * 0.300
$\overline{Y_2: a_w} = -6.8296 + 0.1124X_1 - 0.5358X_2 - 0.0005X_1^2 - 1.4290X_2^2 + 0.0278X_1X_2}$	0.972	Model Lack of fit	0.001 * 0.188
Y <sub>3</sub> : Total color difference ( $\Delta E$ ) =567.1850 - 8.5990X <sub>1</sub> - 84.8561X <sub>2</sub> + 0.0340X <sub>1</sub> <sup>2</sup> + 7.2434X <sub>2</sub> <sup>2</sup> + 0.5550X <sub>1</sub> X <sub>2</sub>	0.949	Model Lack of fit	0.003 * 0.445
$\begin{array}{l} \hline Y_4: DPPH \\ = -588.7650 + 11.6103X_1 - 49.3020X_2 - 0.0528{X_1}^2 - 22.0066{X_2}^2 + 0.8775X_1X_2 \end{array}$	0.892	Model Lack of fit	0.019 * 0.062
$\overline{Y_5: WSI} = -89.3051 + 2.5484X_1 - 166.0150X_2 - 0.0112X_1^2 + 73.8816X_2^2 + 0.7075X_1X_2}$	0.965	Model Lack of fit	0.001 * 0.148
Y6: WAI =109.3600 - 1.5164X <sub>1</sub> - 51.6664X <sub>2</sub> + 0.0058X <sub>1</sub> <sup>2</sup> + 12.6118X <sub>2</sub> <sup>2</sup> + 0.3125X <sub>1</sub> X <sub>2</sub>	0.941	Model Lack of fit	0.009 * 0.244

Note: \* Statistical significance is indicated when  $p \le 0.05$ .

### 3.2. The Effect of Drum Temperature and Drum Rotation Speed on Dependent Variables

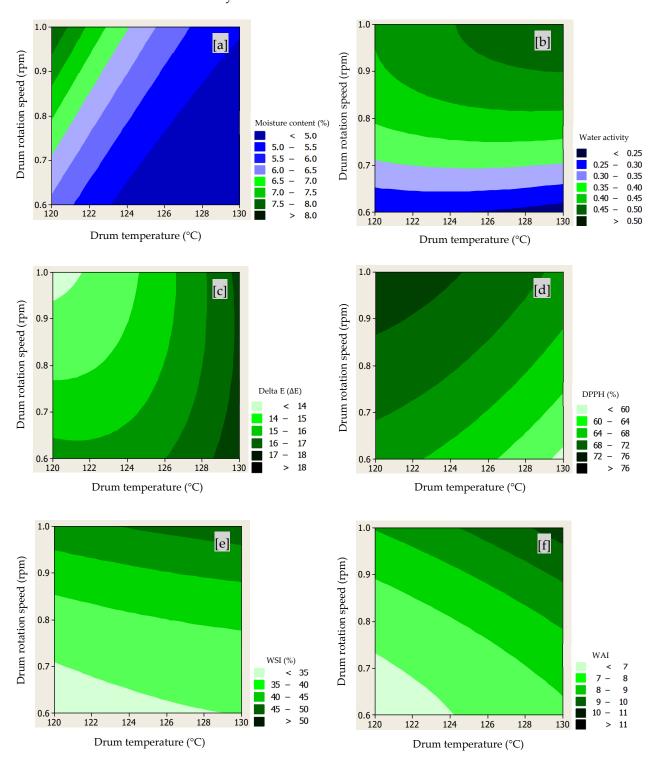
The factual model is plotted as a two-dimensional surface representing the response (moisture content, a<sub>w</sub>, total color difference, DPPH, WSI, and WAI) (Figure 2). Figure 2a,b illustrate contour plots showing the effect of drum drying conditions on the water activity and the moisture content, indicating a reduction in both values with increasing drum temperature and decreasing drum rotation speed. Increasing the drum surface temperatures and decreasing drum rotation speeds allowed the BR slurry to come into contact with the

drum surface for a longer period of time, making it possible to increase the dehydration rate of the water in the BR powder. Similar results have been reported in previous studies on jackfruit seeds [22]. The total color difference of BR powder increased with increasing drum temperature and decreasing drum rotation speed (Figure 2c). On the other hand, the antioxidant activity (DPPH) of BR powder decreased with increasing drum temperature and decreasing drum rotation speed (Figure 2d). Changes in total color difference of BR powder and antioxidant activity may have been the result of the changes in the material surface areas which were contacted when subjected to high temperatures as part of the drum drying procedure. Furthermore, the changes in color can be brought about through chemical reactions which result from the thermal treatment, such as the Millard reaction. An increase in the heating time and temperature could enhance the browning reaction. At high temperatures, it was also observed that antioxidant activity declined significantly. This matched the findings of Kullamathee et al. [23], who revealed that following the process of drum drying, there was a notable decrease in total polyphenol content as well as the DPPH scavenging activity recorded for the young rice flakes. To show the effects of the drum drying conditions, a contour plot of WSI and WAI is shown in Figure 2e,f. For water solubility index (WSI), it was found that the water solubility index increased when the drum rotation speed and the drum temperature increased. Using a high drum drying temperature caused the BR powder to have a more porous appearance and increased the contact area with the water. Thus, it improved the water solubility [24,25]. In a similar result, the water absorption index of BR powder increased when the drum rotation speed and the drum surface temperature increased (Figure 2f). This may occur due to the carbohydrate content of riceberry rice when heated to high temperatures. Therefore, the hydrogen bonds between the starch molecules are broken, which can trap more water, resulting in the BR powder absorbing water well. The influence of drum drying upon both the physical properties and the antioxidant capabilities of pregelatinized riceberry flour was examined by Wiriyawattana et al. [12], who found that the WSI and SP (swelling power) could reach a much higher level than was the case for riceberry flour samples which had not been heated. It was possible to assess the volume of water within the granules or starch polymers using WAI to serve as an indicator once the maximum amount of water had been absorbed. As moisture content rose, typically as a consequence of gelatinization and lateral expansion of the starch, WSI would also increase [26].

#### 3.3. Optimized Drum Drying Conditon and Verification

Parameters governing the process of drum drying, including feed rate, film thickness, the gap between drums, drum surface temperature, and drum rotation speed serve to ensure that the physicochemical properties of the film remain constant on the drum surface, resulting in suitably consistent levels of final moisture content in the pregelatinized powder [27,28].

The desirability function was then used in the simultaneous optimization procedure so as to emphasize water activity < 0.6 and moisture content < 7% in line with Thai Industrial Standard No. 315-2005. In addition, the optimization of drum drying conditions was considered for high antioxidant activity, WSI, and WAI with a low total color difference that indicated good BR powder quality. From the results, the optimized drum drying conditions were determined as drum temperature and drum rotation speed of 125 °C and 1.0 rpm, respectively. Under these conditions, moisture content, water activity, total color difference, DPPH scavenging activity, water solubility index (WSI), and water absorption index (WAI) (predicted values) were calculated from predictive regression model (Table 3) as 6.11%, 0.511, 15.32, 75.74%, 50.54%, and 10.44, respectively. The verification studies were carried out to validate the optimization. Using optimized drum drying conditions, we produced a BR powder that contained moisture content =  $5.81 \pm 0.25\%$ , water activity =  $0.494 \pm 0.002$ , total color difference  $15.45 \pm 0.87$ , DPPH scavenging activity =  $73.93 \pm 2.33\%$ , water solubility index (WSI) =  $52.33 \pm 1.20\%$ , and water absorption index (WAI) =  $10.52 \pm 0.32$ . The observed and predicted values were within the small error range (0.8–4.9\%) and did



not vary at 5% level of significance, meaning that the response model was appropriate for the optimization [29]. Therefore, this BR powder was utilized in instant beverages for further study.

**Figure 2.** Contour plots for (**a**) moisture content, (**b**)  $a_w$ , (**c**) Delta E ( $\Delta$ E), (**d**) DPPH, (**e**) WSI, and (**f**) WAI as a function of drum temperature and drum rotation speed.

### 3.4. The Utilization of BR Powder for the Development of Instant Beverages

Three formulas of instant beverages from BR powder were developed in different flavors. The sensory evaluation using a nine-point hedonic scale indicated that the lik-

ing score of instant beverages in terms of odor, flavor, and overall liking of the different three flavors (cocoa flavor, vanilla flavor, and pandan flavor) showed significant differences ( $p \le 0.05$ ). In contrast, the color liking scores of the three flavors showed no significant differences (p > 0.05) (Table 4). Formulation B (vanilla flavor) was the best in sensory attributes and received the highest liking score in terms of color (6.6 = like moderately), odor (6.8 = like moderately), flavor (6.8 = like moderately), and overall liking (7.3 = like moderately).

Treatment	Color <sup>ns</sup>	Odor	Flavor	Overall Liking
Formulation A (Cocoa flavor)	$6.4\pm0.6$	$6.0\pm0.4$ <sup>b</sup>	$6.0\pm0.6$ <sup>b</sup>	$6.3\pm0.6$ <sup>b</sup>
Formulation B (Vanilla flavor)	$6.6\pm0.8$	$6.8\pm0.6$ a	$6.8\pm0.2$ a	$7.3\pm0.2$ a
Formulation C (Pandan flavor)	$6.5\pm0.4$	$6.6\pm0.2$ a	$6.3\pm0.6~^{ m ab}$	$6.5\pm0.5$ b
Commercial brand (Natural flavor)	$6.5\pm0.6$	$6.6\pm0.6$ a	$6.6\pm0.4$ a	$6.7\pm0.4$ <sup>b</sup>

Table 4. Sensory properties of instant beverage from BR powder in various flavors.

Notes: <sup>ab</sup> . . . Mean values of the same column with different superscripts are significantly different ( $p \le 0.05$ ) <sup>ns</sup> Not significantly different.

The comparative liking score of sensory attributes of our formulated instant BR beverage and commercial brand revealed that liking score of formulation B was higher than the commercial brand for all attributes, indicating its overall acceptability. Thus, formulation B appeared to be preferable to the commercial brand in terms of all sensory attributes. Similar to our result, Sutinium et al. [30] developed an instant nutritious beverage from germinated jasmine brown rice and reported the overall liking score as 7.3 (like moderately). Therefore, the formulation B was chosen for further analysis.

#### 3.5. The Developed Instant Beverage Quality

The developed instant beverage was a fine powder that was light purple in color (L\* = 72.10  $\pm$  0.62, a\* = 6.76  $\pm$  0.19, and b\* = 4.43  $\pm$  0.08), and after dissolving in hot water it turned slightly darker. For the physical analysis, the water activity of the instant beverage was 0.354, which made it safe from spoilage caused by microorganisms [31]. The water solubility index of the instant beverage was 65.75  $\pm$  1.08%, with a 12.25  $\pm$  0.87 water absorption index. The developed instant beverage contained 4.28  $\pm$  0.25% moisture, 13.89  $\pm$  0.79% protein, 12.42  $\pm$  1.05% fat, 4.23  $\pm$  0.23% crude fiber, and 2.23  $\pm$  0.15% ash. The DPPH scavenging activity was 45% inhibition. Measurements for microbial properties were <10 CFU/g of aerobic plate count and <10 CFU/g of yeast and mold. This was within the limits recommended under the microbial standards set in the Thai Industrial Standard No. 315-2005.

## 4. Conclusions

In conclusion, BR powder was produced under optimized drum drying conditions at drum temperature = 125 °C and drum rotation speed = 1.0 rpm. These optimized conditions provided <7% moisture content and <0.6 water activity of the BR powder. This conformed to Thai Industrial Standard No. 315-2005. The BR powder was high in DPPH scavenging activity, WSI, and WAI, and low in total color difference. From the practical point of view, the utilization of BR powder can be developed as an instant beverage with good taste and quality. However, further studies should be conducted to investigate the utilization of BR powder such as instant porridge, bakery products, or Thai desserts in order to add greater value to the BR powder.

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