

Article

Extraction of Phosphorous from a Phosphorous-Containing Vanadium Titano-Magnetite Tailings by Direct Flotation

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Abstract: In this study, there is 1.42% P₂O₅ in the P-containing V-Ti magnetite tailings in Miyi Region of China, with the valuable minerals mainly including apatite, and aluminosilicate minerals as the main gangue components. The direction flotation process was used to recover phosphorous from the low-grade phosphorous-bearing V-Ti magnetite tailings. The results showed that an optimized phosphorous concentrate with a P₂O₅ grade of 31.35% and P₂O₅ recovery of 88.02% was obtained by flotation process of one roughing, three scavengings, and three cleanings under roughing conditions, which employed pulp pH of 9, grinding fineness of <0.039 mm occupying 90%, flotation concentration of 25%, and dosages of carboxymethylcellulose, oxidized paraffin wax soap, and pine oil of 400 g/t, 300 g/t, and 20 g/t, respectively. Optimized one scavenging, two scavenging, and three scavenging conditions used a pulp pH of 9, and dosages of carboxymethylcellulose, oxidized paraffin wax soap, and pine oil of 200 g/t, 150 g/t, 10 g/t; 100 g/t, 75 g/t, and 5 g/t; and 100 g/t, 75 g/t, and 5 g/t, respectively. Optimized one cleaning, two cleaning, and three cleaning condition dosages of carboxymethylcellulose of 100 g/t, 50 g/t, and 25 g/t, respectively. Study of analysis and characterization of phosphorous concentrate by X-ray diffraction (XRD), scanning electron microscopy (SEM), and energy dispersive spectroscopy (EDS) show that most gangue minerals enter the flotation tailings, the main minerals in phosphorous concentrate are apatite, olivine, and feldspar.

Keywords: phosphorous; apatite; vanadium titano-magnetite tailings; direct flotation

1. Introduction

Phosphorus is an important non-metallic mineral resource, which is widely used in agriculture, chemical industry, medicine, food, and other industrial sectors. The global phosphate mineral resources are very rich, but the distribution is extremely uneven, among which the phosphate mineral reserves in Morocco and Western Sahara, China, and Syria account for more than 80% of the total proved phosphorus reserves in the world. With the continuous exploration and development of global phosphate ore, high grade of P₂O₅ and low harmful impurities of high-quality phosphate ore resources are gradually decreasing, the overall development of global phosphate ore resources is developing towards the direction of low-quality phosphate ore resources [1].

According to the statistical data of the international fertilizer organization, it was concluded that the decline in the global raw ore quality leads to the continuous decline in the proportion of the world's P_2O_5 grade to more than 32% of the high-quality commodity phosphate ore. P_2O_5 grade has been an important supply source of phosphorus around the world in recent years. P_2O_5 grade and below 30% of the proportion of phosphate ore development is continuing to increase, and this is expected to take a very important market share in the future. Although in the long run, the global phosphate mining is developing towards the direction of low-quality phosphate mining, in the short term, with the large-scale development of high-quality phosphate mining in Morocco and other countries in North Africa, the global high-quality phosphate mining resources will account for a relatively large proportion of the development [2–5].

There are about 120 kinds of known phosphate minerals in nature, which are widely distributed. The earth could be a phosphorus resource and utilization of phosphate rock minerals if apatite, in igneous, sedimentary, metamorphic ore deposits are formed, its output accounts for about 95% of the total output. Apatite minerals can form the base for five kinds of mineral deposits: Fluorapatite, hydroxyapatite, carbon hydroxyapatite, francolite, and kursk stone. Other available phosphate minerals include refractory svanbergite, struvite, and blue-iron stone. The average grade of phosphorus resources in China is low, and it contains high impurities such as MgO , Al_2O_3 , and Fe_2O_3 , which is difficult to select. The phosphate ore dressing process mainly includes scabbing-stripping, flotation, and heavy medium dressing. In 2018, the national average recovery rate was 86.1%, among which the average recovery rate was 94.3% for the cleaning and desilting process, 86.9% for the flotation process, and 83.5% for the heavy medium processing process. Due to the different occurrence conditions of phosphate ore resources, the grade of phosphate ore in the main phosphate ore areas is quite different. The grade of phosphate ore in Hubei province is about 20%, and in the Yunnan and Guizhou provinces it is 24%. With the continuous exploitation of phosphate ore resources, the ore grade is decreasing. Theoretically, the technology of phosphate ore grade reduction is feasible, but economic rationality is the key factor [6–8].

According to the mineralogical characteristics of phosphate ore, the phosphate ore treatment process includes flotation, attrition scrubbing and desliming, electrostatic separation, magnetic separation, gravity separation, acid leaching, and calcination. The application of attrition scrubbing and desliming, magnetic separation, and gravity separation should be referred to the characteristics of the phosphate ores in chemical composition and texture. In that case, the pre-concentration of valuable minerals and cost reduction are achieved. For example, coarser phosphate concentrates are obtained when using attrition scrubbing, desliming, and gravity separation to beneficiate weathered phosphate ores and banded structural sedimentary phosphate ores, respectively. Subsequently, the ultrafine components and overflow products are subjected to flotation for the further recovery of phosphate minerals. Due to the high efficiency in the removal of silicate and carbonate gangue minerals, froth flotation is dominantly employed for the beneficiation of phosphate ore, especially for low-grade sedimentary phosphate rocks. Generally, direct flotation by anionic surfactants or reverse flotation by cationic surfactants are conducted to remove the silicate gangues from phosphate. The phosphate ores mainly contain the siliceous phosphate rock, calcareous phosphate rock, and calcareous-siliceous phosphate rock. Both of the anionic direct flotation and cationic reverse flotation are applied for the beneficiation of siliceous phosphate rock, while the single anionic reverse flotation is preferred to beneficiate the calcareous phosphate rock [9–14].

Apatite in V-Ti magnetite ore is a kind of accessory mineral widely distributed. The content of apatite varies greatly in different ores in different mining areas and ore sections. It is mainly concentrated in gabbro type ores, while other types are only distributed sporadically or rarely appear. The content of apatite in Taihe and Hongge mining areas is relatively high, generally 1% to 9%. Although the grade of associated phosphorus in vanadium titanium magnetite tailings in Panxi is low, and it may be a valuable element for comprehensive utilization due to its certain enrichment channels, which can promote the economical and intensive utilization of resources. After the comprehensive utilization of phosphate

minerals, the content of phosphate minerals in tailings will be further reduced, which can reduce the pollution of soil caused by phosphorus in tailings. At the same time, the comprehensive utilization of phosphorus can effectively promote the new round of research on associated valuable elements in the Miyi region of China, and has a certain promoting effect on improving the comprehensive utilization process of V-Ti magnetite resources [15–19].

2. Materials and Methods

2.1. Sampling

The ore samples used in this study were from a low-grade phosphorus-containing vanadium titano-magnetite tailings produced by a concentrator in Miyi region after recovering iron and titanium using magnetic separation and flotation. The particle size was between 0.019 and 3.0 mm. It was found that the blend ore samples were all caused by fine-grained caking. In order to ensure that the sample is representative, the agglomerated samples were crushed and then shrunk in advance for reserve. The main chemical composition analysis of the P-bearing V-Ti magnetite tailings is shown in Table 1, and the grain size analysis of the samples is shown in Table 2. The main mineral composition of the P-bearing V-Ti magnetite tailings is shown in Figure 1. The content of silicoaluminite mineral is higher, and the main minerals contain apatite, hornblende, feldspar, serpentine, chlorite, mica, quartz, dolomite, and calcite in the vanadium titano-magnetite tailings.

Table 1. Main chemical composition analysis of the P-Containing V-Ti magnetite tailings (%).

Fe	TiO ₂	S	P ₂ O ₅	Na ₂ O	K ₂ O	CaO	Al ₂ O ₃	MgO	SiO ₂
6.73	2.73	0.132	1.42	6.29	1.06	12.86	22.29	13.67	30.73

Table 2. A grain size analysis of the P-Containing V-Ti magnetite tailings (%).

Fraction (mm)	Yield		P ₂ O ₅ Content	P ₂ O ₅ Distribution
	Individual	Cumulative		
−5.00~+3.00	3.56	3.56	0.56	1.39
−3.00~+2.00	4.18	7.74	0.78	2.27
−2.00~+1.00	6.99	14.73	0.43	2.10
−1.00~+0.50	9.23	23.96	1.12	7.21
−0.50~+0.25	8.36	32.32	0.79	4.61
−0.25~+0.154	10.67	42.99	1.02	7.60
−0.154~+0.100	15.22	58.21	0.99	10.51
−0.100~+0.074	10.96	69.17	1.05	8.03
−0.074~+0.038	12.33	81.5	2.23	19.18
−0.038~+0.019	11.22	92.72	2.89	22.62
−0.019~0	7.28	100	2.85	14.48
Totals	100.00		1.43	100.00

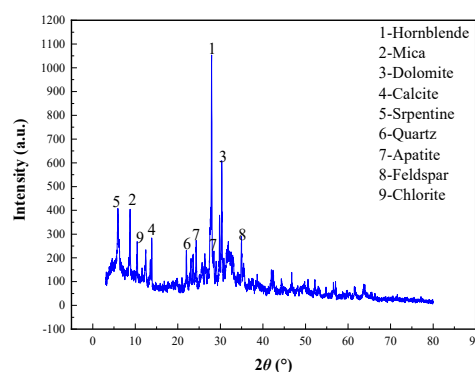


Figure 1. XRD diffractograms of the P-Containing V-Ti magnetite tailings.

2.2. Flotation Reagent and Equipment

The main chemical reagents used in this experiment are oleic acid, oxidized paraffin soap, hydroxamic acid, benzyl arsenic acid, sodium bicarbonate, lime, sodium carbonate, sodium hydroxide, sodium hexametaphosphate, carboxymethylcellulose (CMC), sodium fluosilicate, and sodium silicate, all of which have analytical purity and a producing area Shanghai AiBi Chemistry Preparation Co., Ltd., Shanghai, China.

The main equipment used in the flotation test included an XFD-1.5 L machine (Jinlin Exploration Machinery Plant, Changchun, China), an XFD-1.0 L hanging tank flotation machine (Jinlin Exploration Machinery Plant, Changchun, China), a cone ball mill (XMQ— Φ 240 \times 90 mm, Jilin Exploration Machinery Factory, Changchun, China), disc grinder (Φ 300 \times 150 mm, Jilin Exploration Machinery Factory, Changchun, China), drying box (Shanghai Shiyan Yan Electric Furnace Co., Ltd. Shanghai, China), and vacuum filter (Φ 300, Southwest Chengdu Experimental Equipment Co., Ltd. Chendu, China).

2.3. Procedure Design

Flotation (roughing, scavenging), aimed at increasing the P_2O_5 grade and phosphorous recovery of phosphorous concentrate, was carried out using an XFD-1.5 L hanging tank flotation operating at a spindle speed of 1650 r/min. A 500 g mass of phosphorous containing vanadium-titanium magnetite tailings was added to the 1.5 L flotation tank. Flotation (cleaning), aimed at increasing the P_2O_5 grade of phosphorous concentrate, was carried out using an XFD-1.0 L hanging tank flotation machine (Jinlin Exploration Machinery Plant, Changchun, China) operating at a spindle speed of 1650 r/min. A 200–300 g mass of phosphorous concentrate was added to the 1.0 L flotation tank. Distilled water (1.0 L) was added and the pulp stirred and mixed for about 3 min, followed by adjustment to the required pH using NaOH, $NaHCO_3$, CaO, or Na_2CO_3 . After 5–10 min of pulping, the depressants were added to the slurry and conditioned for about 3 min. Then, the collectors for improving phosphorous grade and recovery were added and agitated for about 3 min. Before aeration, the frothers (pine oil) for improving the bubble were added, with another about 3 min of stirring. After about 3 min of flotation, the froth (phosphorous concentrate) and in-tank product (flotation tailings) were separately filtered, dried at 85 °C for 1.5–2 h, and weighed. Quantitative analyses of phosphorous grade were conducted to calculate the phosphorous recovery. Calculation of the phosphorous recovery is shown in Equation (1).

$$\text{Phosphorus recovery} = (Q_1 \times \beta_1) / (Q_1 \times \beta_1 + Q_2 \times \beta_2) \times 100\% \quad (1)$$

where, Q_1 is the weight of phosphorus concentrate/g, Q_2 is the weight of flotation tailings/g, β_1 is the P_2O_5 content of phosphorus concentrate/%, and β_2 is the P_2O_5 content flotation tailings/%.

2.4. Analysis and Characterization

The chemical composition of P-containing vanadium titano-magnetite tailings, phosphorus concentrate, and flotation tailings was analyzed by a Z-2000 atomic absorption spectrophotometer (Hitachi Co., Ltd. Tokyo, Japan). The mineral phase compositions of P-containing vanadium titano-magnetite tailings, phosphorus concentrate, and flotation tailings were analyzed by X-ray diffraction (XRD, X Pert pro, Panaco, The Netherlands). The microstructure of the solid products was observed by SEM (S440, Hirschmann Laborgerate GmbH & Co. KG, Eberstadt, Germany) equipped with an energy-dispersive X-ray spectroscopy (EDS) detector (Ultra55, CarlzeissNTS GmbH, Hirschmann Laborgerate GmbH & Co. KG, Eberstadt, Germany).

3. Results and Discussion

3.1. Effect of Different Collectors

The commonly used collectors for phosphate ore flotation include oleic acid, sodium oleate, oxidized paraffin soap, hydroxamic acid, and benzyl arsenate, among which oleic acid, sodium oleate, oxidized paraffin soap, and other fatty acid collectors have a wide range of sources, low price, mild reaction conditions, and can achieve phosphate mineral flotation under alkaline conditions. Oxidized paraffin soap (RCO_2Na) contains more than $\text{C}_{18}\text{--C}_{32}$ long chain fatty acids, and can form complexes on the surface of various mineral metals, which can greatly improve the hydrophobicity of the mineral surface, and at the same time have foaming property, so it can replace anion harvesters of various fatty acid soaps and be used in the flotation of various mineral products. Hydroxyl oxime arsenic acid and benzyl arsenic acid contain a toxic element and have strong foaming performance, then in the process of flotation test, we found that when the flotation foam is bigger with more viscosity, the water content is high, which eventually led to the foam product of phosphorus grade and recovery index was not ideal [20–22].

Results in Figure 2 reveal that the selectivity of oleic acid in the flotation process is relatively poor, which also leads to the lower phosphorus grade and recovery of the obtained flotation phosphorus concentrate. Oleic acid, oxidized paraffin soap, hydroxamic acid, and benzyl arsenic acid can realize the flotation of phosphate minerals. The flotation effect of oxidized paraffin soap as a collector is the most obvious, and phosphorus concentrate with a P_2O_5 grade of 12.65%, and P_2O_5 recovery of 65.31% can be obtained. Therefore, oxidized paraffin is suitable as a flotation collector.

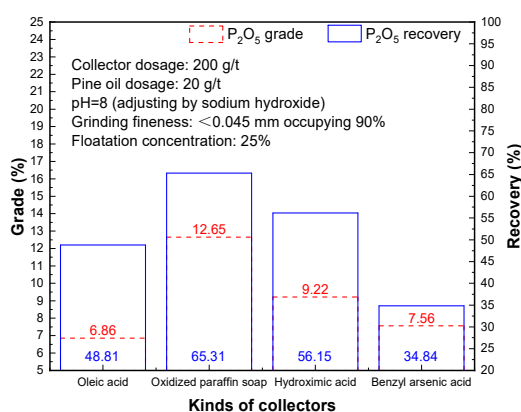


Figure 2. Effect of different collectors on extracting phosphorous.

3.2. Effect of Oxidized Paraffin Soap Dosage

In the process of flotation, the function of the collector is to strengthen the mineral adhesion to the foam, so as to change the hydrophobicity of the mineral surface, so as to realize the purpose of the mineral entering the flotation foam and becoming the concentrate product [23–25].

It is known from Figure 3 that the amount of oxidized paraffin soap can improve the flotation index of phosphorus concentrate. When the amount of oxidized paraffin was in the range of 100–300 g/t, the P_2O_5 grade of phosphorus concentrate decreased from 13.66% to 12.05%, and the P_2O_5 recovery rate increased from 59.80% to 66.28%. When the dosage of oxidized paraffin soap ranged from 400–600 g/t, the P_2O_5 grade of phosphorus concentrate decreased from 10.65% to 7.56%, and the P_2O_5 recovery increased from 66.62% to 69.34%. It shows that increasing the amount of collector is beneficial to improving the separation index of phosphate concentrate, but too much is not conducive to the flotation of phosphate minerals, and other minerals are easy to be floated, thus affecting the quality of concentrate products. Therefore, oxidized paraffin soap dosage of 300 g/t is reasonable, and phosphorous concentrate with a P_2O_5 grade of 12.05% and P_2O_5 recovery of 66.28% was obtained.

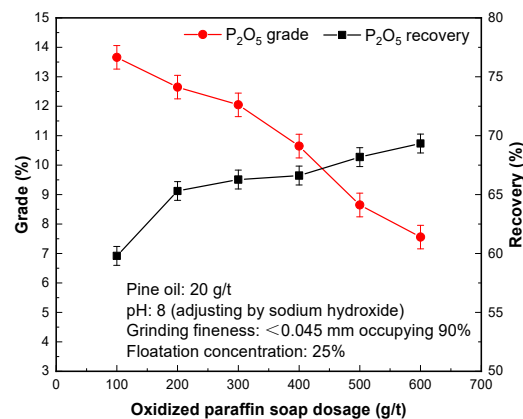


Figure 3. Effect of oxidized paraffin soap dosage on extracting phosphorous.

3.3. Effect of Different Depressants

The main gangue minerals in the vanadium titanium magnetite tailings contain mica, feldspar, chlorite, hornblende, and other silica-aluminate minerals. The common depressants of gangue minerals are sodium silicate, sodium hexametaphosphate, sodium fluosilicate, and carboxymethyl cellulose. The results in Figure 4 show that the addition of carboxymethyl cellulose as an inhibitor is the most obvious to improve the quality of phosphorus concentrate. Carboxymethylcellulose molecule is composed of a number of glucose units, each unit of glucose with three base, namely in the C₂ and C₃ position para hydroxy and primary hydroxyl in C₆ location, and the base to compare live dial by the base of the extent of the hydrogen atoms are replaced by carboxymethyl called substitution degree, the higher the degree of substitution of spindle methyl cellulose charged, the more easily dissolved in the aqueous solution. In aqueous solution, carboxymethylcellulose or ionization which makes its molecular burden on electric carboxymethylcellulose with slurry surface, make the slime superficiality magnesium silicate minerals which are the main gangue mineral, this kind of ore including serpentine, hornblende, and olivine changes, thereby corresponding inhibition [26–29].

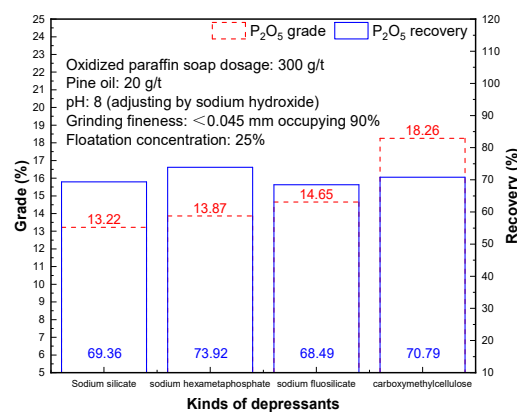


Figure 4. Effect of different depressants on extracting phosphorous.

Therefore, the highest P₂O₅ recovery of phosphate concentrate obtained by sodium hexametaphosphate as a depressant was 73.92%, and the highest P₂O₅ grade of carboxymethyl cellulose as an inhibitor of phosphate concentrate was 18.26%. After comprehensive consideration, phosphorous concentrate with a P₂O₅ of 18.26% and P₂O₅ recovery of 70.79% can be obtained by selecting carboxymethylcellulose as the depressant of the flotation process.

3.4. Effect of Depressant Dosage

The purpose of adding carboxymethylcellulose is to enhance the hydrophilicity of gangue minerals, weaken the effect between the gangue minerals and the collectors, and, thus, to strengthen the separation of gangue minerals from apatite. Increasing the dosage of carboxymethylcellulose is beneficial to improving P_2O_5 grade and recovery of phosphorus concentrate.

The test results in Figure 5 show that the appropriate addition of carboxymethylcellulose as an inhibitor can improve the effect of phosphorus flotation; too little, and the degree of inhibition of gangue ore is not enough and too much, and it is easy to interfere with the target mineral, but led to gangue mineral into phosphorus concentrate, affecting the quality of phosphorus concentrate products. Carboxymethylcellulose is a polymer inhibitor, and can produce flocculation to fine minerals. When the amount is too large, it will interfere with the separation of phosphate minerals, reduce the phosphorus grade, and recovery of phosphorus concentrate products [30]. It is reasonable to use 400 g/t carboxymethylcellulose, and a phosphorous concentrate with a P_2O_5 of 22.53% and P_2O_5 recovery of 72.51% can be obtained.

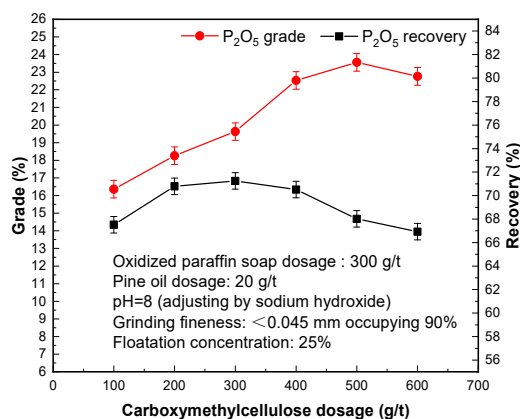


Figure 5. Effect of carboxymethylcellulose dosage on extracting phosphorous.

3.5. Effect of Grinding Fineness

Apatite and fine-grained gangue minerals are inset and symbiosis in the form of mechanical mixing. It is necessary to achieve high grinding fineness to realize monomer dissociation of most gangue minerals such as collophosphate and quartz. However, if grinding fineness is too high, over-grinding will occur, and the sorting effect will be reduced.

Results in Figure 6 show that with the increase of grinding fineness, P_2O_5 grade of phosphorus concentrate changed regularly. When < 0.038 mm occupying 90%, the maximum value of P_2O_5 grade is 25.63%. The P_2O_5 grade of concentrate begins to decline with grinding fineness increasing. The principle is that with the increase of grinding fineness, the dissociation degree of mineral monomer increases continuously, but when the grinding fineness is too high, it will result in over-grinding phenomenon, gangue minerals float up in large quantities, causing the grade of concentrate to drop. After comprehensive consideration of the concentrate grade and recovery, grinding fineness < 0.039 mm occupying 90% of phosphorous flotation, and phosphorous concentrate with a P_2O_5 grade of 25.63% and P_2O_5 recovery of 70.26% can be obtained.

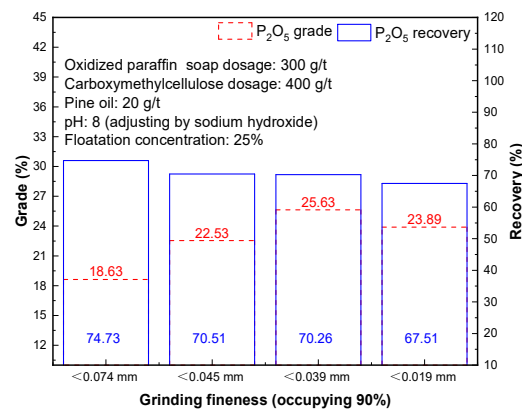


Figure 6. Effect of grinding fineness on extracting phosphorous.

3.6. Effect of Pulp pH

The effect of different flotation pH values on phosphorus flotation separation is shown in Figure 7. In the process of flotation, the pH value of the pulp has a great influence on the physical and chemical properties of the mineral surface, especially whether the flotation agents can produce a certain physical or chemical adsorption on the mineral, so as to achieve the wettability change between the target mineral and non-target mineral [31]. Increasing the pH value of flotation pulp is beneficial to raising P_2O_5 grade of phosphorus concentrate. When the pH value exceeds 9, P_2O_5 grade and recovery of phosphorus concentrate begin to decrease, indicating that slurry flotation at pH = 9 is conducive to the separation of phosphate minerals. The P_2O_5 grade and P_2O_5 recovery of phosphorus concentrate were 28.33% and 73.64%, respectively.

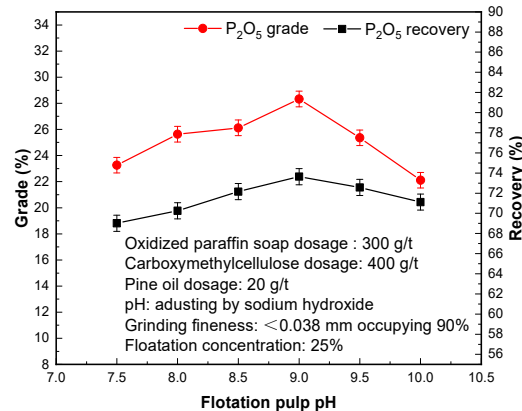


Figure 7. Effect of and flotation pulp pH on extracting phosphorous.

3.7. Effect of Flotation Concentration

The concentration of flotation has a great influence on the physicochemical adsorption of flotation agents and minerals. As the concentration increases, the slurry viscosity increases, and the mechanical resistance between minerals increases, the adhesion between minerals and bubbles are affected, and the target minerals are easily separated from bubbles and the separation indexes are affected. On the contrary, if the concentration decreases, the concentration of flotation agents will decrease, resulting in an increase in the consumption of agents [32]. Under the premise of the same drug dose, if the concentration is too low, it will have a certain impact on the concentrate recovery.

It can be seen from Figure 8 that when the flotation concentration was 20–30%, the P_2O_5 grade of phosphorus concentrate decreased from 28.66% to 28.29%, and the P_2O_5 recovery increased from 63.75% to 74.87%. When the flotation concentration was 35–45%, the P_2O_5 grade of phosphorus concentrate decreased from 25.11% to 17.56%, and the P_2O_5 recovery rate increased from 75.12% to

76.89%. This indicates that the concentration of flotation pulp is 30%, and the P_2O_5 grade and recovery rate of the obtained phosphorus concentrate are 28.29% and 73.64%, respectively.

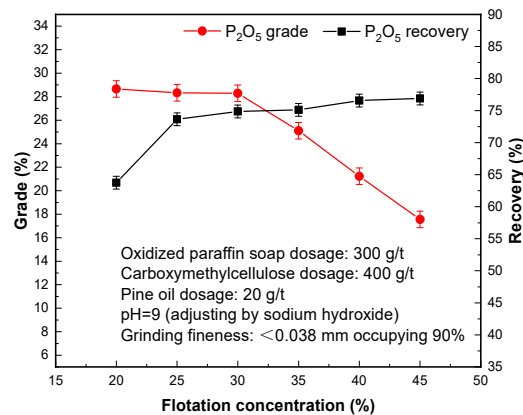


Figure 8. Effect of flotation concentration on extracting phosphorous.

3.8. Effect of Different pH Regulators

The effect of different flotation pH regulators on phosphorus flotation separation is shown in Figure 9. The effect of sodium hydroxide and lime as pH regulator of flotation is obviously worse than that of sodium carbonate and sodium hydroxide. When sodium carbonate was used as a pH regulator, phosphorus concentrate with P_2O_5 grade of 28.69% and P_2O_5 recovery of 76.02% was produced. When sodium hydroxide was used as a pH regulator, phosphorus concentrate with P_2O_5 grade of 28.29% and P_2O_5 recovery of 74.87% was obtained. The reasons for this phenomenon are with amine cationic collector gangue mineral separation of phosphate rock minerals and effect is poorer, and Ca^{2+} , Mg^{2+} , $Ca(OH)^+$, and $Mg(OH)^+$ in the solution later living fossil of the flotation of gangue, such as lower mineral separation, so the fatty acid collector (oxidized paraffin soap) sorted, Na_2CO_3 as pH adjusting agent, CO_3^{2-} in the solution, and HCO_3^- and Ca^{2+} on the surface of the quartz. Ca^{2+} , Mg^{2+} , $Ca(OH)^+$, and $Mg(OH)^+$ created $CaCO_3$ and $MgCO_3$, and then from the gangue mineral surface and the purpose of separation will be achieved [33–35].

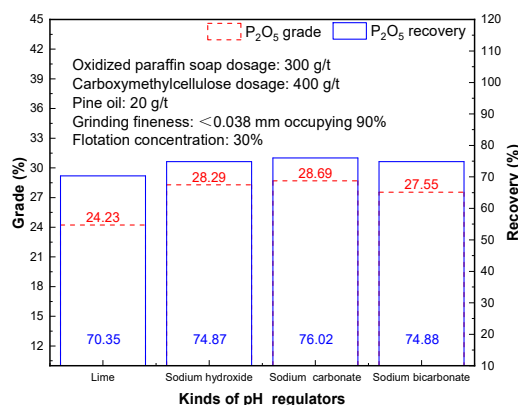


Figure 9. Effect of different pH regulators on extracting phosphorous.

3.9. Effect of Stage on Flotation Scavenging Process

Phosphorus concentrate with P_2O_5 grade of 28.69% and P_2O_5 recovery of 76.02% was obtained by one rough flotation process from the low-grade phosphorus-bearing V-Ti magnetite tailings. In order to further upgrade the phosphorus comprehensive recovery, scavenging time tests were carried out to investigate on P_2O_5 grade and recovery of froth products. The flotation scavenging process was shown in Figure 10, and the test results were shown in Table 3.

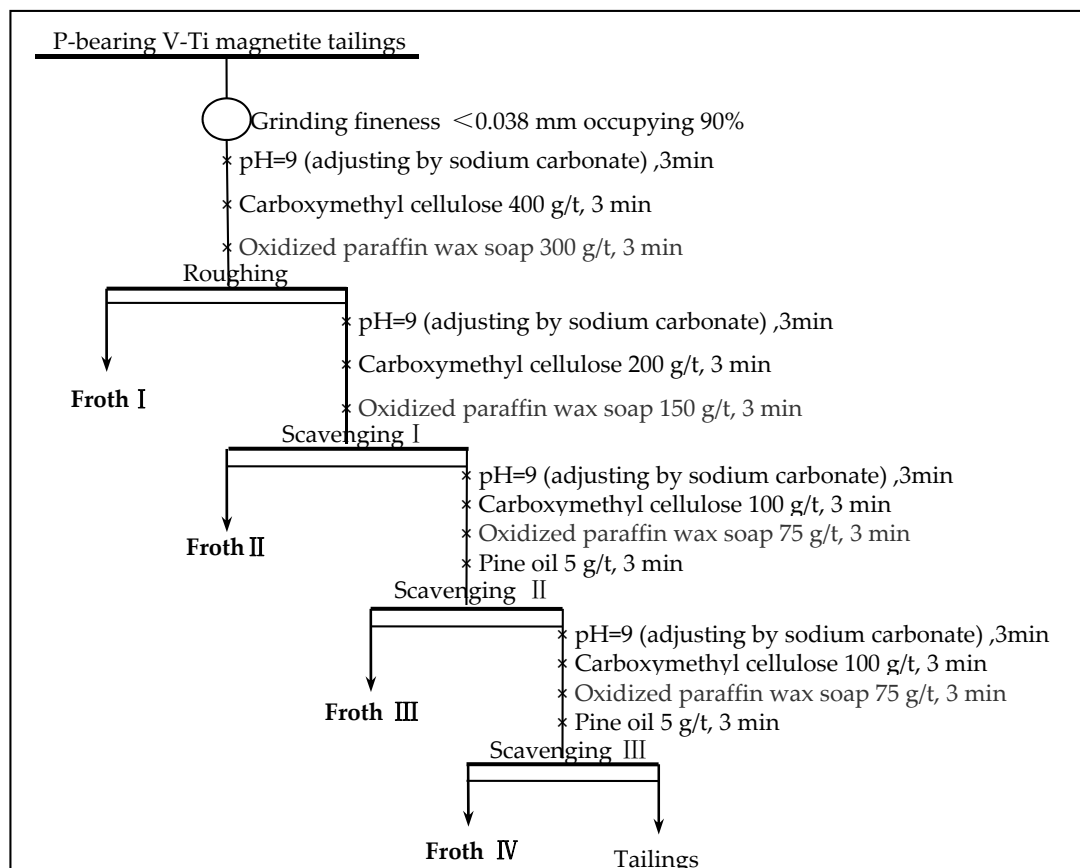


Figure 10. Time on flotation scavenging flowsheet.

Table 3. Effect of scavenging time on P_2O_5 grade and recovery in flotation (%).

Products	Yield		P_2O_5 Grade		P_2O_5 Recovery	
	Individual	Cumulative	Individual	Cumulative	Individual	Cumulative
FrothI	3.78	3.78	28.69	28.69	75.83	75.83
FrothII	1.26	5.04	15.26	25.33	13.44	89.27
FrothIII	0.56	5.6	10.13	23.81	3.97	93.24
FrothIV	0.22	5.82	5.42	23.12	0.83	94.07
Tailings	94.18	100.00	0.09	1.43	5.93	100.00
Totals	100.00		1.43		100.00	

The direction flotation process of phosphorous-bearing V-Ti magnetite tailings after one roughing and three scavengings can obtain the separation index of phosphorous concentrate, with a P_2O_5 grade of 23.12% and P_2O_5 recovery of 94.07%. Compared with the primary roughing, the grade of cobalt decreased by $(28.69 - 23.12)\% = 5.57$ percentage points, and the recovery of P_2O_5 increased by $(94.07 - 75.83)\% = 18.24$ percentage points. The index increased slightly, which was related to the occurrence of phosphorous in tailings. Increasing the number of scavenging is mainly reflected in increasing the number of flotation machine slots in production, thus increasing the investment of pre-equipment. However, considering the high economic value of phosphorous, although increasing scavenging time will lead to decreasing P_2O_5 grade of phosphorous concentrate, from the perspective of comprehensive utilization of resources, it is still reasonable to obtain rough phosphorous concentrate by the direction flotation process of one roughing and three scavenging.

3.10. Effect of Stage on Flotation Cleaning Process

Through the effect experiment of flotation scavenging on P_2O_5 grade and recovery, with the flotation process of one roughing and three scavenging, phosphorus rough concentrate with a P_2O_5 grade of 23.12% and P_2O_5 recovery of 94.07% was obtained. According to the quality standard of phosphorous concentrate with the grade of $P_2O_5 \geq 28\%$). Therefore, the phosphorus rough concentrate should be further processed by cleaning to improve the P_2O_5 grade. The technological process is shown in Figure 11, and the results are shown in Table 4.

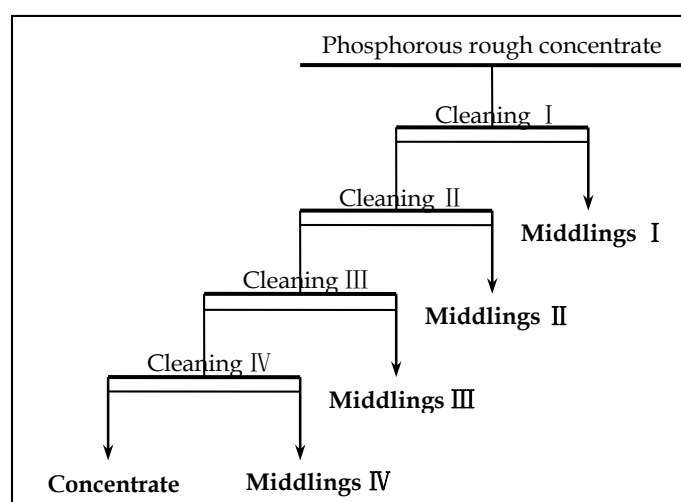


Figure 11. Time on flotation cleaning flowsheet.

Table 4. Effect of cleaning time on P_2O_5 grade and recovery in flotation (%).

Products	Yield		P_2O_5 Grade		P_2O_5 Recovery	
	Individual	Cumulative	Individual	Cumulative	Individual	Cumulative
Concentrate	57.65	57.65	32.11	32.11	80.00	80.00
MiddlingIV	4.61	62.26	21.12	31.29	4.21	84.21
MiddlingIII	8.12	70.38	18.11	29.77	6.36	90.57
MiddlingII	11.21	81.59	11.63	27.28	5.63	96.20
MiddlingI	18.41	100.00	4.78	23.14	3.80	100.00
Totals	100.00		23.14		100.00	

Results in Table 4 show that the improvement of P_2O_5 grade is obviously with the increase of concentrating times. Through the direction flotation process of one roughing, three scavenging, and four concentrating, the highest phosphorus separation indexes can be obtained from the low-grade P-containing vanadium titanomagnetite tailings: P_2O_5 grade of 32.11% and P_2O_5 recovery of 79.99%. Compared with the indexes of phosphorous rough concentrate before concentration, the P_2O_5 grade increased by $(32.11 - 23.14) \% = 8.97\%$ and cobalt recovery rate decreased by $(94.07 - 80.00\% \times 94.07) \% = 18.81\%$. Therefore, an optimized phosphorous concentrate with P_2O_5 grade of 29.77% and P_2O_5 recovery of 90.57% can be produced using a three-stage concentration process.

3.11. The Whole Flotation Flowsheet Test of Recovering Phosphorous

Combined with the technological mineralogical characteristics of phosphorous in the P-bearing V-Ti magnetite tailings, technological conditions test, scavenging, and concentrating test results, the separation process of phosphorous is optimized and the closed-circuit flotation process of one roughing, three scavenging, and three concentrating is adopted. The gangue minerals are further inhibited by increasing the amount of CMC in the concentrating process to ensure that the P_2O_5 grade of the

phosphorous concentrate is increased to more than 30% and the test indexes of the whole process flow are also examined. The flotation process (shown as Figure 12) was used to carry out the whole process test. The results are shown in Table 5.

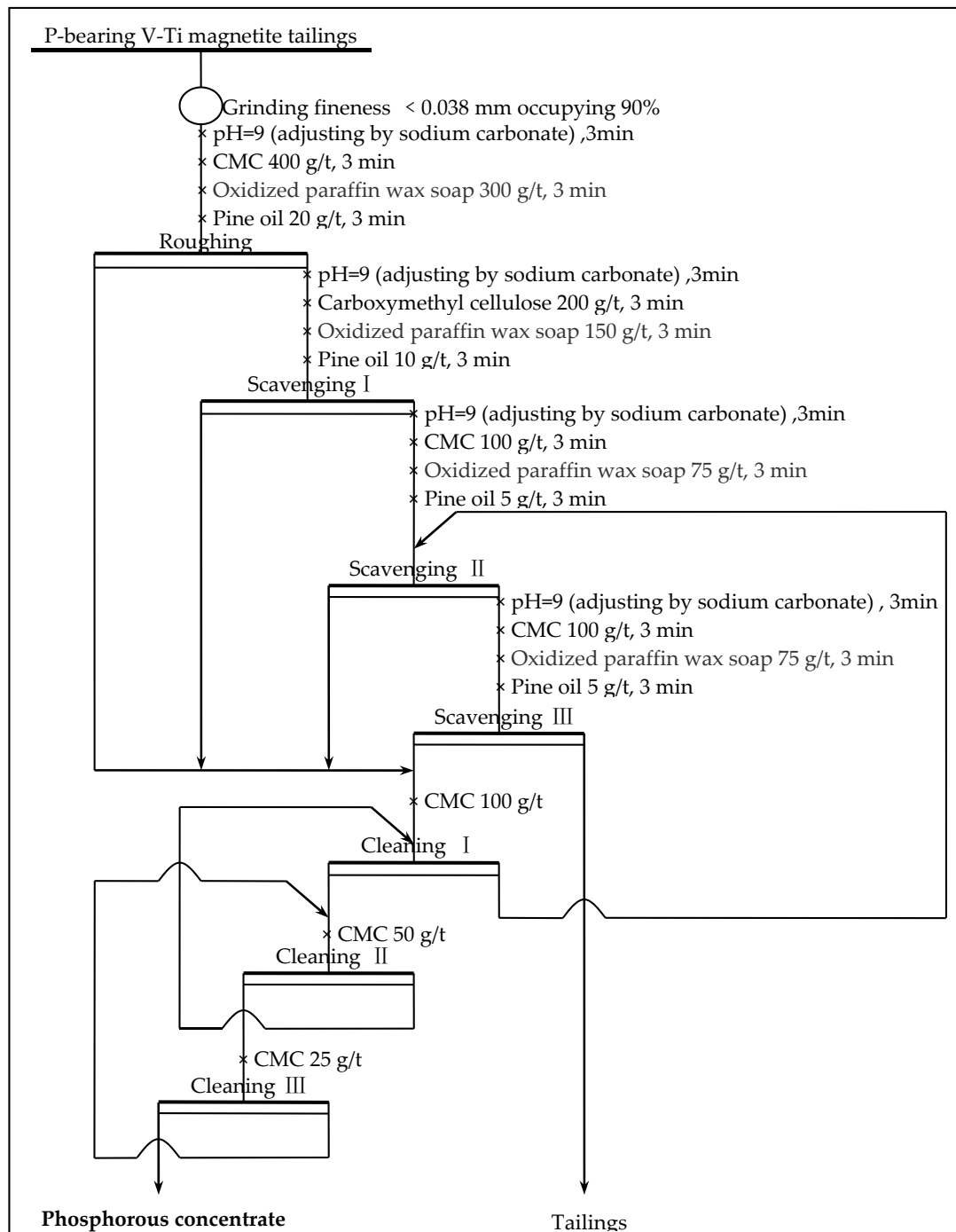


Figure 12. The whole direction flotation flowsheet of recovering phosphorous.

Table 5. Results of the whole flotation test flowsheet of recovering phosphorus (%).

Repeated	Products	Yield	P ₂ O ₅ Grade	P ₂ O ₅ Recovery
1	Phosphorus concentrate	4.05	31.26	87.94
2	Phosphorus concentrate	3.85	31.86	87.56
3	Phosphorus concentrate	4.11	31.04	88.62
4	Phosphorus concentrate	3.94	31.25	87.96
Average		3.99	31.35	88.02
Range ($R = E_{\max} - E_{\min}$)		0.26	0.82	1.06
Arithmetic mean error ($\delta = \frac{\sum_{i=1}^N d_i }{N}$)		0.09	0.33	0.30
um square variation ($SS = \sum_{i=1}^N d_i^2 = \sum_{i=1}^N (E_i - \bar{E})^2$)		0.04	0.79	0.37
Average deviation ($MS = \frac{SS}{f}$)		0.01	0.26	0.12
Standard deviation ($s = \sqrt{\frac{\sum_{i=1}^N (E_i - \bar{E})^2}{N-1}} = \sqrt{MS}$)		0.32	0.51	0.35

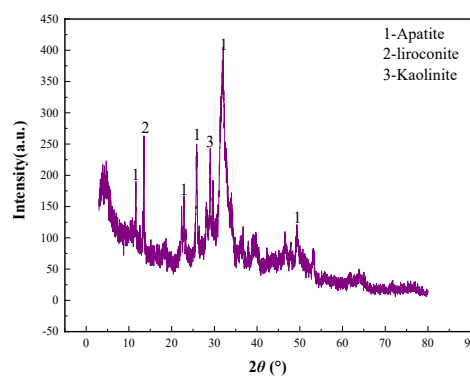
This study adopted the direction flotation process of one roughing, three scavengings, and three cleanings to recover phosphorous from the low-grade P-bearing V-Ti magnetite tailings, obtaining the phosphorous concentrate with a P₂O₅ grade of 31.35% and P₂O₅ recovery of 88.02%, which were superior to the single-condition test results, and further showed that the flotation process had good repeatability.

3.12. Analysis and Characterization of Phosphous Concentrate

Low grade P-Containing vanadium titano-magnetite tailings from iron and titanium separation in the Miyi Region were treated using a direction flotation process. The separation indexes of phosphorous concentrate with a P₂O₅ grade of 31.25% and P₂O₅ recovery of 87.94% were obtained, realizing the recovery of valuable element phosphorous. The main chemical composition of phosphorous concentrate was analyzed by XRF smear quantitative analysis method, and the results are shown in Table 6. The main mineral of phosphorous concentrate was analyzed and characterized by X-ray diffraction and scanning electron microscope-energy disperse spectroscopy (SEM-EDS). The analysis and characterization of XRD and SEM-EDS results were shown in Figures 13 and 14 respectively.

Table 6. Main chemical composition analysis of phosphorous concentrate (%).

P ₂ O ₅	TiO ₂	S	Fe	Na ₂ O	K ₂ O	CaO	Al ₂ O ₃	MgO	SiO ₂
31.25	1.56	0.11	4.63	3.29	0.36	6.96	16.29	8.67	20.73

**Figure 13.** XRD diffractograms of the P-Containing V-Ti magnetite tailings.

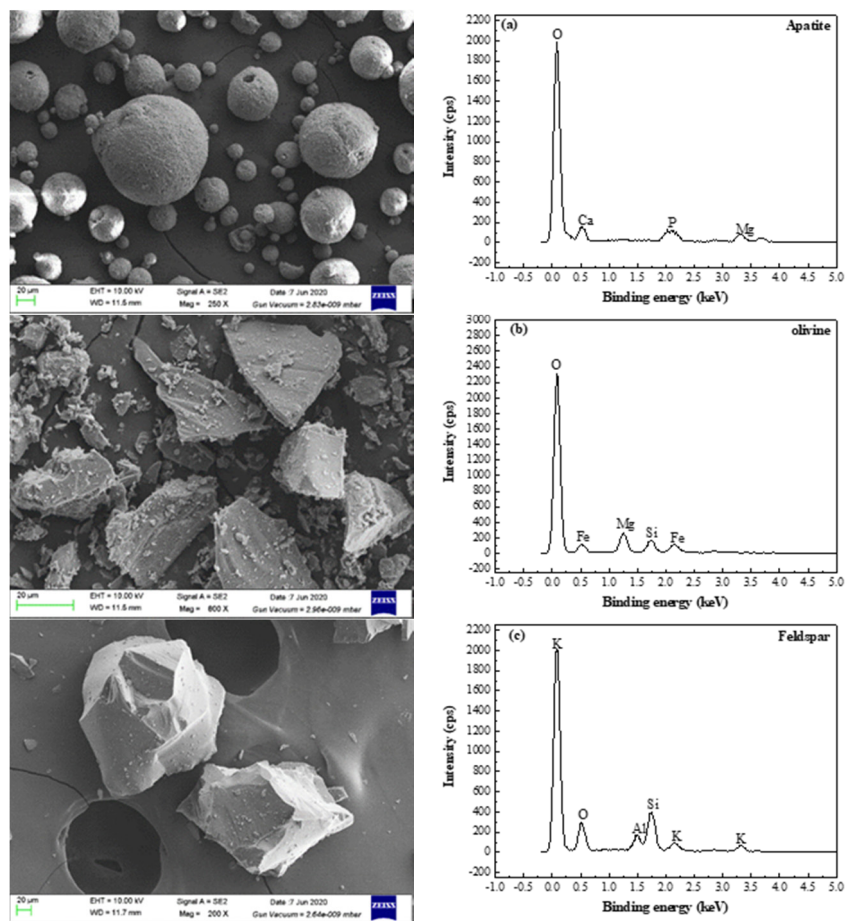


Figure 14. SEM-EDS images of apatite (a), olivine (b), and feldspar (c).

Analysis and characterization results from Table 6 and Figures 13 and 14 show that direction flotation process of one roughing, three scavengings, and three cleanings was suitable for recovering phosphorous from the low-grade P-bearing V-Ti magnetite tailings. Most gangue minerals enter the flotation tailings, and a phosphorus concentrate with P_2O_5 grade of 31.25% was obtained. Compared with the P-bearing vanadium titanomagnetite, gangue minerals such as olivine, hornblende, feldspar, chlorite, mica, quartz, dolomite, and calcite decrease obviously after flotation. The main minerals in phosphorous concentrate are apatite, olivine, and feldspar.

4. Conclusions

Based on the direct flotation results of extracting phosphorous obtained in this study, we drew the main following conclusions:

- (1) The low-grade P-bearing V-Ti magnetite tailings sample was collected from a V-Ti magnetite dressing plant by magnetic separation and flotation in the Miyi area of China, and the P-bearing V-Ti magnetite tailings contained P_2O_5 of 1.42%. Apatite was the main valuable mineral; gangue minerals were mica, chlorite, feldspar, calcite, etc.
- (2) The effect of different flotation conditions on phosphorus separation shows that using oxidized paraffin soap as flotation collector of phosphate minerals and carboxymethylcellulose as gangue mineral inhibitor can effectively recover the valuable element phosphorus in vanadium-titanium magnetite tailings. Phosphorous concentrate with a P_2O_5 grade of 31.35% and P_2O_5 recovery of 88.02% was obtained by a direction flotation process of one roughing, three scavengings, and three cleanings from the P-bearing V-Ti magnetite tailings. The extraction of phosphorus is remarkable,

and the efficient utilization of phosphorous of low-grade phosphorous-bearing V-Ti tailings in the Miyi region of China can be realized finally.

- (3) Studies of the characterization and analysis of phosphorous concentrate by XRD, SEM, and EDS indicated that the main minerals in phosphorous concentrate are apatite, olivine, and feldspar. It also further shows that carboxymethylcellulose, as an inhibitor of gangue ore, can significantly reduce the gangue mineral content in phosphorus concentrate, such as most gangue minerals olivine, hornblende, feldspar, chlorite, mica, quartz, dolomite, and calcite enter into flotation tailings. In addition, hornblende, as one of the main scandium bearing minerals in vanadium-titanium magnetite tailings, enters into flotation tailings, creating favorable conditions for the next step of scandium separation and extraction.

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