

Review

# Recent Advances on the Production of Itaconic Acid via the Fermentation and Metabolic Engineering

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**Abstract:** Itaconic acid (ITA) is one of the top 12 platform chemicals. The global ITA market is expanding due to the rising demand for bio-based unsaturated polyester resin and its non-toxic qualities. Although bioconversion using microbes is the main approach in the current industrial production of ITA, ecological production of bio-based ITA faces several issues due to: low production efficiency, the difficulty to employ inexpensive raw materials, and high manufacturing costs. As metabolic engineering advances, the engineering of microorganisms offers a novel strategy for the promotion of ITA bio-production. In this review, the most recent developments in the production of ITA through fermentation and metabolic engineering are compiled from a variety of perspectives, including the identification of the ITA synthesis pathway, the metabolic engineering of natural ITA producers, the design and construction of the ITA synthesis pathway in model chassis, and the creation, as well as application, of new metabolic engineering strategies in ITA production. The challenges encountered in the bio-production of ITA in microbial cell factories are discussed, and some suggestions for future study are also proposed, which it is hoped offers insightful views to promote the cost-efficient and sustainable industrial production of ITA.

**Keywords:** itaconic acid; metabolic engineering; biosensor; *Aspergillus terreus*; fermentation



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## 1. Introduction

Itaconic acid (ITA) is an important dibasic organic carboxylic acid. It contains two carboxyl groups and an unsaturated carbon-carbon double bond, which makes it an important raw material for the chemical synthesis industry [1]. ITA was selected as one of the 12 most promising platform compounds in the report “High Value Added Chemicals from Biological Sources” by the US Energy Agency in 2004 [2]. It is thus widely used in the fields of coatings, adhesives, plastics, resins, textiles, and polymers [1,3]. The two carboxyl groups in the ITA monomer can form polyesters through esterification reactions, while its double bond structure facilitates cross-linking and curing in subsequent processing to produce various light and thermosets cured polyesters [4–6]. Moreover, ITA is also an intermediate for the production of 3-methyltetrahydrofuran, which is a potential biofuel [7–9]. Recently, ITA was reported to be a mammalian metabolite during macrophage activation, and 4-octyl itaconate has shown potent antiviral and anti-inflammatory effects against various human pathogenic viral infections, including SARS-CoV2 [10,11]. Thus, ITA has great potential applications in the fabrication of biomaterials and biopharmaceuticals.

Both chemical and biological methods have been explored to produce ITA. Initially, ITA was discovered through the thermal decomposition of citric acid in 1836 [12]. Although several chemical methods have been developed for the synthesis of ITA, the complex separation and purification process limits industrial applications. In addition, chemical synthesis is mostly based on petrochemicals, which leads to high production costs and serious environmental pollution [13–15]. Therefore, the current industrial production of

ITA mainly depends on biorefineries, in which glucose, starch and other renewable biomass are utilized to produce ITA via the conversion of microbes [16]. With the increasing depletion of fossil fuels, the demand for environmentally friendly bio-based ITA is expanding. The market size of ITA in 2021 has already reached 105 million USD and is expected to reach 135.6 million USD by 2028, which poses a huge challenge for the production of ITA [17,18]. However, the bio-production of ITA still faces problems of low production efficiency, inability to use cheap raw materials, and high production costs, which limit its development [19]. With the development of synthetic biology and metabolic engineering, the biosynthetic pathway of ITA has been clearly identified, and the genetic modification of microbes is regarded as an available and potential way to solve these problems [19,20].

In this review, the recent research progress on the biological production of ITA is summarized from several aspects including the identification of the ITA synthesis pathway, the metabolic engineering of natural ITA producers, the design and construction of the ITA synthesis pathway in model chassis, and the development, as well as application, of new metabolic engineering strategies in the production of ITA. We also discuss the challenges faced in the bio-production of ITA in microbial cell factories, and put forward some views for future research, which it is hoped provide valuable insights to facilitate the industrial bio-production of ITA.

## 2. The Recent Research on the Bio-Production of ITA

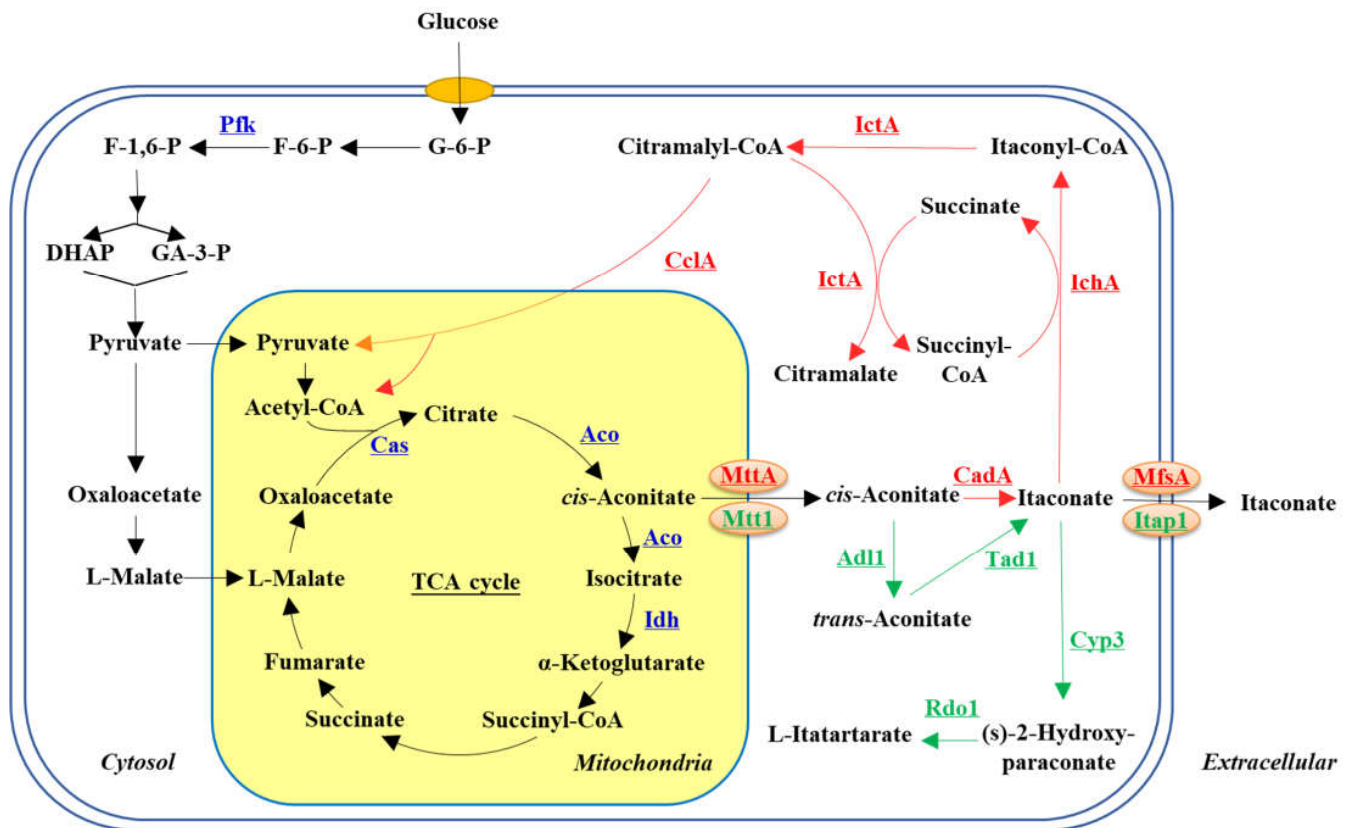
### 2.1. The Identification of the ITA Synthesis Pathway in Microbes

In 1936, Kinoshita et al. [21] first discovered the biosynthesis of ITA in *Aspergillus itaconicus* and postulated that the decarboxylation reaction of cis-aconitate was the key process in the biosynthesis of ITA. Subsequently, Bentley and Thiessen et al. [22] identified cis-aconitate dehydrogenase (CadA) in *Aspergillus terreus*, which converted cis-aconitate to ITA, and confirmed that citric acid was the precursor for ITA synthesis. It was thus proposed that the biosynthesis pathway of ITA originated from the shunt of the tricarboxylic acid cycle (TCA cycle) [23]. Namely, glucose was metabolized to pyruvate via the glycolytic pathway and then transported to the mitochondria where it was converted to acetyl coenzyme A, and entered the TCA cycle to produce cis-aconitate and then generate ITA (Figure 1). It was shown that cis-aconitate was an unstable intermediate, which needed to be transported to the cytosol by the mitochondrial carboxylic acid protein (MttA), and then converted to ITA by the catalysis of CadA [24]. ITA was finally released out of the cell via the function of the major facilitator superfamily protein MfsA [25]. Therefore, these two transporters were essential for ITA production. Moreover, Shin et al. found that the transcription factor Reg also played an important role in the synthesis of ITA, which impacted the activity of CadA, Aco, MttA and MfsA in *A. terreus* [26].

Besides the synthesis pathway, the degradation pathway of ITA has also been identified in *A. terreus*. ITA is first converted to itaconic acyl-CoA by the catalysis of itaconic acyl-Coenzyme A transferase (LctA), and then hydrated to form citric acyl-CoA by itaconic acyl-Coenzyme A hydratase (LchA). Citric acyl-CoA is finally cleaved to pyruvate and acetyl-CoA by citric coenzyme A lyase (CclA), or can be converted to citraconic acid and succinyl-CoA by LctA, which is finally metabolized via the TCA cycle [27].

In addition to *A. terreus*, *Ustilago maydis* has also been reported as an excellent ITA producer. However, the synthesis and degradation pathways are completely different from those in *A. terreus*. Although cis-aconitate is also the precursor in ITA synthesis, it is first converted to trans-aconitate by aconitic acid isomerase (Adi1), and then to ITA by the function of trans-aconitic acid dehydrogenase in *U. maydis* (Tda1) [28]. Moreover, the protein Itp1 was mainly responsible for the efflux of the ITA, while Ria1 was identified as the transcriptional factor regulating the activity of the ITA synthesis pathway in *U. maydis* [29]. In the degradation of ITA, P450 monooxygenase (Cyp3) catalyzes the ITA to generate (s)-2-Hydroxy-paraconate, which is then converted to L-itatartarate by the catalysis of cyclic dioxygenase (rod1) (Figure 1) [28,30]. The two completely different ITA metabolic pathways show the diversity of metabolic libraries in wild microbes, and more work needs

to be conducted to explore the metabolic mechanisms of ITA in natural producers, which could help to better design microcell factories and optimize fermentation processes.



**Figure 1.** The synthesis and degradation pathways of ITA in microbes. Pfk, 6-phosphofructo-1-kinase; Cas, citrate synthase; Aco, aconitase; Idh, isocitrate dehydrogenase; CadA, cis-aconitase decarboxylase; MttA/Mtt1, mitochondrial tricarboxylate transport protein; Mfsa, major facilitator superfamily protein; IchA, itaconyl-CoA hydratase; IctA, itaconyl-CoA transferase; CclA, citramalyl-CoA lyase; AdI1, aconitate-Δ-isomerase; Tad1, trans-aconitate decarboxylase; Itap1, itaconate transporter protein; Cyp3, P450 monooxygenase; Rdo1, ring-cleaving dioxygenase; G-6-P, glucose-6-phosphate; F-6-P, fructose-6-phosphate; F-1,6-P, fructose-1,6-bisphosphate; DHAP, dihydroxyacetone phosphate; GA-3-P, glyceraldehyde-3-phosphate. The synthesis pathway identified in *A. terreus* was present in the red line, while that identified in *U. maydis* was present in the green line.

## 2.2. Enhancement of ITA Production via the Genetic Modification of Natural Producers

### 2.2.1. *Aspergillus* Species

Currently, *A. terreus* is the main strain used for the industrial production of ITA. Glucose and sucrose are commonly considered to be the best carbon sources for the fermentation of *A. terreus* to produce ITA [31]. But pure monosaccharides or disaccharides are expensive, which leads to a high production cost of ITA. Therefore, cheaper and renewable carbon sources were explored to replace glucose in the production of ITA, including glycerol, food waste, lignocellulose, etc. [19,20]. Glycerol is a primary by-product in the biodiesel industry, and the utilization of glycerol as a feedstock to produce higher added-value products by microbes is a promising way to improve the re-cycling of the glycerol [32]. Juy et al. explored using glycerol as the carbon source to produce ITA by *A. terreus*, and the titer reached 27.6 g/L, which suggested that glycerol could be used as a potential substrate in ITA production [33]. Food waste, rich in carbohydrates and protein, is also considered a promising potential feedstock for renewable bio-based chemicals [34,35]. Narisetty et al. screened a thermophilic *A. terreus*, which could produce 41.1 g/L ITA using the hydrolysates of food waste as a substrate [36]. Lignocellulose has great potential as

a non-food carbon source, and it is usually pretreated to form hydrolysates containing glucose and xylose by chemical and biological methods before being used as a feedstock. But the furan derivatives and phenolic compounds in the lignocellulose hydrolysates inhibited the growth of the microbes [37–39]. Krull et al. reported pretreating the hydrolysate using a cation exchange resin to obtain the detoxified hydrolysates, which was then used to produce ITA, leading to the production of up to 27.7 g/L [40]. Kerssemakers pretreated eucalyptus fiber pulp with cellulase to obtain hydrolysates, and the ITA production reached 37.5 g/L using the hydrolysates as a feedstock [41]. Sun et al. isolated and identified an ionic liquid tolerant strain *A. terreus* NRAU-7 with cellulase production ability, which had great potential in the conversion of lignocellulose to ITA [42]. However, the lignocellulose degradation efficiency still requires improvement. Although food waste and lignocellulose can be hydrolyzed into available monosaccharides and disaccharides, the yield of ITA is still low when the hydrolysates are used as the substrate. The main reason, is that more weak acids, furans, phenols and metal ions are formed during the pretreatment process, which are toxic to *A. terreus* and negatively affect the production of ITA. Therefore, the improvement of the tolerance and productivity of *A. terreus* is a critical step to solving the problem.

Traditionally, physical and chemical mutagenesis are usually used to screen the mutants with high yields of ITA. For instance, Yahiro et al. reported mutagenizing *A. terreus* TN-484 with nitrosoguanidine and screened a preferable mutant that produced 82 g/L of ITA from glucose, about 1.3 times higher than that of the original strain [43]. Wu et al. treated *A. terreus* CICC40205 using UV light, and a 33.4% increase in ITA production was obtained by the mutant using the hydrolysate of wheat bran as a substrate [44]. Similarly, Yang et al. treated *A. terreus* No. 2433 using UV-LiCl mutagenesis, and 19.35 g/L of ITA production was achieved from the hydrolysate of bamboo by the final mutant [45]. Compared with physical and chemical mutagenesis, the protoplasmic fusion technique is a more rational approach to obtain stable recombinants, which allows the fusant to combine the genetic traits of both parents [46]. Kirimura et al. obtained an ITA producing fusant F-112 via the fusion of the starch glycosylase producing strain *Aspergillus usamii* IAM 2185 with *A. terreus* IFO6123. The fusant F-112 was able to produce ITA by direct fermentation of soluble starch with a yield of 35.9 g/L, which was about a five-fold increase compared to that of *A. terreus* IFO6123 [47]. It has been suggested that protoplasmic fusion is an available route to improve the performance of natural strains. Although the traditional physical and chemical mutagenesis have the advantages of low cost and simple operation, the high randomness and blindness of the mutagenesis makes the process more complex and unpredictable. The lack of high throughput screening methods also limits the screening efficiency and application.

As the synthesis pathway of ITA in *A. terreus* has been gradually identified, the genetic modification of the pathway has been a hot topic of current research to improve ITA synthesis through metabolic engineering. Glucose is converted to pyruvate via the glycolytic pathway, to enter the tricarboxylic acid cycle to generate citric acid as the precursor of ITA. It has been reported that the activity of 6-phosphofructokinase (PfkA) is negatively affected by the feedback inhibition of citric acid, which is considered to be the rate-limiting step in the synthesis of ITA by *A. terreus* [48]. To avoid the inhibition, and improve ITA production, Tevz et al. altered the phosphorylation site and deleted the inhibitor-binding region of PfkA. After the overexpression of the PfkA mutant in the wide *A. terreus*, the production of ITA was increased from 13.5 g/L to 31 g/L (Table 1) [49]. Huang et al. explored the effects on ITA accumulation of overexpressing CadA, MfsA, MttA, GpdA, AcoA, t-PfkA, CitA, ATEG\_09969 (putative regulator protein which contains a zinc finger motif characteristic of the eukaryotic transcription factors), and ATEG\_01954 genes in *A. terreus* NIH 2624. It was indicated that the overexpression of CadA and MfsA could significantly promote the production of ITA [50]. Similarly, Shin et al. overexpressed the CadA, MfsA, MttA and Reg in *A. terreus* AN37, respectively. They found that the overexpression of MfsA led to the titer of ITA up to 75 g/L, a 18.3% increase compared to the original strain (Table 1) [51]. Since



the natural ITA producer was unable to utilize starch directly, it was needed to prepare the hydrolysate of starch before the fermentation process, which resulted in a large amount of wastewater and improved the production costs. Haung et al. introduced the amylase *GlaA*, from *A. niger*, into *A. terreus*, and achieved ITA production from the recombinant using liquefied starch as a substrate [52]. This laid the foundation for the study of simultaneous saccharification and fermentation of starch for ITA production.

In addition to *A. terreus*, some other *Aspergillus* species have also been genetically modified to improve ITA production. *Aspergillus pseudoterreus* ATCC32359 was considered a good ITA producer, which could rapidly consume hexose and pentose at low pH and had the potential to produce ITA from lignocellulose hydrolysates [53]. Pomraning et al. overexpressed the global regulator *LaeA* in *A. pseudoterreus*, which increased ITA production by 13% (Table 1) [54]. However, there were limited genetic manipulation tools available for filamentous fungi, and this impacted the efficiency of the modification of the natural ITA producer. Therefore, the development of new gene editing tools was also the focus. *Ku* proteins were the DNA binding proteins, and could repair DNA double strand breaks through homologous end joining, which competed with homologous recombination and reduced the gene editing efficiency. Guo et al. improved gene targeting efficiency by knocking out the protein *kusA* in *A. terreus*, and successfully obtained the uracil-deficient NIH 2624 strain by knocking out *pyrG* [55]. On this basis, Huang et al. knocked out *ku80* in *A. terreus* CICC40205, and constructed the uracil nutrient-deficient strain by knocking out the *pyrG* with the defective marker recovered by the application of the Cre/loxP system [56]. Yao et al. established the CRISPR-Cas9 system in *A. terreus* RA2905, and improved the knockout efficiency to 71% [57]. Sra-Yh Shih et al. further optimized the CRISPR-Cas9 system in *A. terreus* ATCC20542, and co-delivering two sgRNA/Cas9 expression plasmids resulted in precise gene deletion in the *ku70* and *pyrG* genes [58]. The development of these new genetic manipulation tools promotes the modification of the natural ITA producer *A. terreus*. However, the application of these technologies in *A. terreus* is still not enough, and the optimization of the genetic toolbox needs further study.

### 2.2.2. *Ustilaginaceae* Species

The *Ustilaginaceae* species are pathogenic fungi of plant black powdery mildew and have been extensively studied in plant pathology. Most of them were found to have the ability to produce ITA, such as *Ustilago vetiveriae*, *Ustilago vetiveriae*, *Ustilago rabenhorstiana*, *Ustilago cynodonti* and *U. maydis* [59–62].

The production of ITA by *U. maydis* was first reported as early as 1955 [62]. *U. maydis* has both mycelial and yeast-like morphology in cultivation, and the latter has the potential to avoid the problems of high viscosity and low oxygen transfer caused by mycelium during the fermentation process [63]. Upon the control of morphology, and optimization of the fermentation conditions, *U. maydis* reached a level of ITA production comparable to that of *A. terreus* [64]. According to the study, *U. maydis* is a pH-sensitive fungus, and neutral conditions were beneficial for the formation of the yeast-like morphology and ITA synthesis [65,66]. Meanwhile, the production of ITA in *U. maydis* is also regulated by the content of nitrogen sources. The limited nitrogen source promoted ITA production, but led to the formation of a mycelium morphology and the accumulation of lipids, which caused the diversion of carbon flow and affected ITA productivity [67]. Therefore, the control of the carbon/nitrogen ratio (C/N) and pH is essential for the production of ITA by *U. maydis*. Maassen et al. optimized the C/N ratio and pH in the cultivation of *U. maydis* MB215, and 44.5 g/L ITA was produced using glucose as substrate [68]. In addition, *U. maydis* showed preferable tolerance to lignocellulose hydrolysates. It was reported that *U. maydis* could be co-cultured with *Trichoderma reesei*, which was capable of degrading lignocellulose by secreting cellulase. And 34 g/L ITA was produced in the co-culture process using cellulose as a feedstock, which indicated the potential of *U. maydis* in the production of ITA from renewable biomass [69].

In recent years, the identification of ITA metabolic pathway in *U. maydis* provided a possible strategy to increase ITA production by metabolic engineering (Table 1). Geiser et al. overexpressed the transporter protein MttA and the regulator Ria1 in *U. maydis* MB215, which led to the ITA production increase about two folds compared to the original strain. Coupled with the knockout of the P450 monooxygenase (encoded by *cyp3*) and the inhibition of by-products synthesis, the titer of ITA was increased to over 80 g/L in an acidic condition (pH = 3.5) [70]. On this basis, Becker et al. knocked down the ITA oxidation pathway, the lipids synthesis pathway, and the ustilagic acid synthesis pathway in *U. maydis* MB215 using CRISPER-Cas9 technique to construct a by-product-free platform. After overexpression of Ria1, 53.5 g/L of ITA was produced from 100 g/L of glucose by the engineered strain *U. maydis* MB215 ITA (Table 1) [71].

Due to the advantages of yeast-like morphology in large-scale fermentation, some studies have been conducted to understand the mechanism of morphology formation. It was shown that *Ustilaginaceae* could grow as a yeast-like morphology at neutral pH, and form mycelia morphology at acidic conditions. According to the genomics analysis, Faz7 was a dual specificity serine/threonine and tyrosine kinase, which was identified as the key enzyme regulating the tube formation and filamentous growth of *Ustilaginaceae*. The knockout of the *fuz7* gene allowed *Ustilaginaceae* to better maintain a yeast-like morphology [72]. *U. cynodontis* had preferable tolerance to low pH but easily formed the mycelia morphology in the production of ITA. Tehrani et al. knocked out the *fuz7* in *U. cynodontis* NBRC9727 to promote the formation of the yeast-like morphology. Coupled with the deletion of Cyp3 and the overexpression of MttA and Ria1, the titer of ITA was improved by about 6.5 fold and the yeast-like morphology could be well maintained at a lower pH [73]. A similar strategy was also conducted to engineer *U. maydis* MB215 by knocking out *fuz7* to control the morphology, overexpressing MttA and Ria1 to enhance the accumulation of ITA, and deleting Cyp3 to reduce the consumption of ITA, which led to the titer of ITA up to 220 g/L by the engineered strain in fed-batch fermentation (Table 1) [74]. These works indicate that the control of morphology, and the regulation of the metabolic pathways, are conducive to improving the efficiency of ITA synthesis by *Ustilaginaceae* species. Their modifiable morphology and excellent ITA production ability also demonstrates great potential in industrial application.

**Table 1.** Improving ITA production via the genetic modification of natural ITA producers.

Strains	Genetic Modification Employed	Carbon Sources	Titer (g/L)	Yield (g/g)	Productivity g/(L h)	Reference
<i>A. terreus</i> A156	Overexpression of truncated and mutated <i>pfkA</i> gene from <i>A. niger</i>	Glucose	31	-	0.31	[49]
<i>A. terreus</i> AN37	Overexpression of native <i>cadA</i> and <i>mfsA</i> mutants	Glucose	75	0.68	0.57	[51]
<i>A. terreus</i> CICC 40205	Overexpression of <i>glaA</i> from <i>A. niger</i>	Starch	77.6	-	1.07	[52]
<i>A. pseudoterreus</i> ATCC32359	Overexpression of global regulator <i>LaeA</i>	Glucose	30.4	-	-	[54]
<i>U. maydis</i> MB215	Deletion of <i>cyp3</i> and overexpression of regulator gene <i>ria1</i> under <i>Petef</i> promoter	Glucose	54.8	0.48	0.33	[70]
	Deletion of <i>cyp3</i> , <i>MEL</i> , <i>UA</i> , <i>dgat</i> ; overexpression of <i>ria1</i>	Glucose	53.5	0.47	0.27	[71]
	Overexpression of native <i>rai1</i> and <i>mttA</i> ; deletion of <i>cyp3</i> and <i>fuz7</i>	Glucose	220	0.33	0.46	[74]
<i>U. cynodontis</i> NBRC9727	Overexpression of native <i>rai1</i> and <i>mttA</i> ; deletion of <i>cyp3</i> , <i>fuz7</i> , <i>MEL</i> , <i>UA</i> , <i>dgat</i>	Glucose	74.9	0.54	0.53	[64]
	Overexpression of native <i>rai1</i> and <i>mttA</i> ; deletion of <i>cyp3</i> and <i>fuz7</i>	Glucose	22.3	0.42	0.07	[73]

Current research on the natural ITA producers has mostly focused on *Aspergillus* and *Ustilaginaceae* species, while some other widely studied strains have also been found to produce ITA, such as *Helicobasidium mompa*, *Rhodotorula* sp., *Candida speciesa* and *Pseudozyma antarctica* [75–77]. However, few studies have been conducted on these natural ITA producers, and the mechanism of ITA synthesis in these strains needed to be further explored. This could help to understand the metabolic mechanisms of microbial ITA synthesis and provide a rich research library for improving the efficiency of ITA synthesis.

### 2.3. The Design and Construction of the ITA Synthesis Pathway in Model Hosts

Although the natural producers, *A. terreus* and *U. maydis* have a high yield of ITA, they mainly use glucose as a carbon source and are not capable of using low-cost starch and lignocellulose, which leads to the current high production costs. Moreover, *A. terreus* and *U. maydis* grow relatively slowly, resulting in a low production efficiency. Also, as filamentous fungi, the difficulty in morphology control, laborious handling of spores, high oxygen demand, low reproducibility of fermentation, and complex genetic background still limit the improvement of ITA production. With the development of synthetic biology and metabolic engineering, the synthesis pathways of ITA have been clearly identified, and the design and construction of ITA synthesis pathways in model hosts with a clear genetic background is thus considered a potential way to promote ITA production and compensate for the deficiency.

#### 2.3.1. Genetic Modification of Different Hosts to Produce ITA

Although *A. niger* and *A. terreus* belong to the *Aspergillus* species, *A. niger* has a clear genetic background and has been widely used as a chassis for metabolic engineering and the industrial production of a wide range of biochemicals, including citric acid, gluconic acid and amylase [78,79]. Citric acid is an important precursor for the synthesis of ITA, while *A. niger* has a high capacity for citric acid production (200 g/L) [80]. Therefore, *A. niger* was considered to be the dominant chassis for the synthesis of ITA. Li et al. heterologously expressed CadA from *A. terreus* in *A. niger* AB 1.13, and achieved an engineered ITA producing *A. niger* [81]. Wang et al. proposed overexpressing the two distinct biosynthesis clusters from *A. terreus* and *U. maydis* in *A. niger* ATCC 1015 to improve ITA production. Coupled with increasing the copy number of CadA, down-regulating the expression of IctA, and enhancing the expression of AcoA, the ITA production achieved 9.08 g/L [82]. Based on the strong ability of amylase secretion, Xie et al. introduced the AcoA and CadA from *A. terreus* into *A. niger* YX-1217, and 7.2 g/L ITA was produced from corn flour and crude starch, which indicated that *A. niger* had the potential to produce ITA by simultaneous saccharification and fermentation of low-cost crude starch [83]. However, the low productivity of ITA needed to be further improved.

The yeasts, *Yarrowia lipolytica*, and *Pichia kudriavzevii*, as commonly used chassis, have plenty of advantages, such as a clear genetic background, an abundant genetic manipulation toolbox, a fast growth rate and a good tolerance to low pH [84]. A lot of biochemicals have been produced by engineered yeast cell factories [85–88]. They were thus modified to synthesize ITA (Table 2). Blazeck et al. first introduced the CadA from *Aspergillus oryzae* into *S. cerevisiae* and enhanced its expression via a strong promoter, which led to the final yield of 160 mg/L ITA [89]. Similarly, Sun et al. introduced the CadA from *A. terreus* into *P. kudriavzevii* and overexpressed the endogenous mitochondrial tricarboxylic acid transporter gene (MTT) to promote the synthesis of ITA. Coupled with the knockout of isocitrate dehydrogenase, the titer of ITA reached 1.3 g/L by the engineered *P. kudriavzevii* [90]. *Y. lipolytica* is oleaginous yeast and it was reported that AMP was the essential cofactor for isocitrate dehydrogenase, and adenosine monophosphate deaminase (AMPD) was activated under nitrogen-limited conditions to promote the degradation of AMP, which resulted in a significant accumulation of citric acid in *Y. lipolytica* [91]. The highest titer of citric acid currently reached is over 80 g/L, by the engineered *Y. lipolytica* [92]. Blazeck et al.

overexpressed the native aconitase with a 36 amino acid N-terminal truncation to remove its putative mitochondrial localization signal (ACOnoMLS) in *Y. lipolytica*. Combined with the introduction of CadA from *A. terreus*, 4.6 g/L ITA was obtained by the engineered strain (Table 2) [93]. Based on this work, Zhao et al. further overexpressed MttA and MfsA in *Y. lipolytica*, and the final titer of ITA achieved was 22.03 g/L [94]. This was the highest production of ITA obtained in yeast cell factories and also showed the promising potential of yeast in the production of ITA.

Besides yeast, some bacteria have also been developed as proven platforms for the synthesis of biochemicals. *E. coli* is the most commonly used host in genetic engineering with the advantages of the fast growth of cells, low nutritional requirements, and a well-developed genetic modification toolbox, which has been engineered to produce a variety of bio-products including ITA [95,96]. Harder et al. introduced the gene clusters for ITA synthesis into *E. coli* and 47 g/L ITA was obtained in fed-batch fermentation based on the regulation of knocking down the by-products' synthesis pathways (Table 2) [97]. It has been demonstrated that *E. coli* have a good tolerance to ITA and an excellent synthesis capacity. In addition, *E. coli* as a proven protein expression platform offers the possibility to construct the conversion pathways of multiple carbon sources, enabling the production of ITA from low-cost feedstocks. Okamoto et al. expressed the  $\alpha$ -amylase (SBA) in an engineered ITA producing *E. coli*, and achieved the ITA yield of 0.15 g/L, using 1% starch as the substrate [98]. Jeon et al. enhanced the metabolic pathway of glycerol in *E. coli* and overexpressed the codon-optimized CadA to achieve ITA production from glycerol. Coupled with the optimization of the fermentation process, 7.23 g/L ITA was finally obtained by the engineered strain [99]. Similar to *E. coli*, *Corynebacterium glutamicum* is a model bacterium for the synthesis of amino acid-like products, and has a relatively good acid tolerance which is capable of growing on a variety of carbon sources [100]. It has also been used as a chassis for ITA synthesis. Otten et al. found that the activity of CadA could be enhanced in *C. glutamicum* via the fusion expression of CadA with maltose binding protein (MalE) from *E. coli*. Coupled with the inhibition of isocitrate dehydrogenase (ICD), the final titer of ITA reached 7.8 g/L by the engineered *C. glutamicum* [101]. Joo et al. co-overexpressed CadA and the transcriptional regulator RamA in *C. glutamicum*, which resulted in 0.881 g/L ITA produced using rice wine waste as the substrate [102]. Acetate is one of the major products in the electrocatalytic or biocatalytic conversion of CO<sub>2</sub>, while *C. glutamicum* is also a promising acetate-converter that alternates the carbon source in bioprocesses. Merkel et al. constructed an engineered *C. glutamicum* by expressing the CadA from *A. terreus* and the ICD mutant with a low activity. The production of ITA reached 29.2 g/L using acetate as the substrate [103]. Although *C. glutamicum* has been suggested as a potential host for ITA production, there have been fewer reports on the synthesis of ITA by the modified *C. glutamicum*, and more investigations could be conducted to further improve its ITA production capacity.

Lignocellulose is the most abundant biomass in the world and can be used as a potential raw material in biorefinery. But the hydrolysates of lignocellulose contain toxic compounds including aromatic chemicals, acetic acid and furfural, which limit its application in the synthesis of ITA by microcell factories. Therefore, the development of new hosts based on natural lignocellulose-degrading microbes has been proposed as an available way to promote the conversion of lignocellulose to ITA. *Neurospora crassa* was identified as a natural lignocellulose-degrading microbe. Zhao et al. introduced the codon-optimized CadA into *N. crassa* FGSC 9720 and yielded 20 mg/L ITA using maize straw as the substrate [104]. *Candida lignohabitans* was reported to grow normally in the hydrolysates of lignocellulose without detoxification. Bellasio et al. overexpressed CadA in *C. lignohabitans* CBS 10342, and 2.5 g/L was obtained from the un-pretreated hydrolysates by the engineered strain [105]. Similarly, *Pseudomonas putida* also showed good tolerance to the aromatic compounds in the hydrolysates of lignocellulose, and was also explored as the host to construct the ITA synthesis pathway by overexpressing CadA from *A. terreus*. After the regulation of the by-products' synthesis pathway, 1.4 g/L ITA production was



achieved using the hydrolysates from the alkali-treated lignin as the substrate [106]. The development of lignocellulose-degrading microbes as chassis is still in the initial stage, and the yield of ITA is low compared to that of other established hosts. However, upon the promise of lignocellulose in the biorefinery, the lignocellulose-degrading microbes could be potential microbes for future bioproduction of ITA if more research is conducted.

**Table 2.** Genetic engineering of model host for ITA production.

Hosts	Genetic Modifications	Carbon Source	Titer (g/L)	Yield (g/g)	Productivityg/(L h)	Reference
<i>A. niger</i> AB1.13	Heterologous expression of CadA	Glucose	0.7	0.01	0.0073	[25]
	Heterologous expression of CitB, CadA, MttA and mfsA from <i>A. terreus</i>	Glucose	26.2	0.37	0.35	[93]
<i>A. niger</i> ATCC 1015	Heterologous expression of CadA (multiple copies), MttA, MfsA, Adi1, Tad1, Itp1, AcoA and deletion IctA	Glucose	9.08	0.09	0.063	[82]
<i>A. niger</i> YX-1217	Heterologous expression of AcoA and CadA from <i>A. terreus</i>	Cornmeal	7.2	-	0.7	[83]
<i>S. cerevisiae</i> BY4741	Heterologous expression of CadA from <i>A. terreus</i>	Glucose	0.168			[89]
<i>P. kudriavzevii</i> YB4010	Heterologous expression of CadA from <i>A. terreus</i> , overexpression of native Pk, MttA and deletion of Icd	Glucose	1.23	0.029	0.051	[90]
<i>Y. lipolytica</i> PO1f	Heterologous expression of CadA, MttA, MfsA and AcoA from <i>A. terreus</i>	Glucose	22	0.056	0.111	[92]
<i>Y. lipolytica</i> PO1f	Heterologous expression of CadA from <i>A. terreus</i> , and native AcoA (without mitochondrial signal)	Glucose	4.6	0.06	0.045	[107]
<i>E. coli</i> MG1655	Heterologous expression of CadA from <i>A. terreus</i> ; deletion of the enzymes in the by-products synthesis pathway	Glucose	47	0.44	0.39	[108]
<i>E. coli</i> BW25113	Heterologous expression of CadA from <i>A. terreus</i> , and native AcnB	Glucose	4.34	-	0.04	[109]
	Heterologous expression of CadA from <i>A. terreus</i> , and SBA ( $\alpha$ -amylase) from <i>Streptococcus bovis</i>	Soluble starch	0.15	-	0.002	[98]
<i>E. coli</i> XL1-Blue	Heterologous expression of CadA from <i>A. terreus</i>	Glycerol	7.2	-	0.1	[99]
<i>E. coli</i> MG1655	Heterologous expression of cadA; down-regulation of Icd, pykA, and sucCD by CiMS system	Glucose	3.93	0.98	0.082	[110]

Table 2. Cont.

Hosts	Genetic Modifications	Carbon Source	Titer (g/L)	Yield (g/g)	Productivityg/(L h)	Reference
<i>C. glutamicum</i>	Heterologous fusion expression of CadA from <i>A. terreus</i> with MalE from <i>E. coli</i> , and the isocitrate dehydrogenase mutant	Glucose	7.8	0.29	0.27	[101]
<i>C. glutamicum</i>	Heterologous expression of CadA from <i>A. terreus</i> and a low activity mutated Icd	Acetate	29.2	0.16	1.01	[103]
<i>N. crassa</i> FGSC 9720	Heterologous expression of CadA	Corn straw	0.0204	-	-	[104]
<i>C. lignohabitans</i> CBS 10342	Heterologous expression of CadA from <i>A. terreus</i>	Lignocellulose hydrolysate	2.5	-	0.04	[105]
<i>P. putida</i>	Heterologous expression of CadA from <i>A. terreus</i> controlled by the biosensor $P_{urtA}:T7pol:lysY^+$ ; deletion of PHA synthetases	Alkali pretreated lignin	1.4	-	-	[106]

### 2.3.2. Strategies for the Metabolic Regulation of Itaconic Acid Synthesis

Due to the lack of enzymes in the ITA synthesis pathway in the model strains, the enhancement of the expression and activity of the enzyme CadA was considered a fundamental strategy to improve the ITA synthesis capacity of the engineered strains. The expression of heterologous proteins usually led to the misfolding and the formation of inclusion bodies, while the codon optimization of the sequences was a commonly used method to improve the expression efficiency of heterologous proteins [111]. Vuoristo et al. heterologously overexpressed CadA in *E. coli*, but found that the protein existed mainly in the form of inclusion bodies and resulted in a low production of ITA. After expressing the codon-optimized CadA at a low temperature, the number of inclusion bodies was decreased and the production of ITA increased 24 fold [112]. Similarly, Otten also found the fusion expression of codon-optimized CadA, with maltose binding protein (MalE) from *E. coli*, could reduce the formation of inclusion bodies, which resulted in a 2-fold increase in CadA activity in *C. glutamicum* [101].

The metabolic pool of precursors directly affected the efficiency of product synthesis, and the enhancement of the supply of precursors was also an available way to promote the accumulation of target products. Cis-aconitate was the precursor in the synthesis of ITA. However, in eukaryotes, cis-aconitate as the relatively unstable intermediate in the TCA cycle was generated in mitochondria, while the key enzymes for ITA synthesis (CadA, Tad1 and Adi1) were expressed in the cytosol. Therefore, the overexpression of the mitochondrial transporter protein MttA/Mtt1 was proven to be the important rate-limiting step for ITA synthesis, by accelerating the transportation of cis-aconitate across the mitochondrial membrane into the cytosol to increase the precursor metabolic pool [90,113]. Cis-aconitate was the product derived from citrate, while some hosts showed weak citrate synthesis ability and thus limited the production of ITA, such as *E. coli* and *P. kudriavzevii*. The overexpression of the citrate synthase (GltA), and down-regulation of the isocitrate dehydrogenase (Idh), was usually applied to increase the accumulation of citrate [90,97]. Harder et al. used this strategy to enhance the accumulation of citrate in *E. coli* and the titer of ITA was improved to 32 g/L, coupled with the regulation of by-product synthesis pathways [103]. Similarly, Hossain et al. also overexpressed GltA in *A. niger* AB1.13, leading

to ITA production increasing to 26.2 g/L [79]. These works indicate that the enhancement of the precursor supply is a feasible approach to improve the production of ITA.

Besides the reinforcement of the ITA synthesis pathway, the inhibition of the by-product synthesis was also a preferable strategy to reduce the diversion of the carbon flow and facilitate ITA production. For example, the overexpression of the transporter protein MfsA in *A. niger* led to the formation of the by-product oxalic acid. The deletion of oxaloacetate acetylhydrolase (OahA) was reported to reduce the production of oxalic acid, but has a negative effect on cell growth due to the interruption of the TCA cycle [81]. Van et al. proposed specifically mutating the OahA to down-regulate the activity in *A. niger*. Coupled with the inhibition of the by-products acetate and gluconate synthesis pathways, the production of ITA was significantly improved [114]. In the engineered *E. coli*, acetic acid and lactic acid were the major by-products during ITA production. Knockout of the phosphate acetyltransferase (Pta) and lactate dehydrogenase (LdhA) reduced the generation of acetic acid and lactic acid, which led to more central carbon flux towards the ITA synthesis pathway [112].

The dynamic regulation of metabolic fluxes is a new strategy proposed in recent years, which is beneficial for the improvement of the carbon flux conversion efficiency. Dynamic metabolic regulation can be achieved through biosensors, to automatically keep the metabolic fluxes in balance during ITA production. Hanko et al. identified the ITA-inducible promoter P<sub>ccl</sub>, and its corresponding LysR-type transcriptional regulator YpItcR, from the ITA-degrading strain *Yersinia pseudotuberculosis*, which was composed the YpItcR/P<sub>ccl</sub> ITA biosensor. Combined with the expression of a fluorescent protein, a fluorescence-based ITA biosensor was formed. It was indicated that the fluorescence output was positively correlated with the concentration of ITA, which laid a foundation for the establishment of a high-throughput method for the screening of high-producing engineered ITA microbes [115]. Zhao et al. constructed a CRISPRi mediated self-inducible system (CiMS) based on the YpItcR/P<sub>ccl</sub> biosensor in an engineered ITA producing *E. coli*. Based on the modified system, the engineered *E. coli* predominantly accumulated biomass in the early stage, while CiMS was induced to activate when the accumulation of ITA increased and Icd, pykA and sucCD were inhibited, which led to the carbon flux being almost toward ITA production [110]. Similarly, Elmore et al. developed a nitrogen starvation biosensor, P<sub>urtA</sub>:T7pol:lysY<sup>+</sup>, in *P. putida* [106]. P<sub>urtA</sub> is a nitrogen starvation induced promoter and improved the expression of T7 RNA Polymerase (T7pol) under nitrogen-limited conditions to enhance the strength of the T7 promoter. When the biosensor was applied to control the expression of CadA in *P. putida*, the production of ITA was dynamically divided into two phases. Namely, the expression of CadA was inhibited, and cells grew rapidly with a sufficient nitrogen source in the initial stage, while cell growth was limited with the consumption of the nitrogen source and CadA was highly expressed by the activation of the P<sub>urtA</sub> promoter. Compared to the group using the constitutive promoter to control the expression of CadA, the application of the P<sub>urtA</sub>:T7pol:lysY<sup>+</sup> biosensor showed a 40% increase in ITA production [100]. These works indicate that the regulation of the central carbon flux could promote the accumulation of ITA by the engineered microcell factories, while the dynamic regulation of the carbon flux provides a more reasonable way to automatically balance the diversion of the carbon flow between cell growth and ITA production.

### 3. Conclusions and Prospects

ITA, as an important platform biochemical, is not only an important raw material for biomass polymers, but also has great potential for applications in biomedicine and other fields. According to the report, the market size of ITA in 2021 has already reached 105 million USD and is expected to reach 135.6 million USD by 2028. The increasing demand for bio-based unsaturated polyester resin, and its non-toxic properties, are fueling the growth of the itaconic acid market across the globe. Although the current industrial production of ITA mainly depends on biorefineries, the low production efficiency, inability to use

cheap raw materials, and high production costs pose a huge challenge for the production of environmentally friendly bio-based ITA. With the development of metabolic engineering, the metabolic pathways of ITA in microbes have been gradually clarified, which provides a new approach for the improvement of ITA biosynthesis. Our work provides an overview of the bio-based production of ITA via fermentation and metabolic engineering.

*A. terreus* is the predominant strain used for industrial production of ITA, with yields of up to 160 g/L. But it still suffers from slow growth, shear intolerance of the mycelium, high fermentation viscosity, and a requirement of oxygen supply. *U. maydis* has recently received attention due to its yeast-like morphology and high yield of itaconic acid (220 g/L). However, the poor tolerance of *U. maydis* to low pH has limited its industrial application. Although these natural ITA producers have an excellent ITA production capacity, some issues still need to be further explored, including the lack of ability to utilize low-cost carbon sources, the control of mycelia morphology, the poor tolerance to low pH conditions, and the unclear genetic background to conduct metabolic modifications, which may lead to the further breakthroughs in the economical production of ITA.

The commonly used model hosts have the advantages of proven genetic manipulation, a wide range of carbon source adaption, and easy fermentation control. At present, several hosts have been developed for ITA production, including *A. niger*, *S. cerevisiae*, *P. kudriavzevii*, *Y. lipolytica*, *C. lignohabitans*, *P. putida*, and *E. coli*. Multiple strategies have been applied to the metabolic regulation to improve ITA synthesis. However, ITA production is still far from commercial production compared to that of the natural ITA producing strains. This is possibly caused by several factors: (1) the low activities of the enzymes heterologously expressed in non-homologous hosts; (2) the lack of a regulatory mechanism for the ITA synthesis pathway in the model strains; (3) the imbalance in metabolic fluxes leading to the accumulation of by-products after introducing the ITA synthesis pathway. With the development of synthetic biology and metabolic engineering, more and more new biotechnologies and strategies have been established including the CRISPR-Cas/dCas system, the CRISPRa and CRISPRi technologies, the biosensor-based dynamic control strategies, etc., which provide new insights into further exploration of metabolic regulation. This will possibly be the focus of future research, including understanding the expression and regulation metabolism of the heterologous enzymes in microbes, the development of more efficient metabolic engineering strategies, and the investigation of more potential hosts.

Besides the improvement of strain performance, reducing production costs is another focus in the industrial production of ITA. Feedstock and downstream product separation and purification processes are determinants of production costs. More renewable and cheaper raw materials, such as lignocellulose, food waste, and CO<sub>2</sub>-derived acetic acid could be developed as substrates to reduce the cost of raw materials. On the other hand, the calcium salt-based precipitation method is the commonly used method in the separation process, but leads to a large amount of wastewater, which increases the production cost. Therefore, more environmentally-friendly and cost-efficient separation and purification methods should be explored and applied in the production of ITA, such as ion exchange adsorption, nanofiltration, electrodialysis, etc.. It is believed that the solution to these problems would promote the evolution of the cost-efficient, green and sustainable bio-based production of ITA.

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